

Large Chilled Water System

Design Seminar

Courtesy of Oslin Nation Company

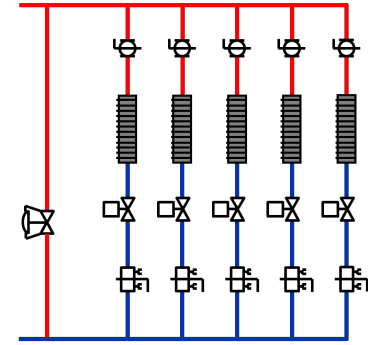
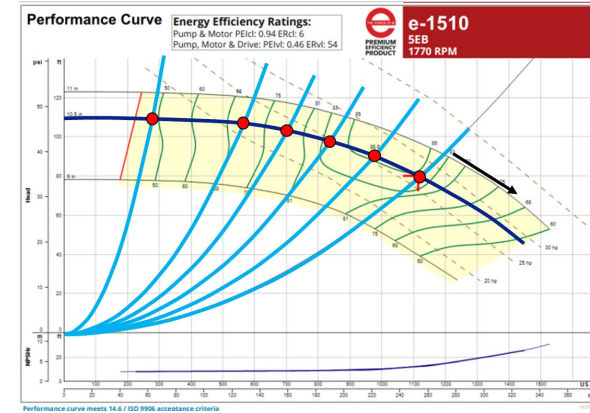
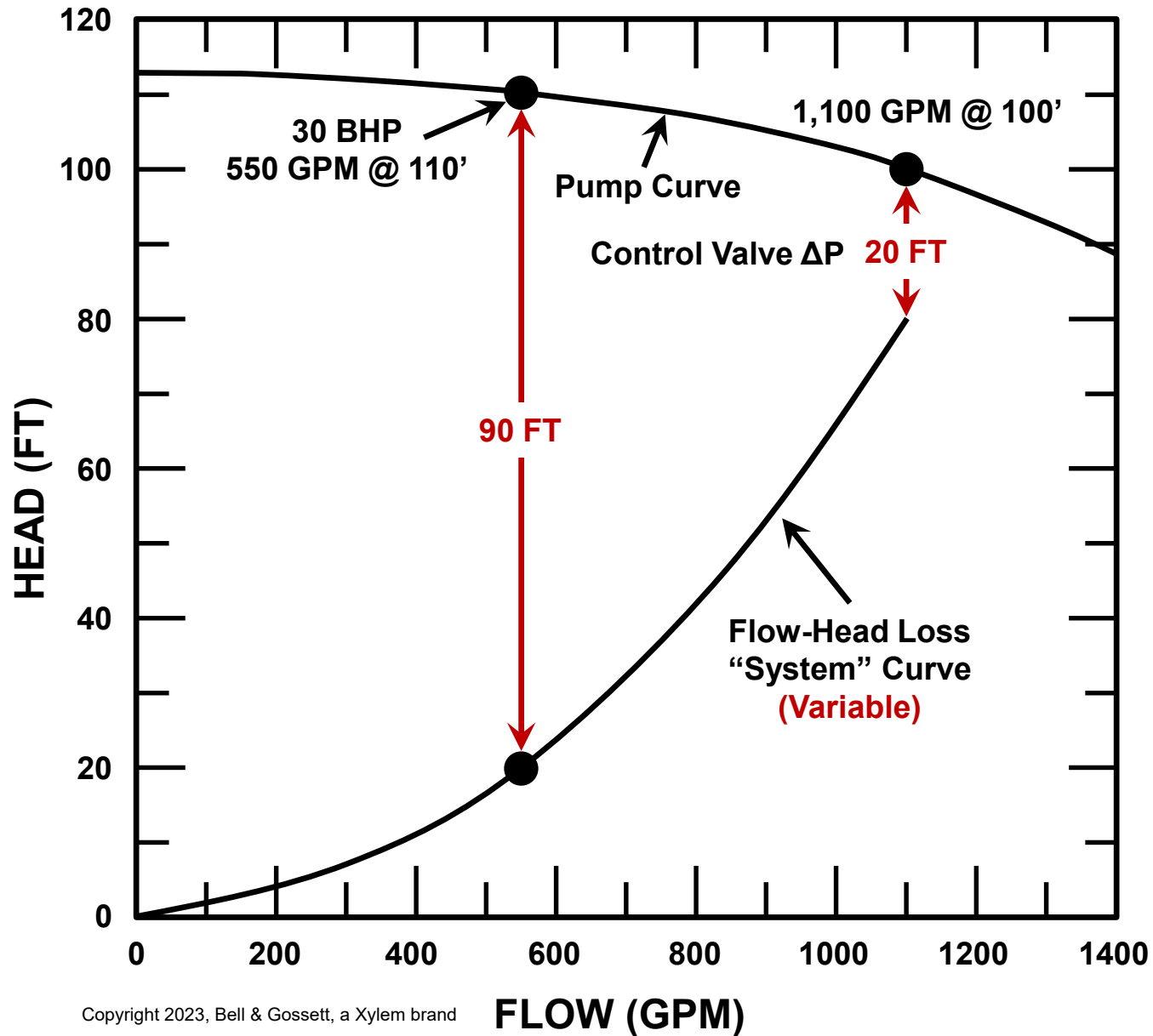
Variable Speed Pumping

ASHRAE 90.1 Section 6.5 – Prescriptive Compliance Path

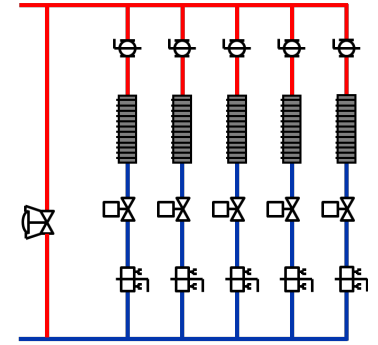
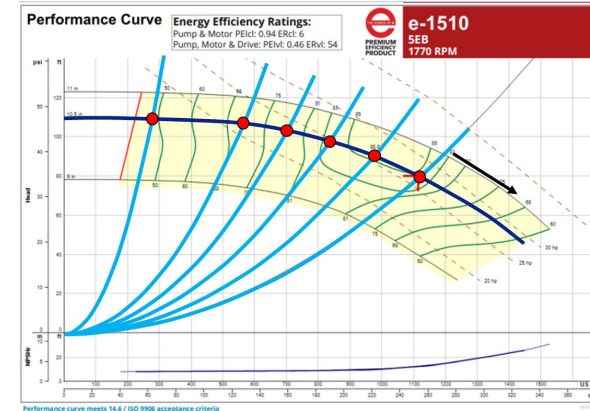
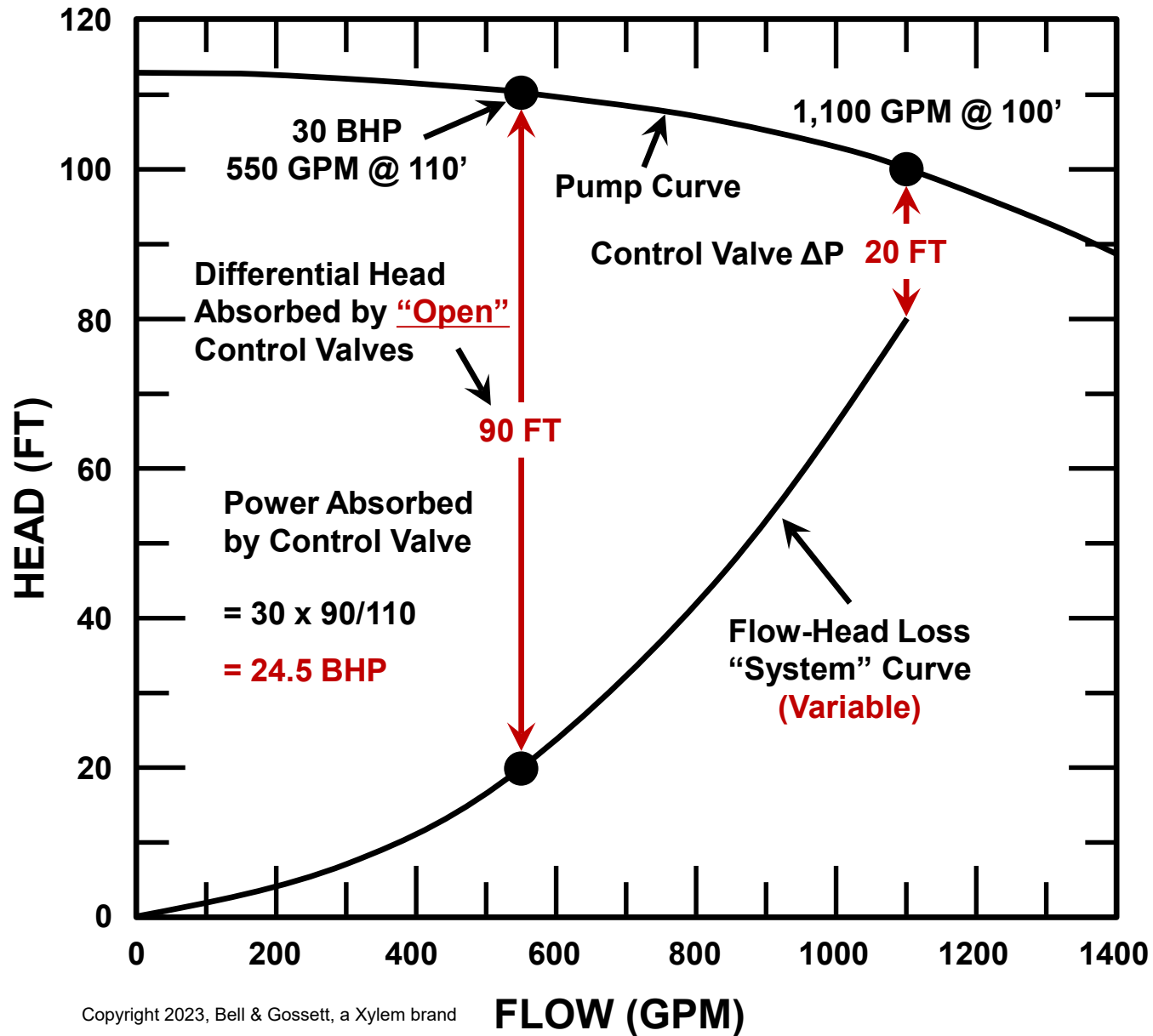
6.5.4.2 Hydronic Variable Flow Systems

Chilled- and – Hot Water *distribution systems* that include **three or more control valves** designed to modulate or step open and close as a function of load shall be designed for variable fluid flow and shall be capable of and configured to **reduce pump flow rates to no more than the larger of 25% of the design flow rate or the minimum flow required by the heating/cooling equipment manufacturer** for the proper operation of *equipment*.

.... Individual or parallel pumps serving variable-flow heating-water or chilled-water *systems*, where the *nameplate horsepower* of the motor or combined parallel motors is at least **2 HP or greater**, shall have *controls* or devices that will result in pump motor demand of **no more than 30% of design wattage at 50% of the design water flow.**



- Pump Head increases with flow reduction
- Piping/Equipment head loss decreases with flow reduction



- Pump Head increases with flow reduction
- Piping/Equipment head loss decreases with flow reduction

- Flow

- $Q_2 = Q_1 (N_2/N_1)$

- Head

- $h_2 = h_1 (N_2/N_1)^2$

- Power

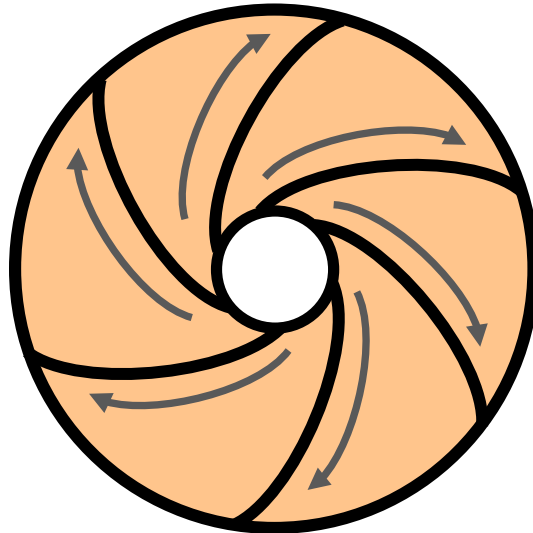
- $bhp_2 = bhp_1 (N_2/N_1)^3$

Q = Flow

N = Speed

h = head

bhp = Horsepower

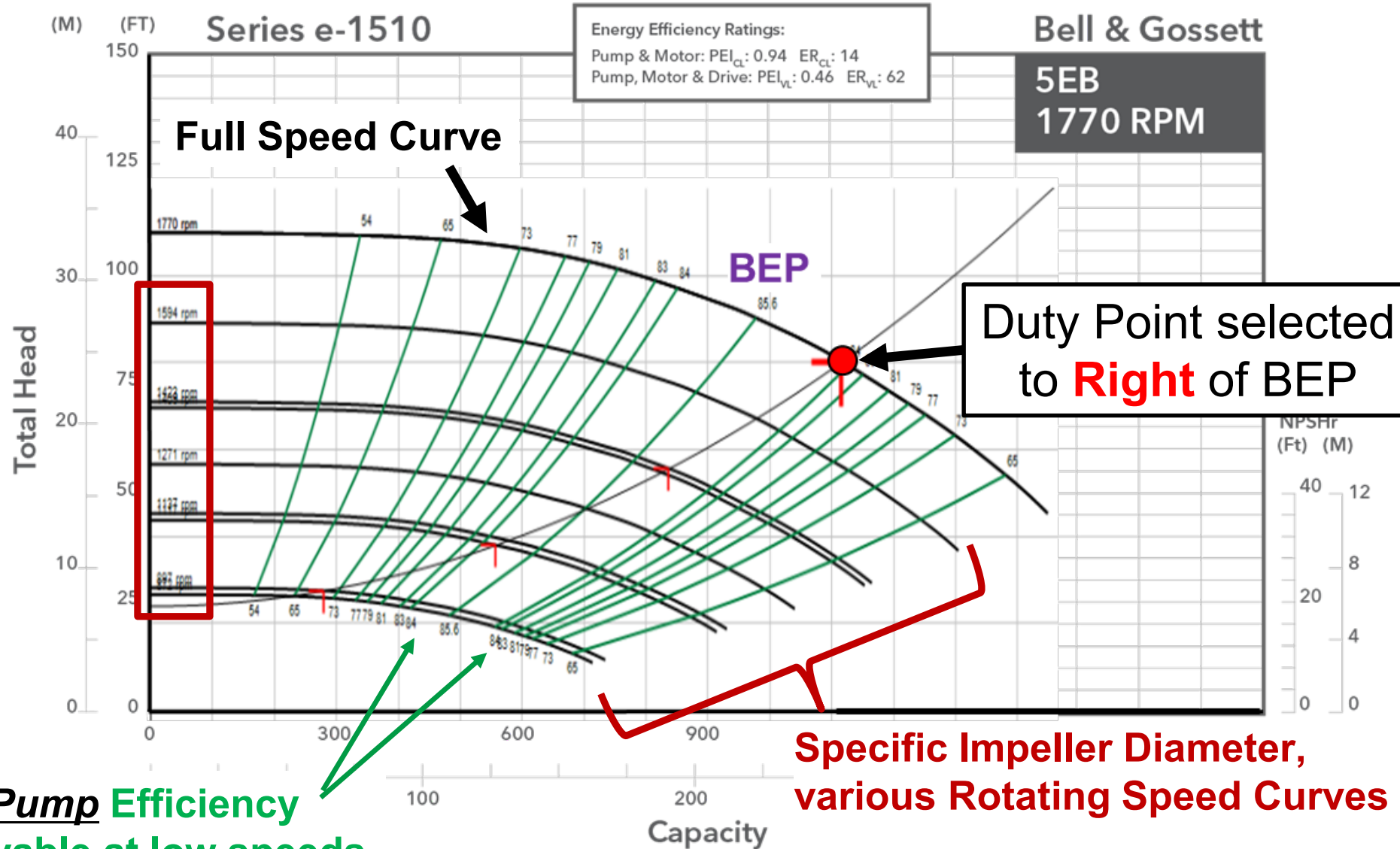


Speed	Flow/Volume	Head	Horsepower Required
100%	100%	100%	100%
90%	90%	81%	73%
80%	80%	64%	51%
70%	70%	49%	34%
60%	60%	36%	22%
50%	50%	25%	13%
40%	40%	16%	6%
30%	30%	9%	3%
20%	20%	4%	-
10%	10%	1%	-
0%	0%	0%	-

Subscript 2 indicates “new condition”

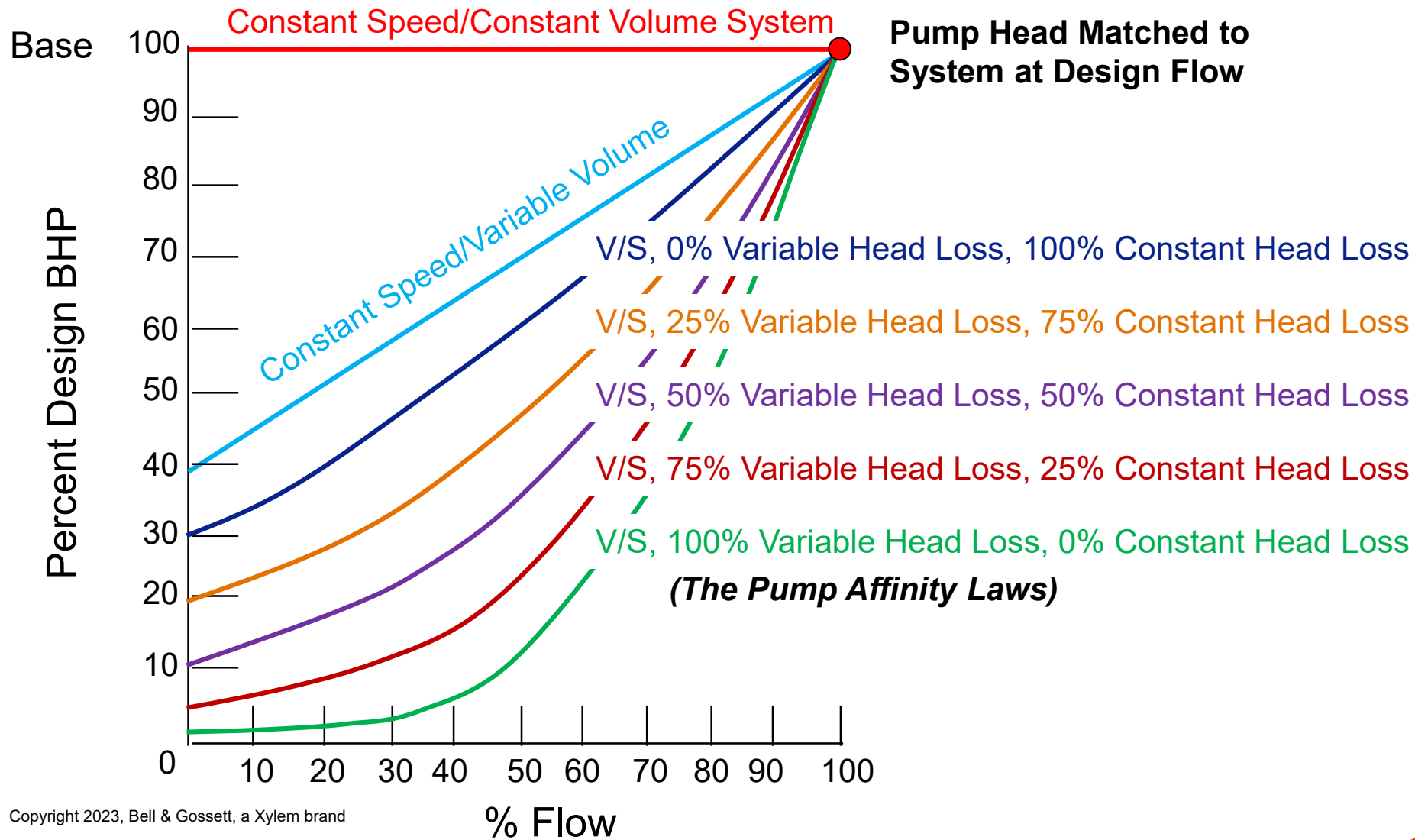
Subscript 1 indicates “old condition”

- Assumes all Head is “Variable”
- Efficiency will remain relatively constant

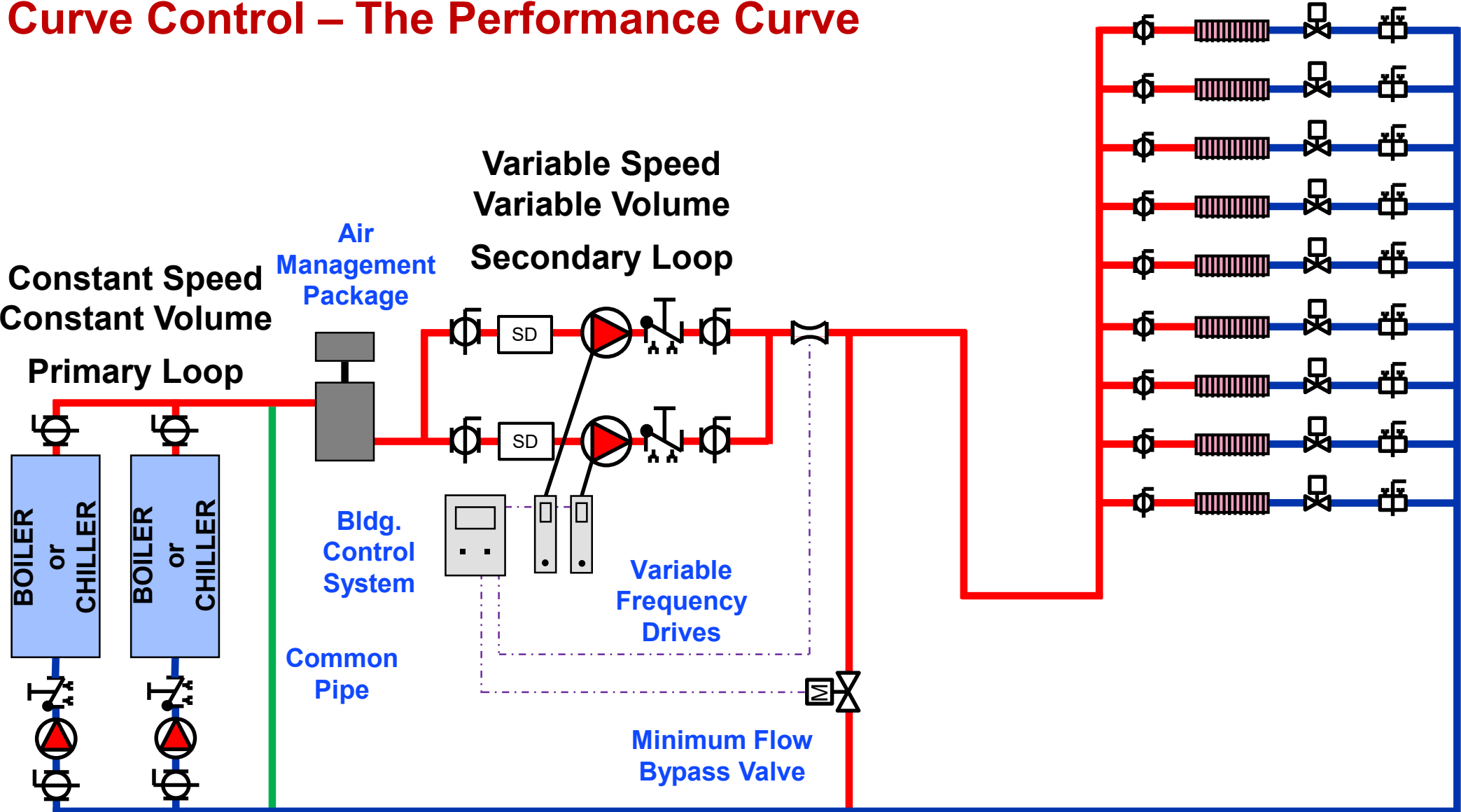


High Pump Efficiency achievable at low speeds

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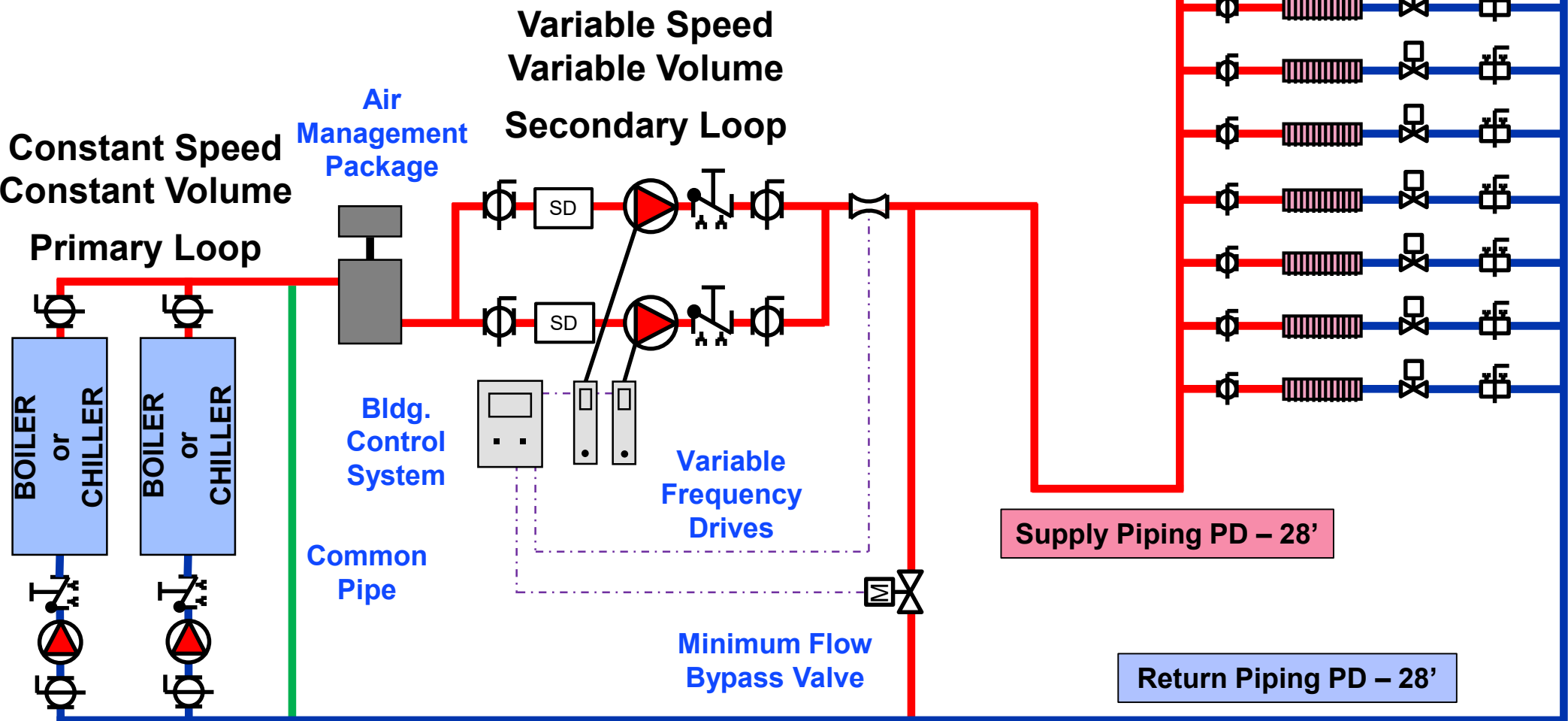


