

# Large Chilled Water System

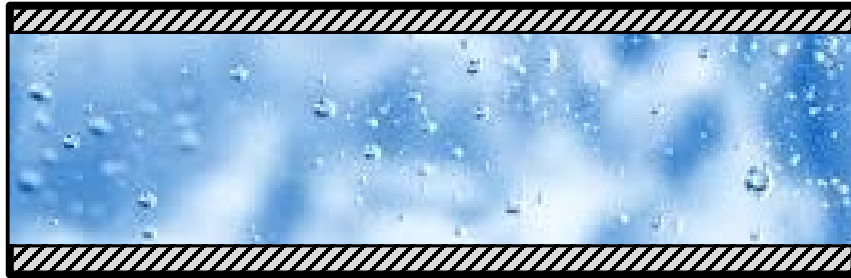
## Design Seminar

Courtesy of Oslin Nation Company

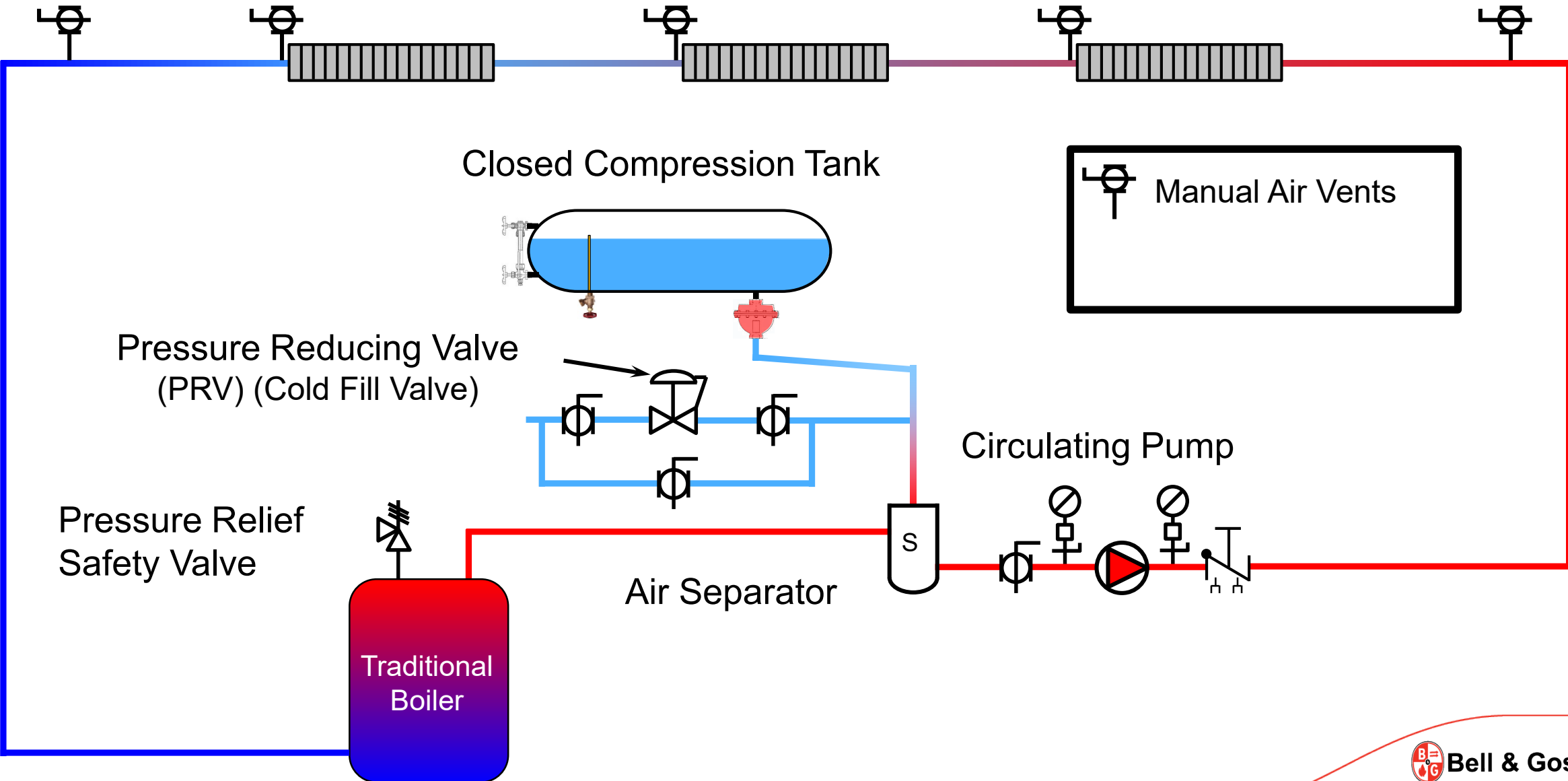
Air Management and System Pressurization

# What Form of Air are we Managing?

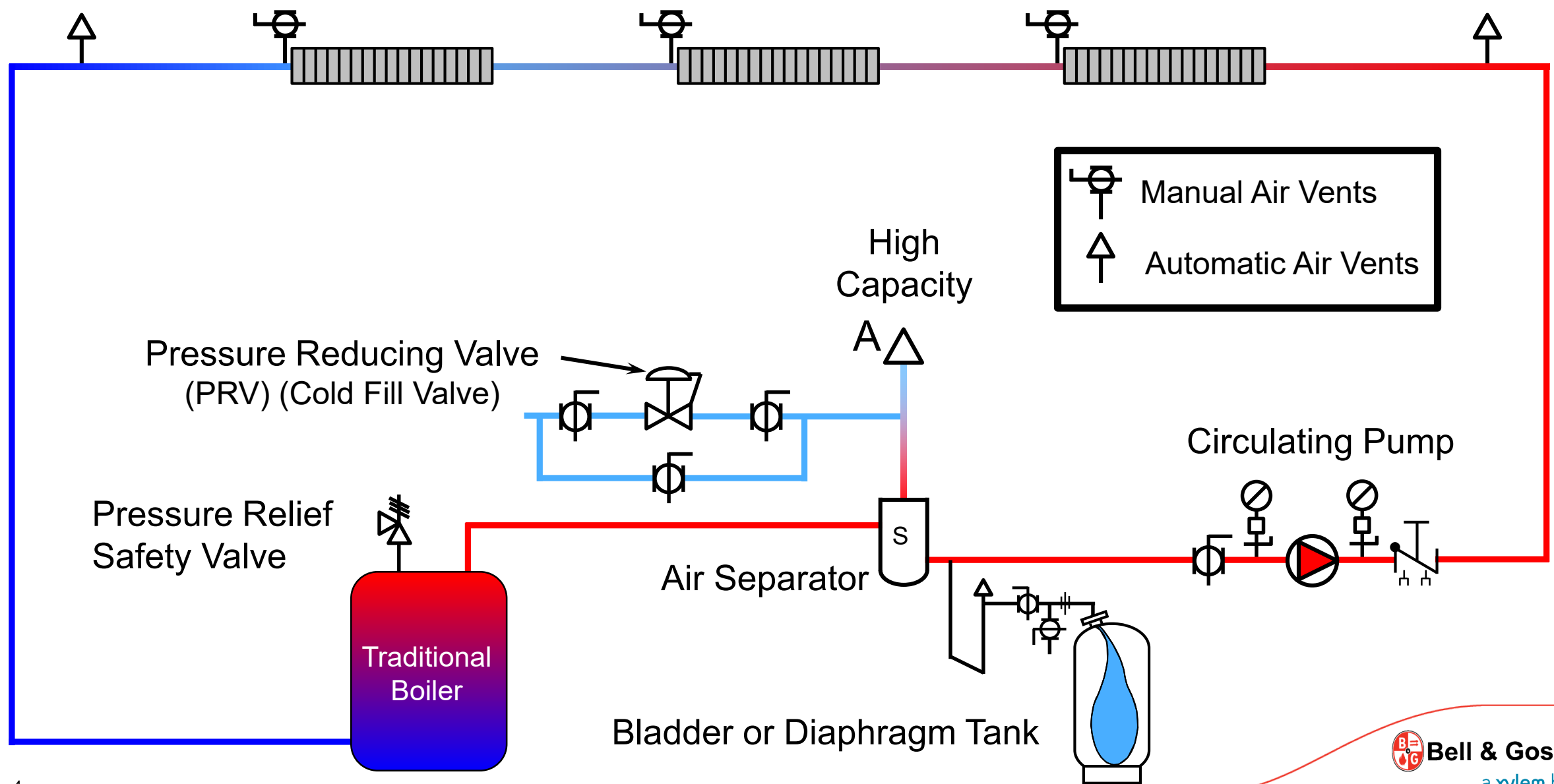
- **Free Air:** Large visible bubbles in the water
- **Entrained Air:** Small micro-bubbles that travel at same velocity as the system water
- **Dissolved or Absorbed Air:** air gases dissolved in solution (mainly  $N_2$  and  $O_2$ )



# Closed Forced Circulation Hot Water System – Air Control

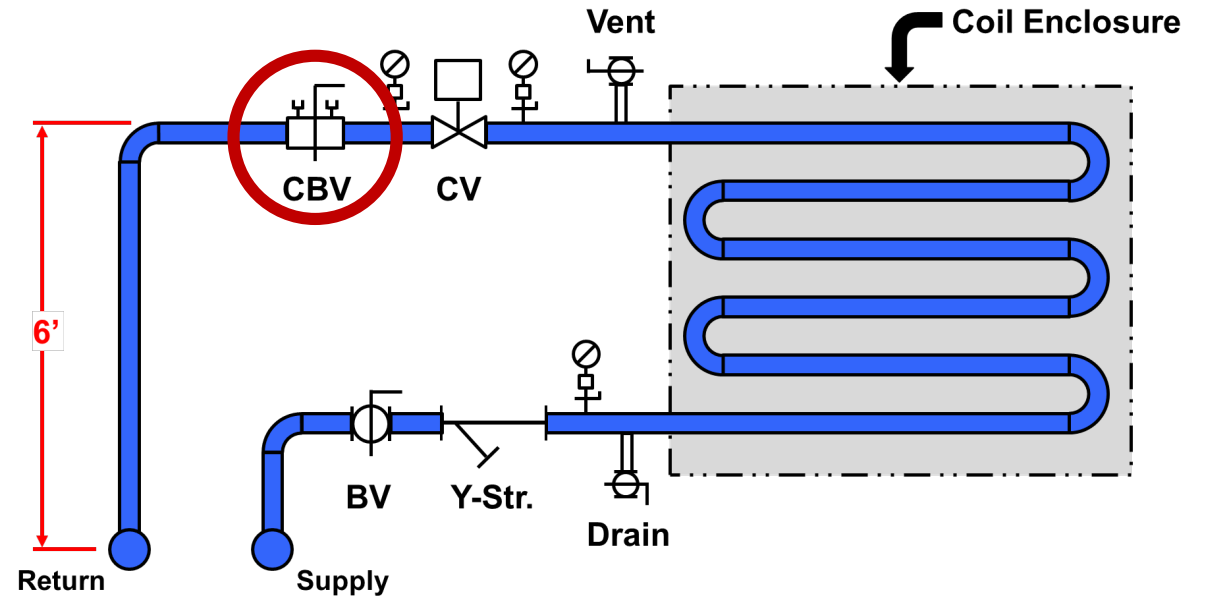
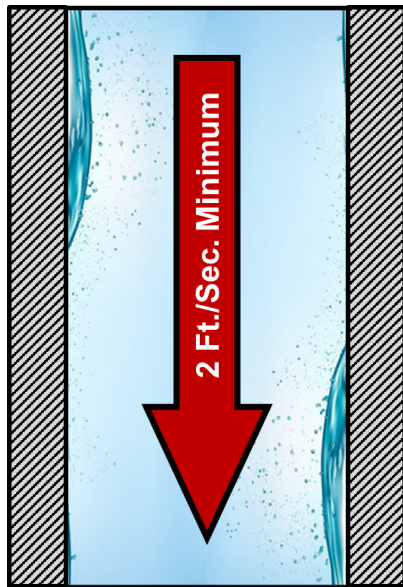


# Closed Forced Circulation Hot Water System – Air Elimination



# Good Piping Design Goals

- Avoid air traps to ensure automatic purging at full flow
- Keep fluid velocity high enough to carry air to desired point of separation
- Proportional Balance flow through each terminal unit



# Air Management in a Closed Loop Hydronic System

- **Initial Fill, Remove Gross Air By:**
  - Venting
  - Purging
- **Operating, Remove Entrained/Dissolved Air Using:**
  - High Temperature
  - Low Pressure
  - Low Velocity
  - Centrifugal Action
  - Coalescence