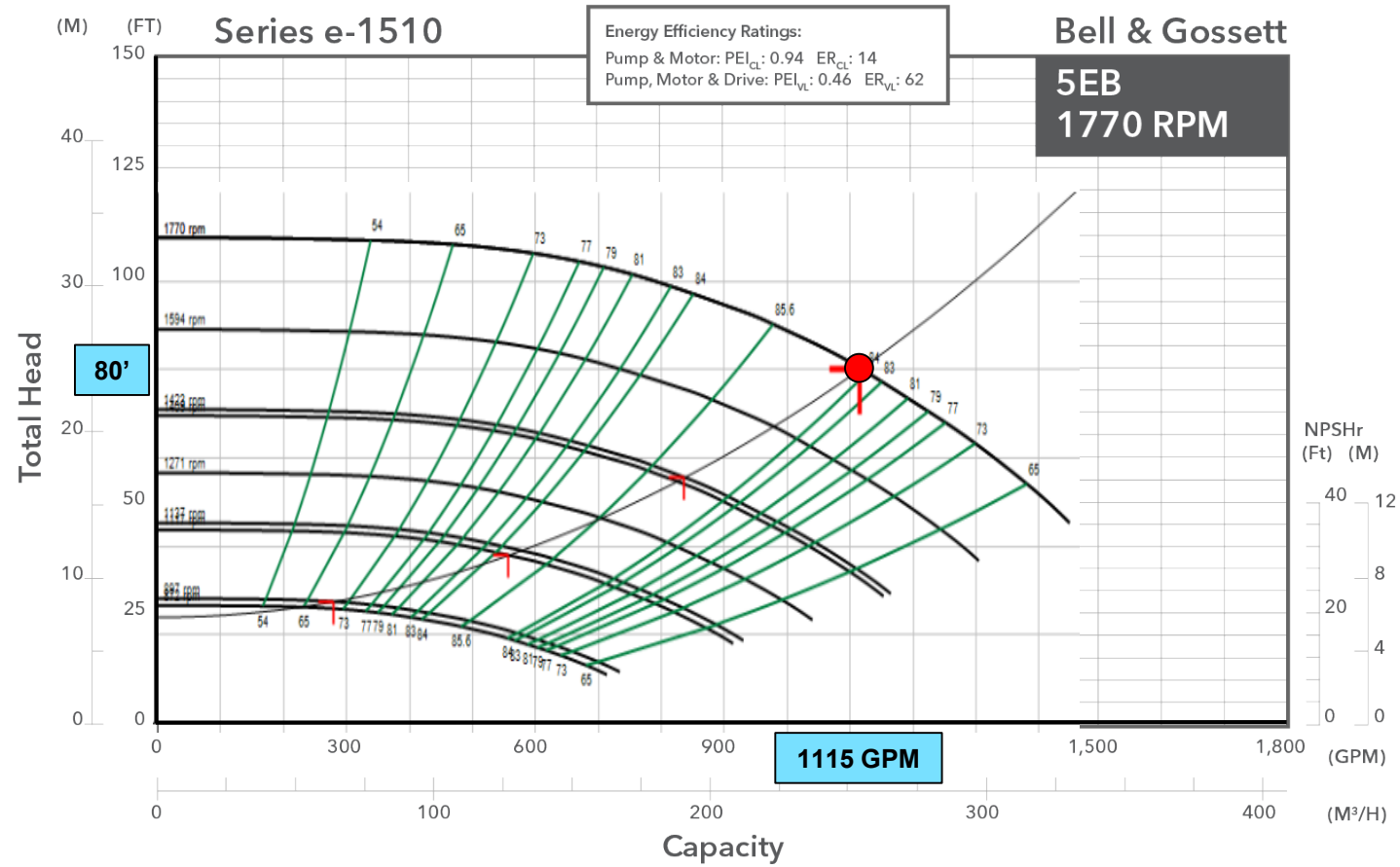
Curve Control – The Performance Curve

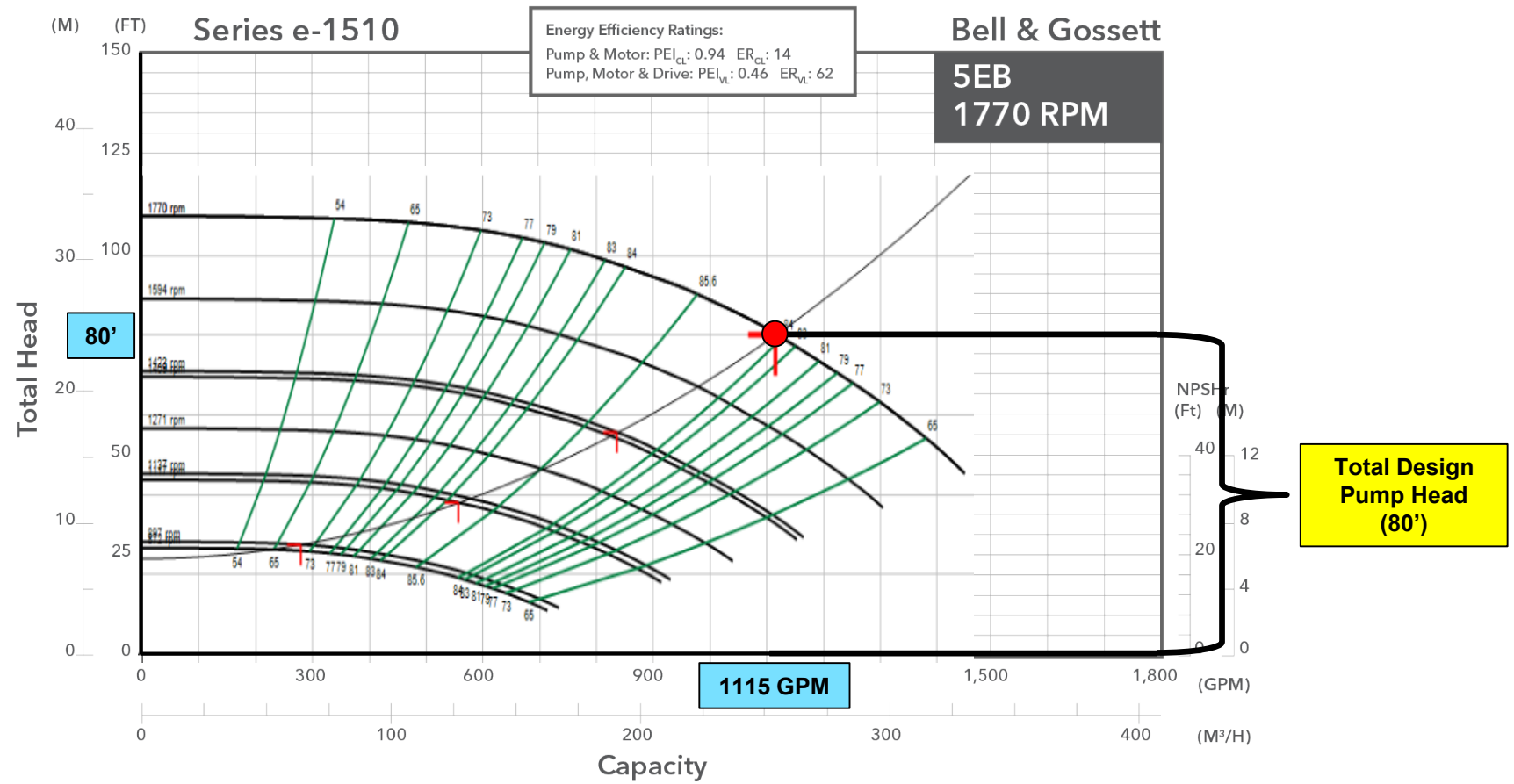


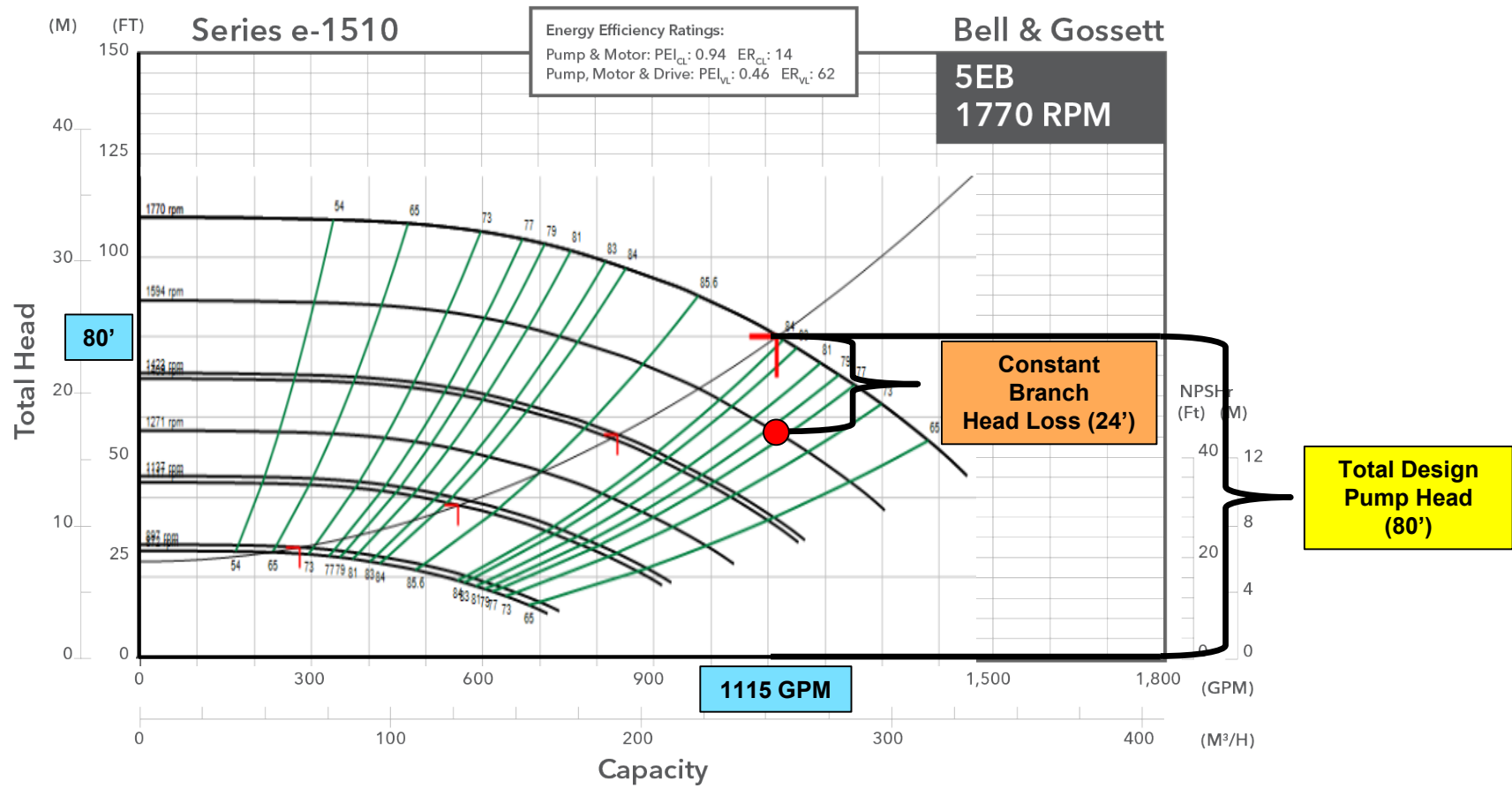
Curve Control – The Performance Curve

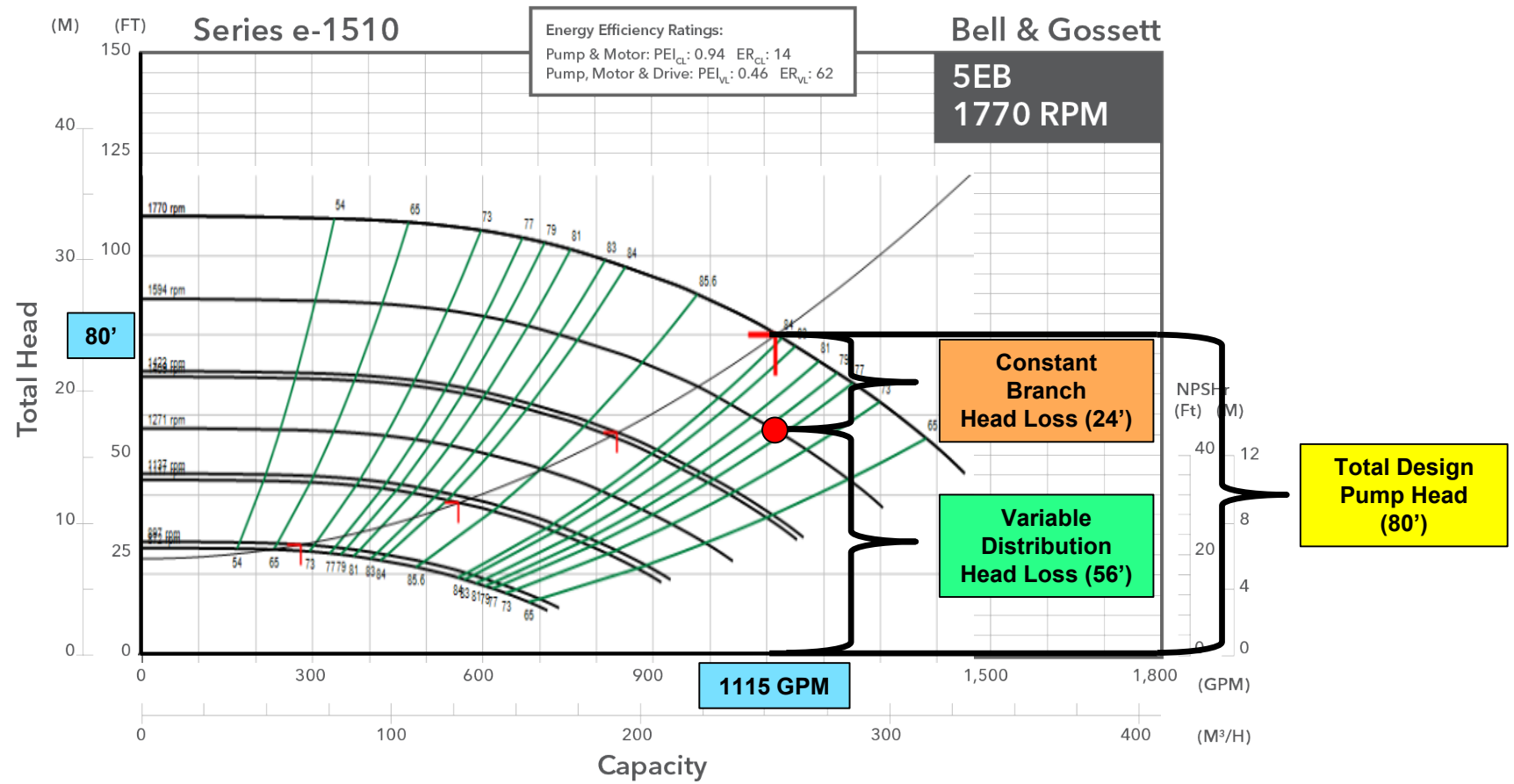
Secondary Pumps – 1115 GPM @ 80'







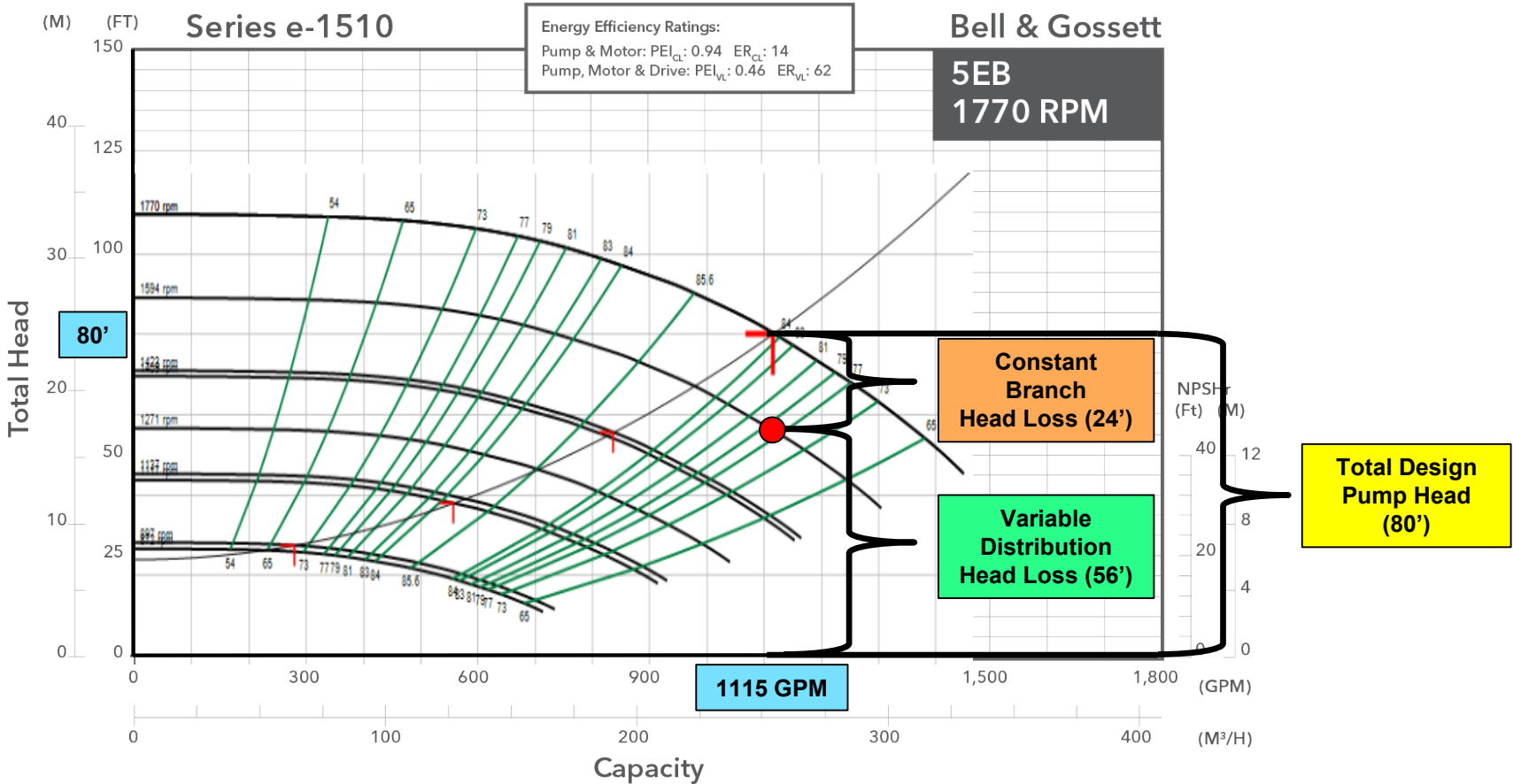




The "System Curve"

$$\left(\frac{Q_2}{Q_1}\right)^2 = \left(\frac{h_2}{h_1}\right)$$

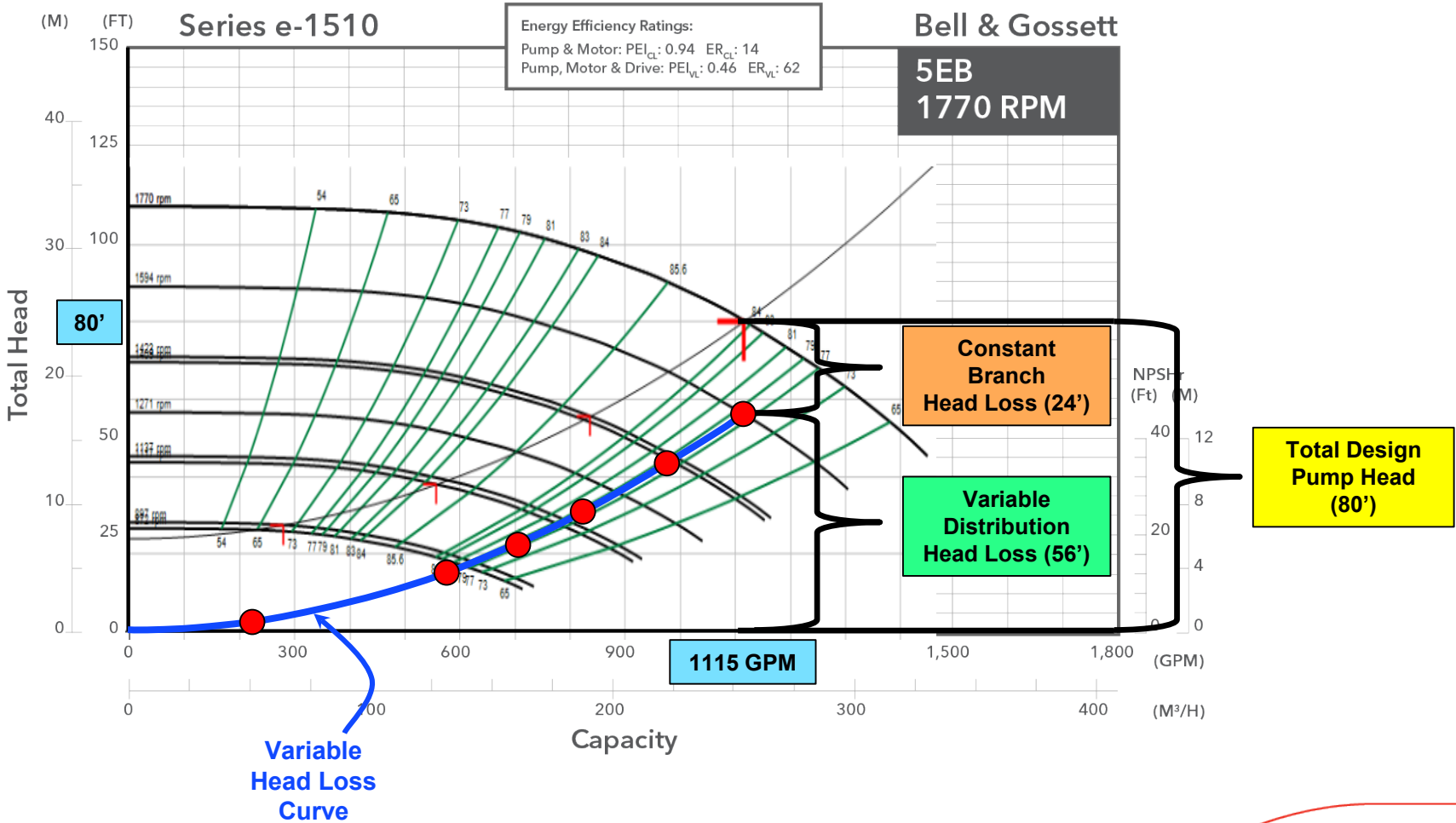
Flow (GPM)	Head (FT)
1115	56
978	43
825	31
705	22
578	15
225	2
0	0



The "System Curve"

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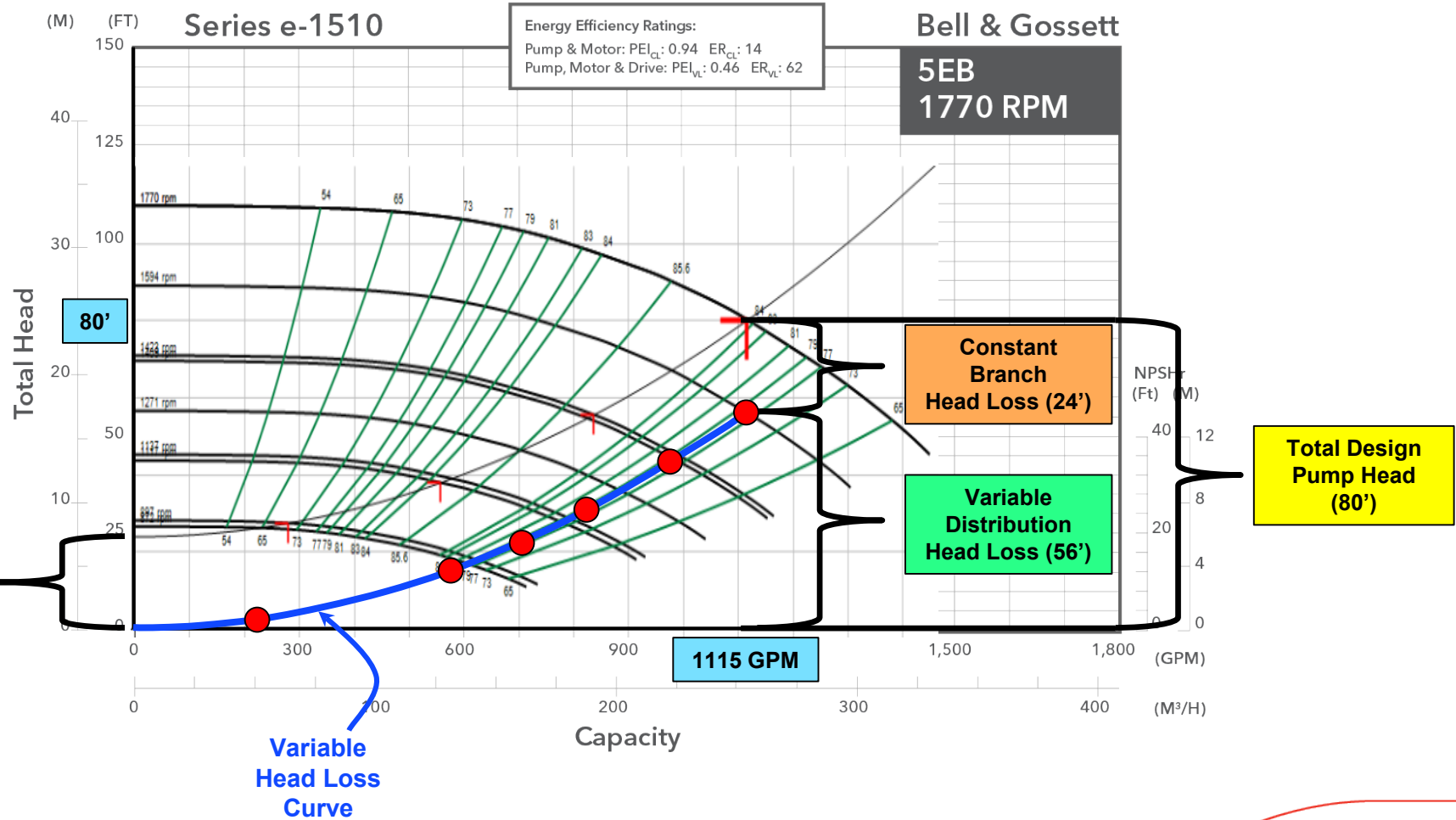
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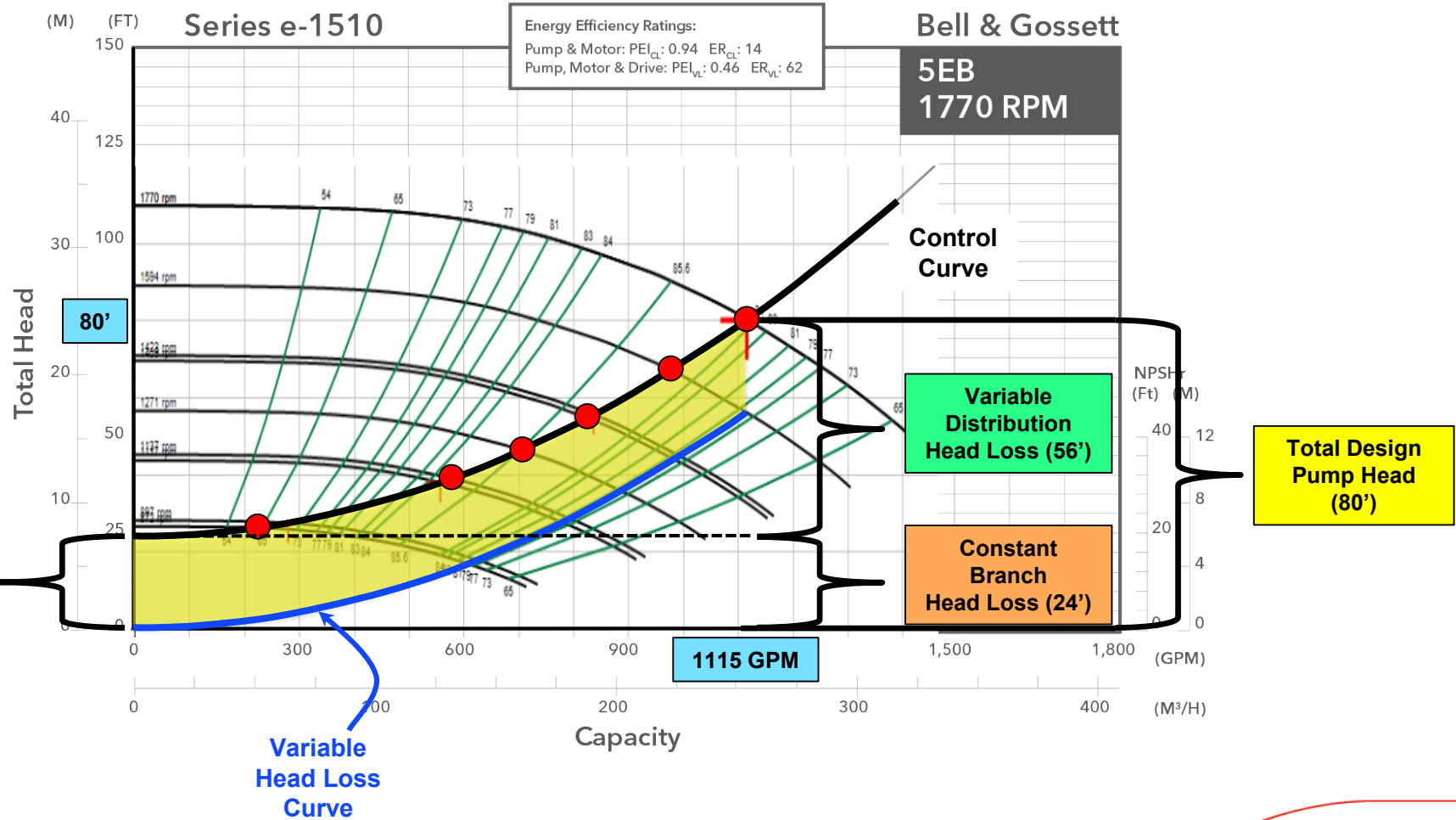
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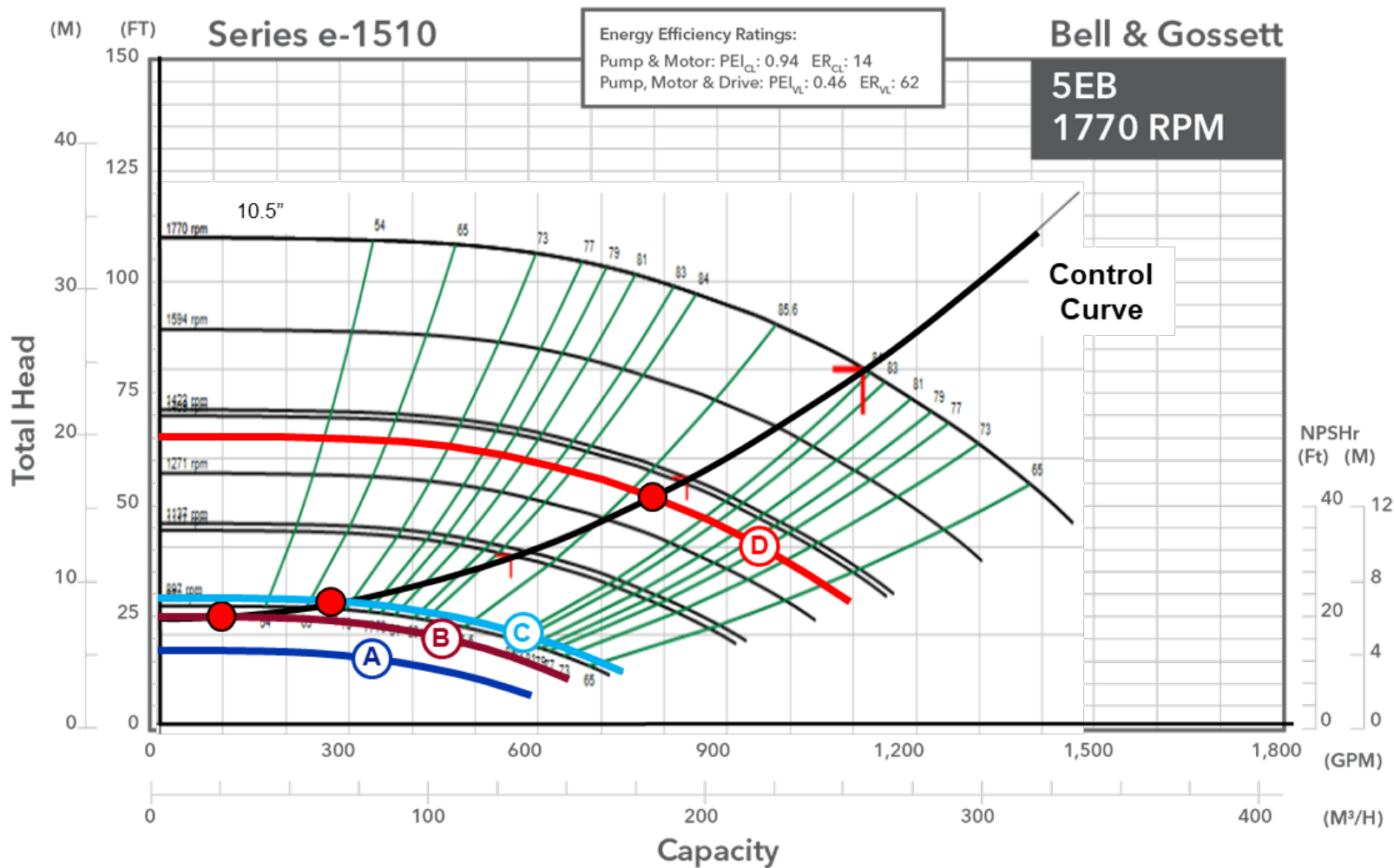


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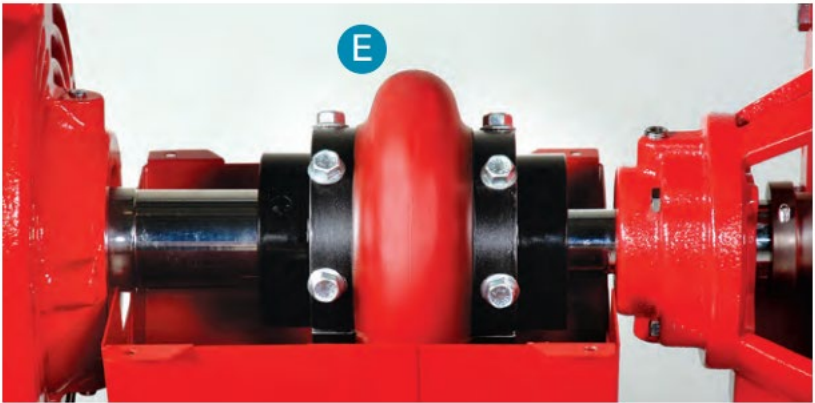
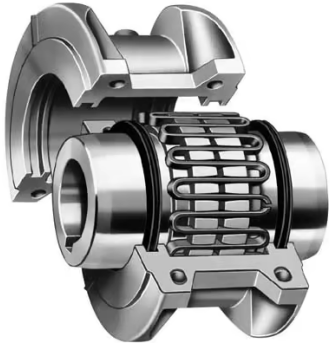
• **All Pump Applications:**

- Ⓐ Minimum recommended speed by motor manufacturer. Typically 20%-30% of rated motor RPM.
- Ⓑ Speed required to generate minimum Control Head
- Ⓒ Speed required to generate minimum Pump Flow

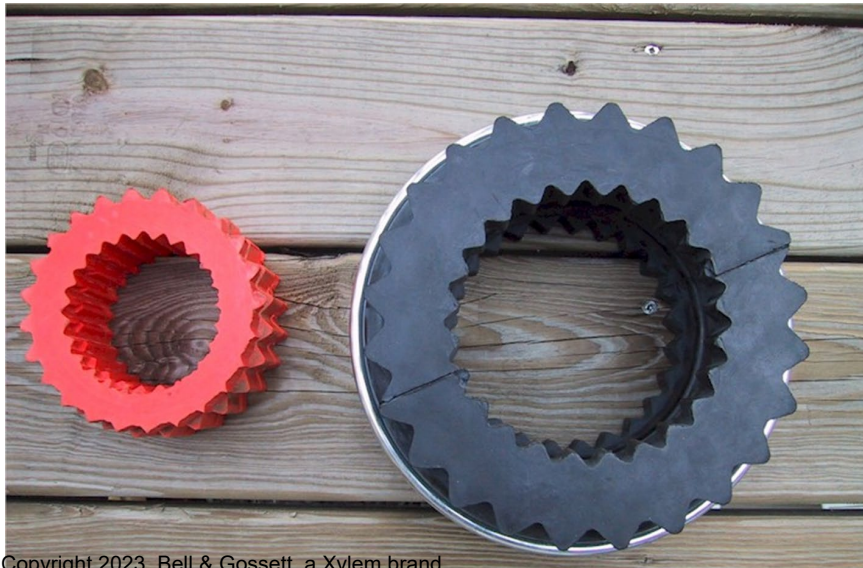
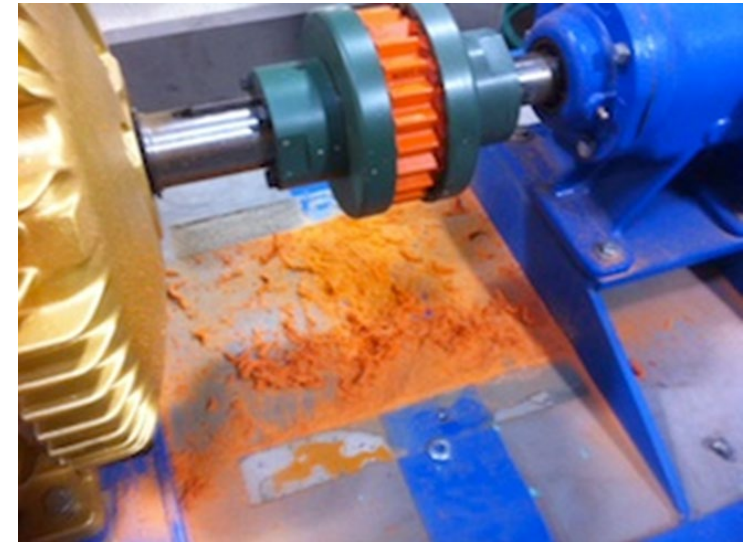
• **Variable Primary Applications:**

- Ⓓ Speed required to provide minimum Equipment Flow (*Chiller, Boiler, Heat Exchanger*)

What type of coupler?



- Hytrel is a stiffer durometer
- Plastic Resin melts and shreds
- EPDM/Neoprene replacement will be larger
- Adequate space between motor and bearing frame required.
- Is motor position adjustable??



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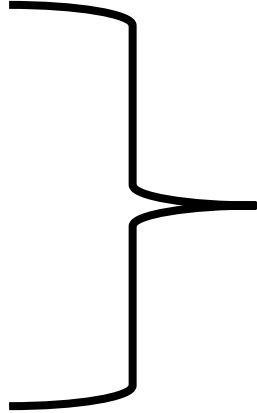


Selecting the correct VSD Control Strategy

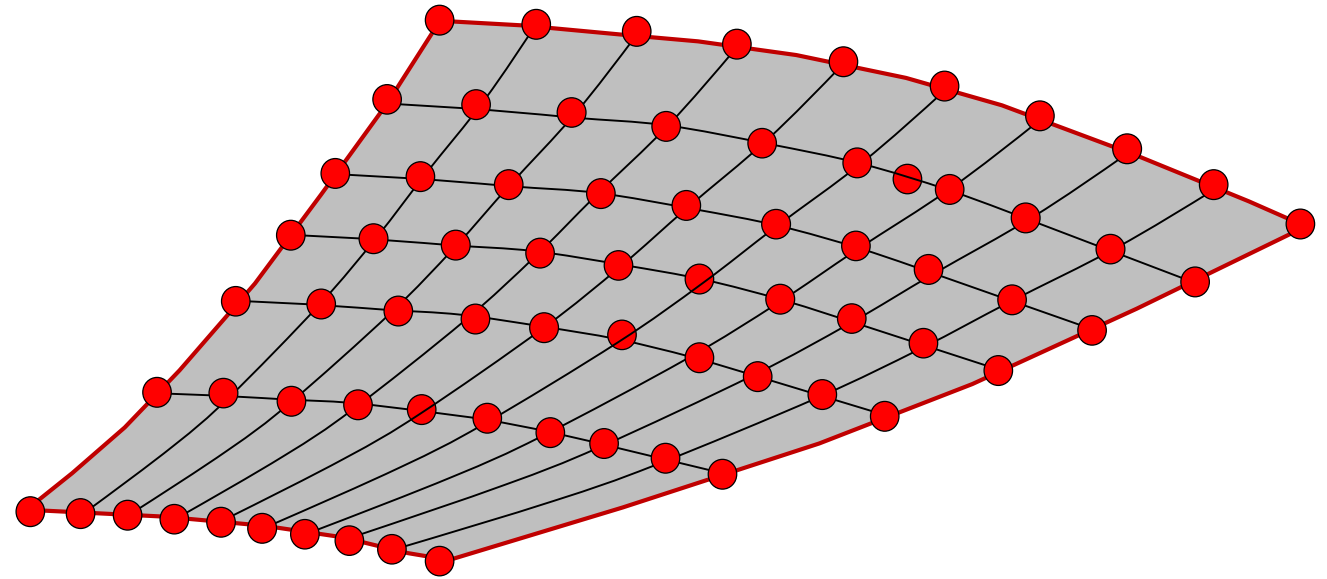
Curve Control

• Factory generated Pump Performance Map

- Flow
- Head
- Power
- Speed
- Torque



7 Speeds
10 Data Pts. Each



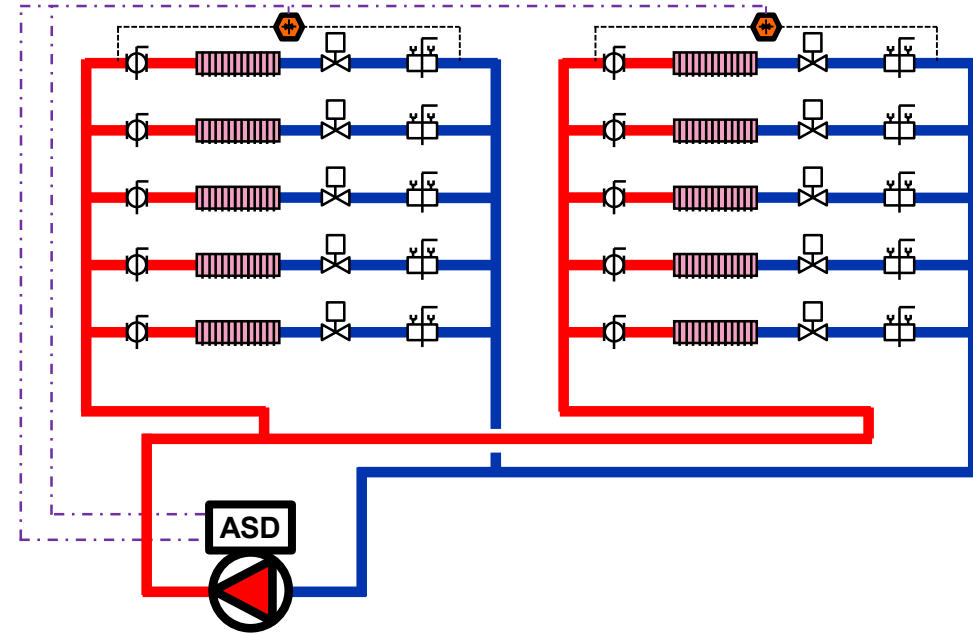
Area Control

- **Feedback Sensor(s) located in the System**

- Wired directly to ASD
- Wired to a BMS

Applications

- High Diversity Hot & Chilled Water Systems
- Large Control Area (*Low BRPDR*)



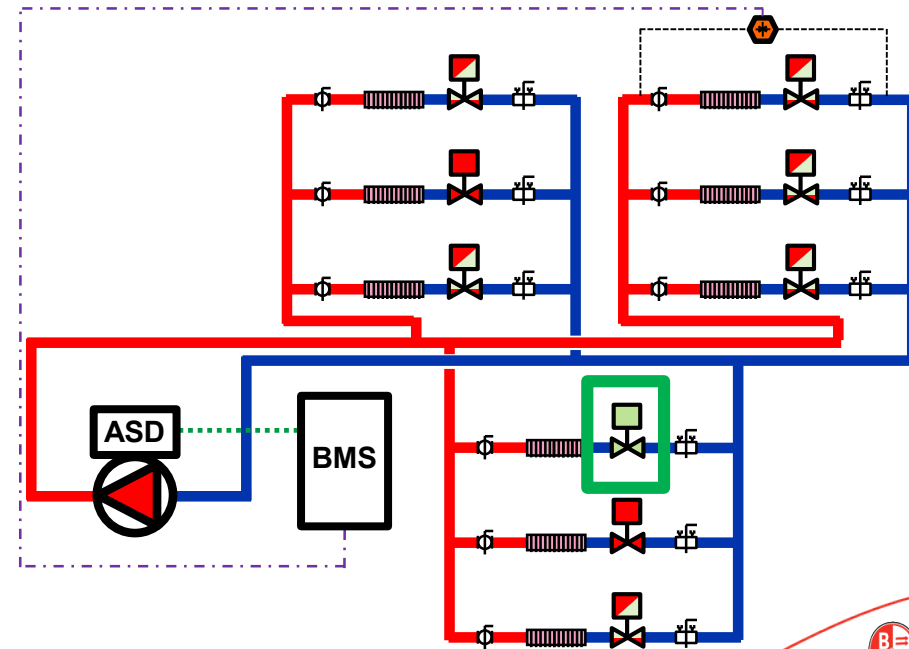
Area Control

- **Control Valve Position (ASHRAE 90.1 “Reset”)**
 - Use Valve Actuator Feedback Signal Only
 - Add Differential Pressure Sensor, modify setpoint

Applications

- Where BMS can monitor valve position
- **Not recommended when PICV's are used**

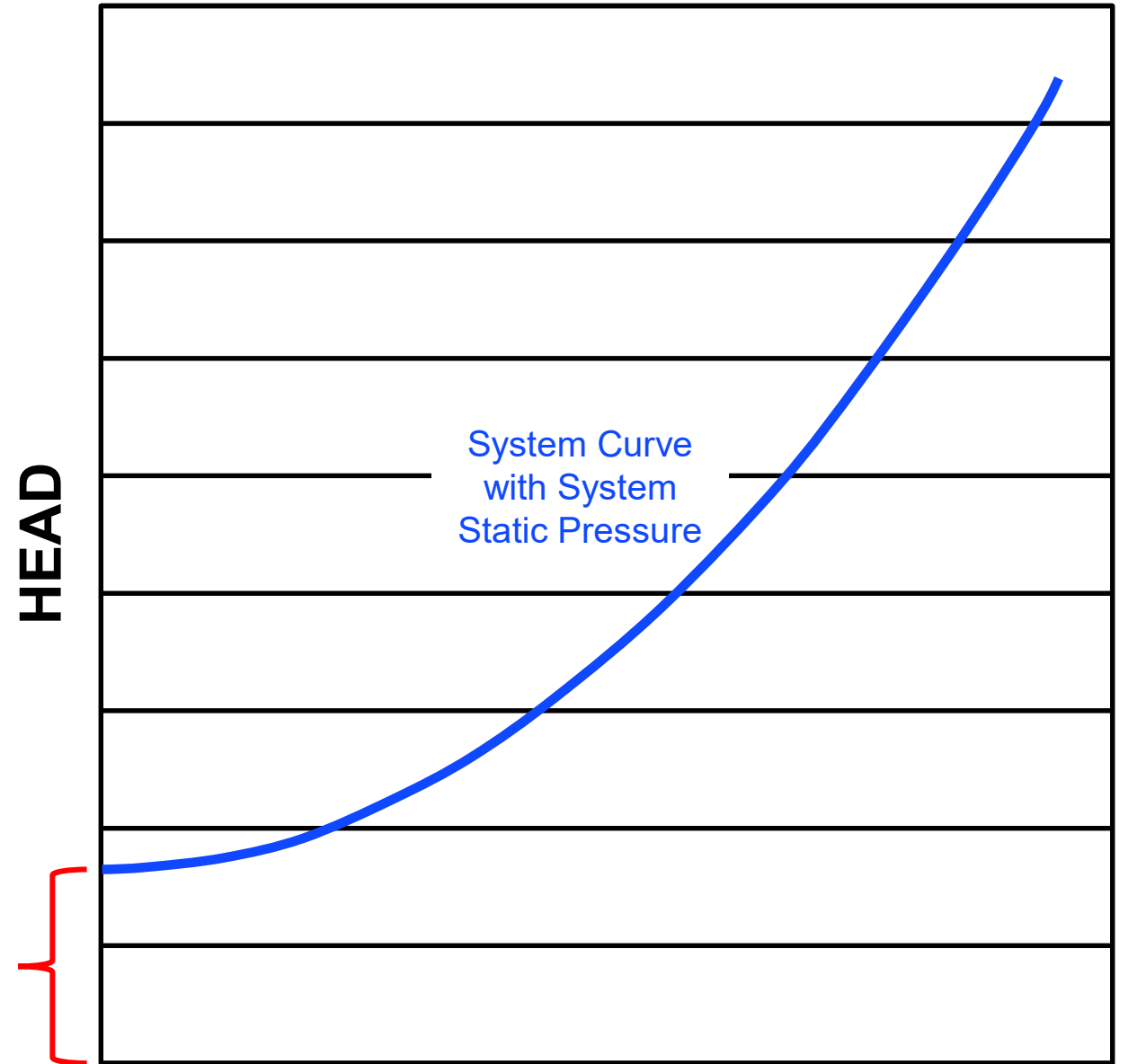
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The “**Control Area**” represents all flow/head operating point possibilities for a specific piping system.