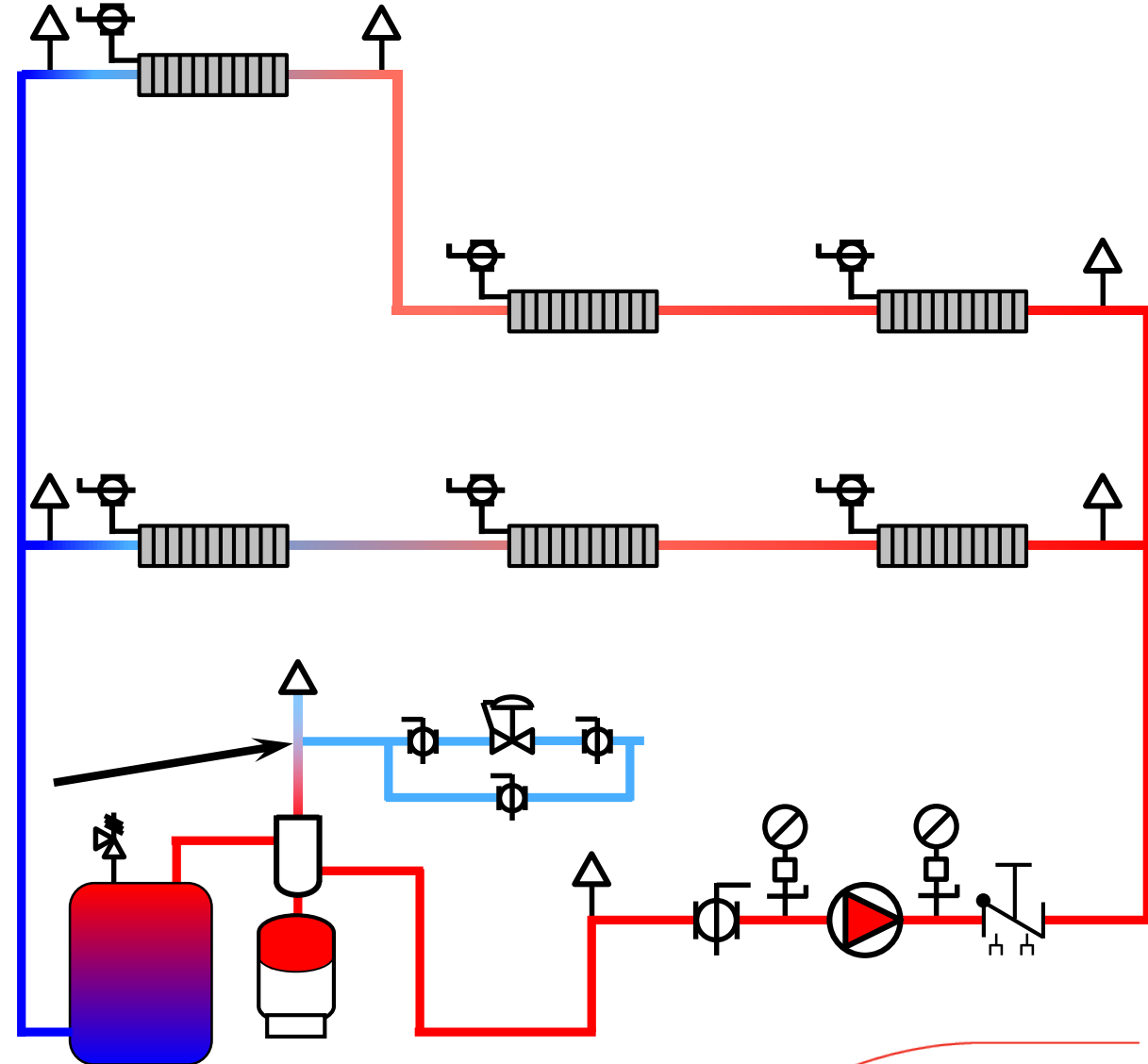
## Venting and Purging a Closed Loop Hydronic System

# System Venting - Water

Liquid fills piping provided:

- Motive pressure is greater than air pressure in piping
- Motive pressure is greater than the static pressure of water column developed