- Accounts for system resistance changes with load adjustments, dependent on where they occur in the piping network
- The size and shape is influenced by piping ***Branch to Riser Pressure Drop Ratio***
- Used for selecting applicable Variable Speed Control Strategy

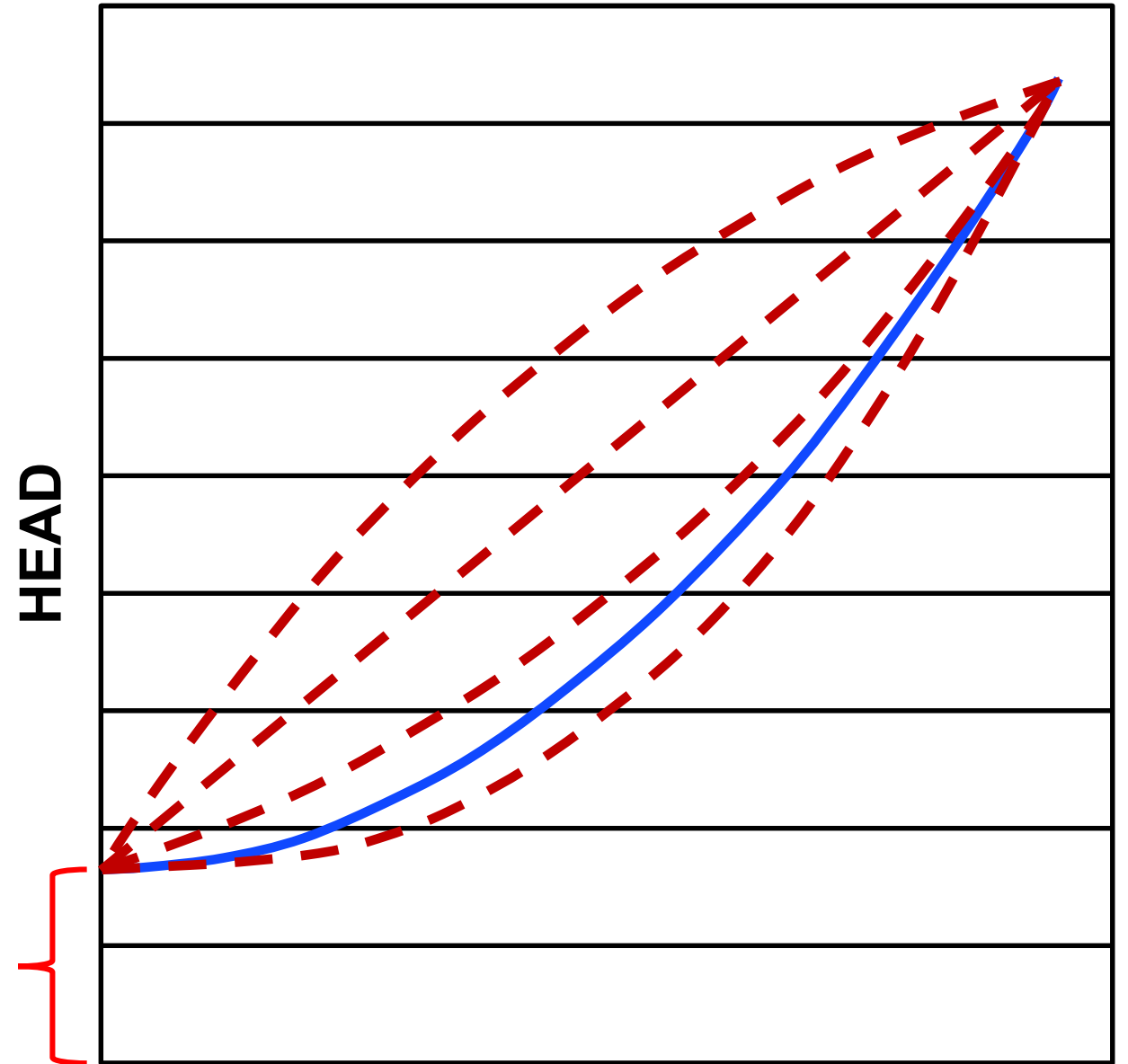
**Static
(Control)
Head**



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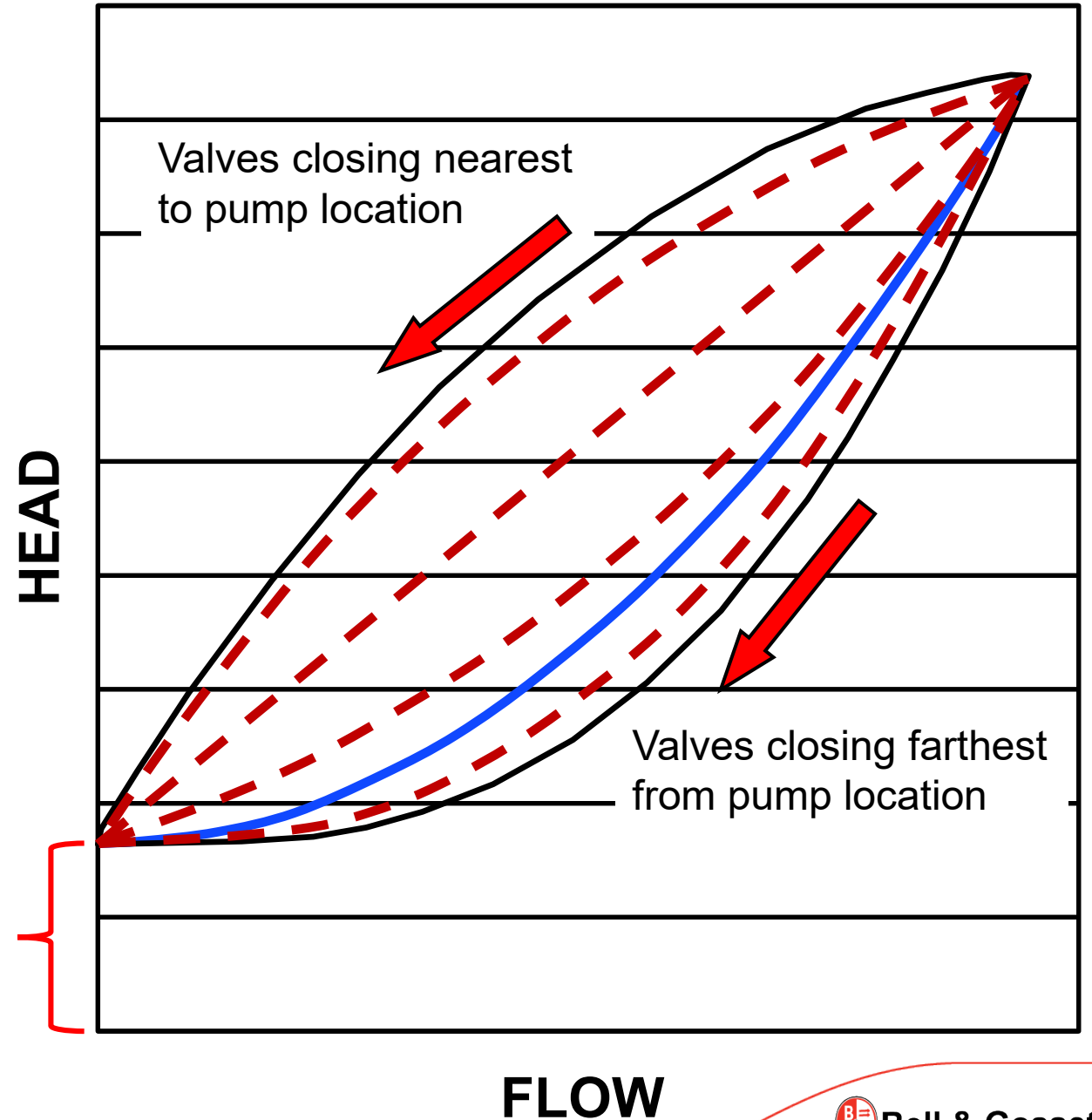
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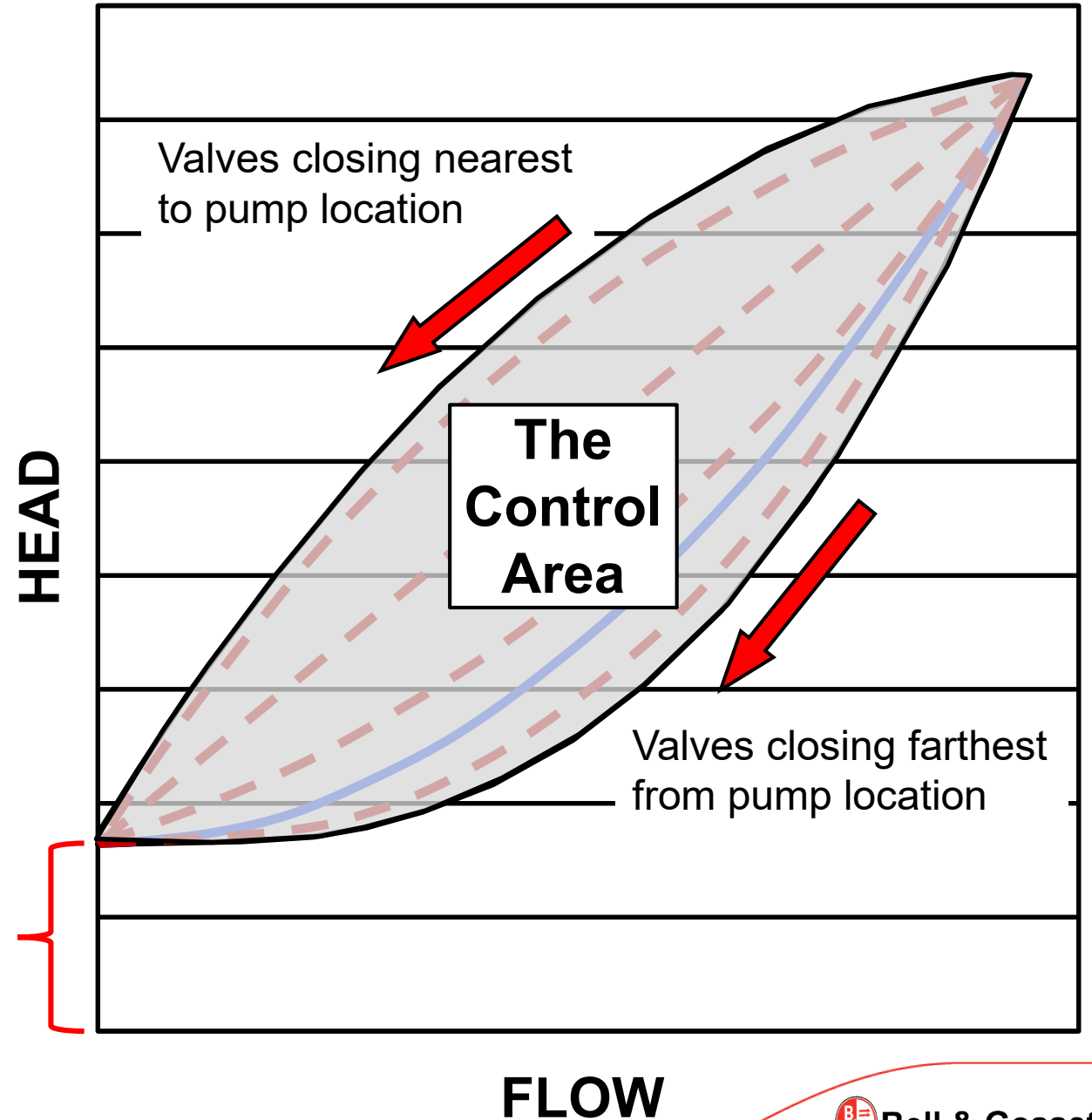
**Static
(Control)
Head**

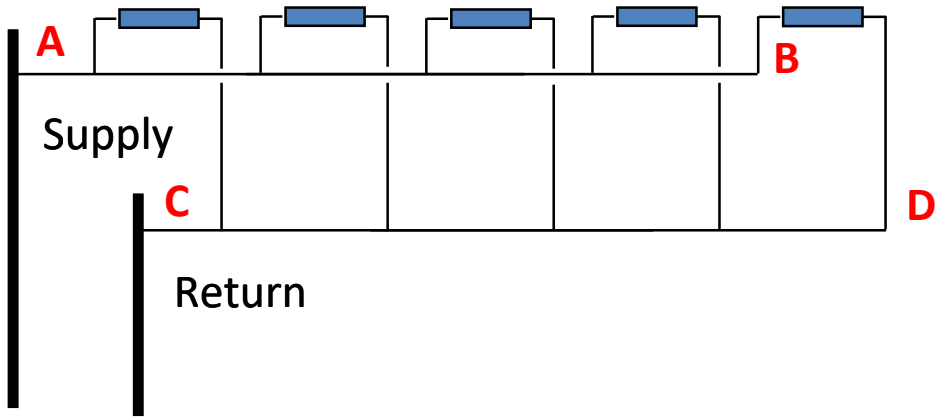


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**Static
(Control)
Head**



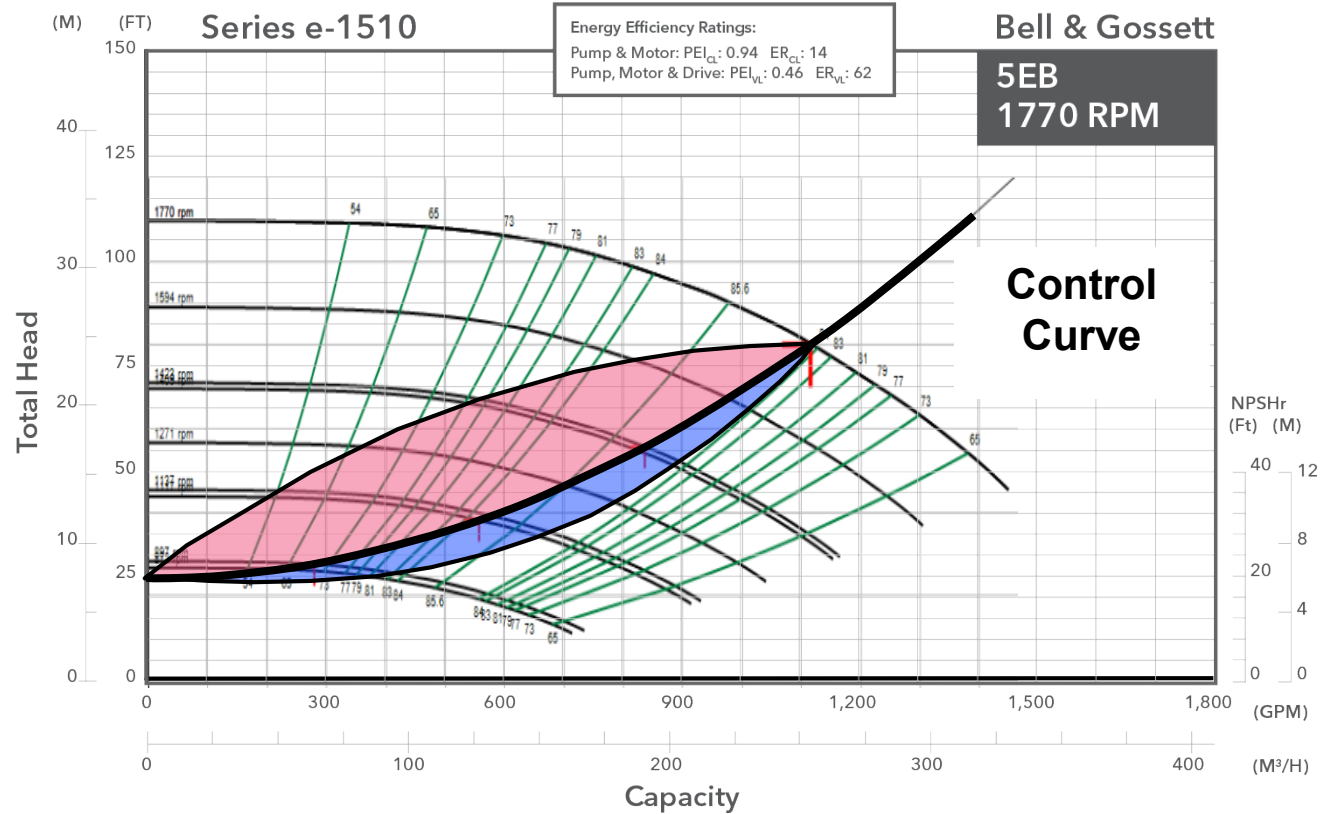


$$\text{BRPDR} = \frac{\text{BD}}{\text{AB} + \text{CD}}$$

BD – The “Branch”

AB – Supply Riser

CD – Return Riser



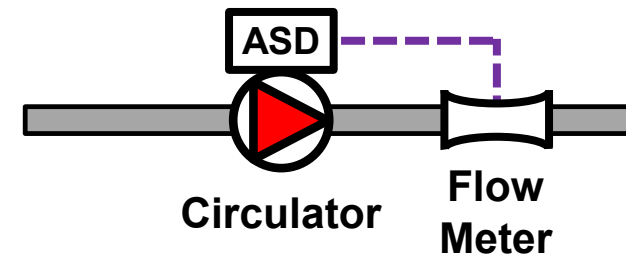
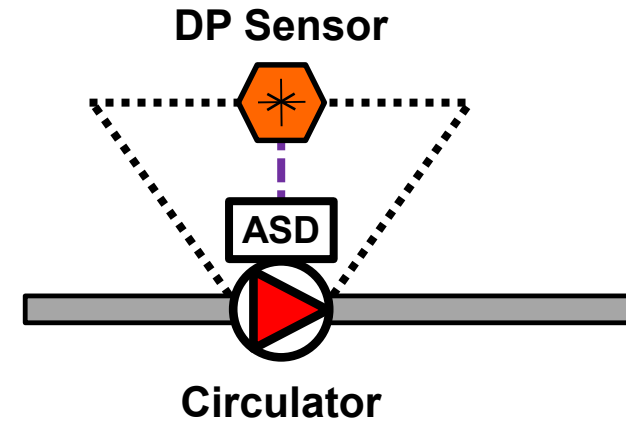
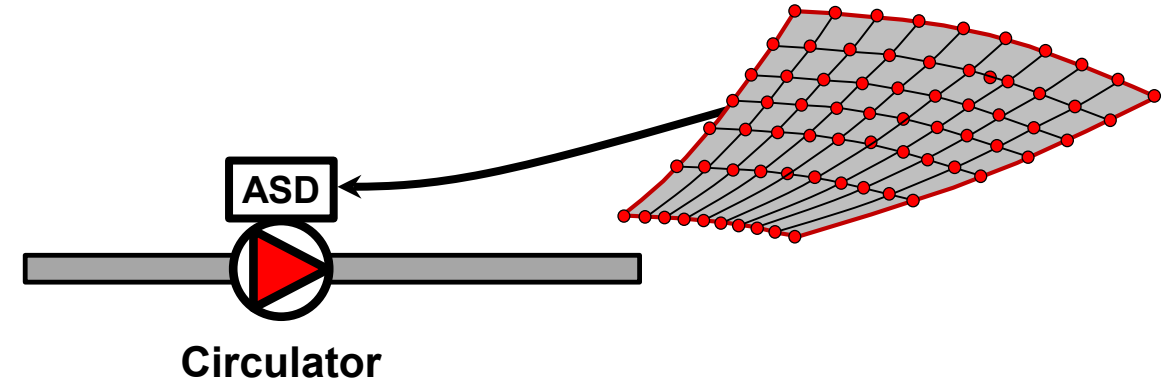
- The **higher** the Ratio, the **smaller** the Control Area

Curve Control

- Uses Factory generated Pump Performance Map
 - Monitor Motor Power & Torque change
 - Measure Differential Pressure across Pump
 - Measure Flow at Pump Outlet

Applications

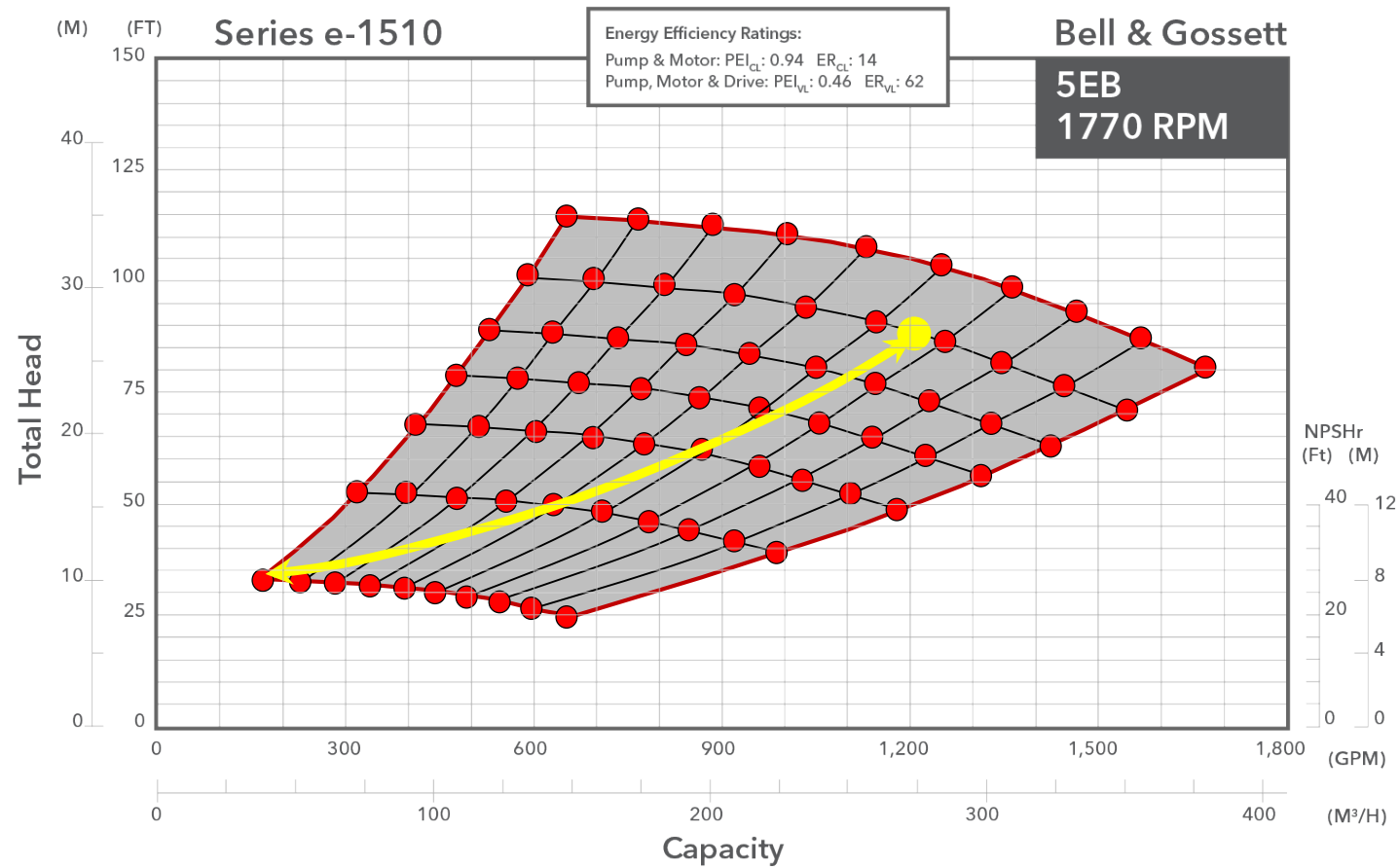
- Small Control Area (*High BRPDR*)
- Where Zones may be equally loaded
- Hot Water Systems where DDC not present
- Retrofit Systems





- Design Flow
- Design Head
- Minimum Control Head

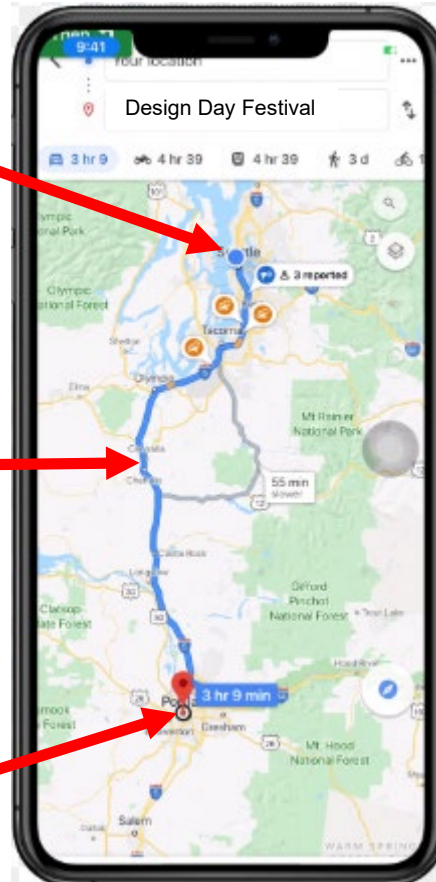
Factory Default is 40% of Pump Design Head

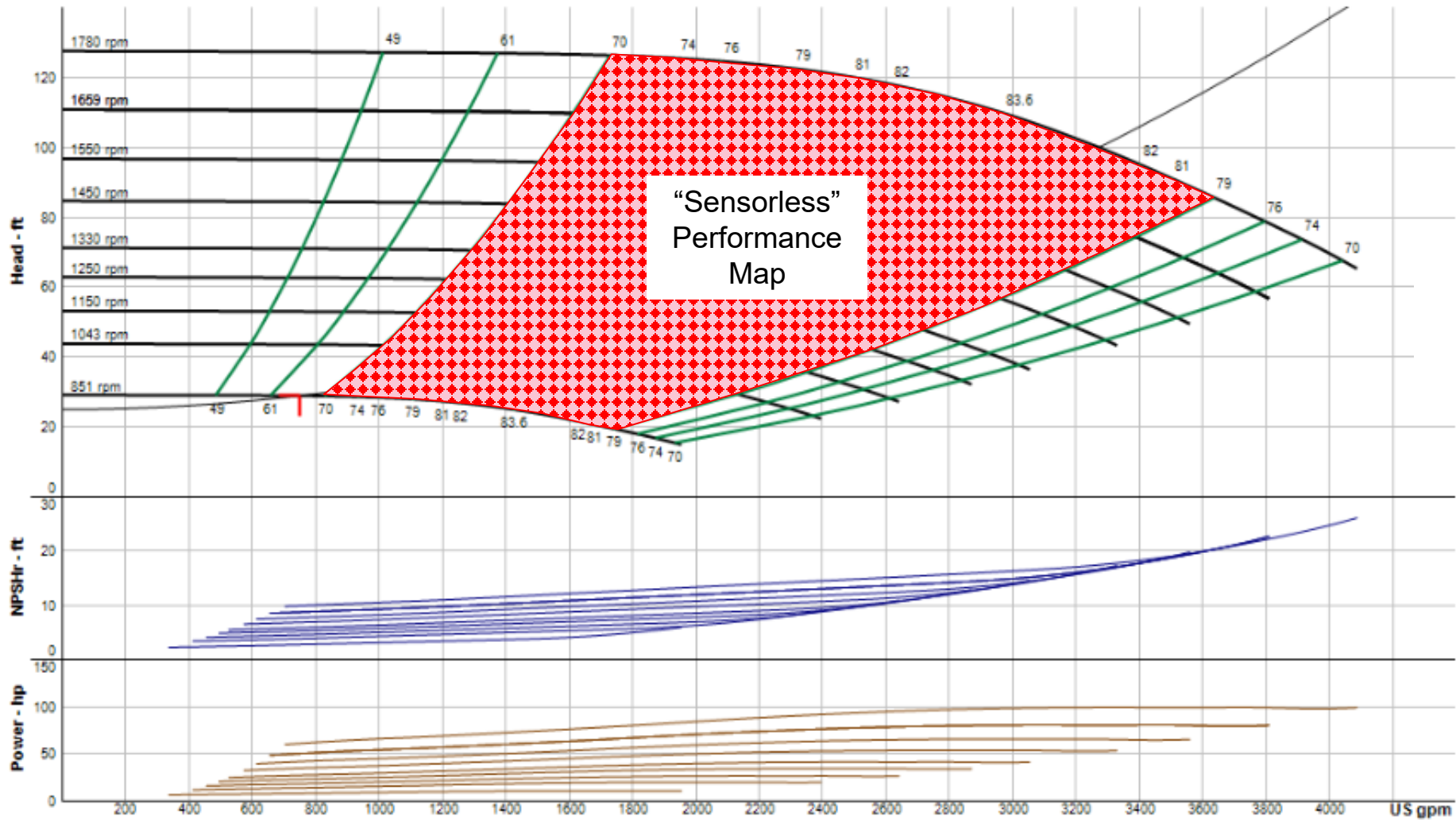


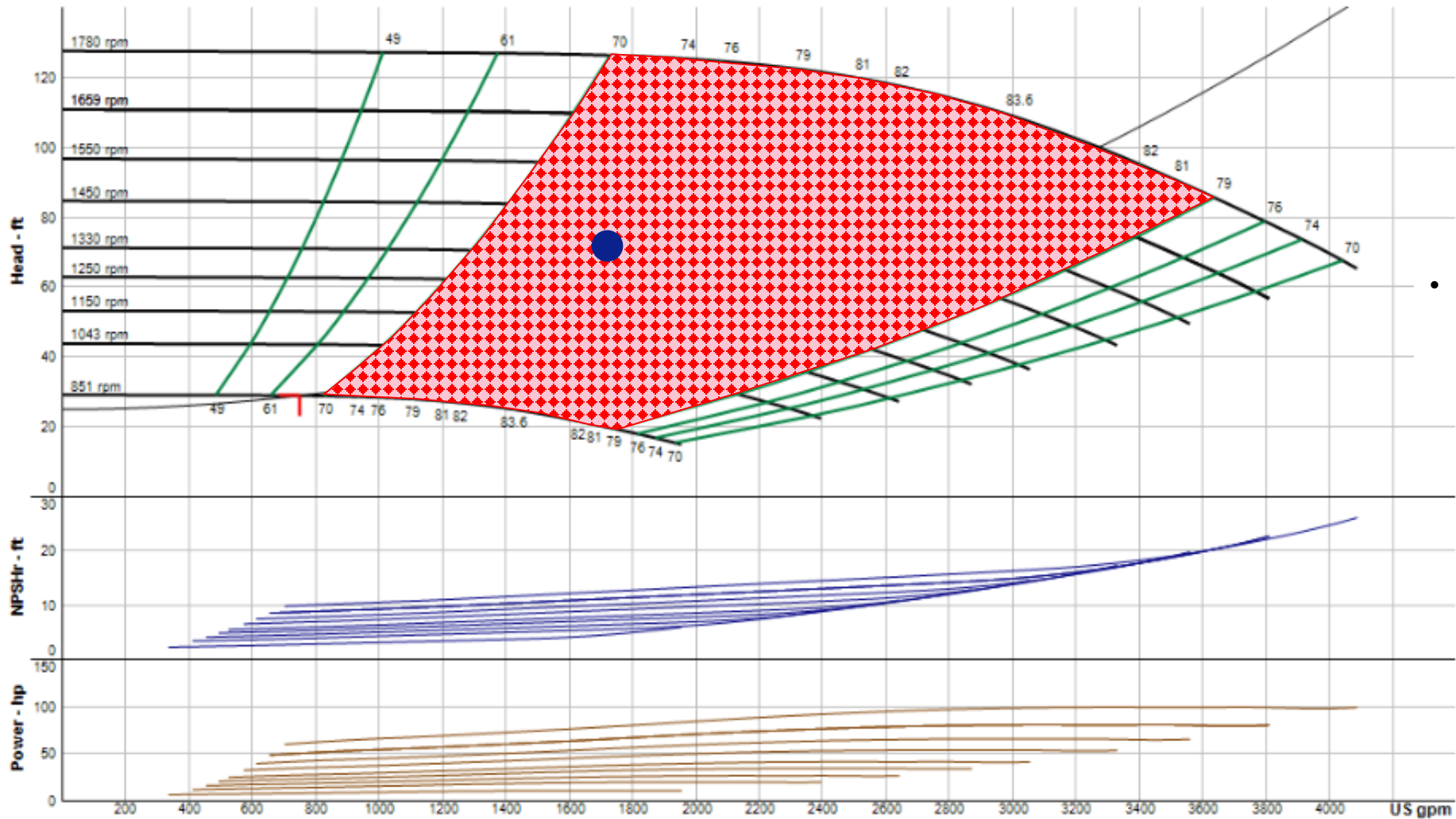
Your House
“Control Head” @ No Flow

Your Planned Route
“The Control Curve”

Your Destination
“Design Flow & Head”