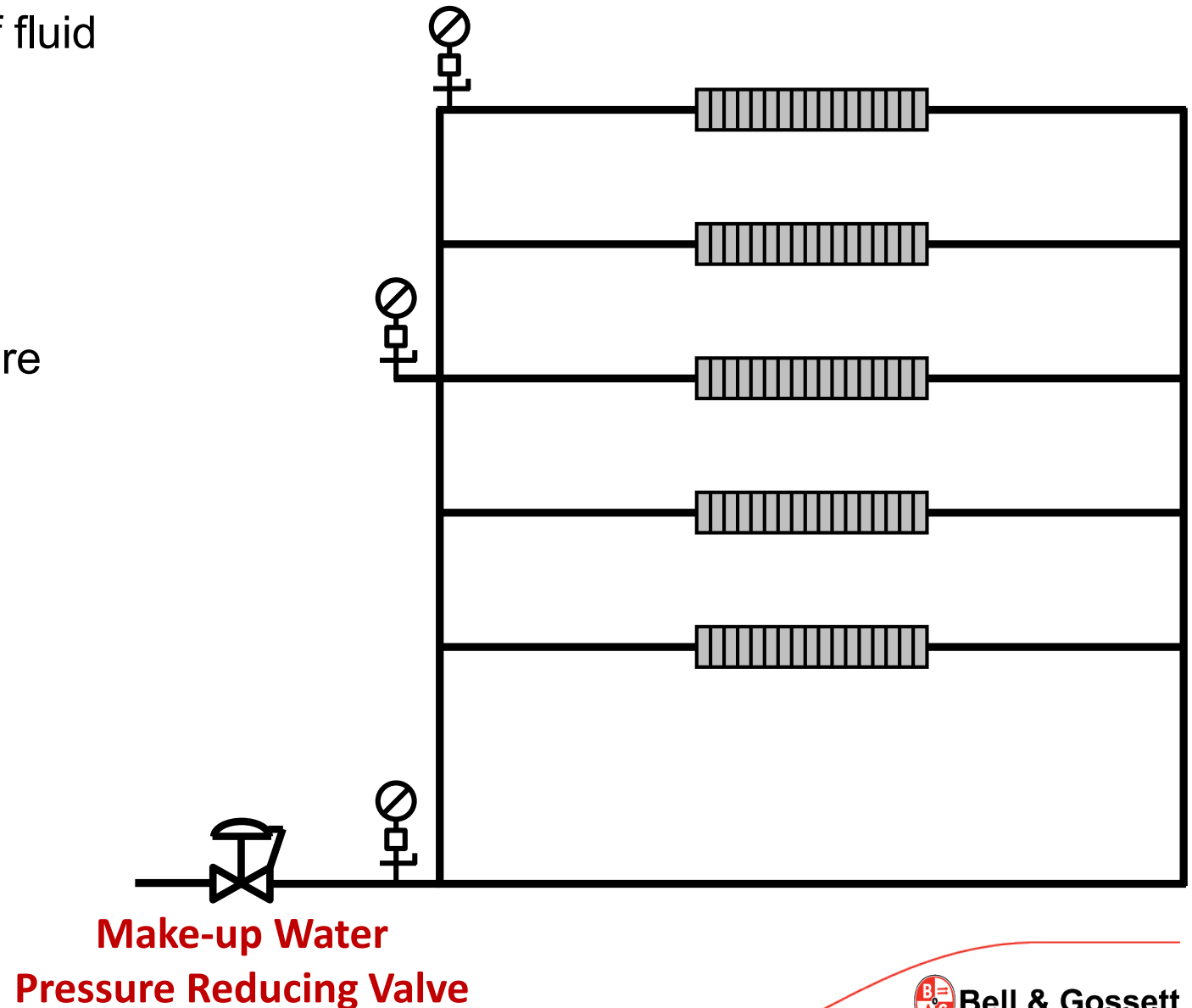
**System Fill Connection**





# Cold Static Fill Pressure: Where is the Make-up Water Valve?

- Pressure caused by weight of a column of fluid
- Influencing Factors
  - Column Height
  - Fluid Type
  - Fluid Density @ Operating Temperature



# Cold Static Fill Pressure: Where is the Make-up Water Valve?

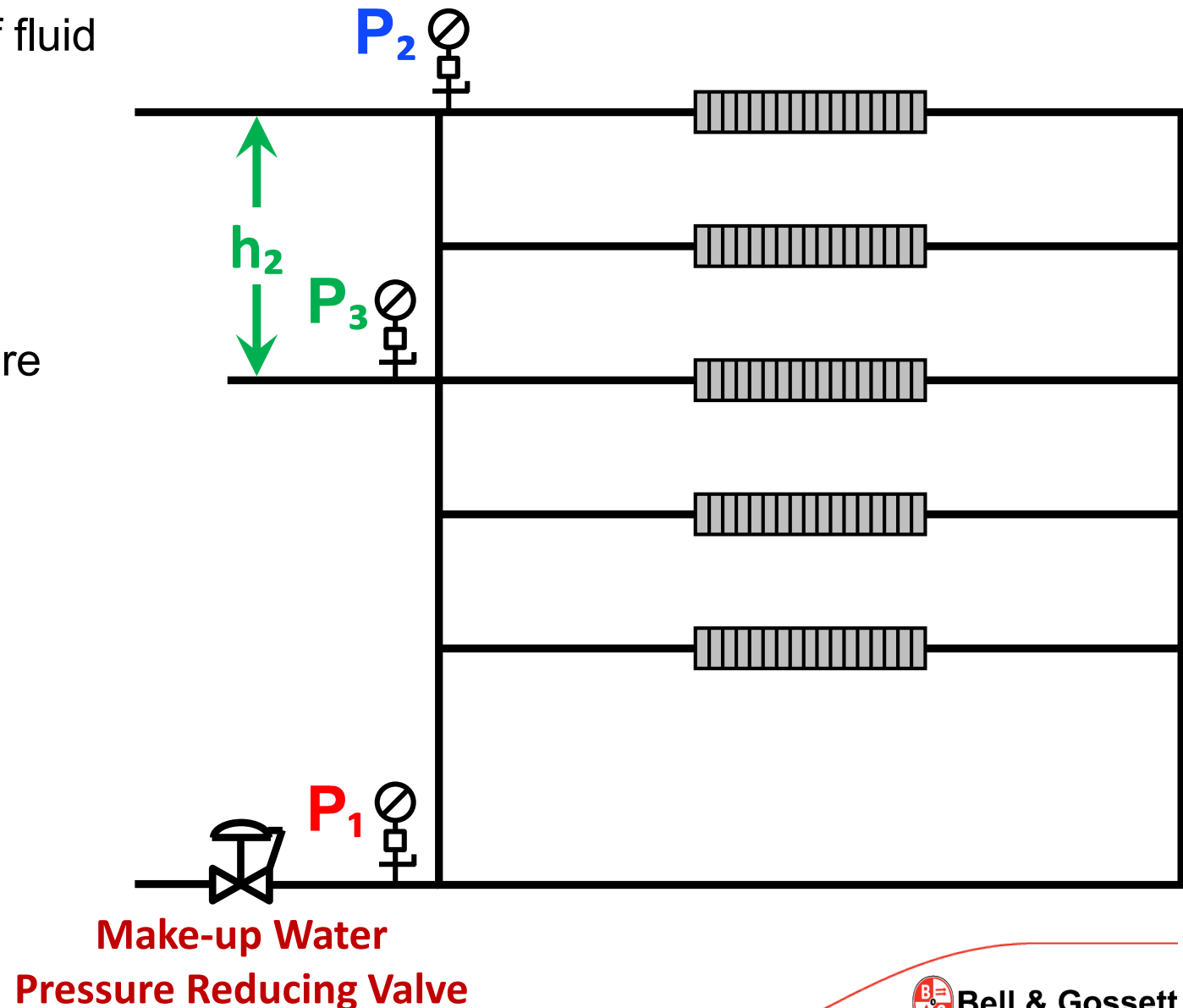
- Pressure caused by weight of a column of fluid
- Influencing Factors
  - Column Height
  - Fluid Type
  - Fluid Density @ Operating Temperature

$$P_1 = P_2 + h_1/(2.31/SG)$$

$$P_3 = P_2 + h_2/(2.31/SG)$$

## NOTES:

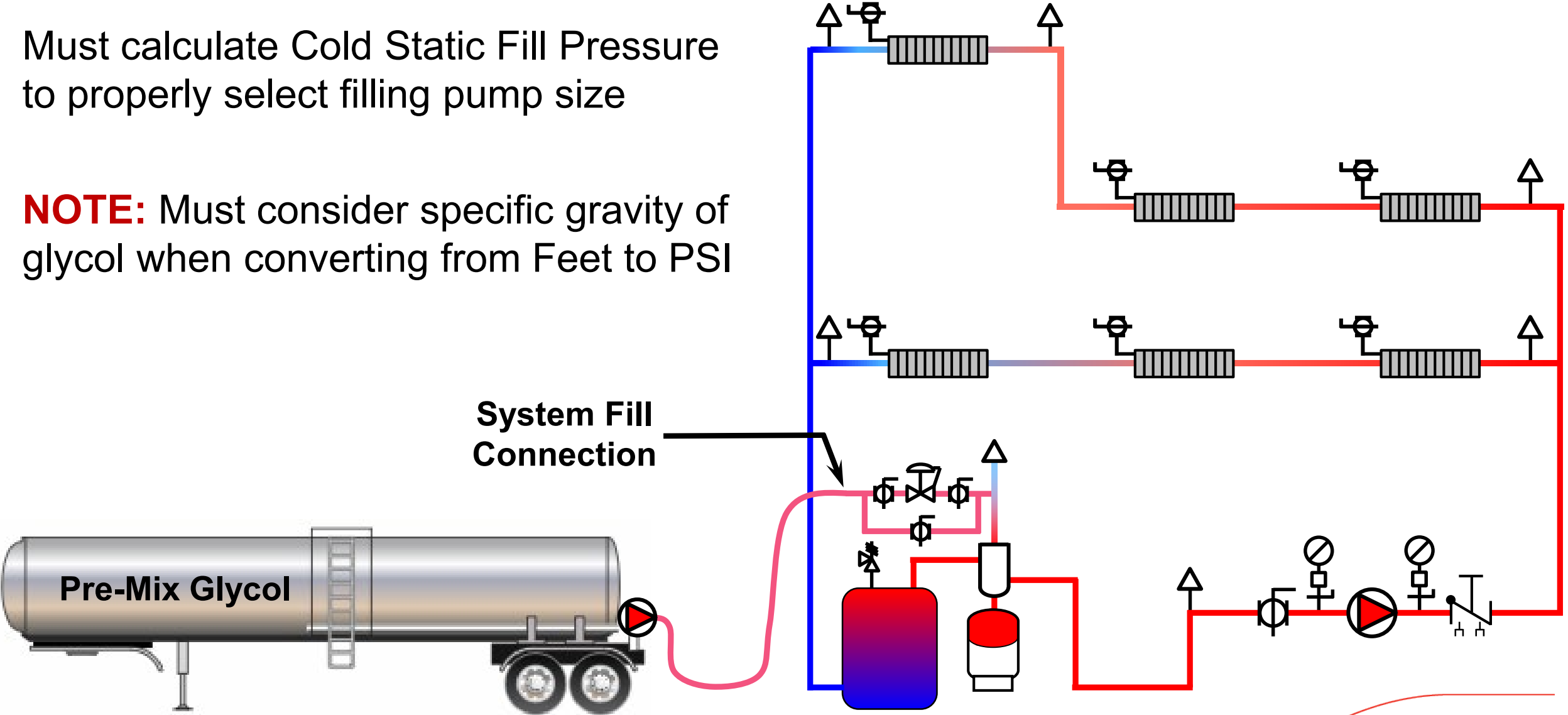
- Specific Gravity of water is 1.0
- $P_2$  should be no less than 4.0 PSI



# System Venting – Pre-Mix Glycol

Must calculate Cold Static Fill Pressure to properly select filling pump size

**NOTE:** Must consider specific gravity of glycol when converting from Feet to PSI



# What's Specific Gravity got to do with it?

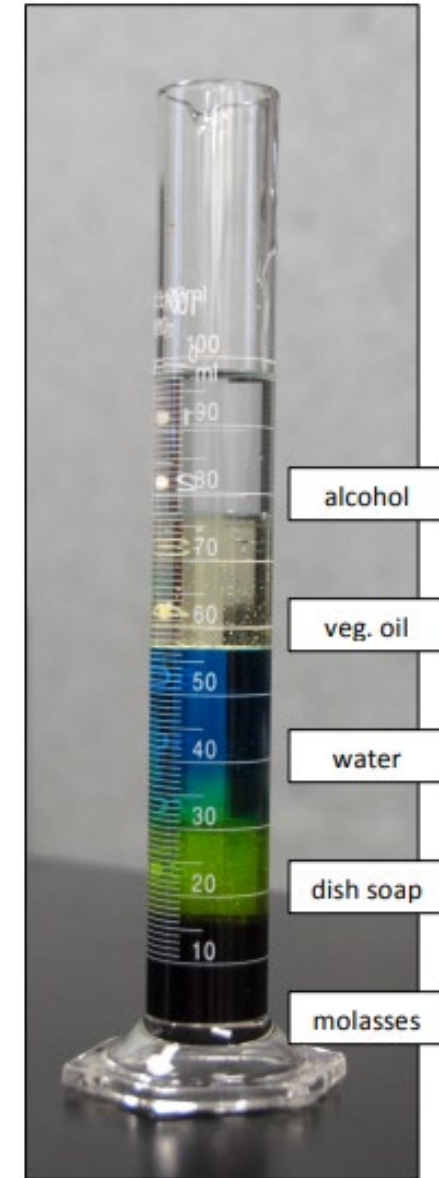
**Density ( $\rho$ ):** How heavy a fluid is for the amount measured (**lbs./ft<sup>3</sup>**)