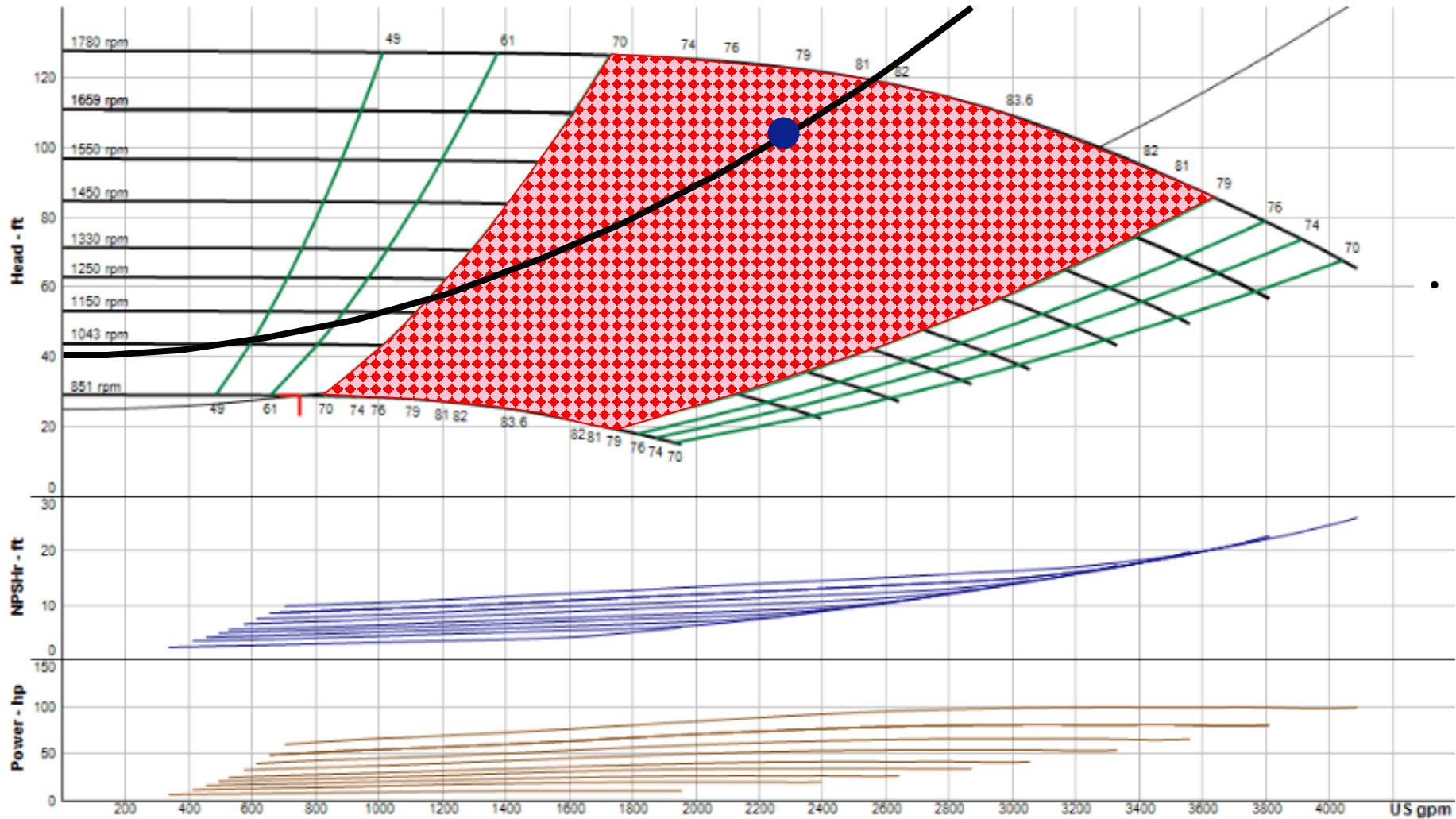






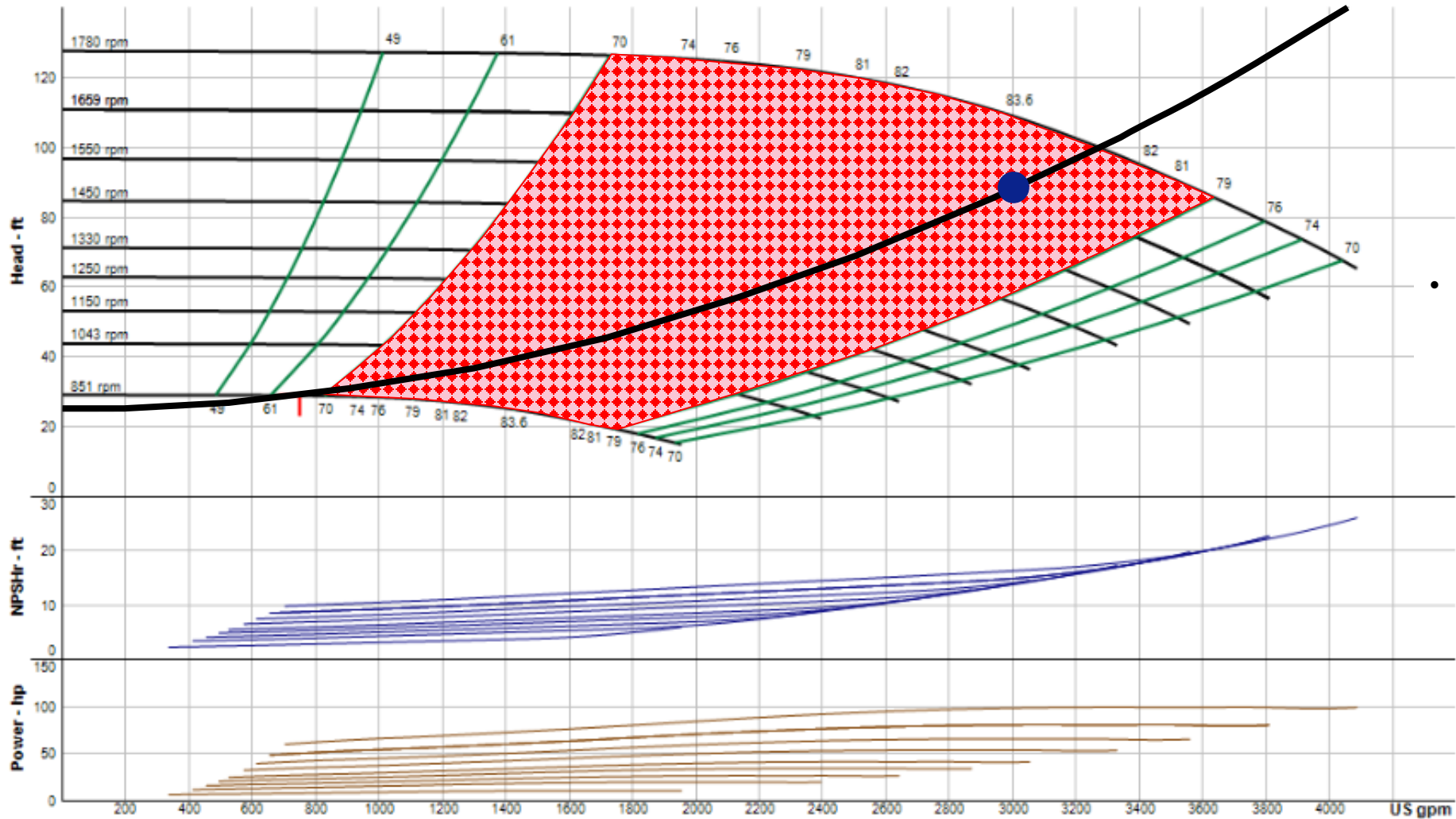
- Design Flow, Head, and Minimum Head can be adjusted in the field without impeller or motor modifications.





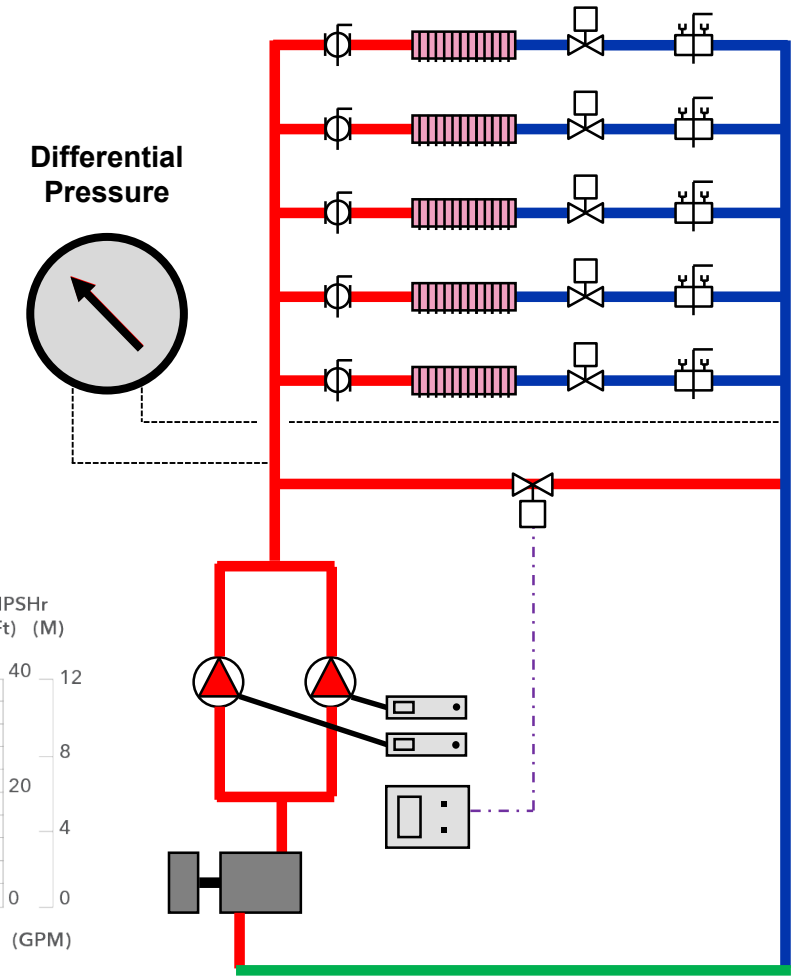
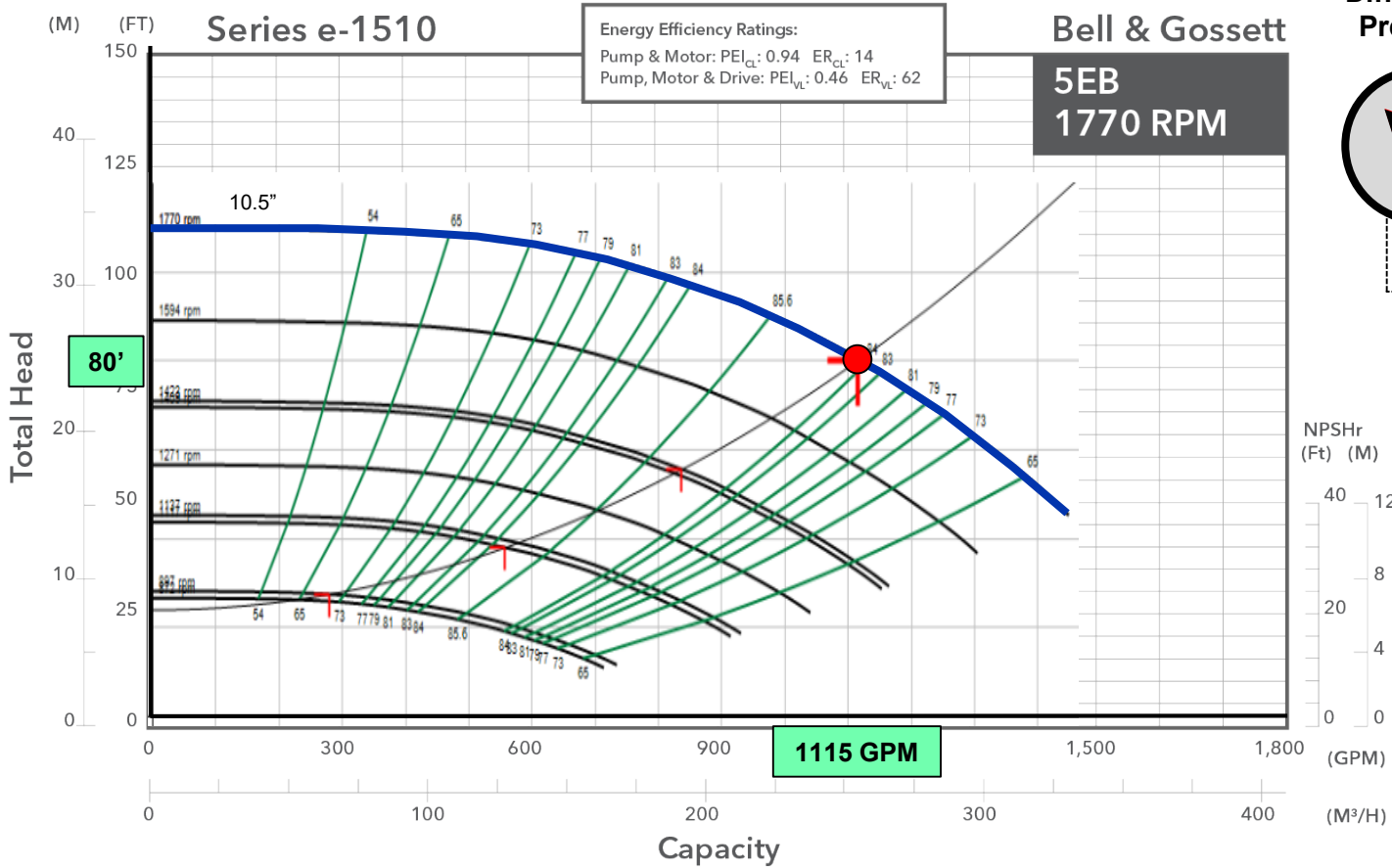
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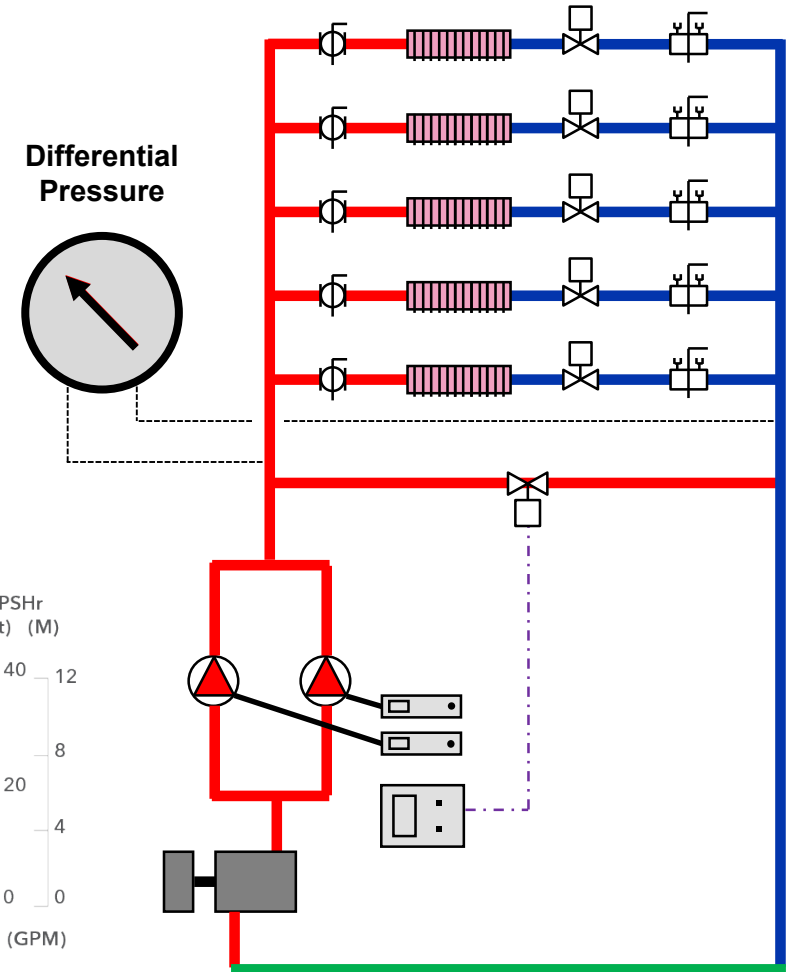
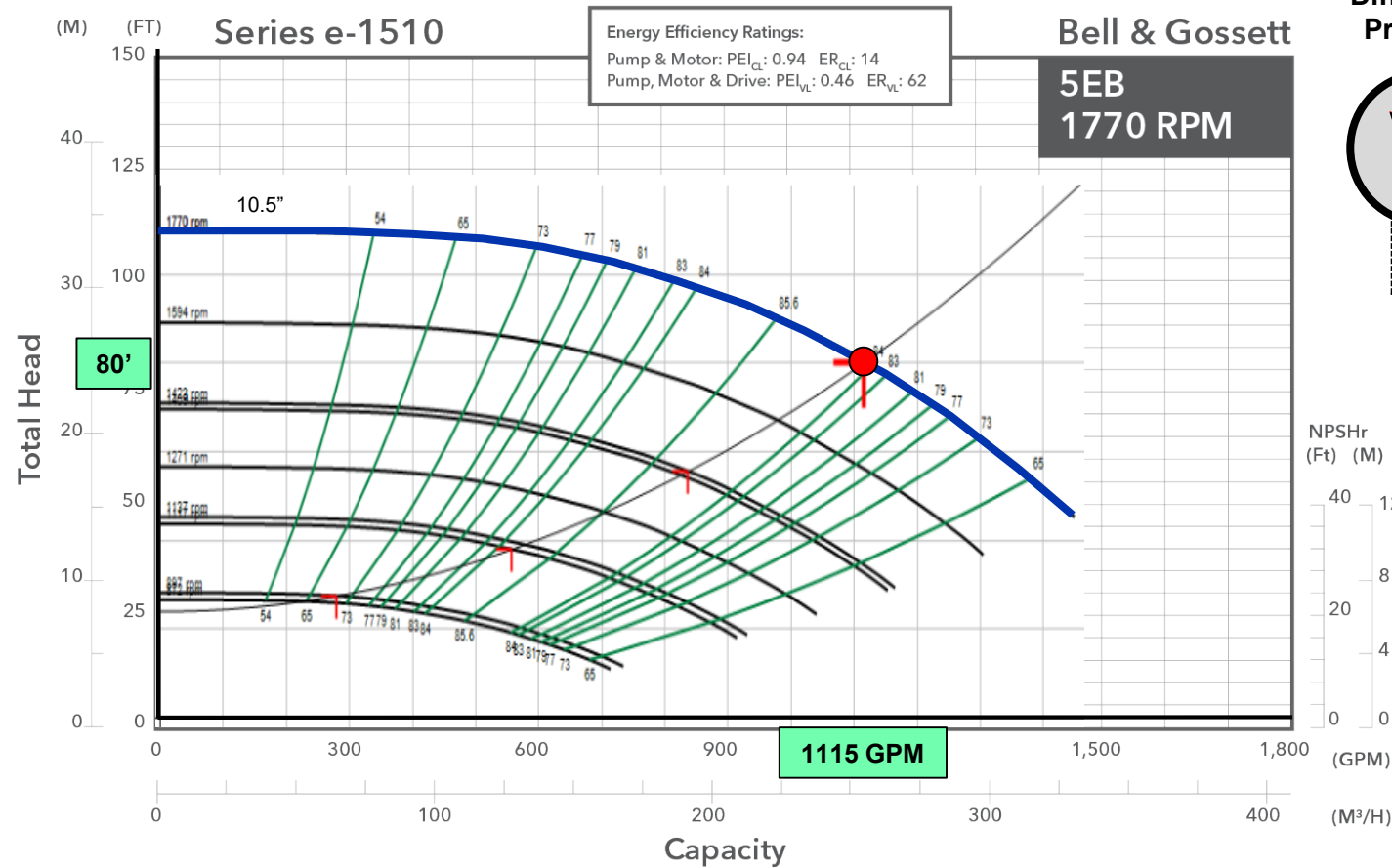


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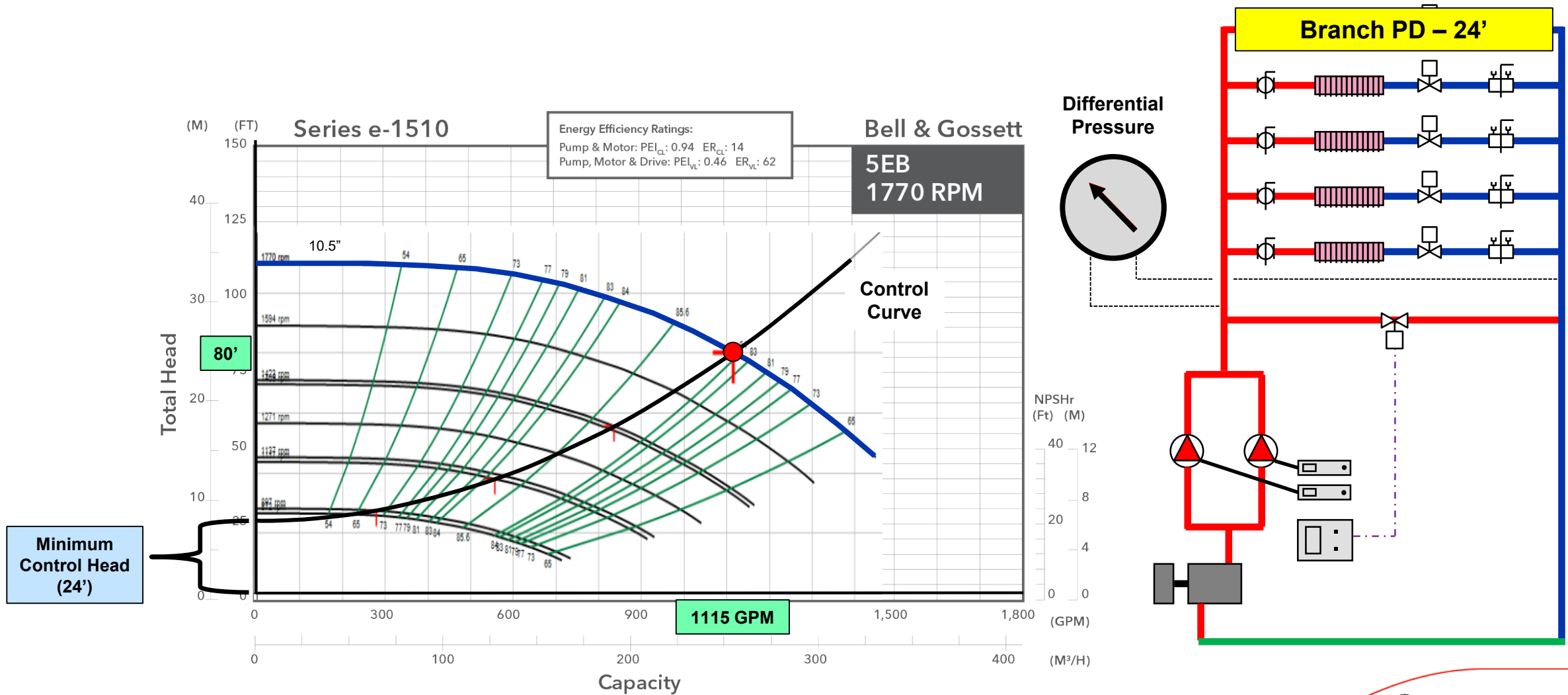




70% Variable Head Loss, 30% Constant Head Loss



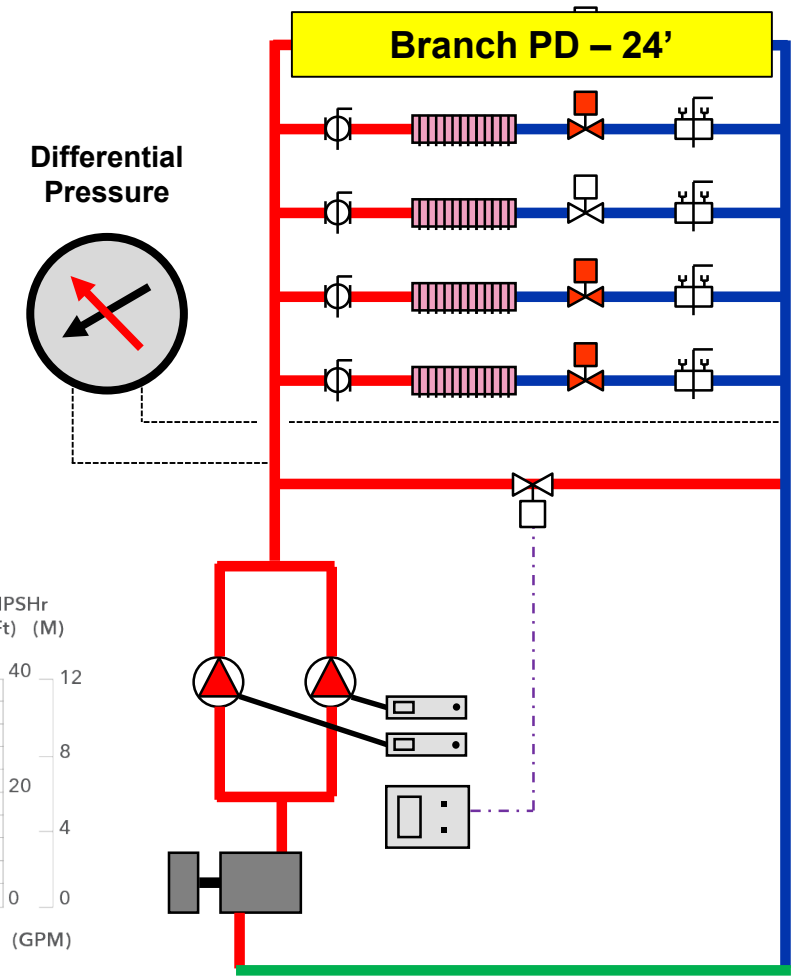
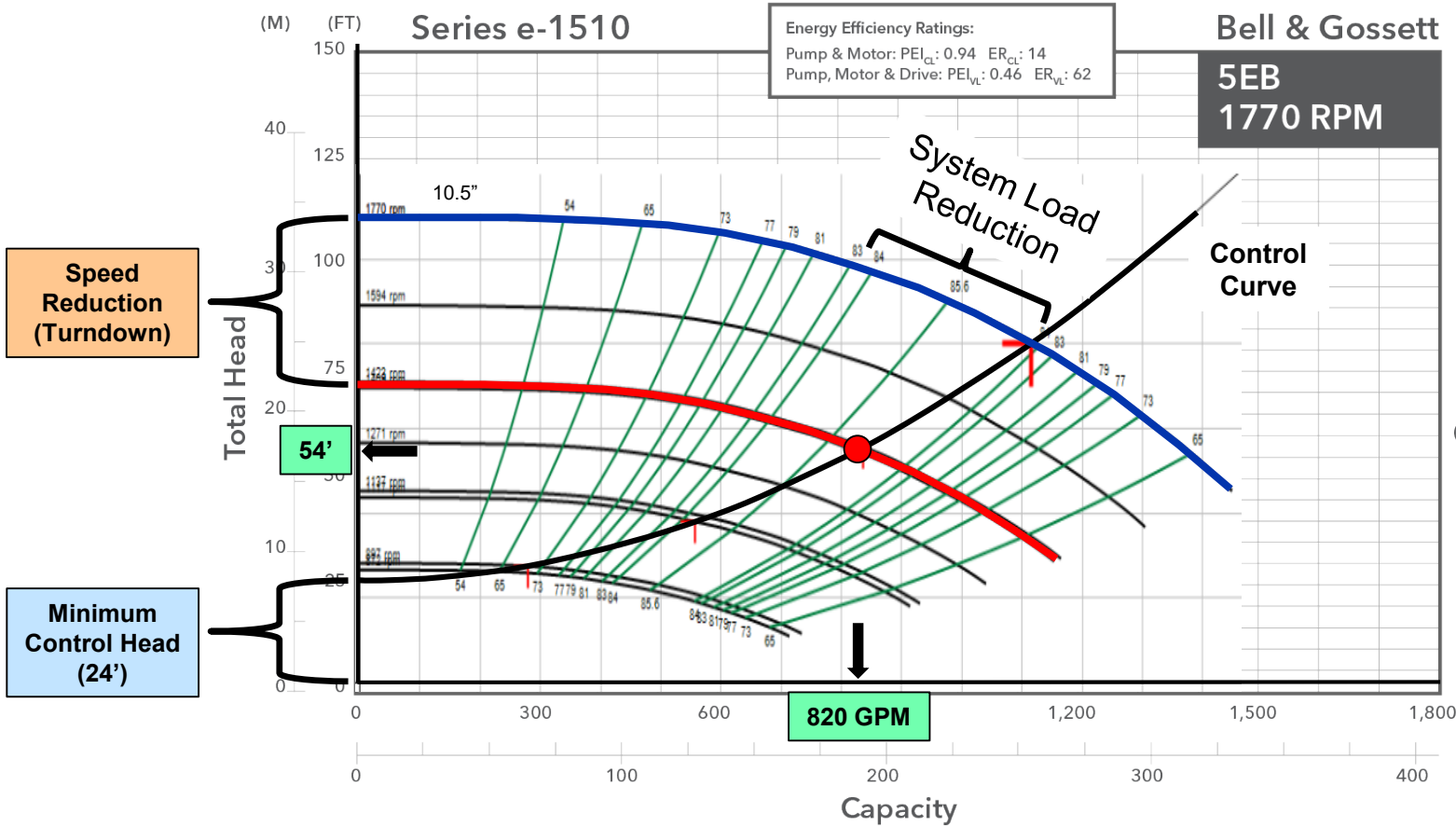
70% Variable Head Loss, 30% Constant Head Loss



70% Variable Head Loss, 30% Constant Head Loss

(1) e-1510 5EB with 10.5" Impeller
820 GPM @ 54' [1404 RPM]

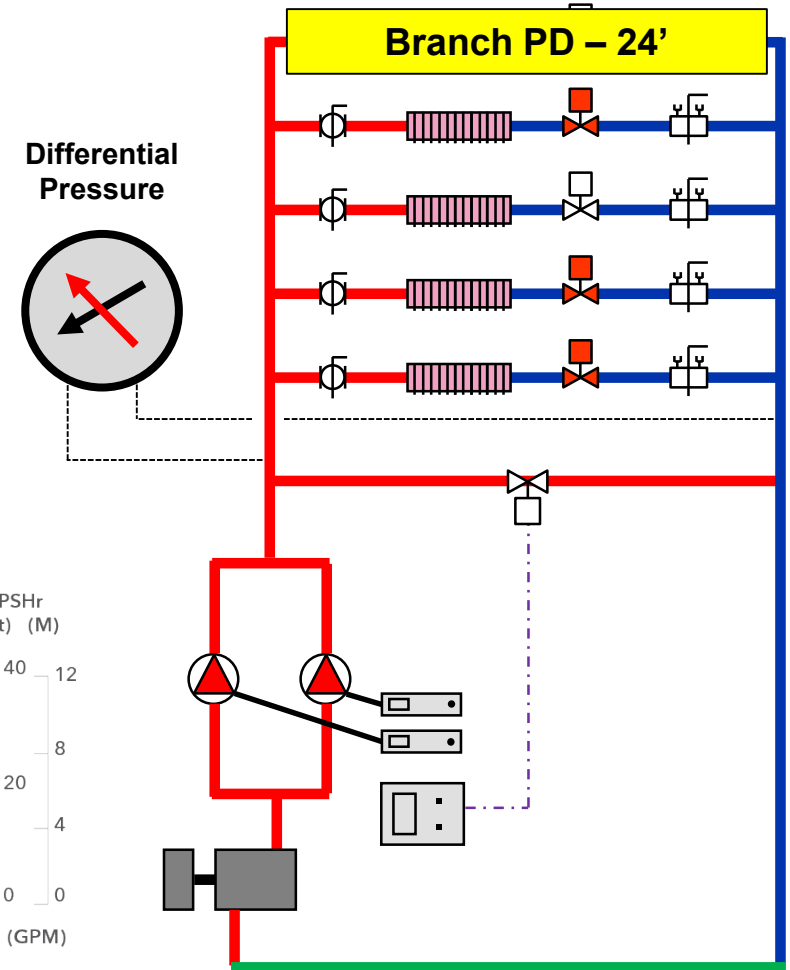
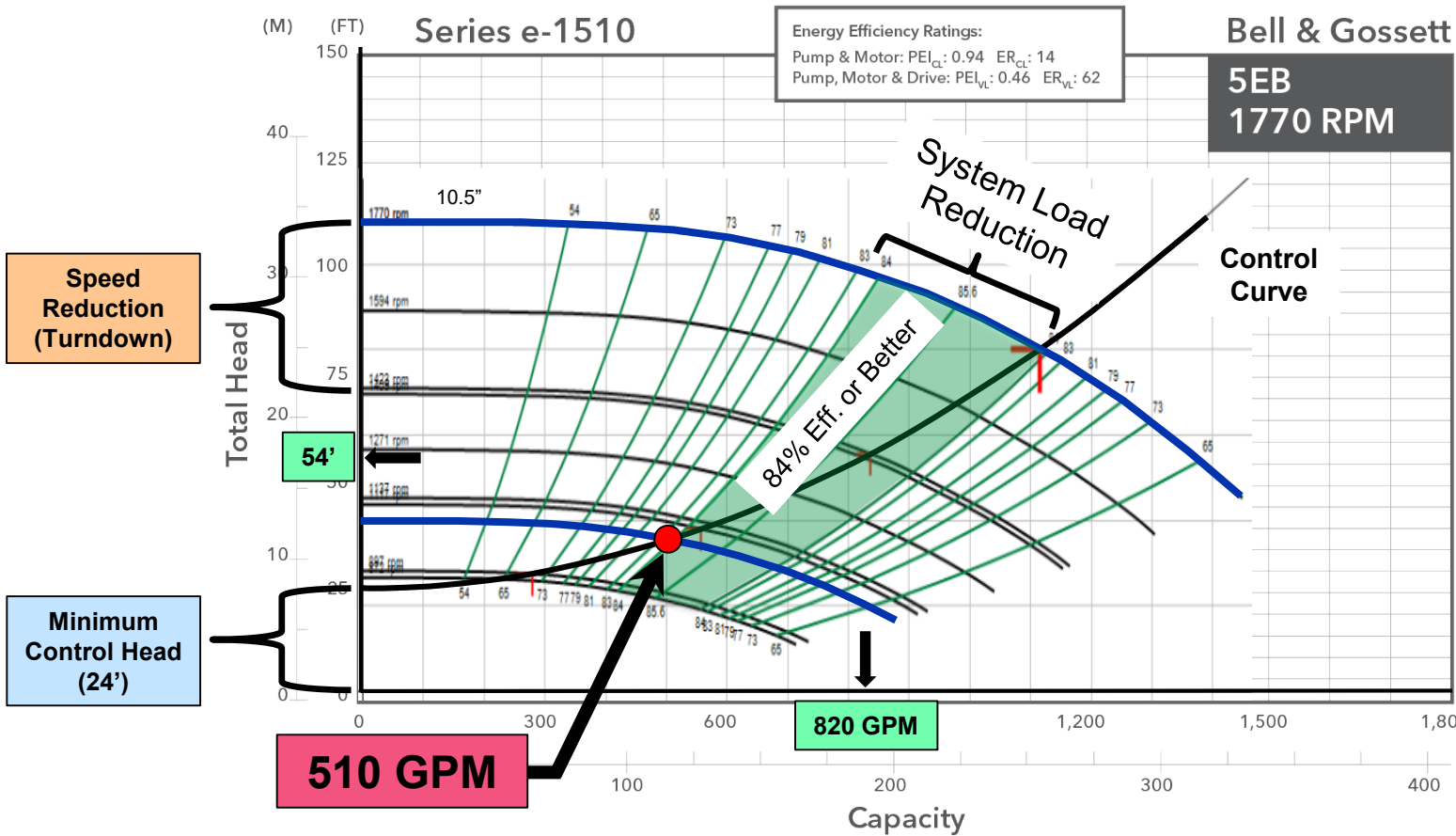
- 13.1 BHP (30HP Mtr. NOL)