**Specific Gravity (SG):** Ratio of a fluid density compared to density of water, at a specific temperature and pressure

$$SG = \frac{\rho \text{ of Fluid}}{\rho \text{ of Water}}$$

**Pump Head (ft-~~lb~~/~~lb~~)**

$$\text{Pump Head (ft)} = \text{PSI} \times \frac{2.31}{SG}$$



# Where does the **2.31** come from?

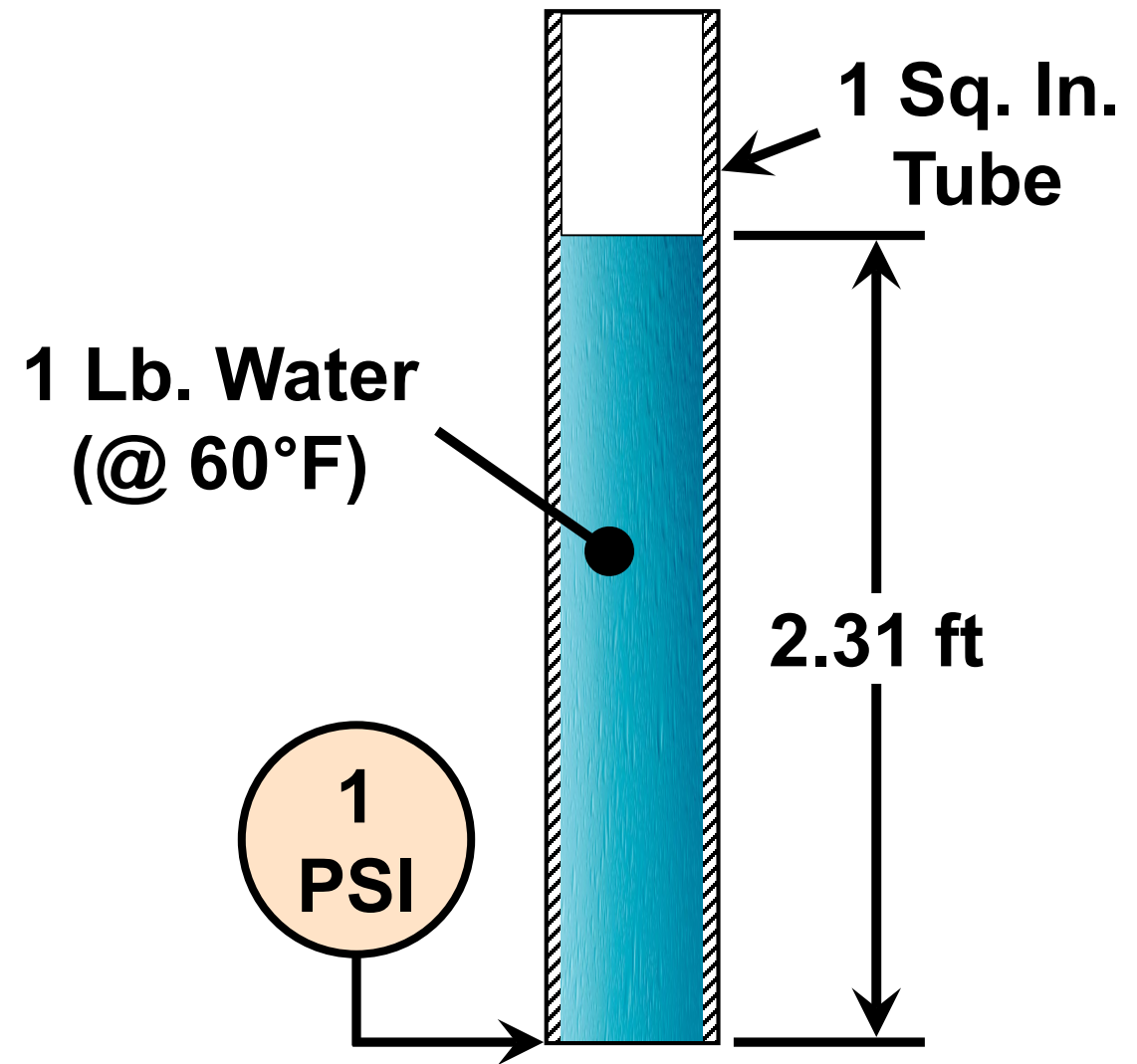
- 1 Cu. Ft. of **water** (@ 60°F) weighs 62.4 lbs
- 1 Sq. Ft. of area has 144 Sq. In.

$$\frac{144}{62.4} = 2.31 \text{ (ft/PSI)}$$

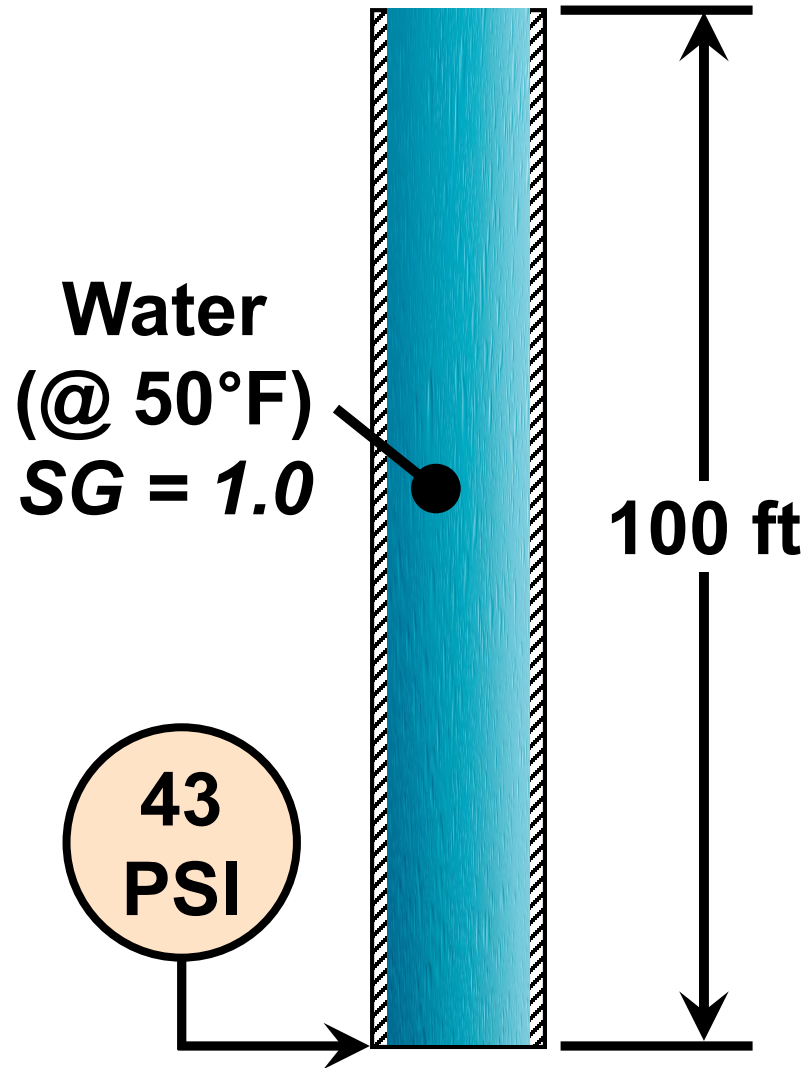
$$\frac{62.4}{144} = .433 \text{ (PSI/ft)}$$