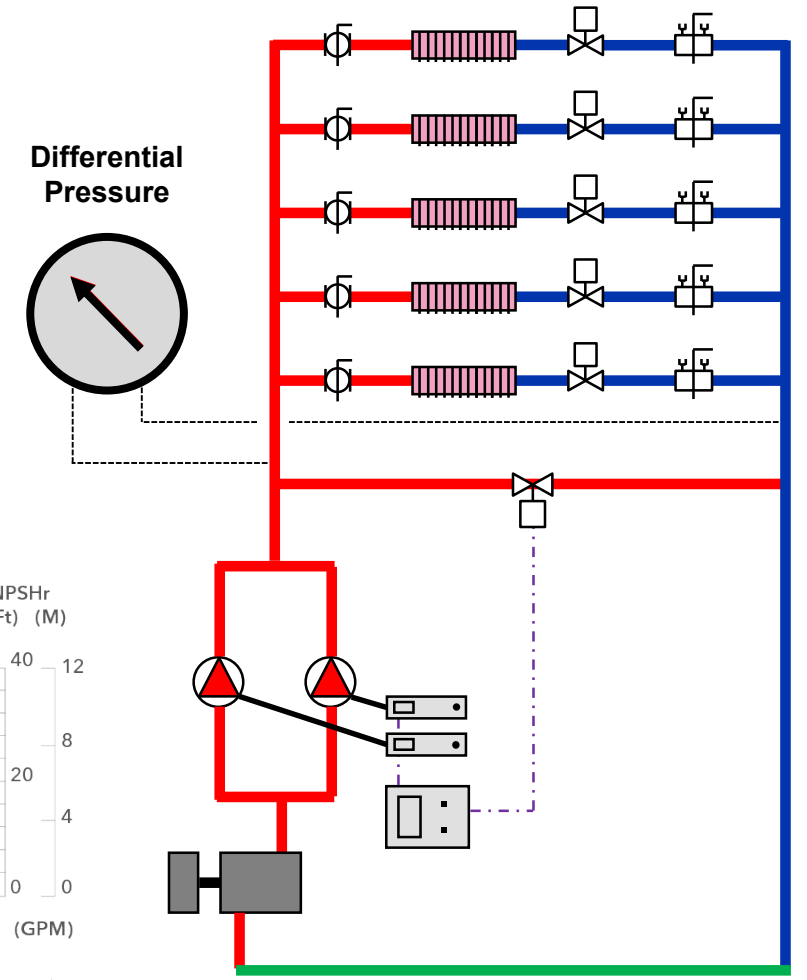
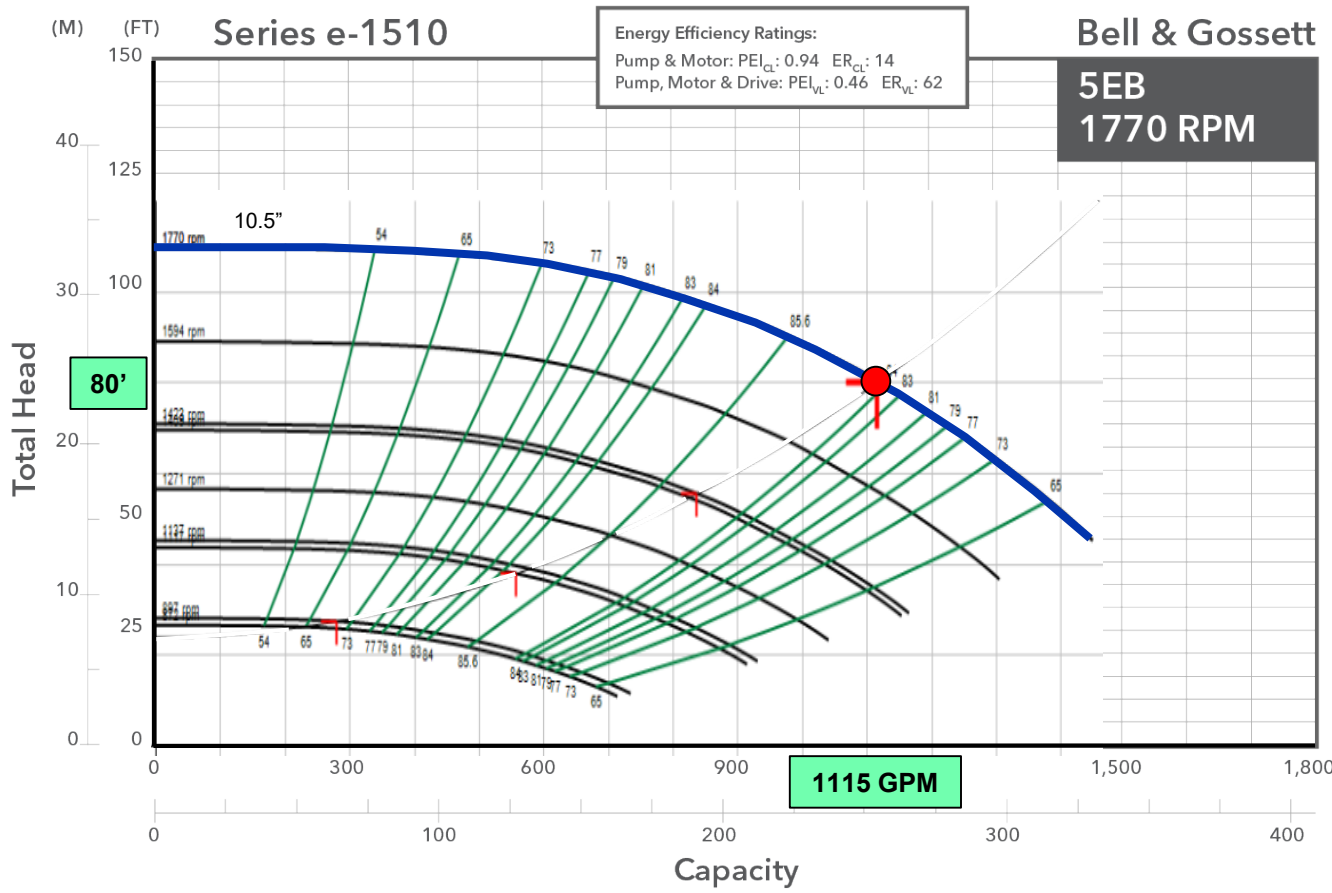


70% Variable Head Loss, 30% Constant Head Loss

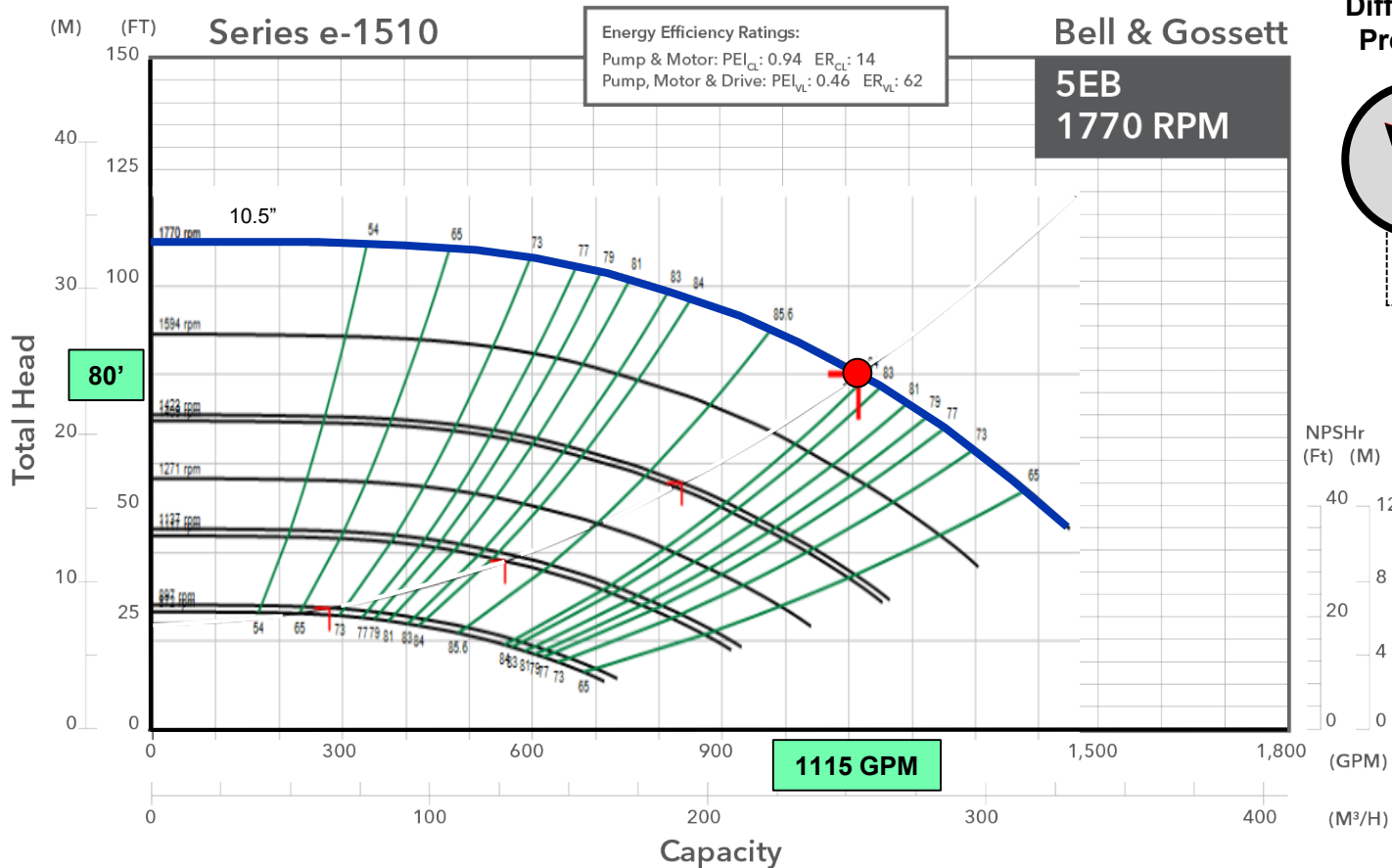
(1) e-1510 5EB with 10.5" Impeller
820 GPM @ 54' [1404 RPM]

- 13.1 BHP (30HP Mtr. NOL)

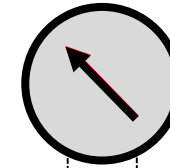




10% Variable Head Loss, 90% Constant Head Loss



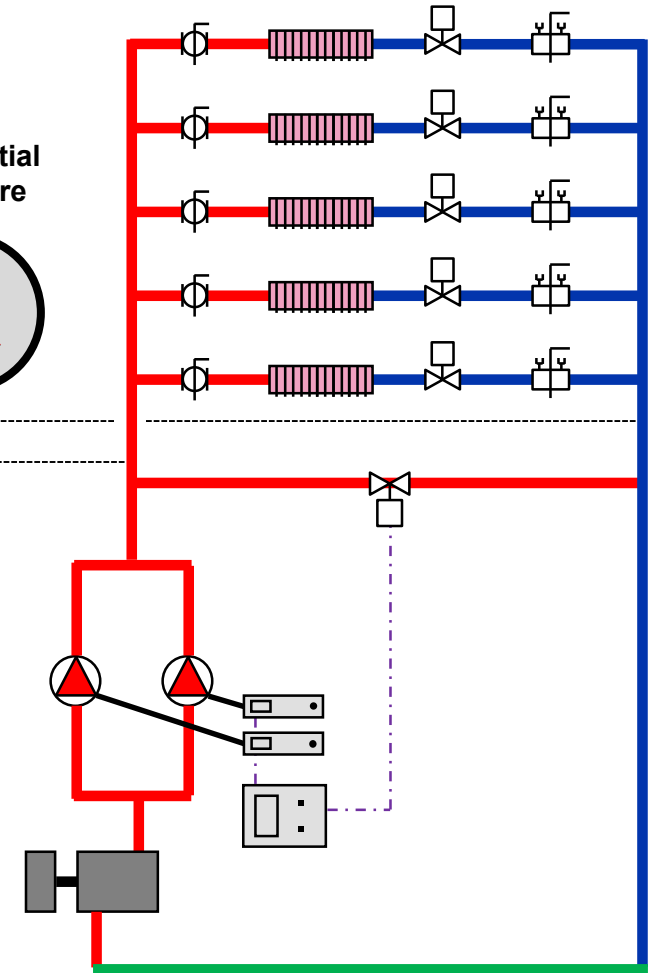
Differential Pressure



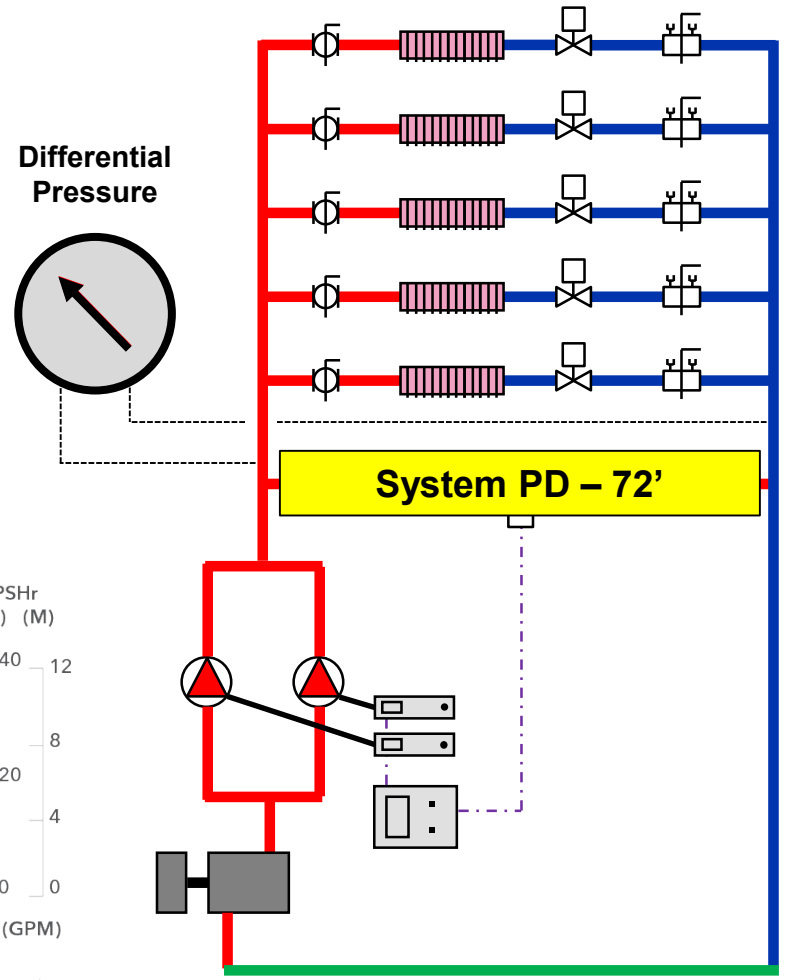
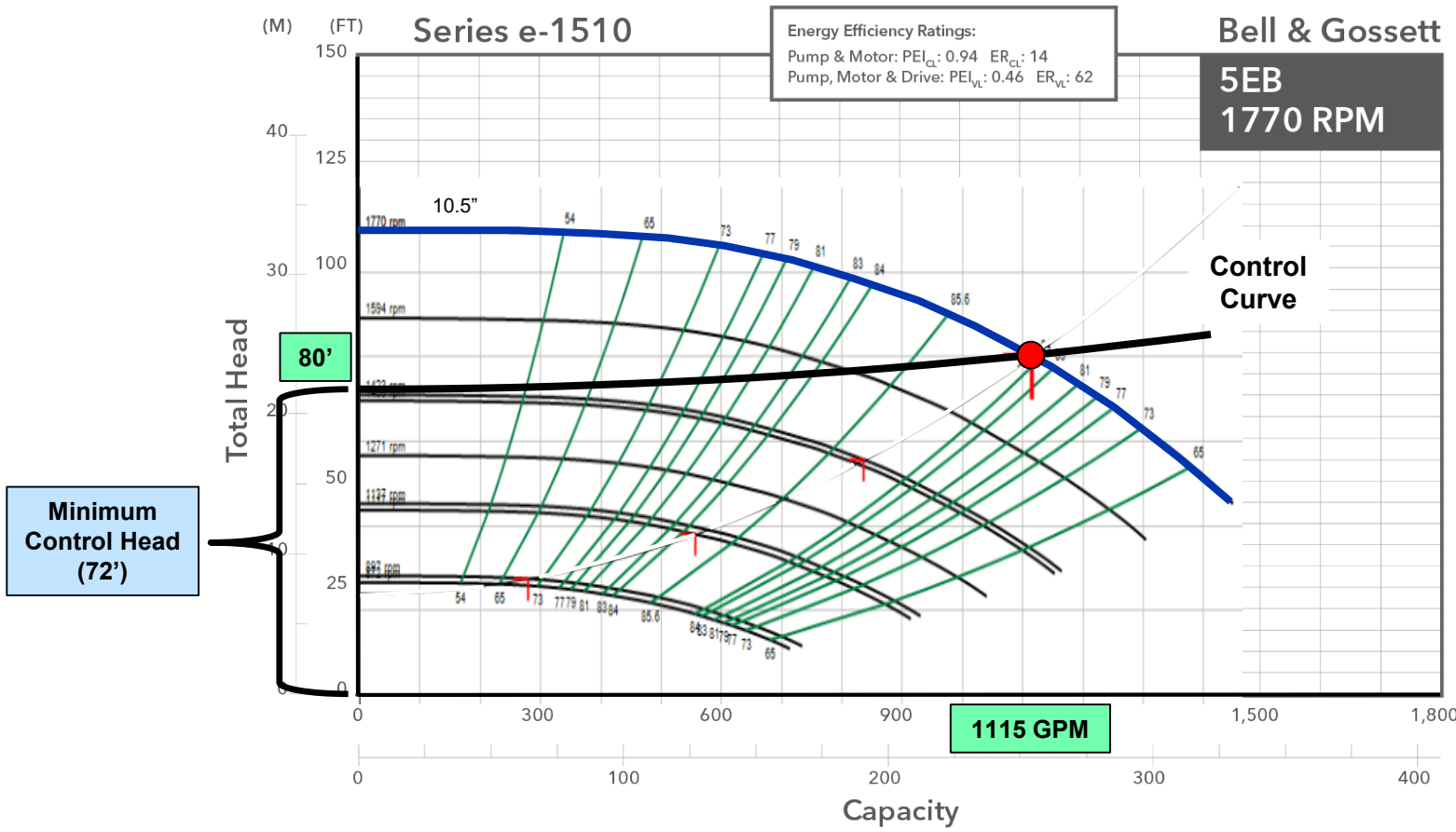
NPSHr (Ft) (M)

40 12
20 8
0 0
(GPM)

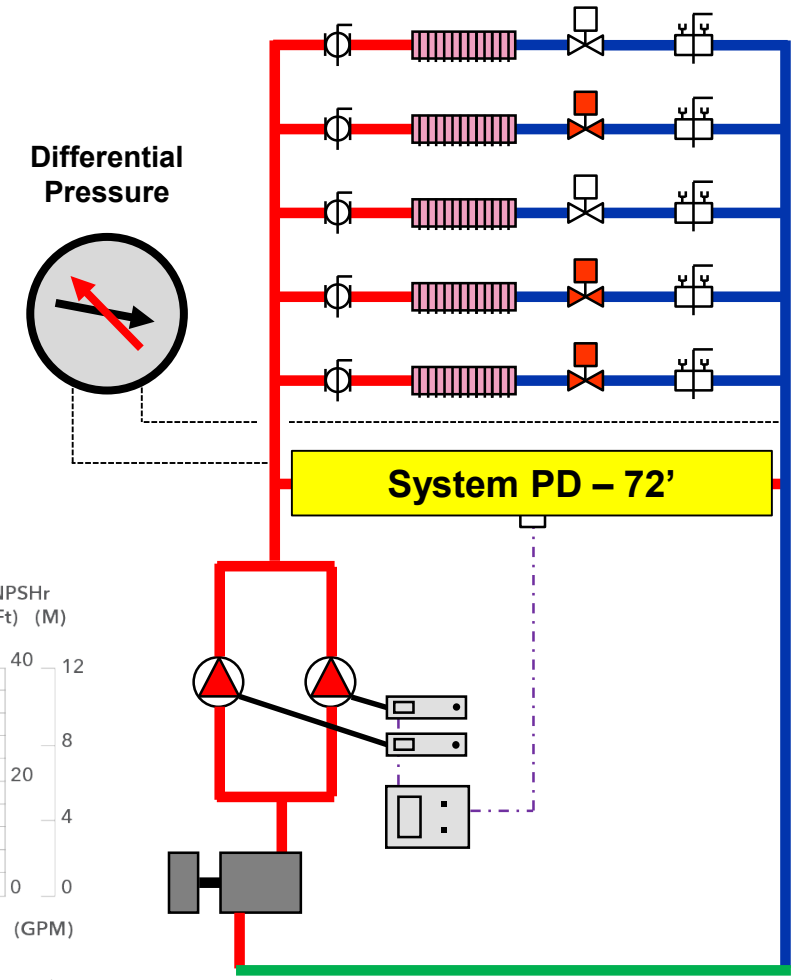
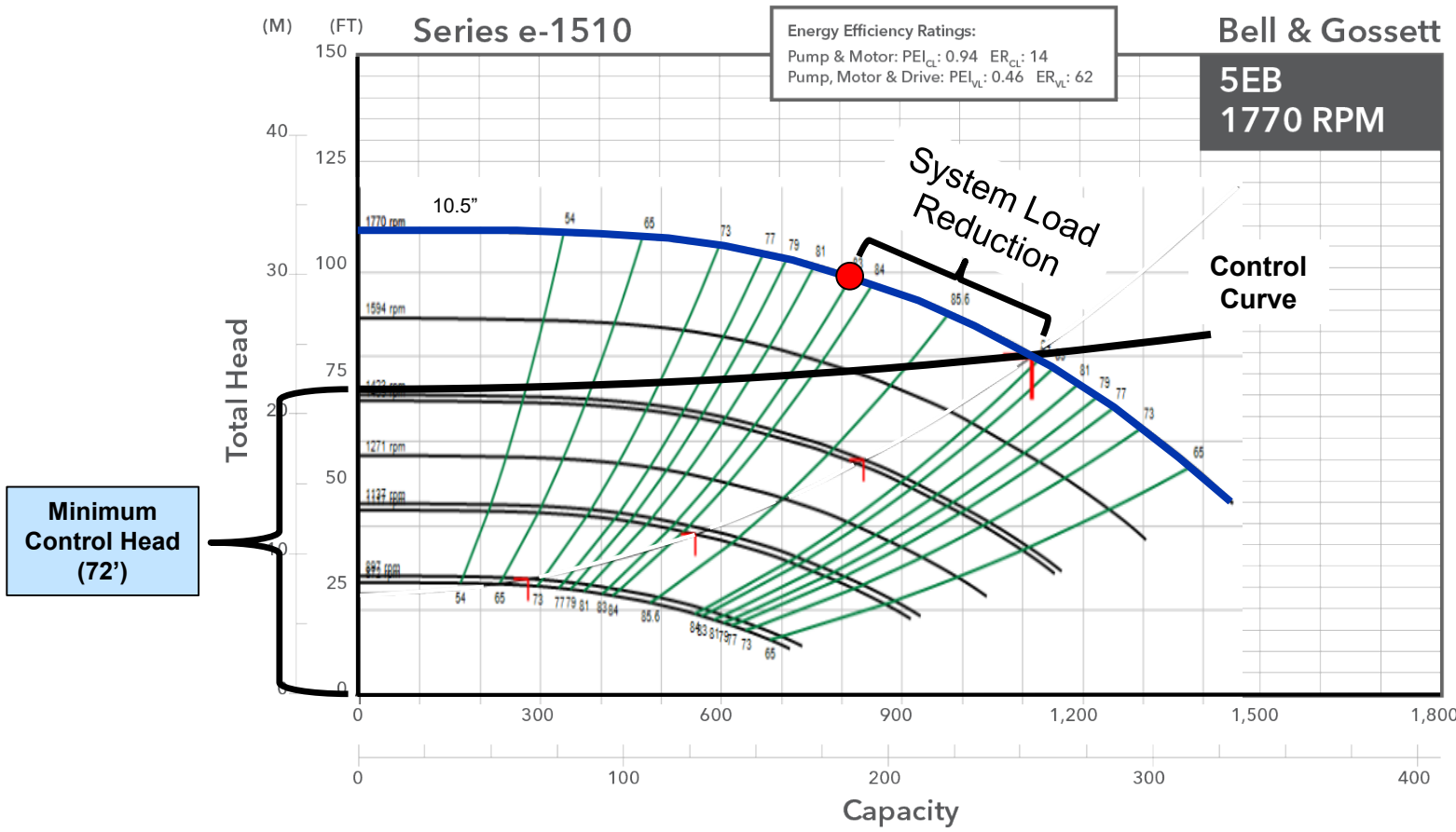
(M³/H)



10% Variable Head Loss, 90% Constant Head Loss



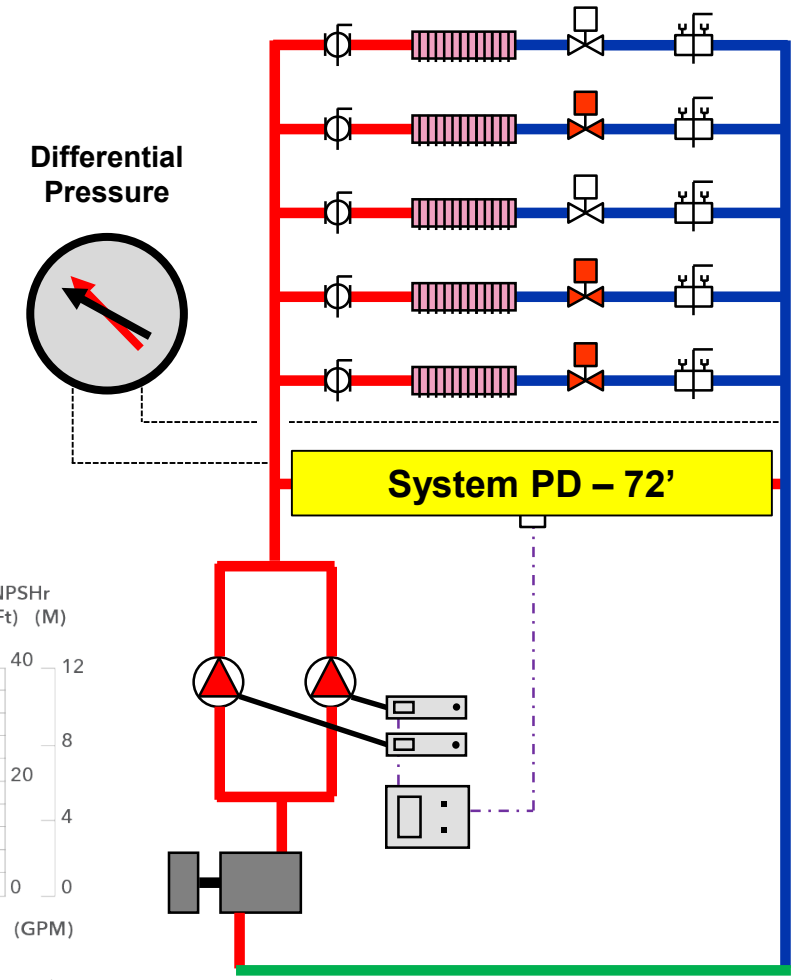
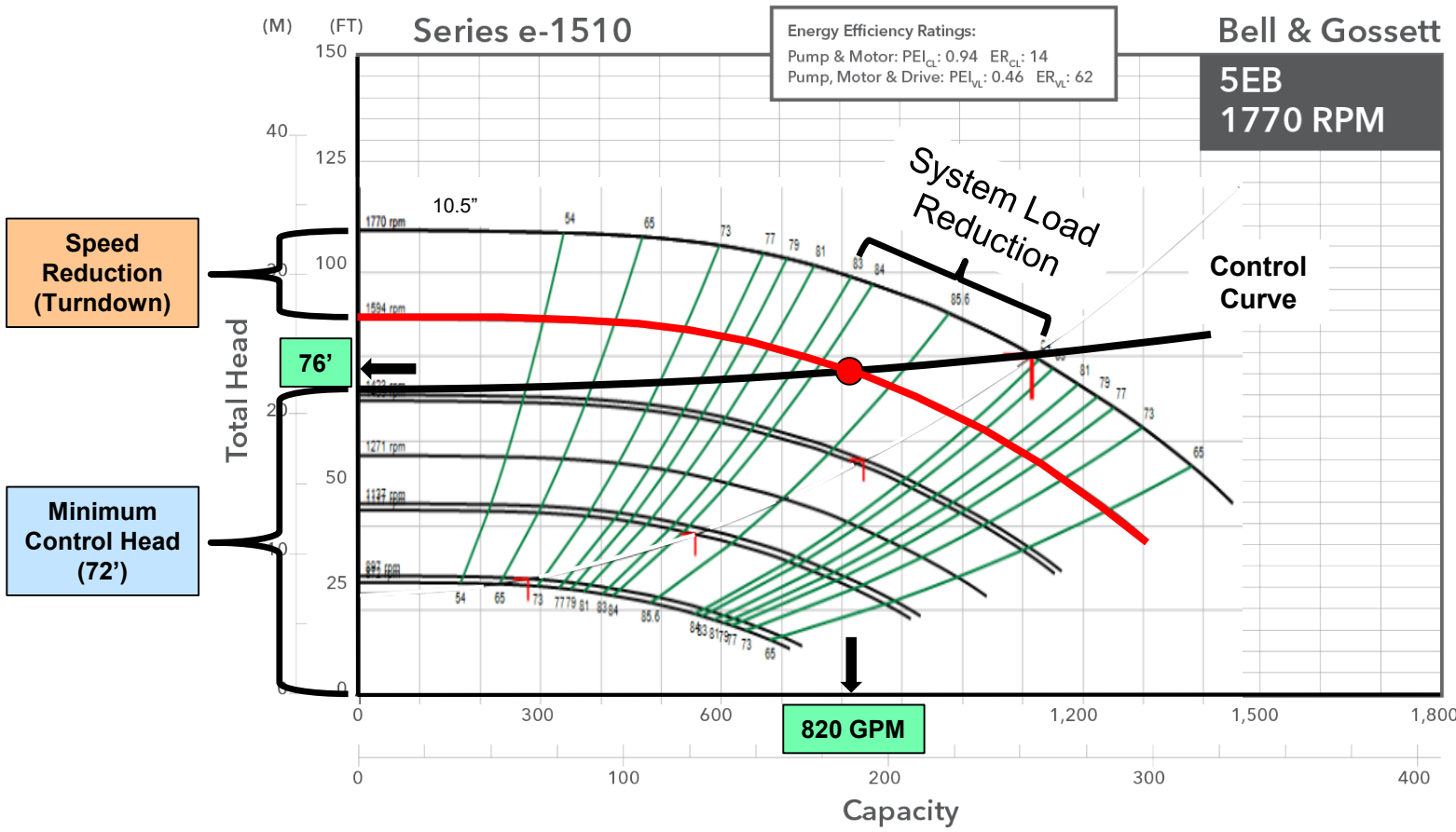
10% Variable Head Loss, 90% Constant Head Loss



10% Variable Head Loss, 90% Constant Head Loss

(1) e-1510 5EB with 10.5" Impeller
820 GPM @ 76' [1594 RPM]

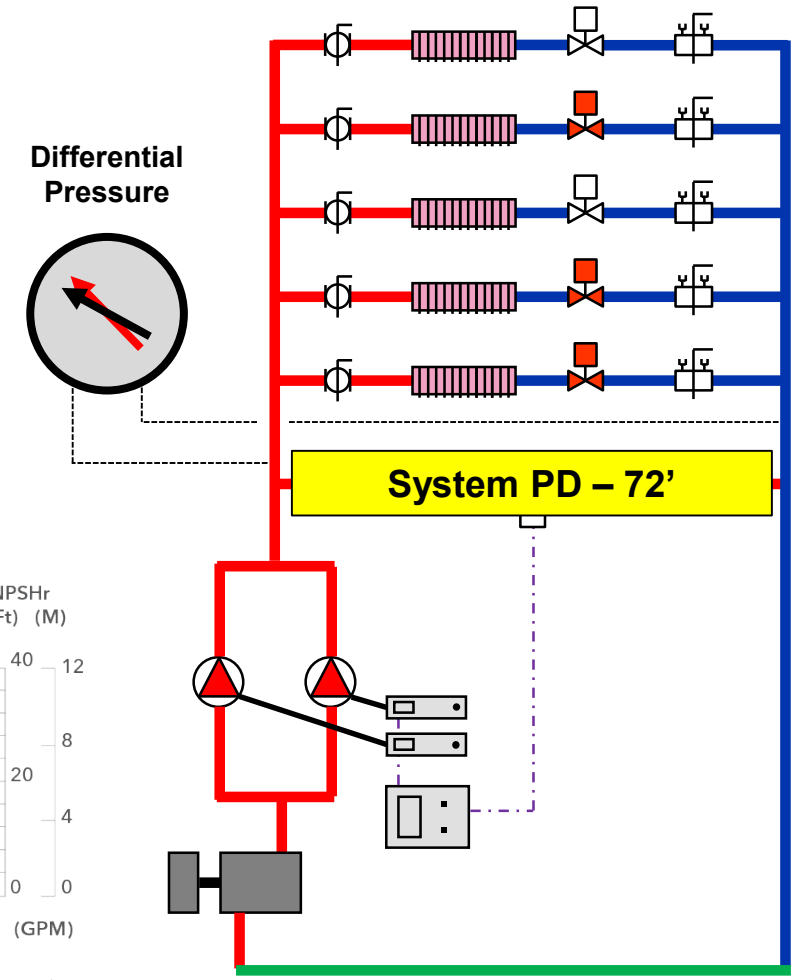
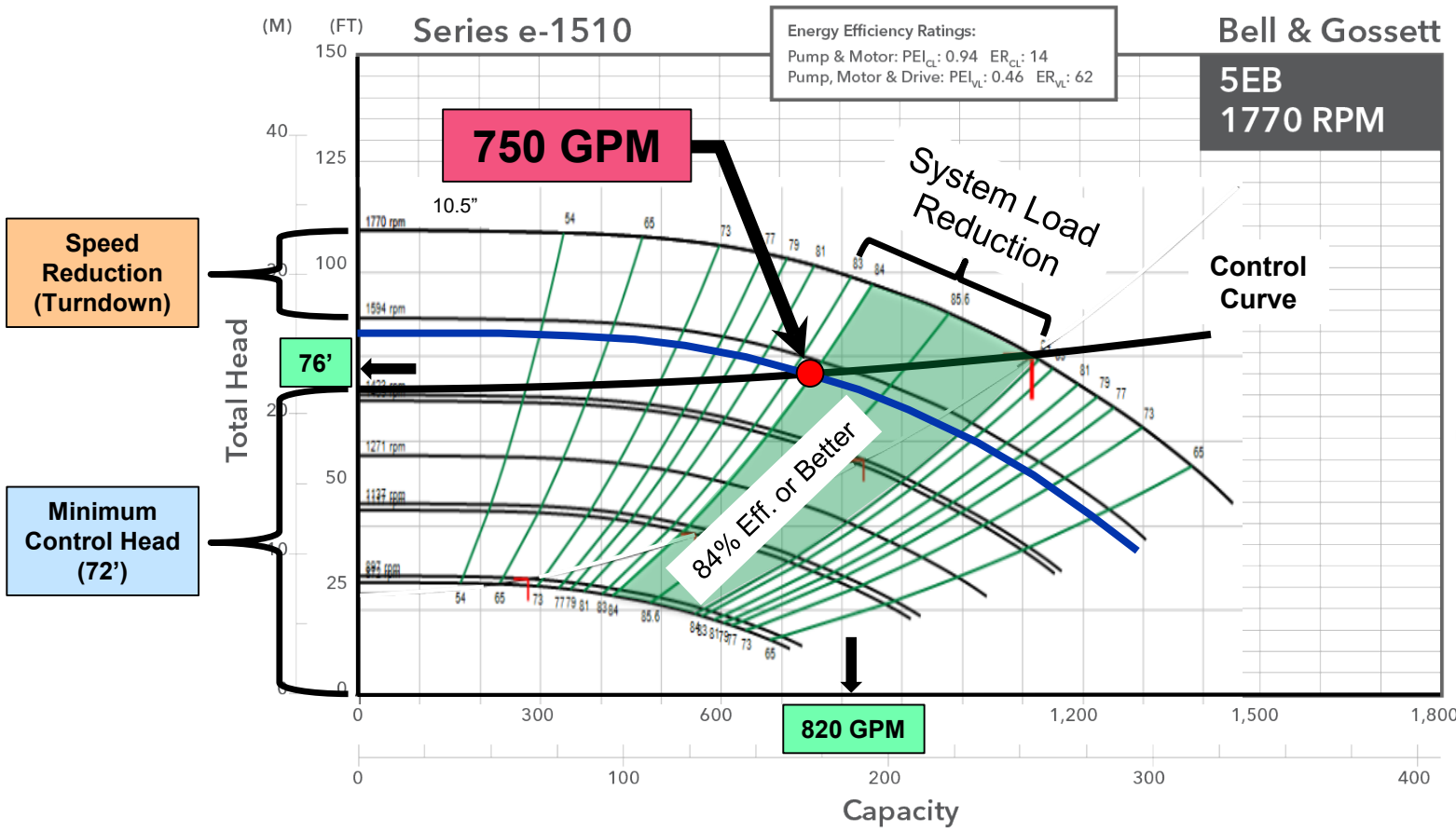
- 18.5 BHP (30HP Mtr. NOL)

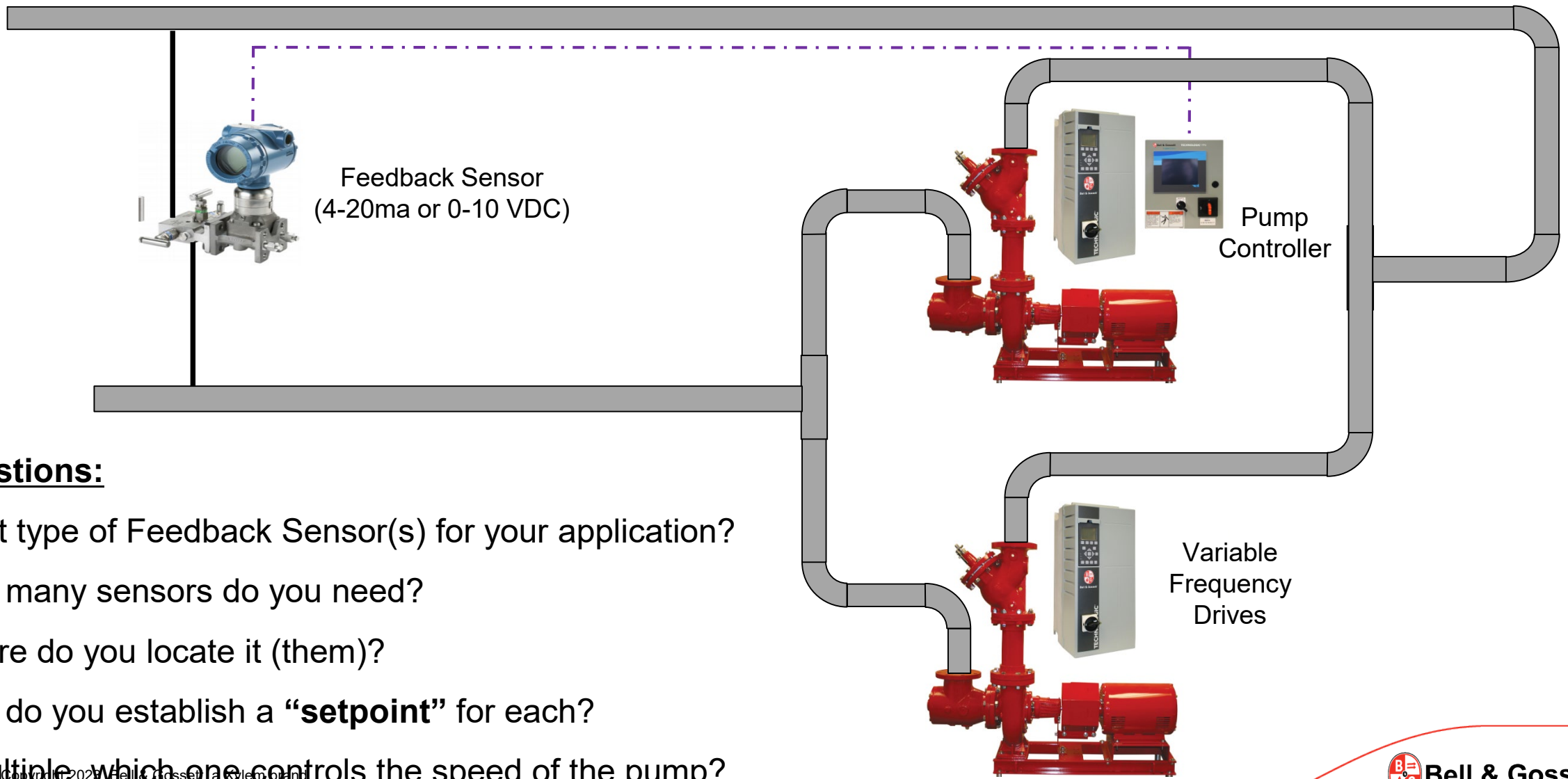


10% Variable Head Loss, 90% Constant Head Loss

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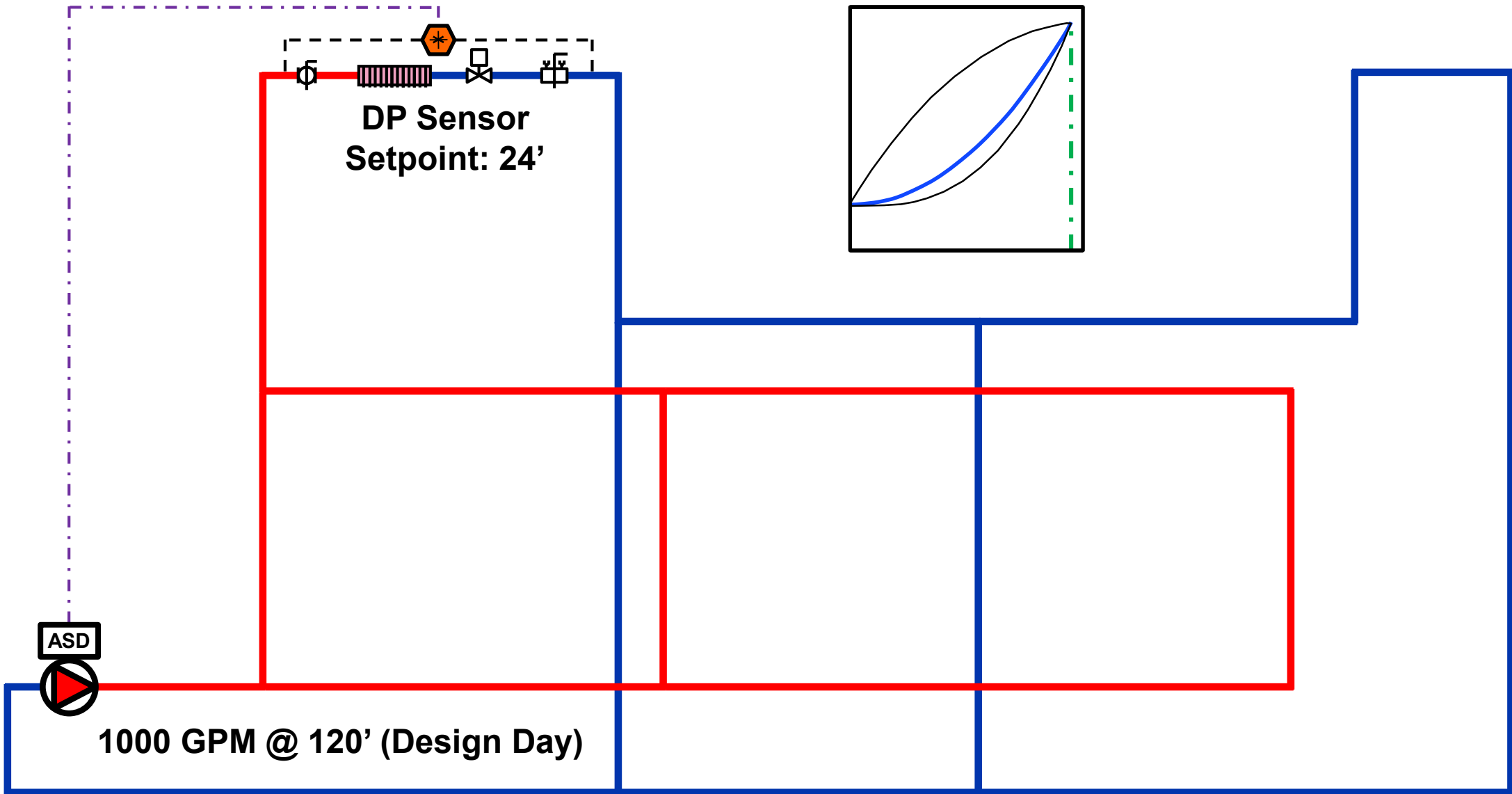
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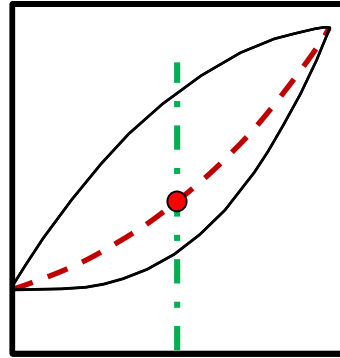
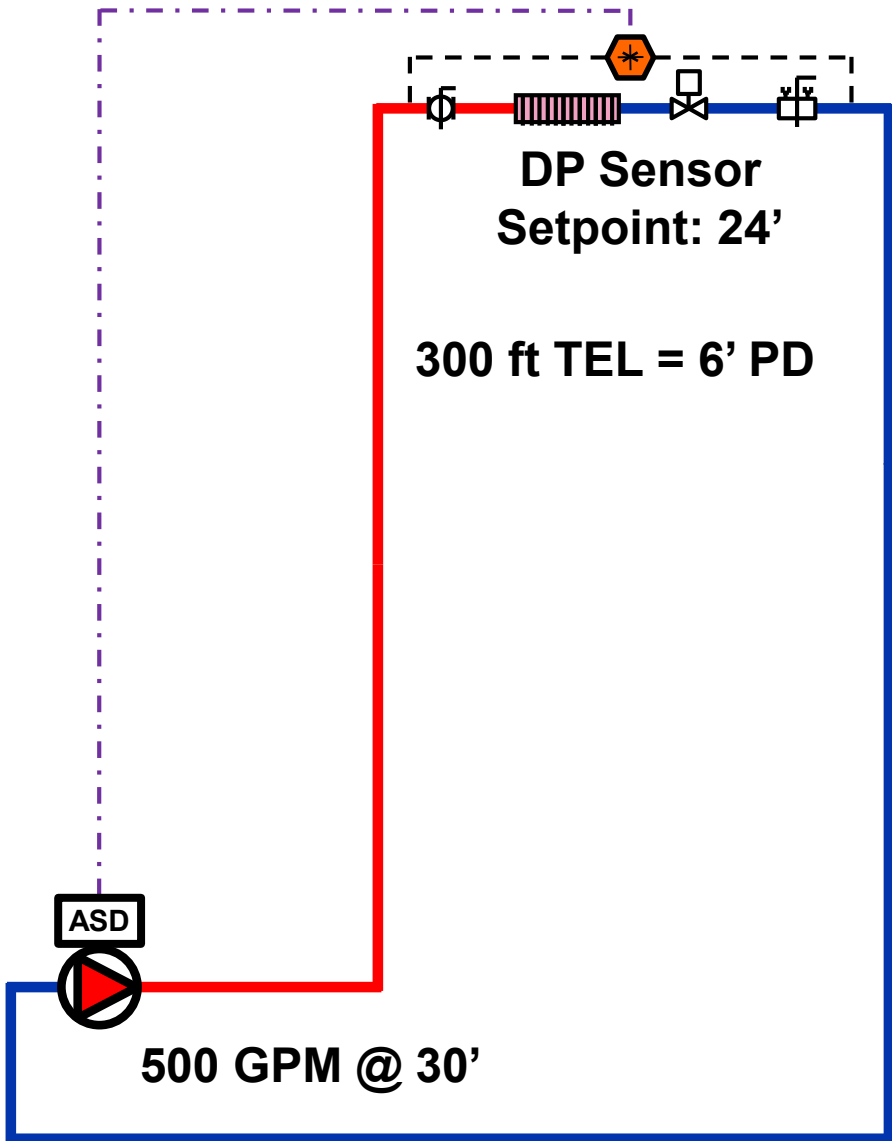




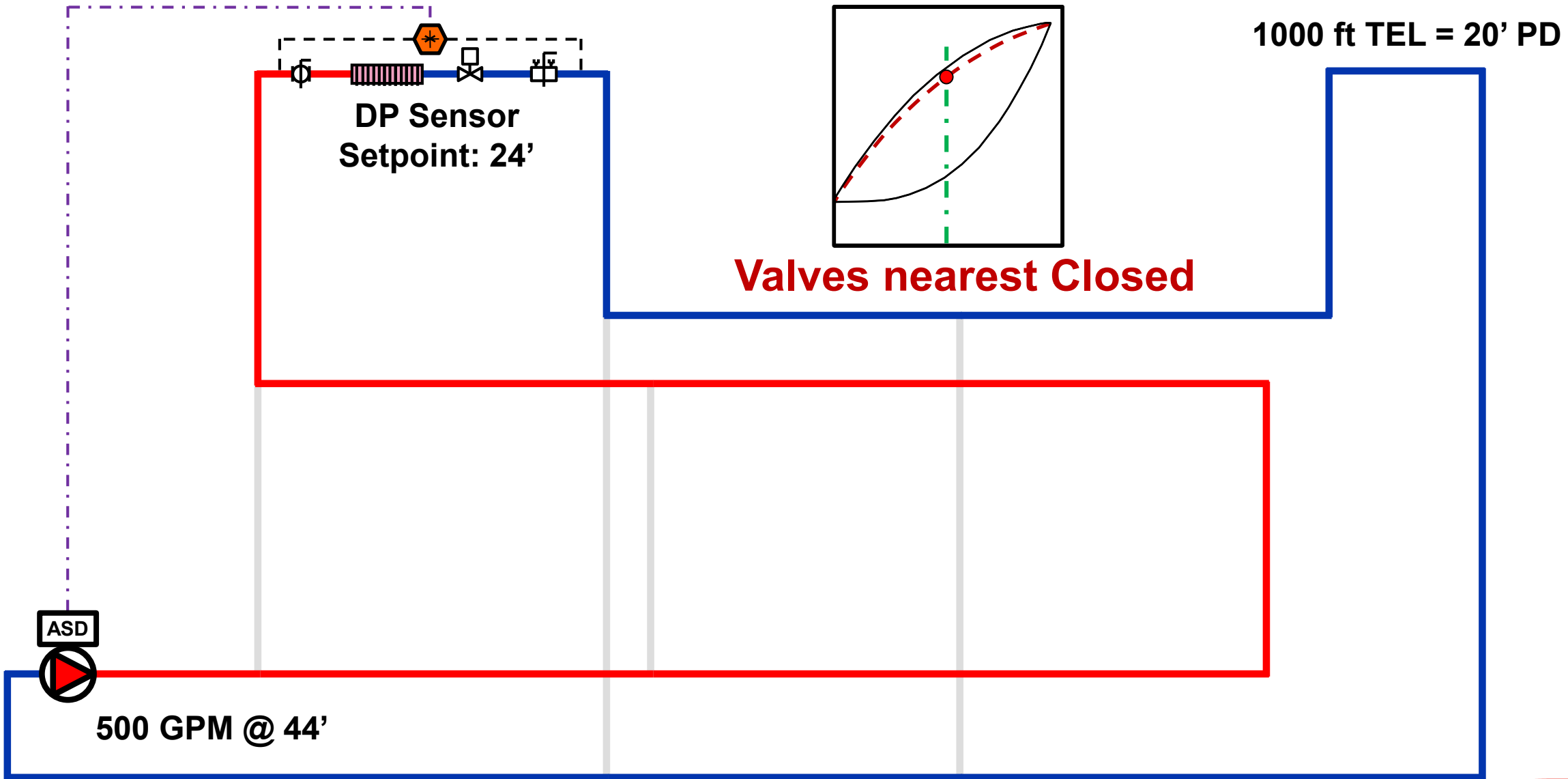
• **Questions:**

- What type of Feedback Sensor(s) for your application?
- How many sensors do you need?
- Where do you locate it (them)?
- How do you establish a “**setpoint**” for each?
- If multiple, which one controls the speed of the pump?





Valves farthest Closed



- **Common Feedback Sensor Options:**

- **Pressure** – Change in pressure at single point (*Potable Water Pressure Boosting*)
- **Differential Pressure** – Change in pressure between two points (*HVAC Heating and Cooling*)
- **Temperature** – Change in temperature at single point (*Batch Process Tank*)
- **Differential Temperature** – Change in temperature between two points (*Air or Water side of HVAC Coils*)
- **Flow Meter** – Change in flowrate in pipe or equipment (*Pump Staging, Backup to other Feedback Sensors*)
- **Discharge Air Temperature** – Air Temperature on discharge side of a water coil (*VFD Zone Pumping*)

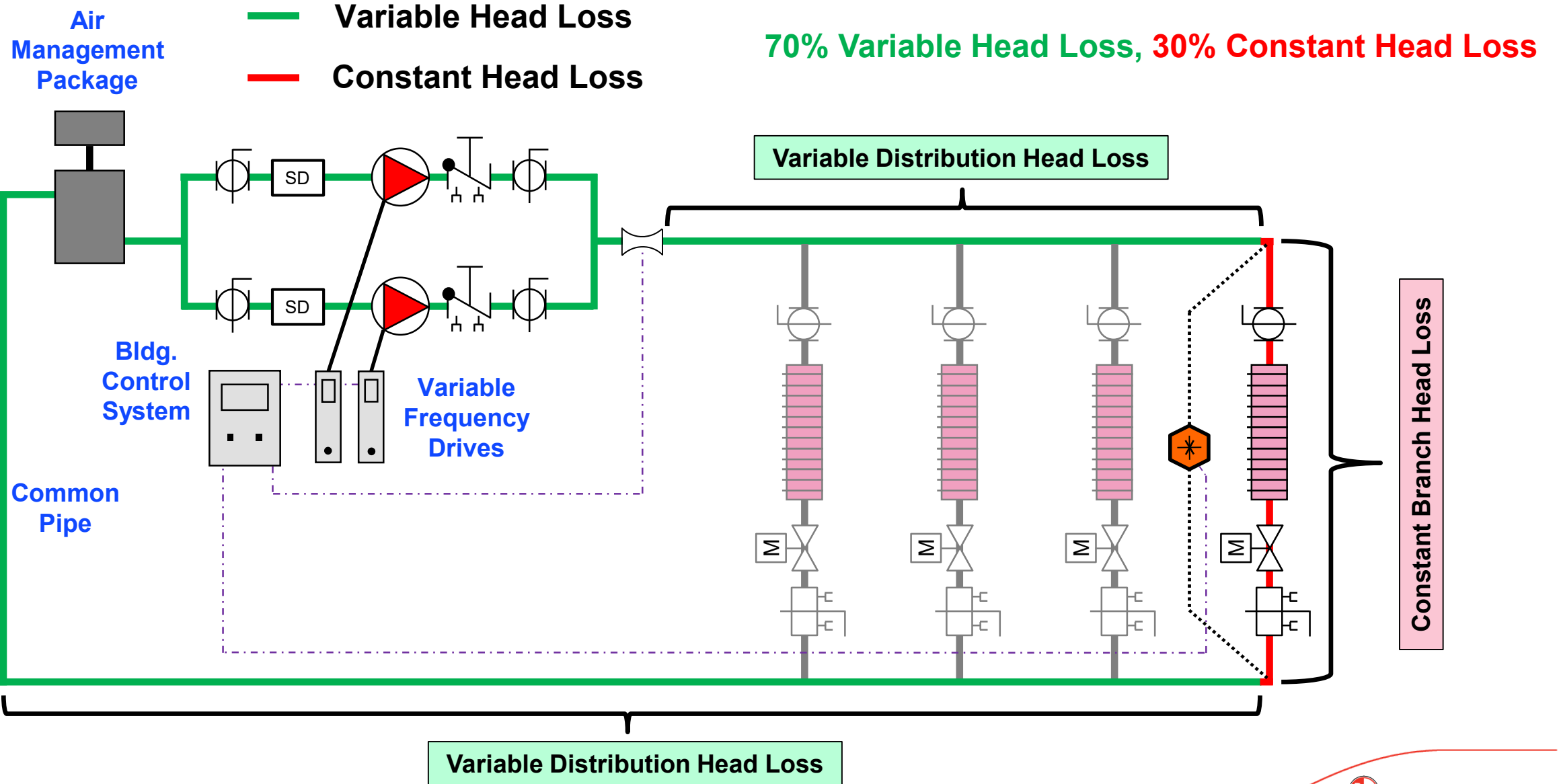
- **Differential Pressure** – Change in pressure between two points (*HVAC Heating and Cooling*)

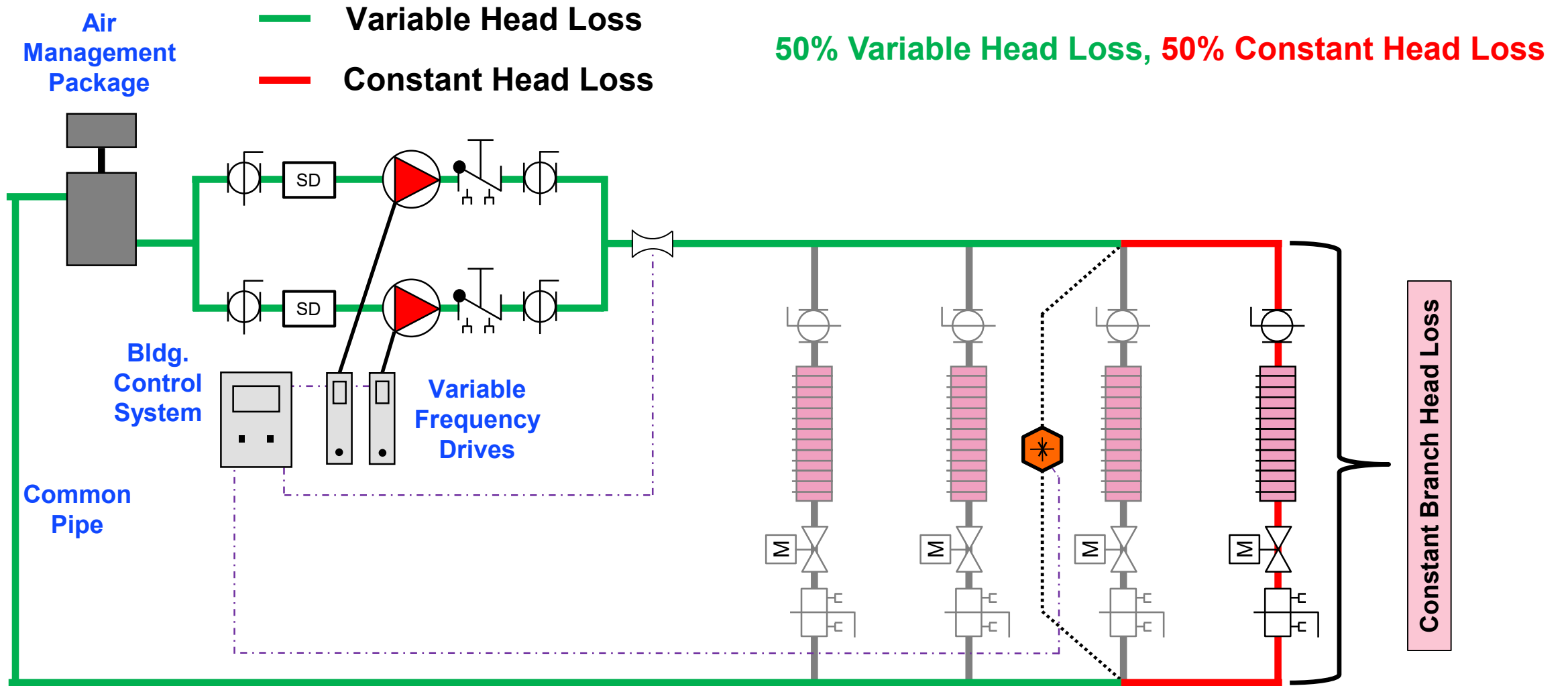
- **Differential Pressure Feedback Sensor Locations:**

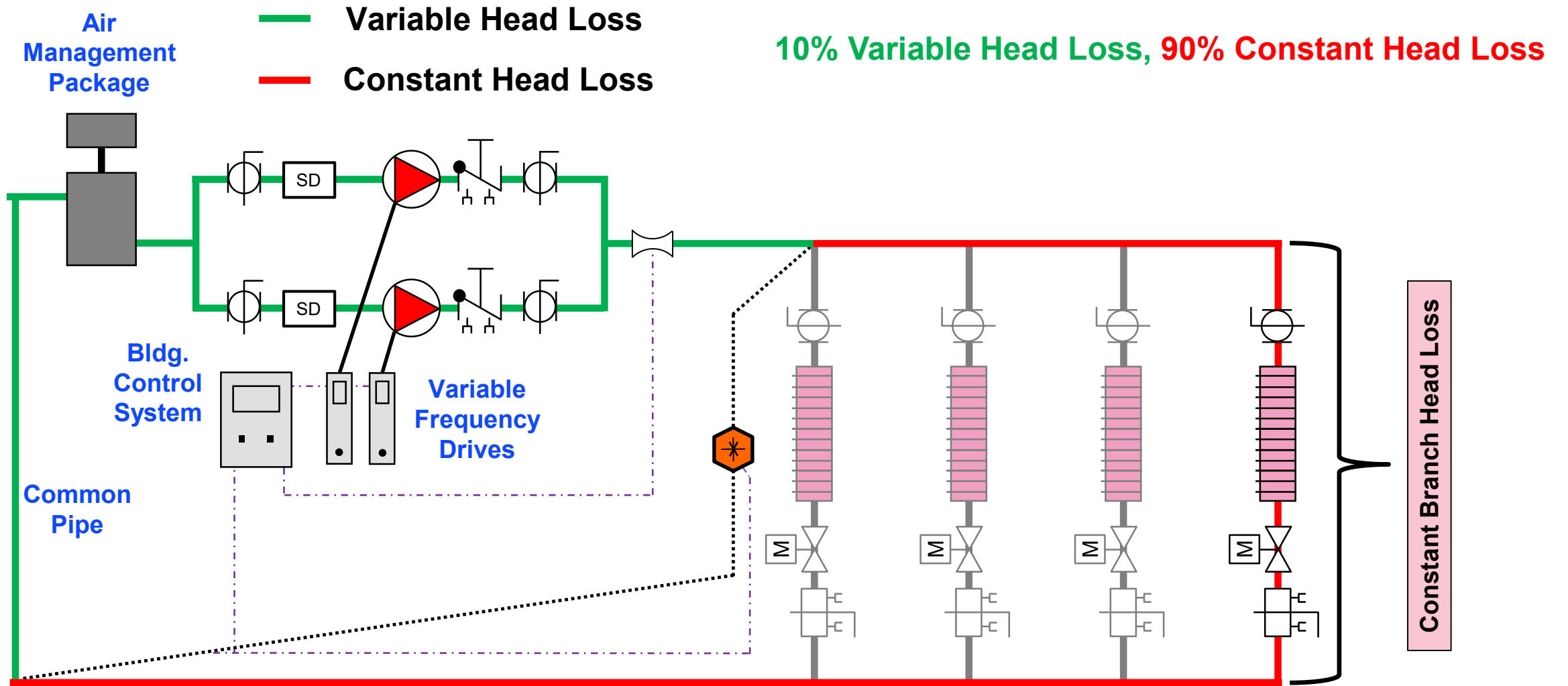
- Mechanical Room
- 2/3 the system piping distance from the Mechanical Room
- Most remote hydraulic head loss circuit pump will serve (*The “Critical Circuit”*)

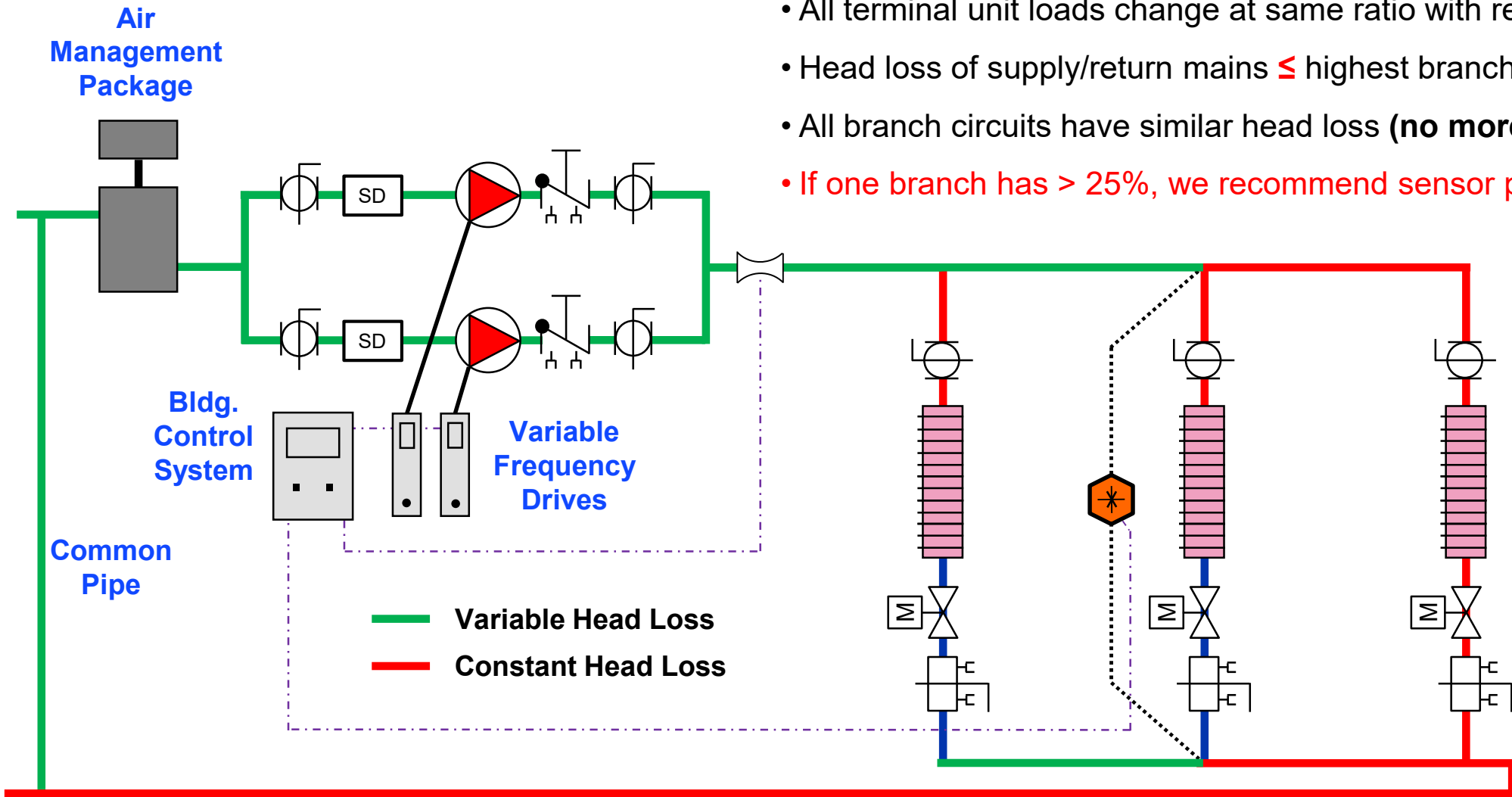
- **It doesn't matter (???)**

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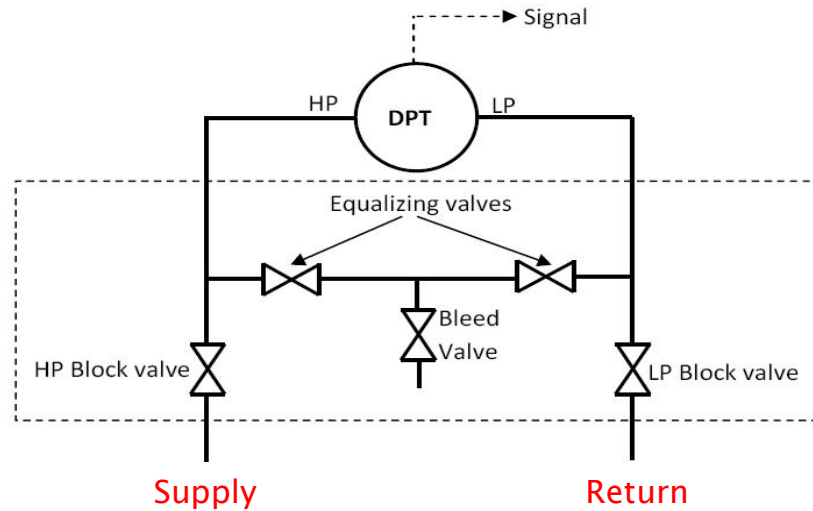






Suggested Sensor Location Assumptions:

- All terminal unit loads change at same ratio with respect to time
- Head loss of supply/return mains \leq highest branch circuit head loss
- All branch circuits have similar head loss (**no more than 25% difference**)
- If one branch has $> 25\%$, we recommend sensor placement at that location.