## Example:

- 1 ft water column = 0.433 PSI
- 2 ft water column = 0.866 PSI
- 3 ft water column = 1.299 PSI



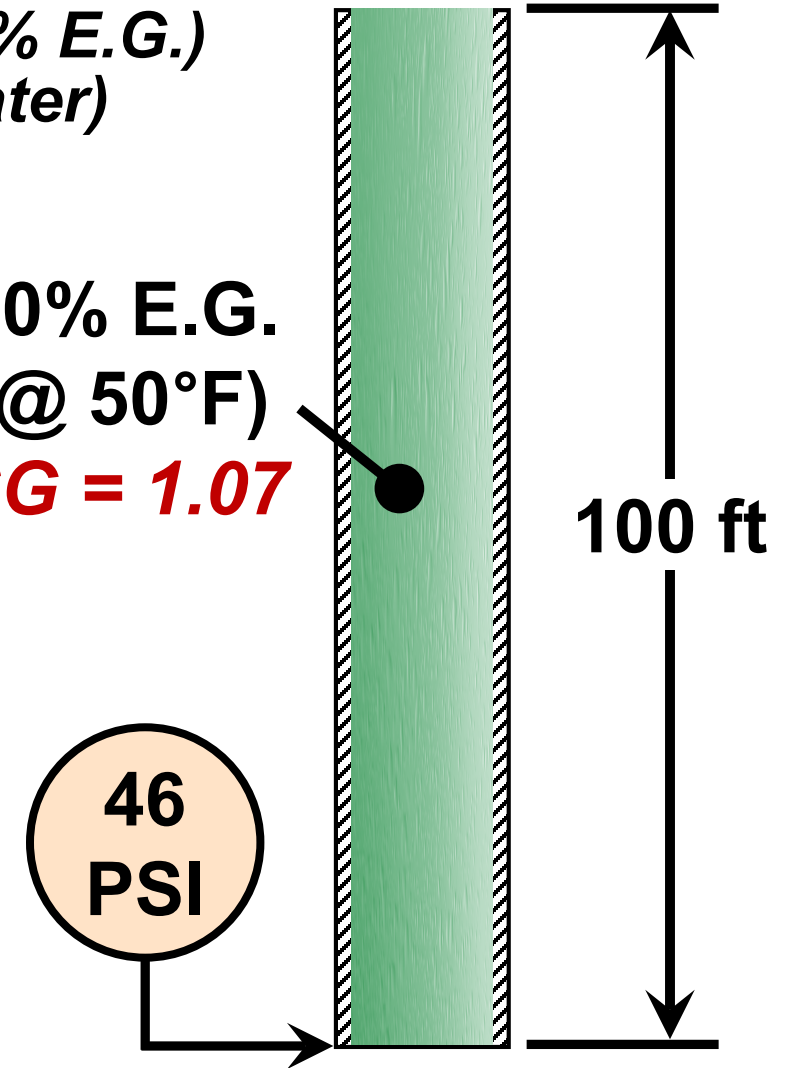
# Another look at Static Pressure using Specific Gravity of a Fluid



$$SG = \frac{66.47 \text{ } (\rho \text{ of } 40\% \text{ E.G.})}{62.41 \text{ } (\rho \text{ of Water})}$$