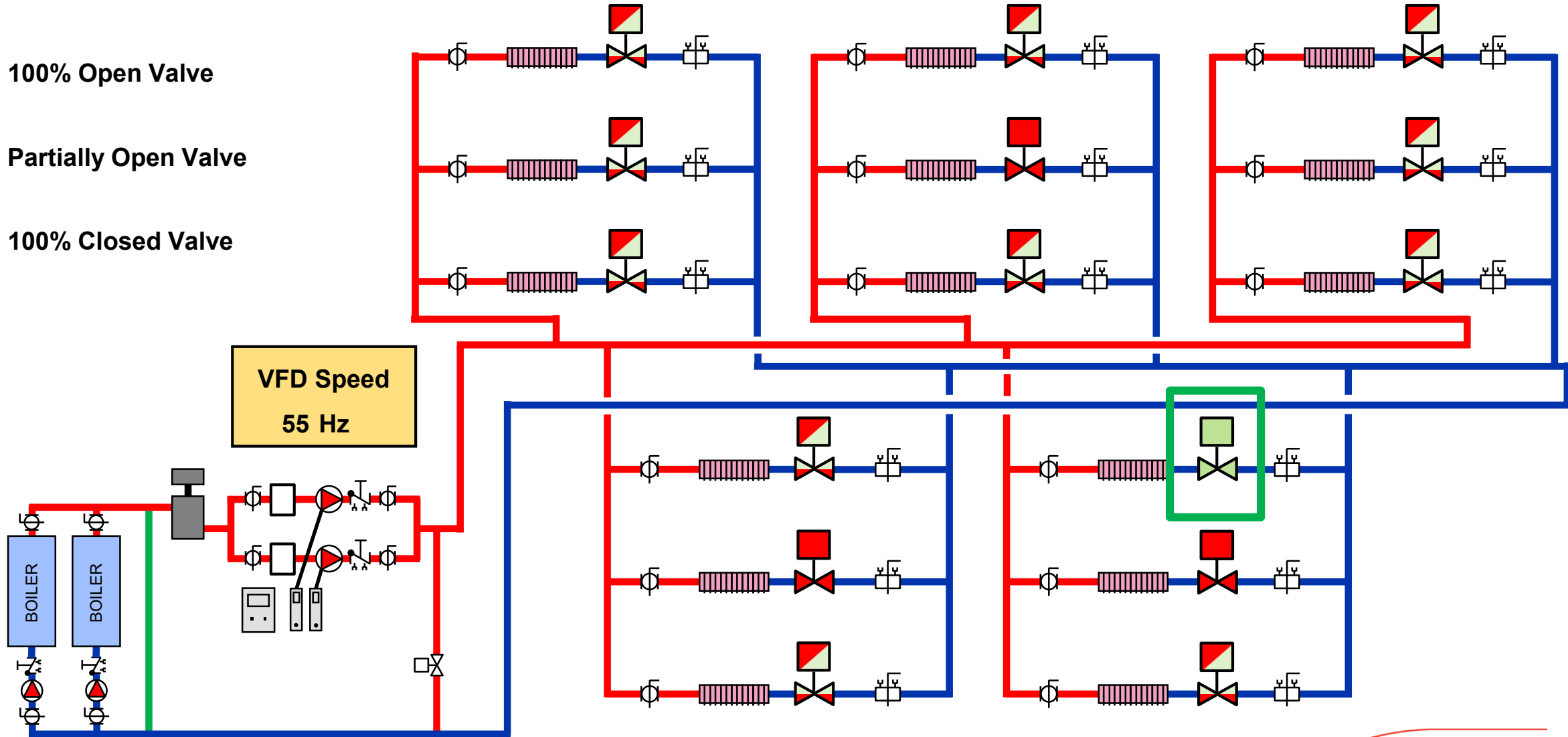
- Measure Pressures at Supply and Return to obtain differential
- Must be done under “Design Day” simulation **after final hydronic system balance has been completed**
- Data must be recorded independently for **each** sensor’s location
- Establish sensor signal range values in pump controller (***i.e. 4ma = 18Hz., 20ma = 60Hz.***)




ASHRAE 90.1 Section 6.5 – Prescriptive Compliance Path

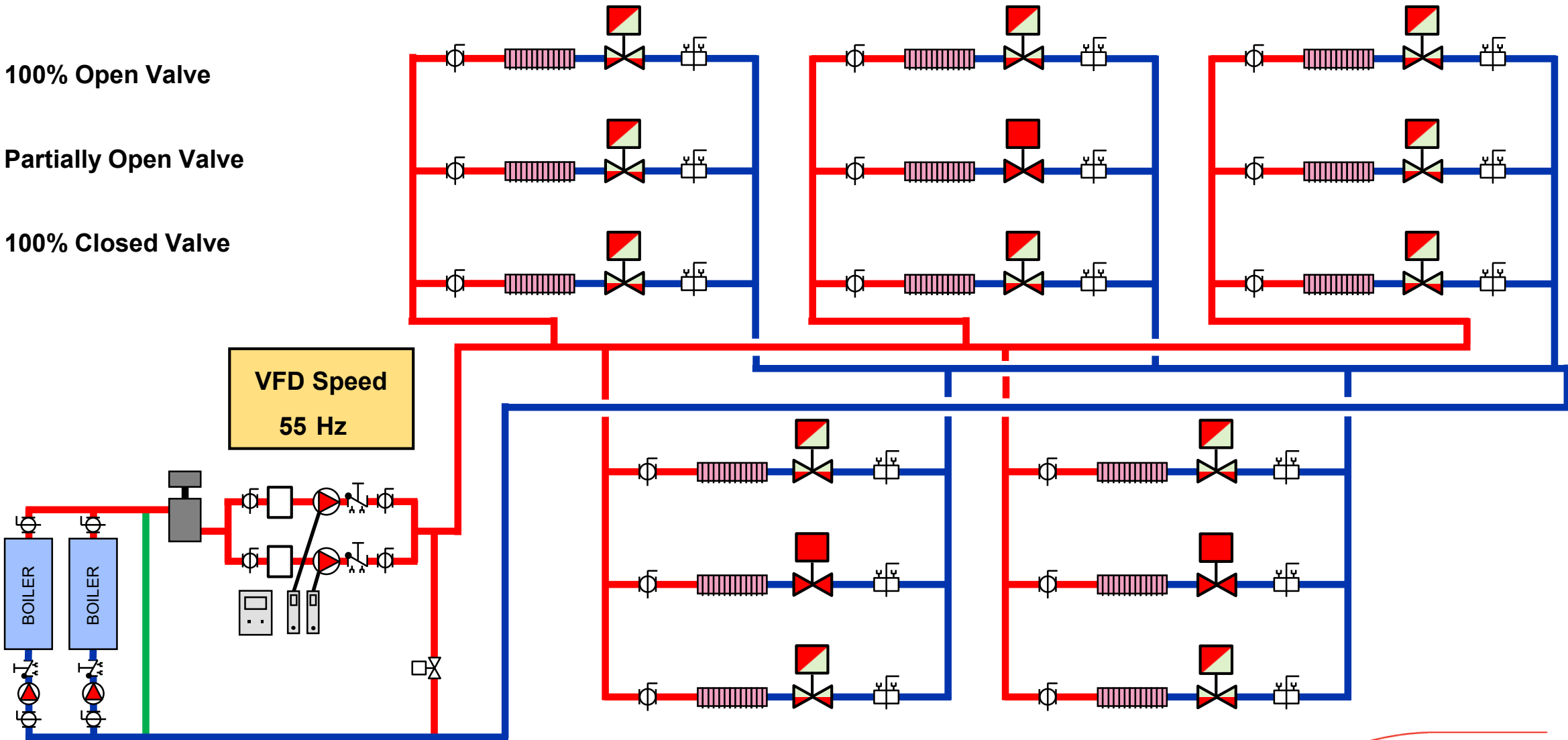
6.5.4.2 Hydronic Variable Flow Systems




.... The *controls* or devices shall be controlled as a function of desired flow or to maintain a minimum required differential pressure. Differential pressure shall be measured at or near the most remote heat exchanger requiring the greatest differential pressure. **Where differential pressure control is used to comply with this section and *DDC systems* are used, the *set point* shall be *reset downward based on valve positions until one valve is nearly wide open.***

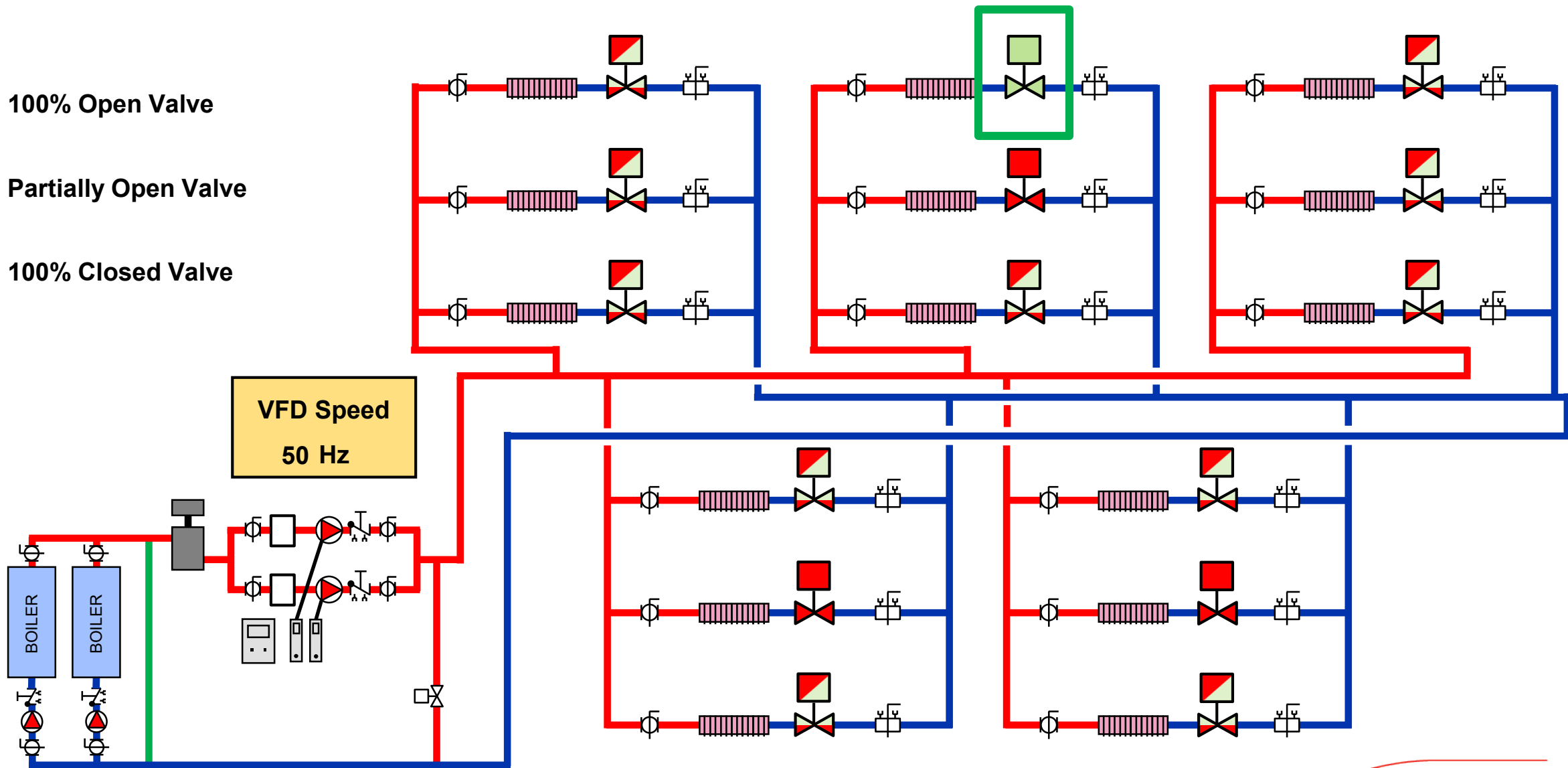
-  - 100% Open Valve
-  - Partially Open Valve
-  - 100% Closed Valve






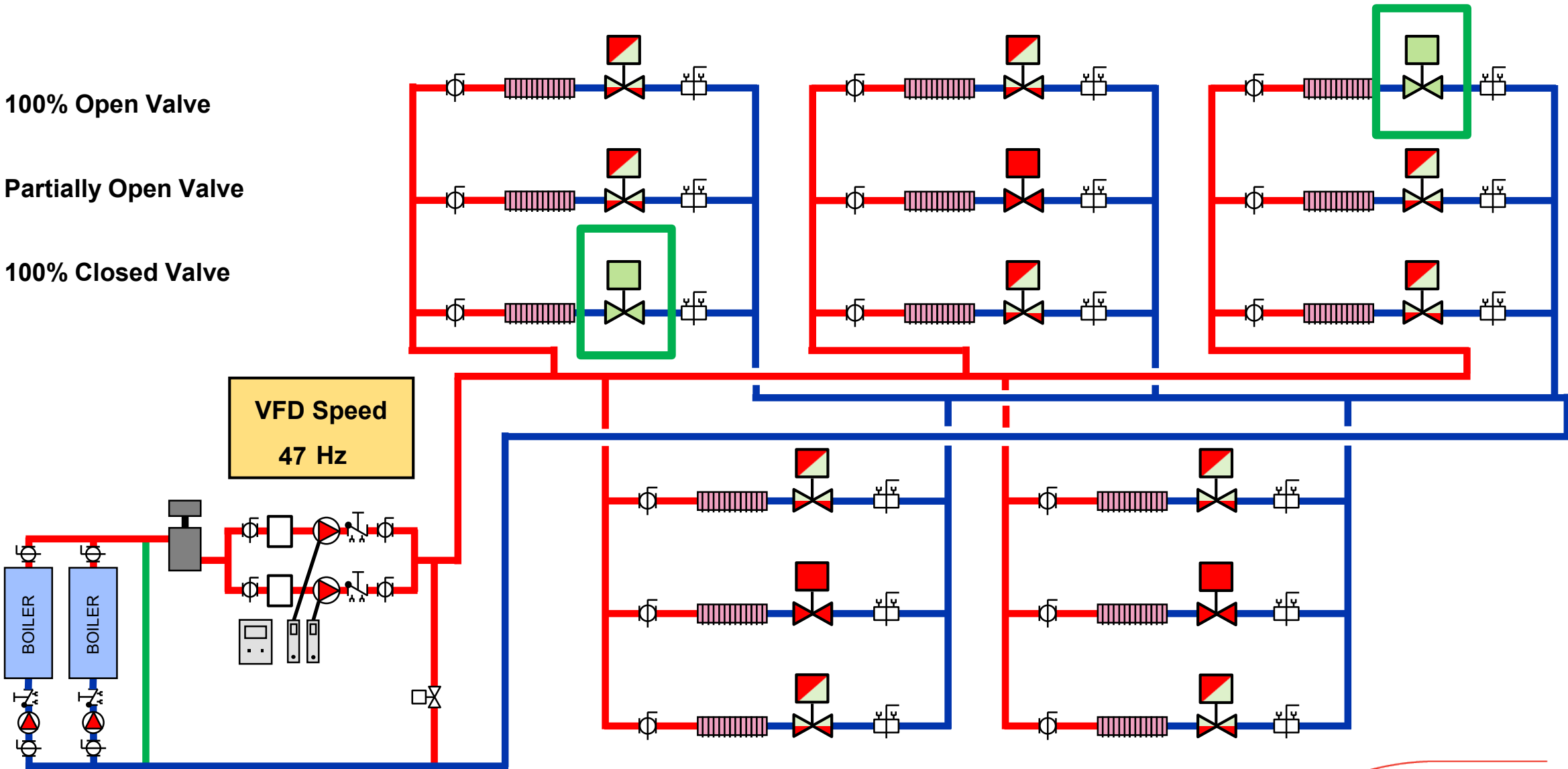
-  - 100% Open Valve
-  - Partially Open Valve
-  - 100% Closed Valve






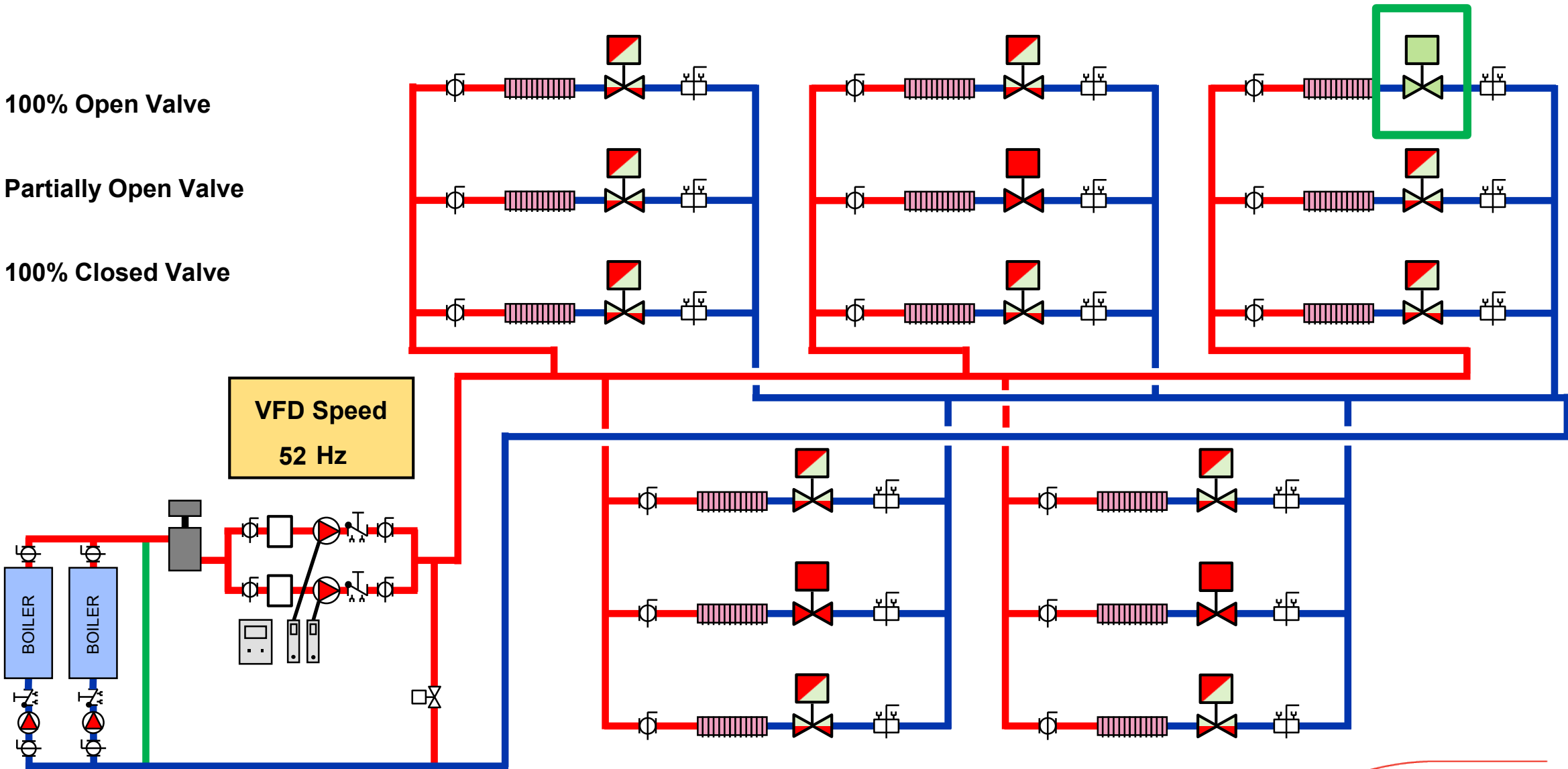
-  - 100% Open Valve
-  - Partially Open Valve
-  - 100% Closed Valve

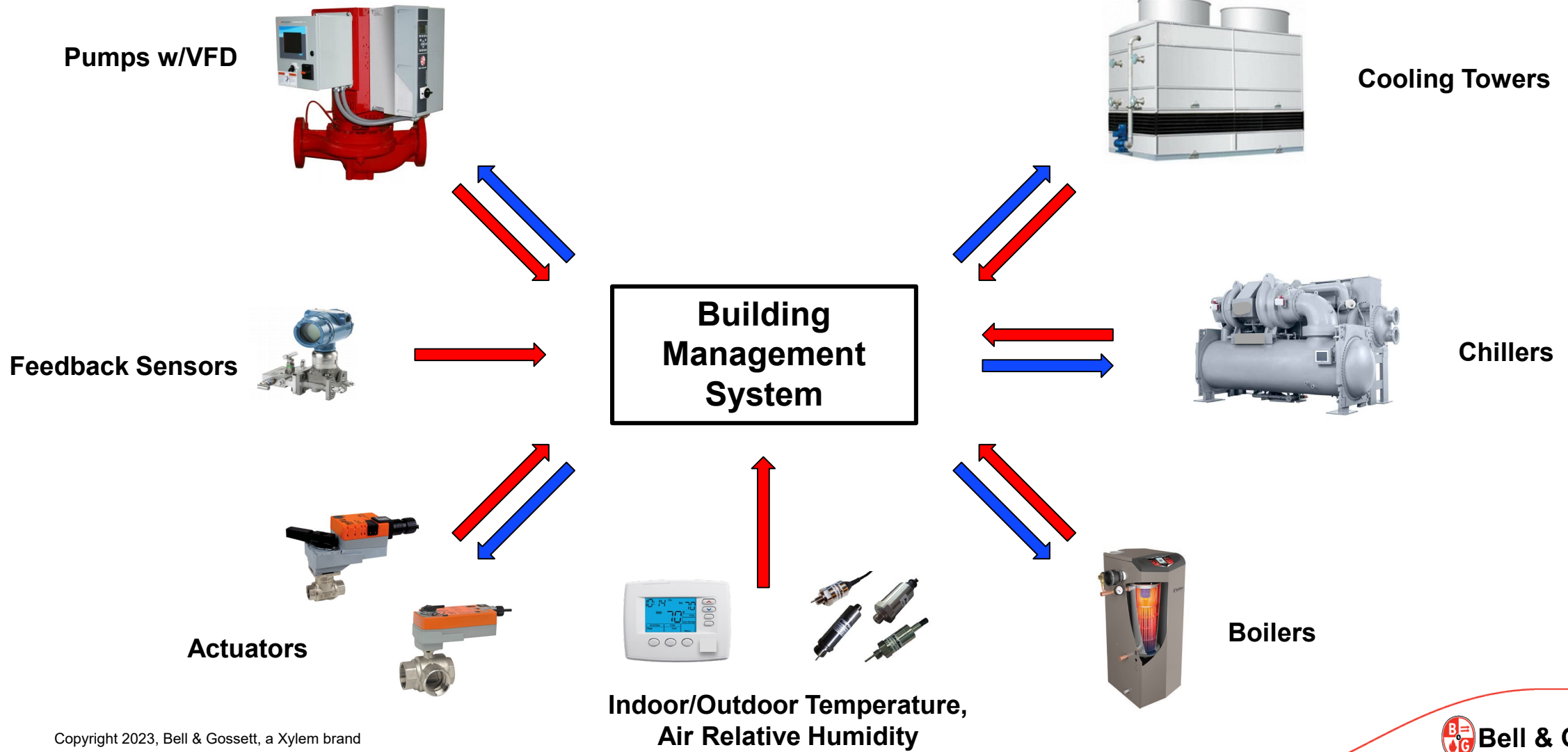


-  - 100% Open Valve
-  - Partially Open Valve
-  - 100% Closed Valve

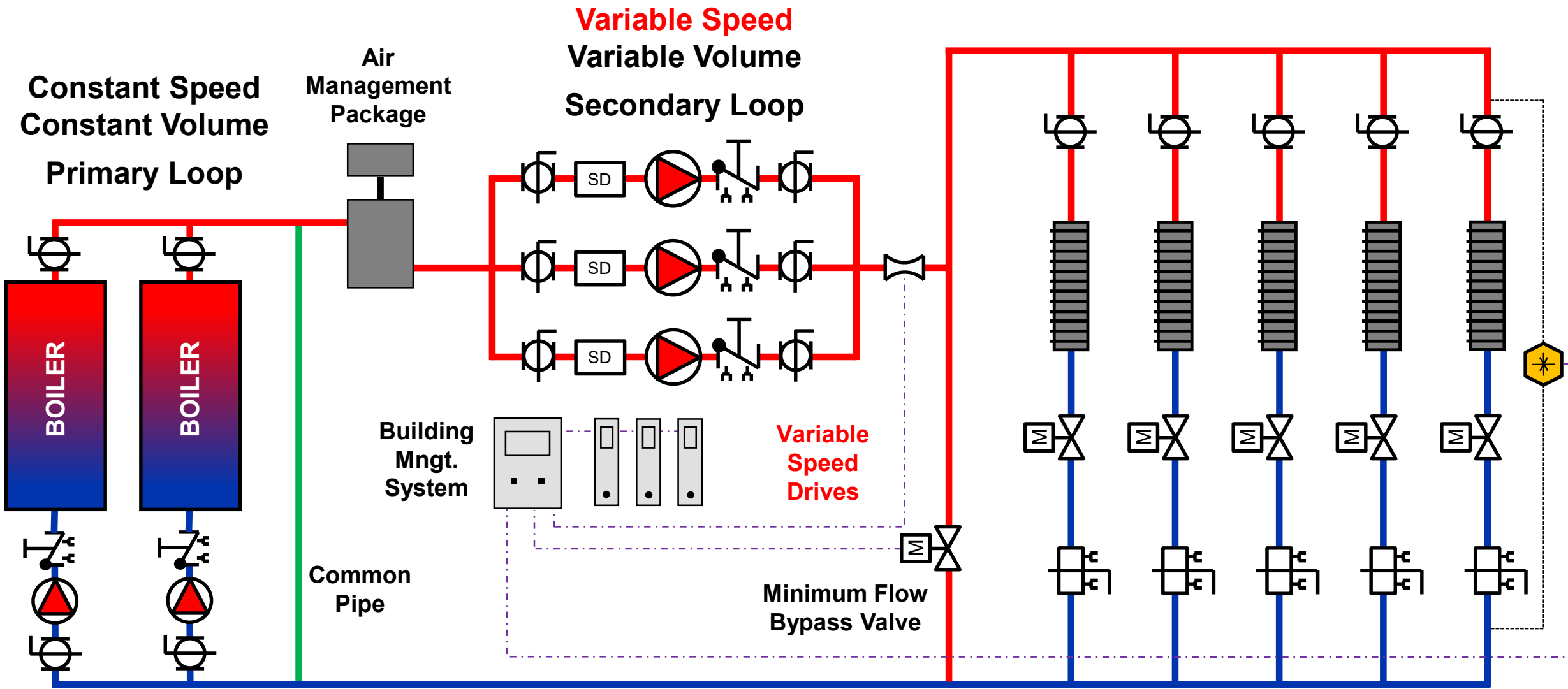


-  - 100% Open Valve
-  - Partially Open Valve
-  - 100% Closed Valve





Parallel Pumping with Variable Speed Drives



Pump > e-1510 5BD

[← Back to Selection](#)



e-1510 5BD

Duty Point Flow: 3000 US gpm: 3 pumps = 1000 US gpm ea
Duty Point Head: 50 ft
Discharge Size (in): 5
Discharge Velocity (fps): 48.0
Suction Size (in): 6
Suction Velocity (fps): 33.3
Weight: 692 lb [i](#)

Motor: 20 hp
End Of Curve: 80%
NPSHr (ft): 12.1
Floor Space (ft²): 7.1 [i](#)

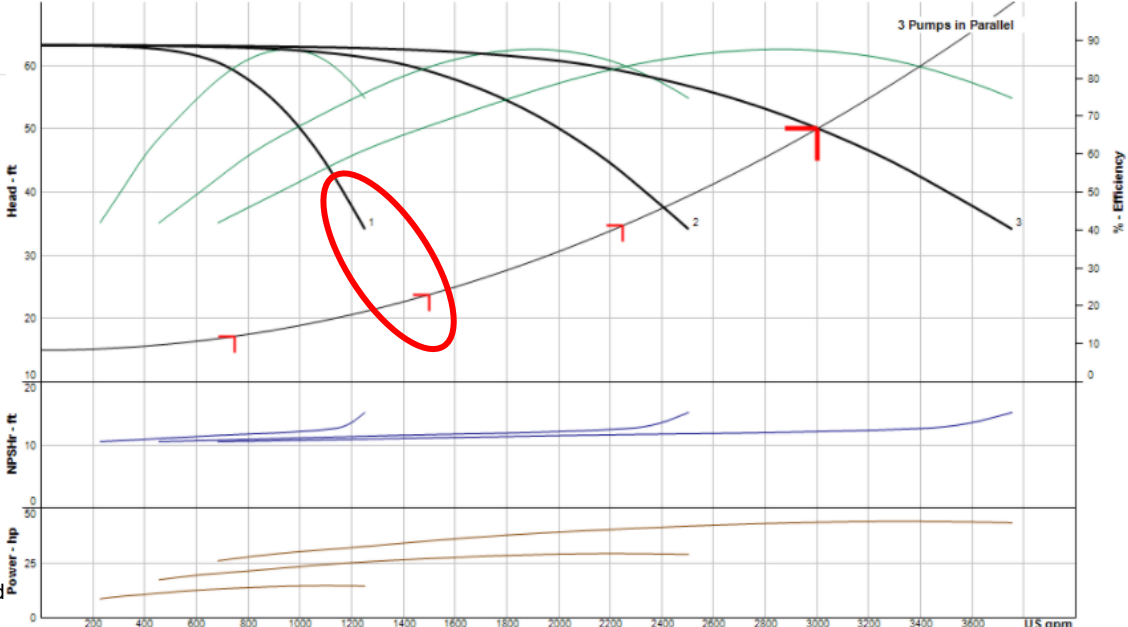
NOL (BHP) at 1770: 19.4
NOL Flow at 1770: 1199 US gpm
Runout Flow at 1770: 1375 US gpm
Shutoff Head at 1770: 76.3 ft

Operating Point [i](#)

Flow: 1001 US gpm **Head:** 50.1 ft **Speed:** 1611 **Efficiency:** 86.6% **Point BHP:** 14.5

Maximum Duty Point(at rated motor speed) [i](#)

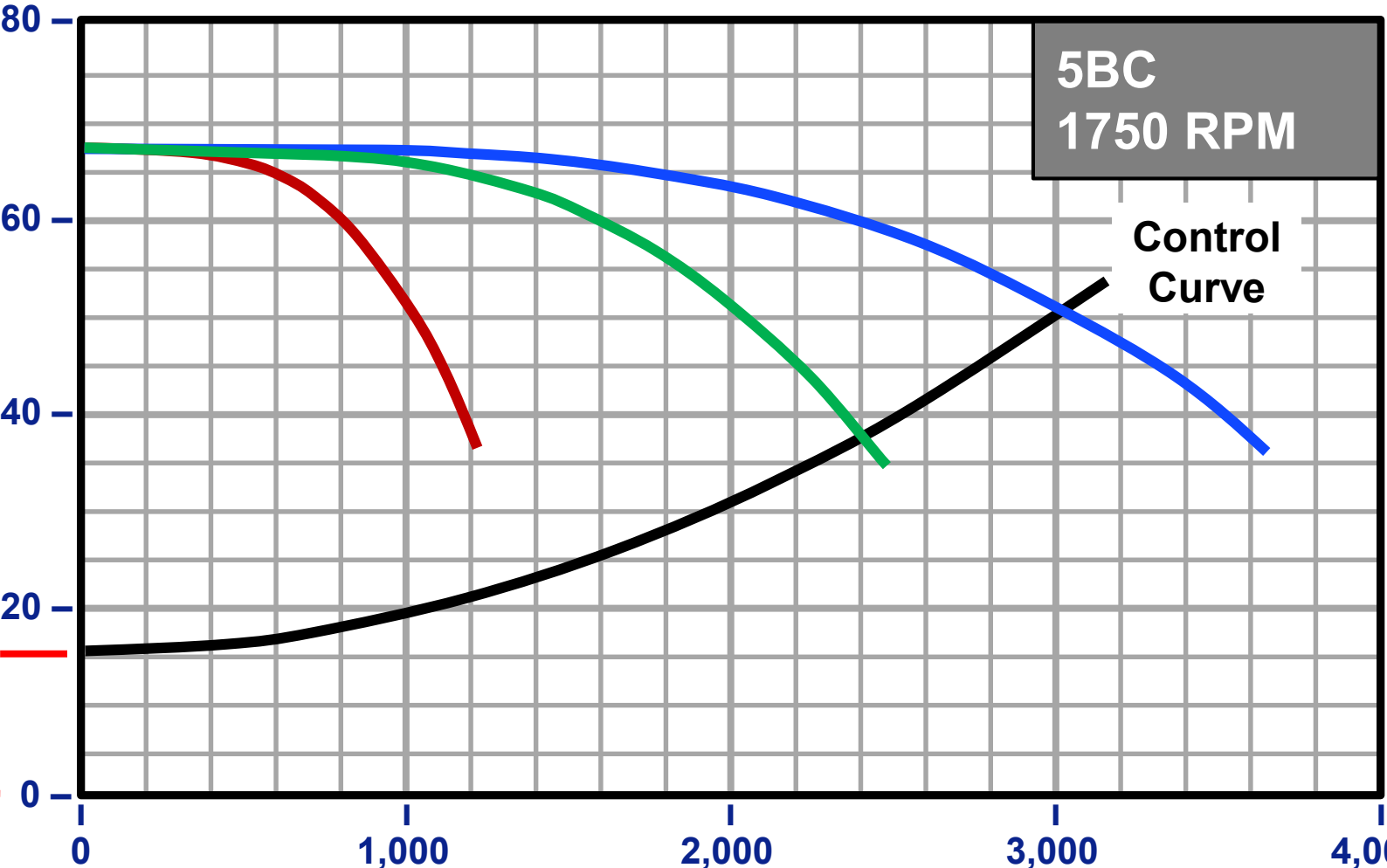
Flow: 1123 US gpm **Head:** 59.1 ft **Speed:** 1770 **Efficiency:** 86.9% **Point BHP:** 19.3



[+ Add to Schedule](#) [↓ Documents](#)

Can a single pump be used?

HEAD (Feet) Pump Series: e-1510

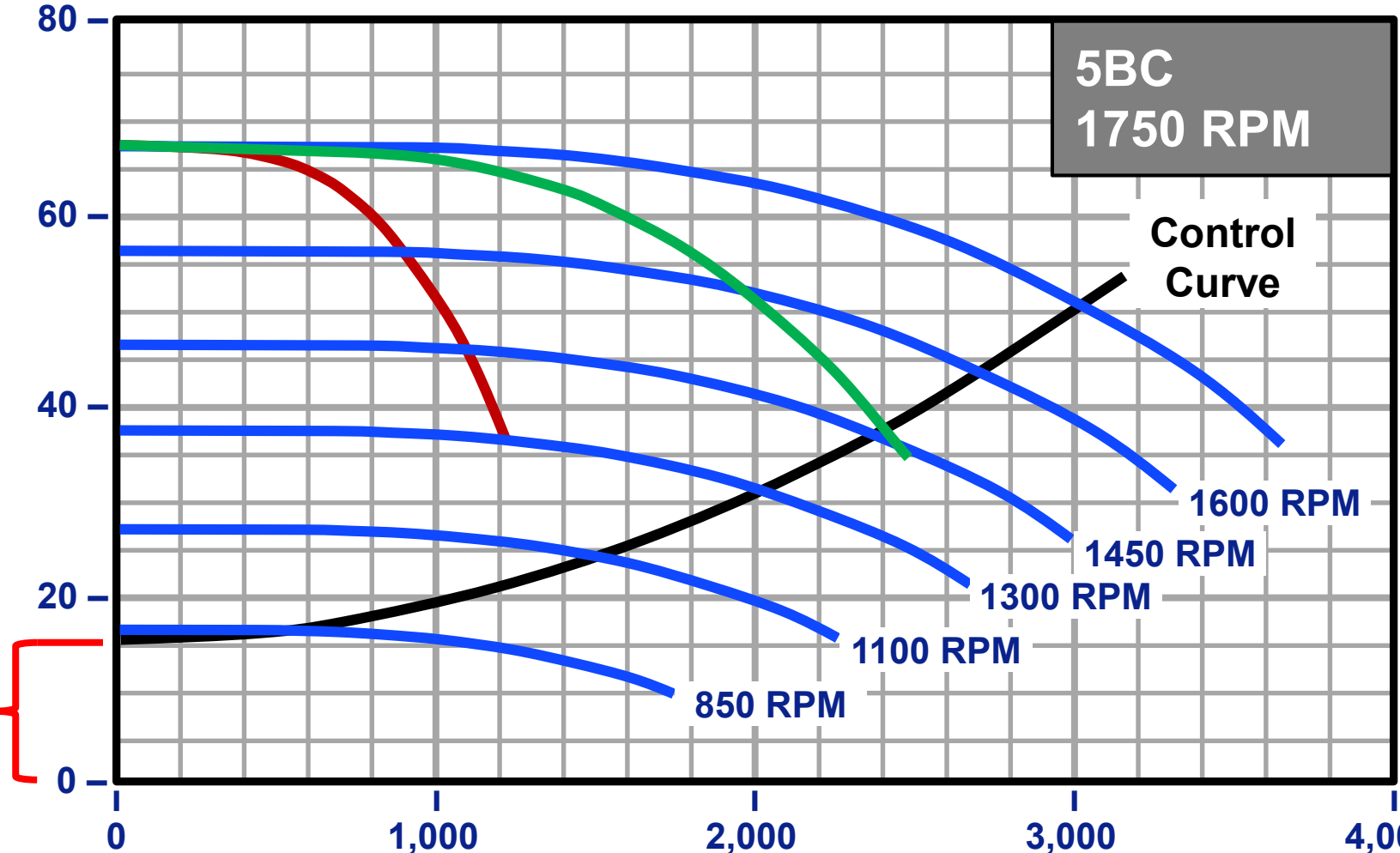


- 3 Pumps Operating Performance Curves
- 2 Pumps Operating Performance Curves
- 1 Pump Operating Performance Curves

Minimum Control Head

Can a single pump be used?

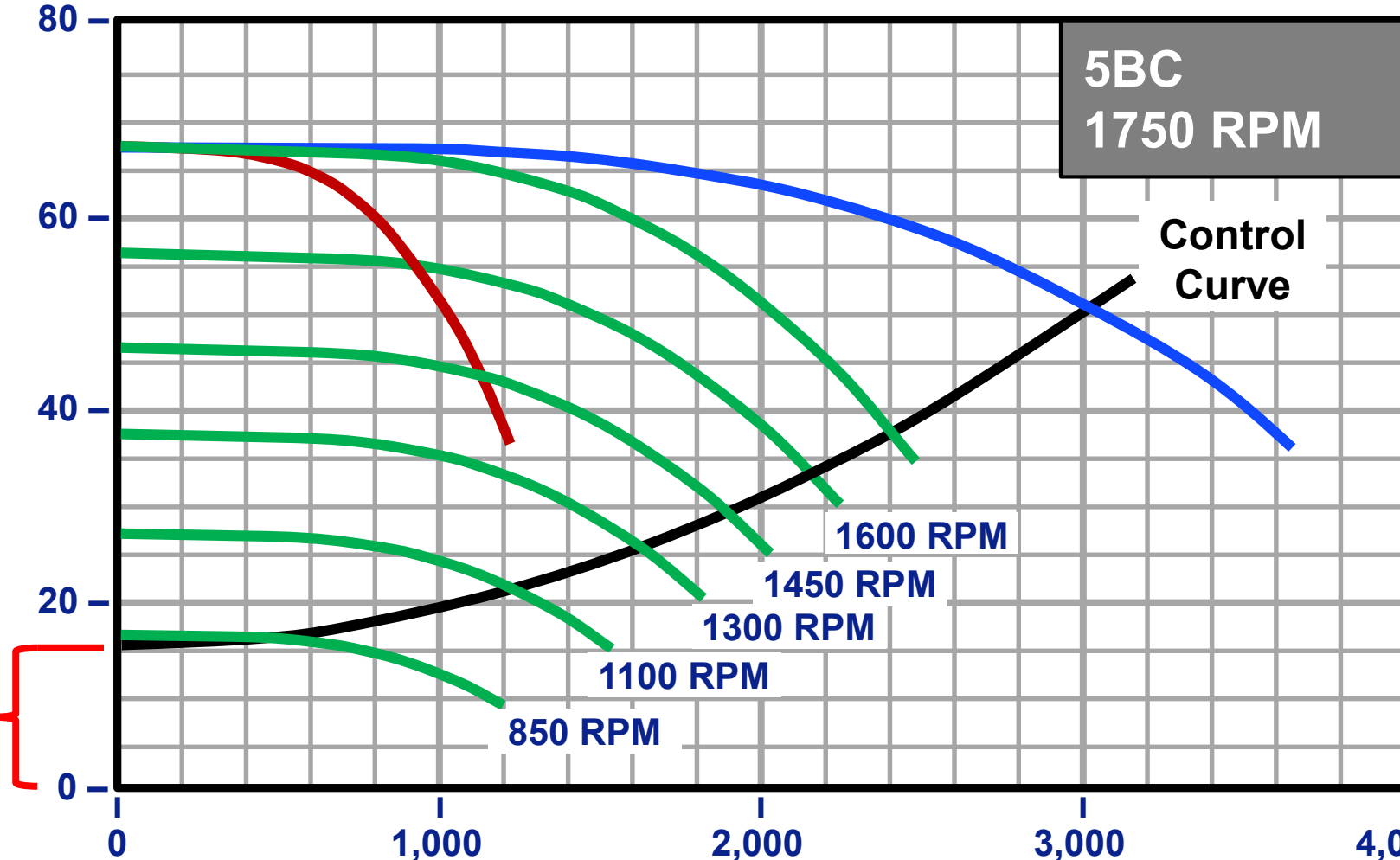
HEAD (Feet) Pump Series: e-1510



- 3 Pumps Operating Performance Curves
- 2 Pumps Operating Performance Curves
- 1 Pump Operating Performance Curves

Can a single pump be used?

HEAD (Feet) Pump Series: e-1510



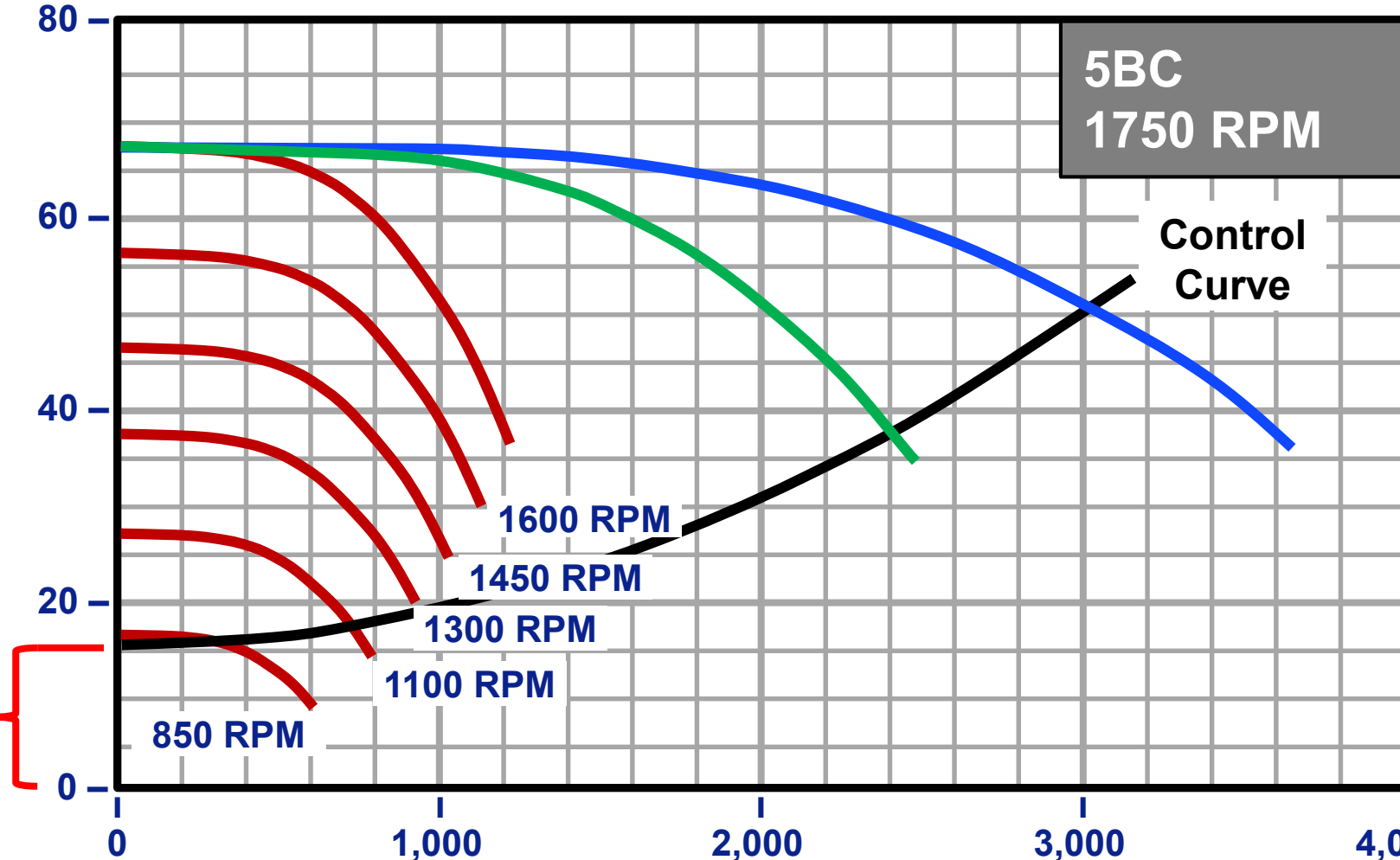
5BC
1750 RPM

- 3 Pumps Operating Performance Curves
- 2 Pumps Operating Performance Curves
- 1 Pump Operating Performance Curves

Minimum Control Head

Can a single pump be used?

HEAD (Feet) Pump Series: e-1510

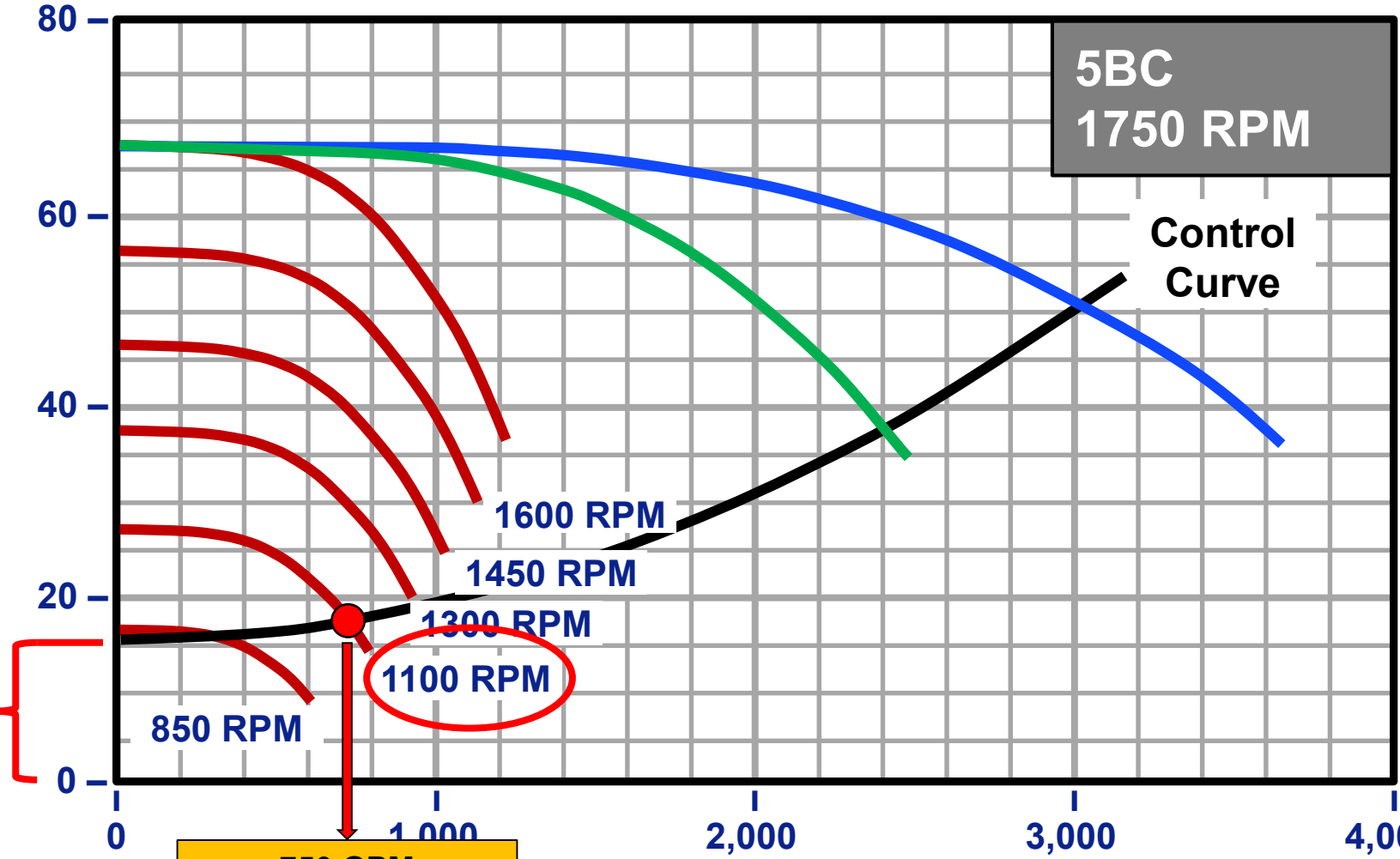


- 3 Pumps Operating Performance Curves
- 2 Pumps Operating Performance Curves
- 1 Pump Operating Performance Curves

Minimum Control Head

Can a single pump be used?

HEAD (Feet) Pump Series: e-1510



- 3 Pumps Operating Performance Curves
- 2 Pumps Operating Performance Curves
- 1 Pump Operating Performance Curves

Minimum Control Head

750 GPM
(25% of 3,000 GPM)

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Performance

Overview

Operating Cost

Best Efficiency Staging

Dimensions

Single pump variable staging possible?			Yes		
System curve crosses full speed curve			No	Yes	Yes
Load	Weighting	Best eff	1 Pump	2 Pumps	3 Pumps
100%	1%	86.6%			86.6
75%	42%	87.3%		79.8%	87.3%
50%	45%	85.3%		85.3%	84.1%
25%	12%	79.5%	66.5%	79.5%	65.4%
Optimal Staging PLEV		85.5%			

Courtesy of **B&G ESP-Systemwize**

Selection Software

The Closing Tip

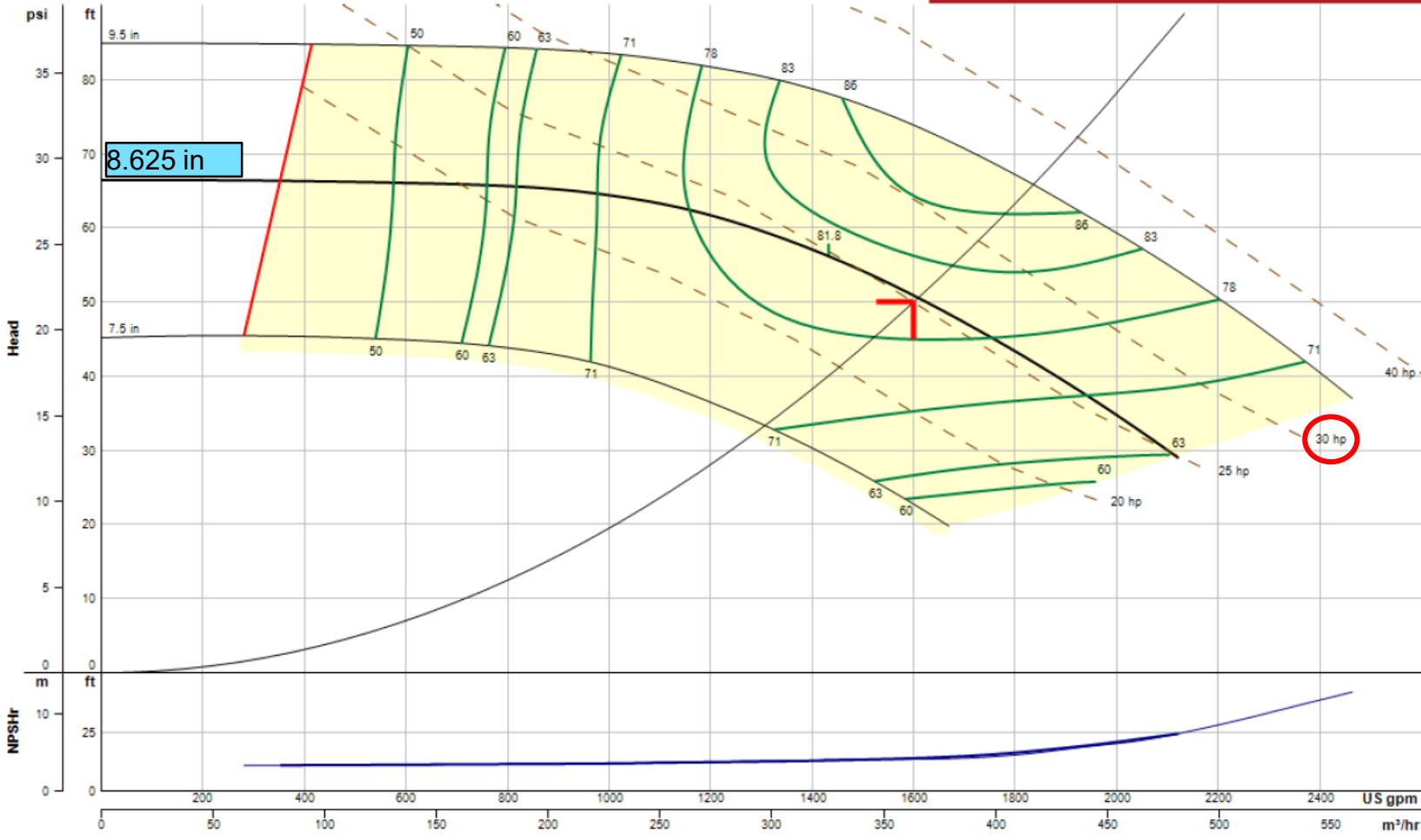
Trimmed to Duty Point

Performance Curve

Energy Efficiency Ratings:
 Pump & Motor PEIcl: 0.93 ERcl: 7
 Pump, Motor & Drive: PEIvl: 0.45 ERvl: 55



e-1510
6BD
1770 RPM



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Pump Selection Summary	
Duty Point Flow	1600 US gpm
Duty Point Head	50 ft
Control Head	0 ft
Duty Point Pump Efficiency	79.7 %
Part Load Efficiency Value (PLEV)	0.0 %
Impeller Diameter	8.625 in
Motor Power	30 hp
Duty Point Power	25.3 bhp
Motor Speed	1800 rpm
RPM @ Duty Point	1770 rpm
NPSHr	14.3 ft
Minimum Shutoff Head	66.4 ft
Minimum Flow at RPM	329 US gpm
Flow @ BEP	1432 US gpm
Fluid Temperature	68 °F
Fluid Type	Water
Weight (approx. - consult rep for exact)	928 lbs
Pump Floor Space Calculation	8.74 ft²

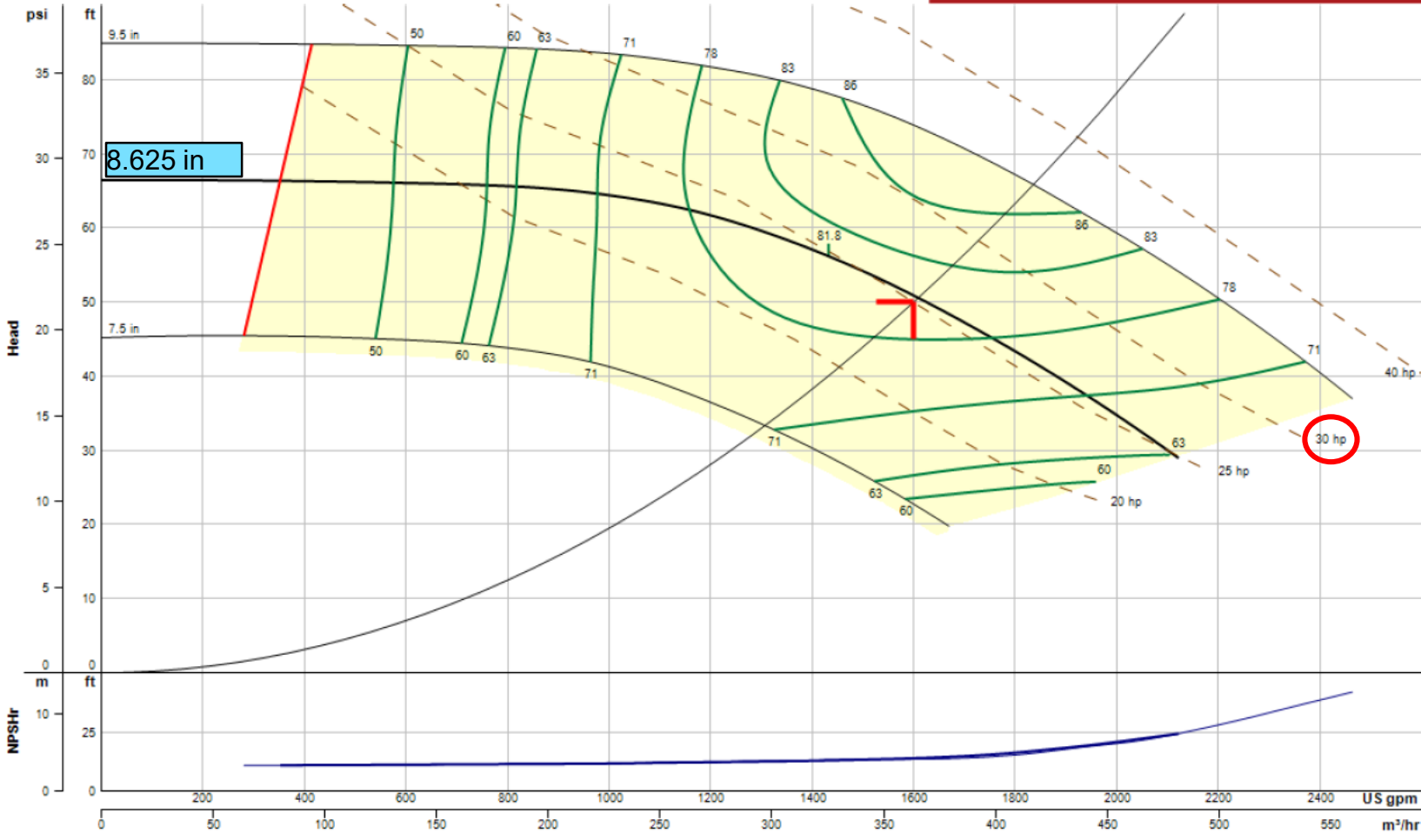
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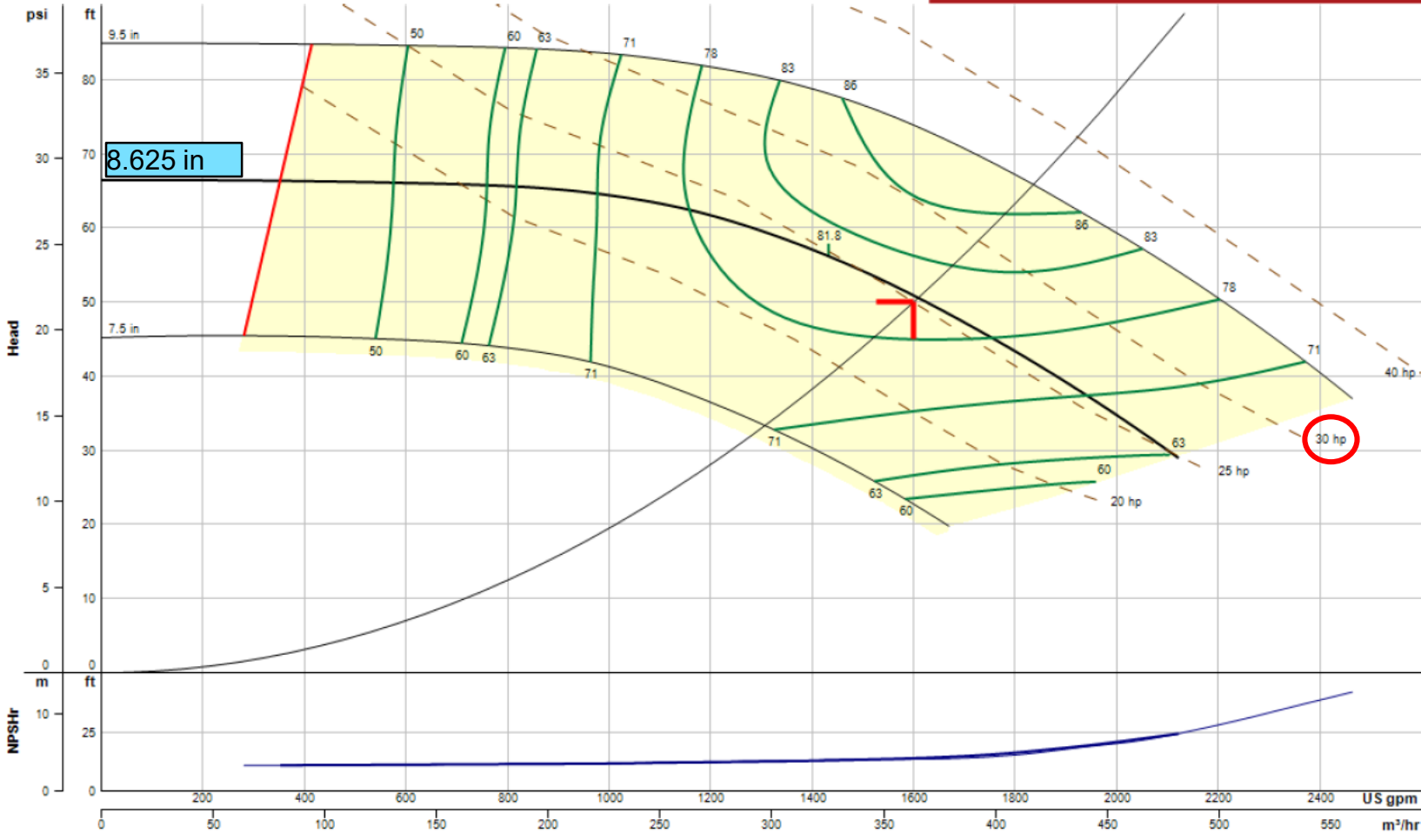
Trimmed to Duty Point

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1770 RPM



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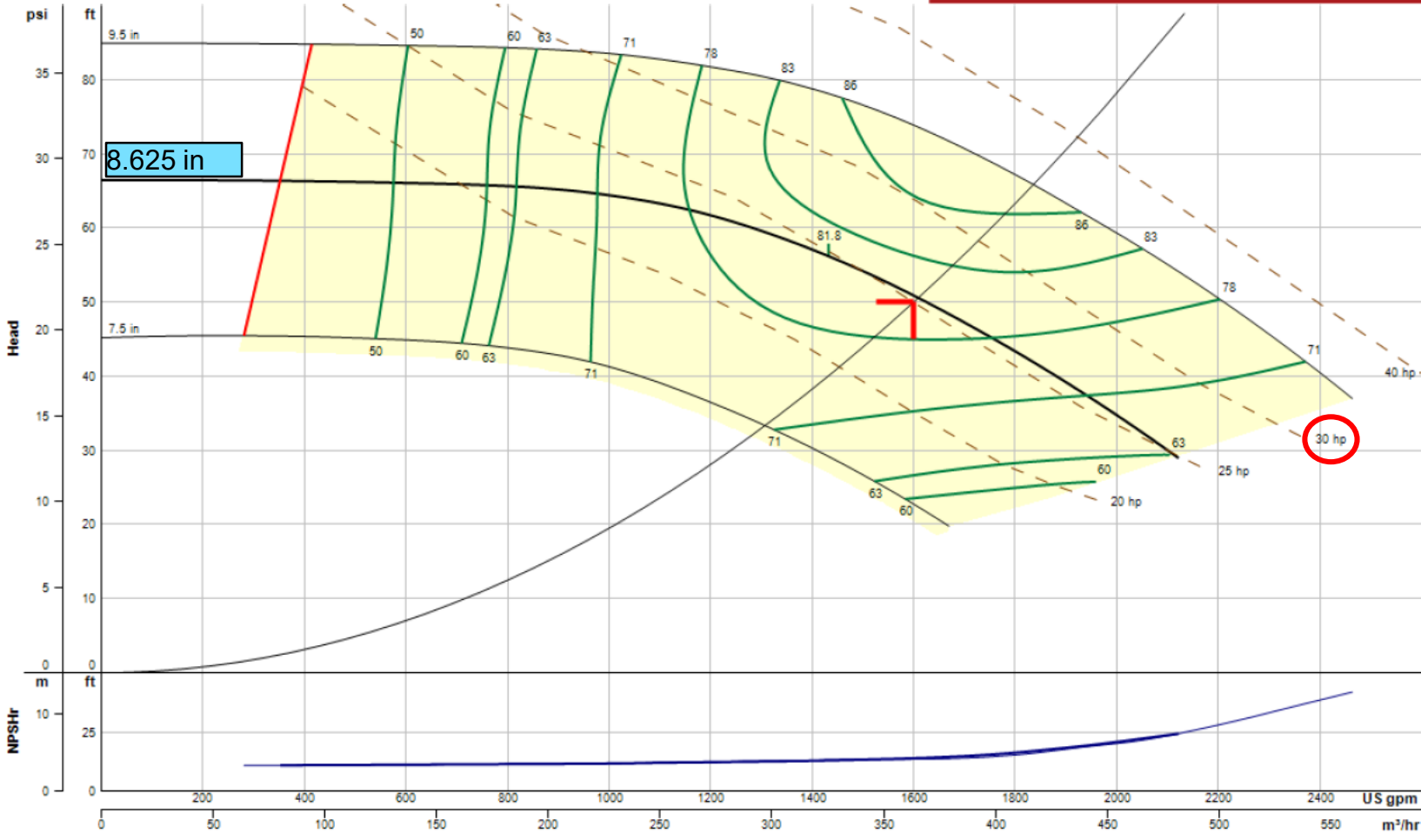
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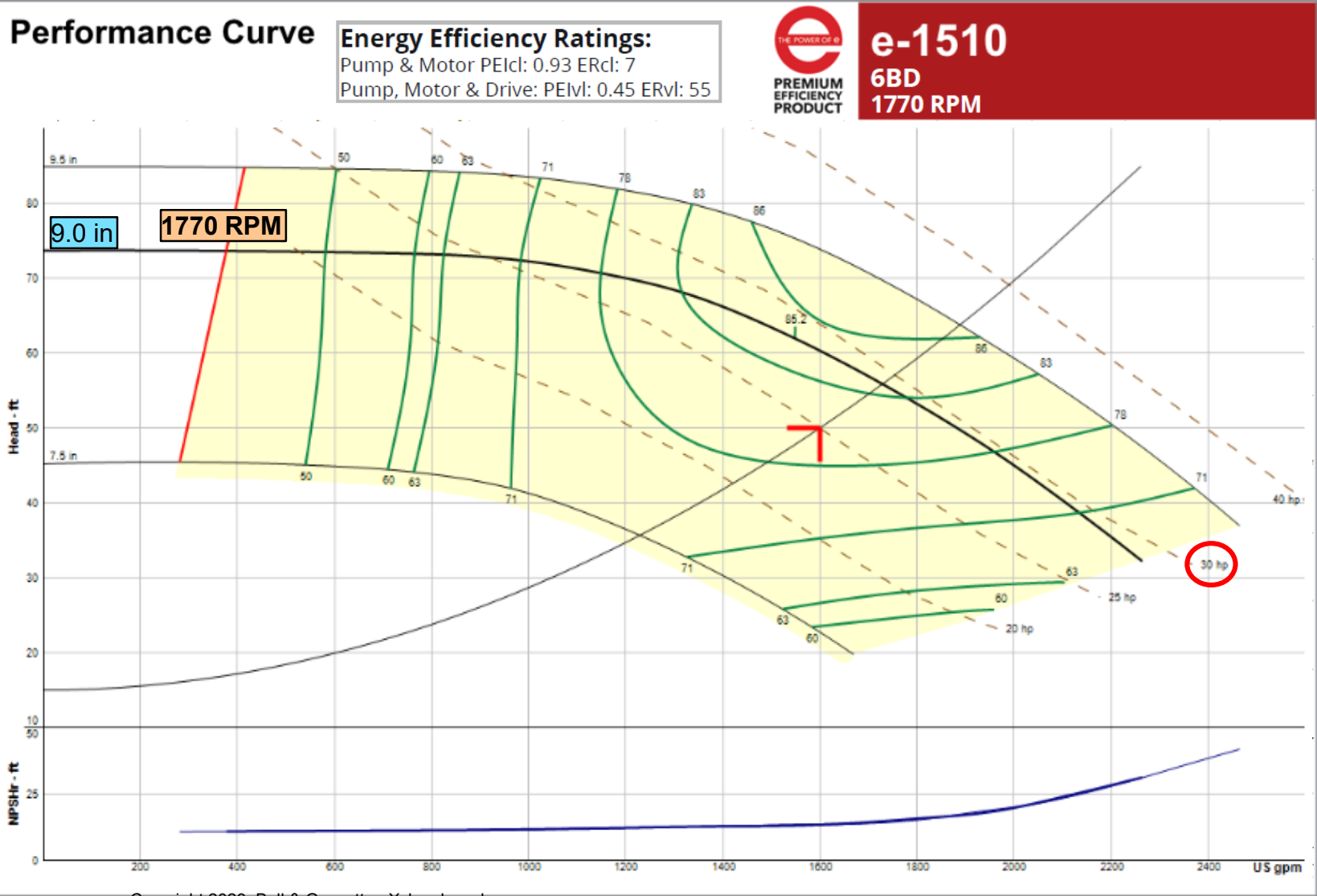
e-1510
6BD
1770 RPM



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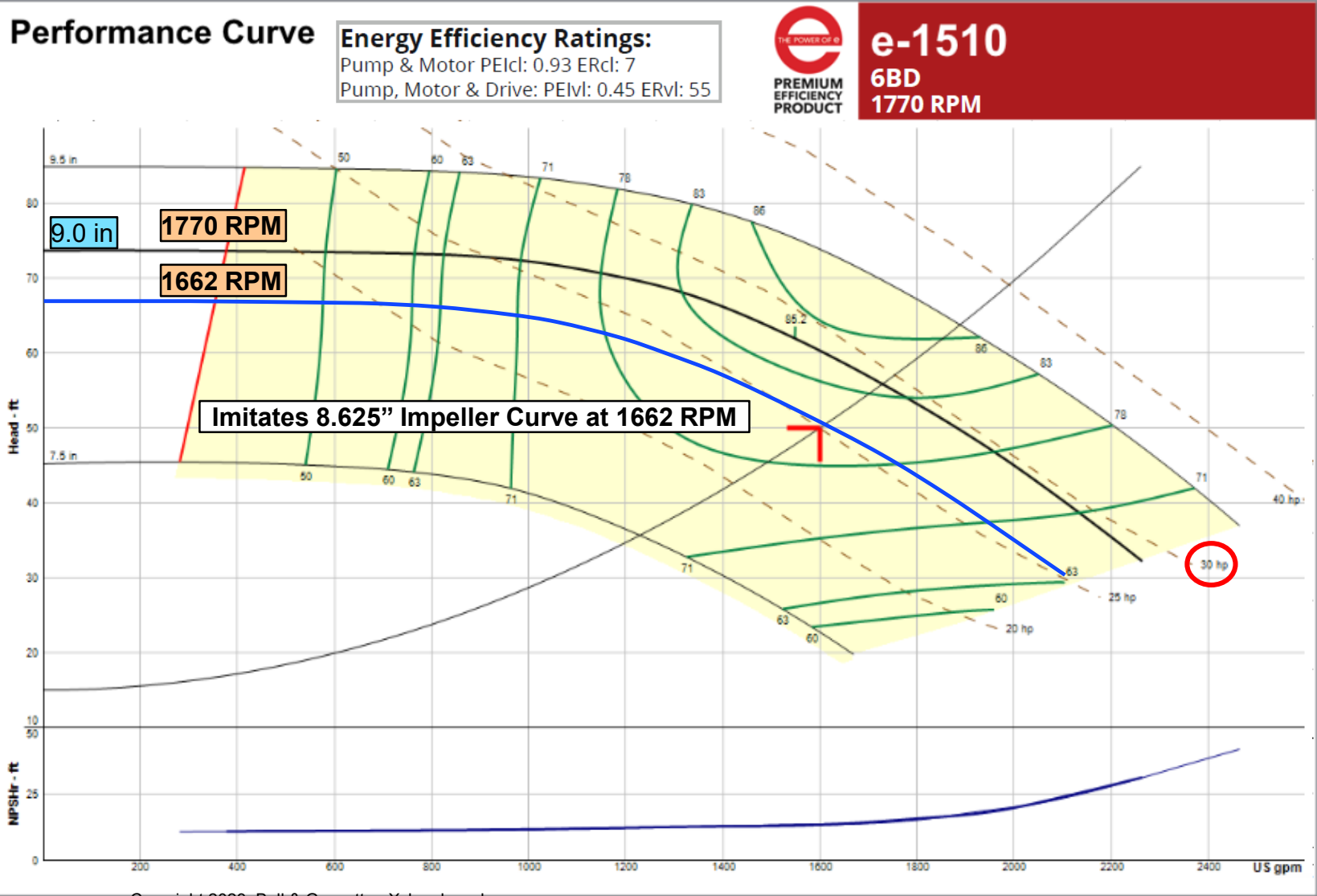
Trimmed to Largest Diameter for Motor Size



Pump Selection Summary	
Duty Point Flow	1600 US gpm
Duty Point Head	50 ft
Control Head	15 ft
Duty Point Pump Efficiency	84 %
Part Load Efficiency Value (PLEV)	80.9 %
Impeller Diameter	9 in
Motor Power	30 hp
Duty Point Power	24 bhp
Motor Speed	1800 rpm
RPM @ Duty Point	1662 rpm
NPSHr	12.8 ft
Minimum Shutoff Head	65 ft
Minimum Flow at RPM	334 US gpm
Flow @ BEP	1454 US gpm
Fluid Temperature	68 °F
Fluid Type	Water
Weight (approx. - consult rep for exact)	928 lbs
Pump Floor Space Calculation	8.74 ft ²

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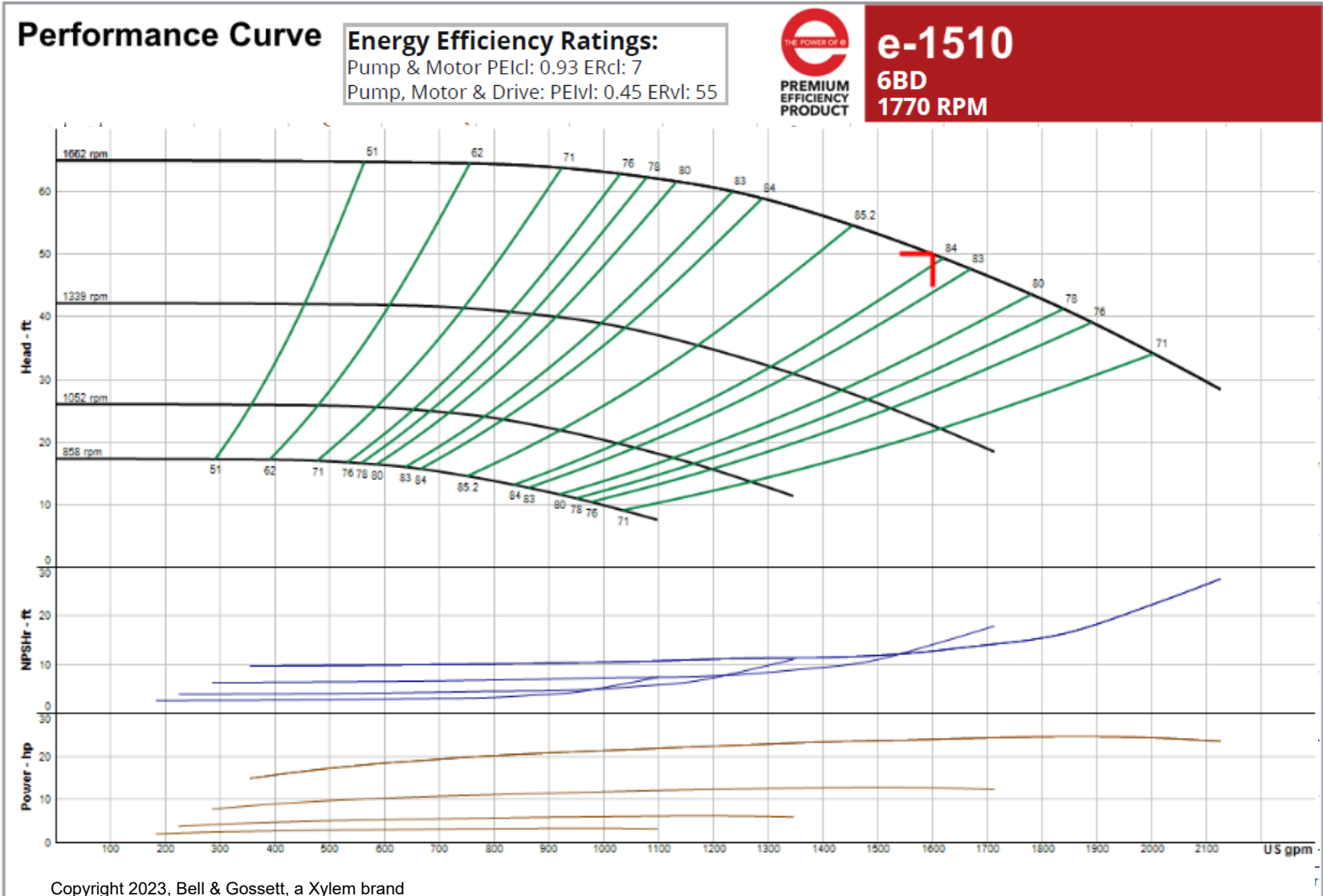
Trimmed to Largest Diameter for Motor Size



Pump Selection Summary	
Duty Point Flow	1600 US gpm
Duty Point Head	50 ft
Control Head	15 ft
Duty Point Pump Efficiency	84 %
Part Load Efficiency Value (PLEV)	80.9 %
Impeller Diameter	9 in
Motor Power	30 hp
Duty Point Power	24 bhp
Motor Speed	1800 rpm
RPM @ Duty Point	1662 rpm
NPSHr	12.8 ft
Minimum Shutoff Head	65 ft
Minimum Flow at RPM	334 US gpm
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Fluid Temperature	68 °F
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Largest Diameter at Reduced Speed to meet Duty Point



Efficiency Gain:

$84\% - 79.7\% = 4.3\%$

BHP Reduction:

$25.3 - 24.0 = 1.3 \text{ BHP}$