$$SG = 1.065 \approx 1.07$$

40% E.G.  
(@ 50°F)  
SG = 1.07

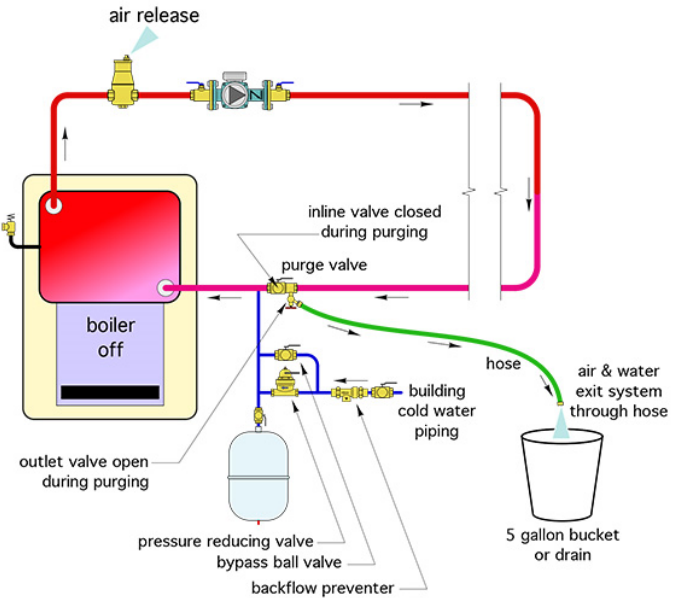


$$PSI = \frac{100 \text{ ft}}{2.31/1.07}$$

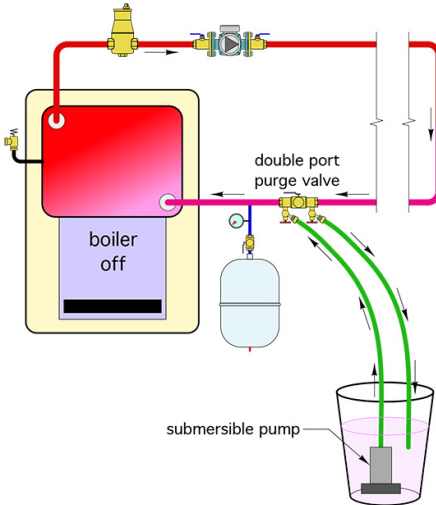
$$PSI = 46.1 \approx 46$$

# System Purging: High Velocity Circulation

**Municipal Pressure**



**Pump Pressure**



**From  
“Cloudy”**



**To  
“Clear”**



## Air Separation Equipment

Capturing the Entrained and Dissolved Air

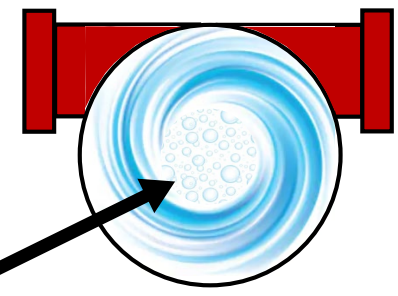
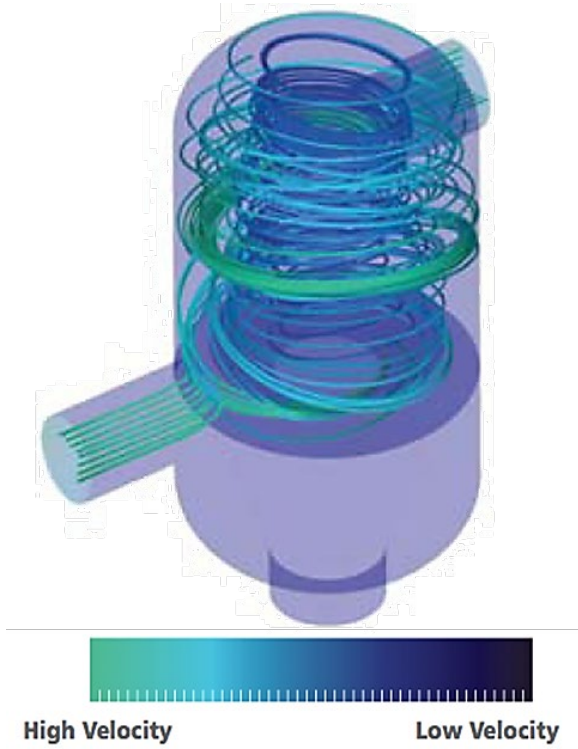
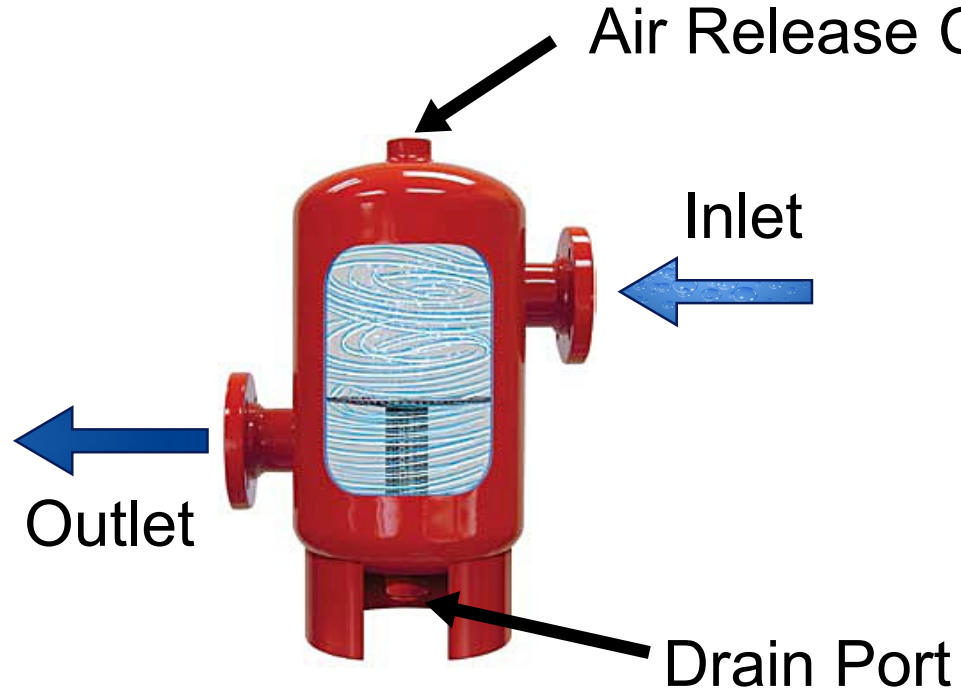


# Air Management in a Closed Loop Hydronic System

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  - Centrifugal Action
  - Coalescence



# Tangential Air Separator – Centrifugal Action

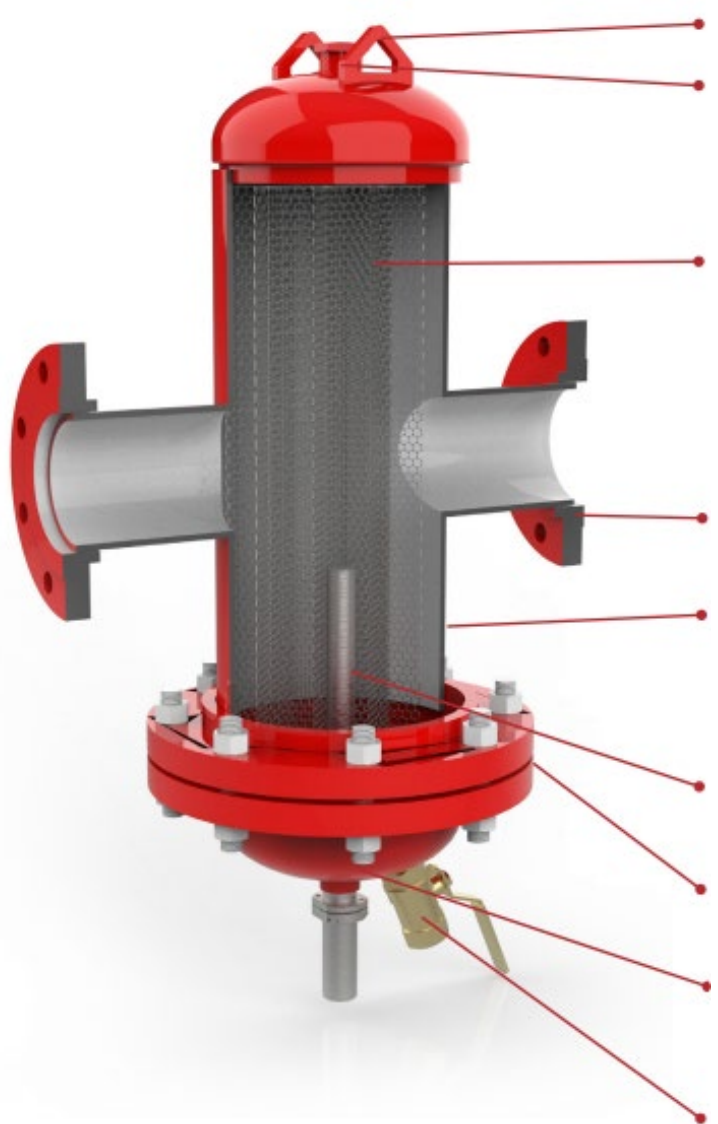


Released Air  
(Lower Fluid Velocity)

**Plan View**

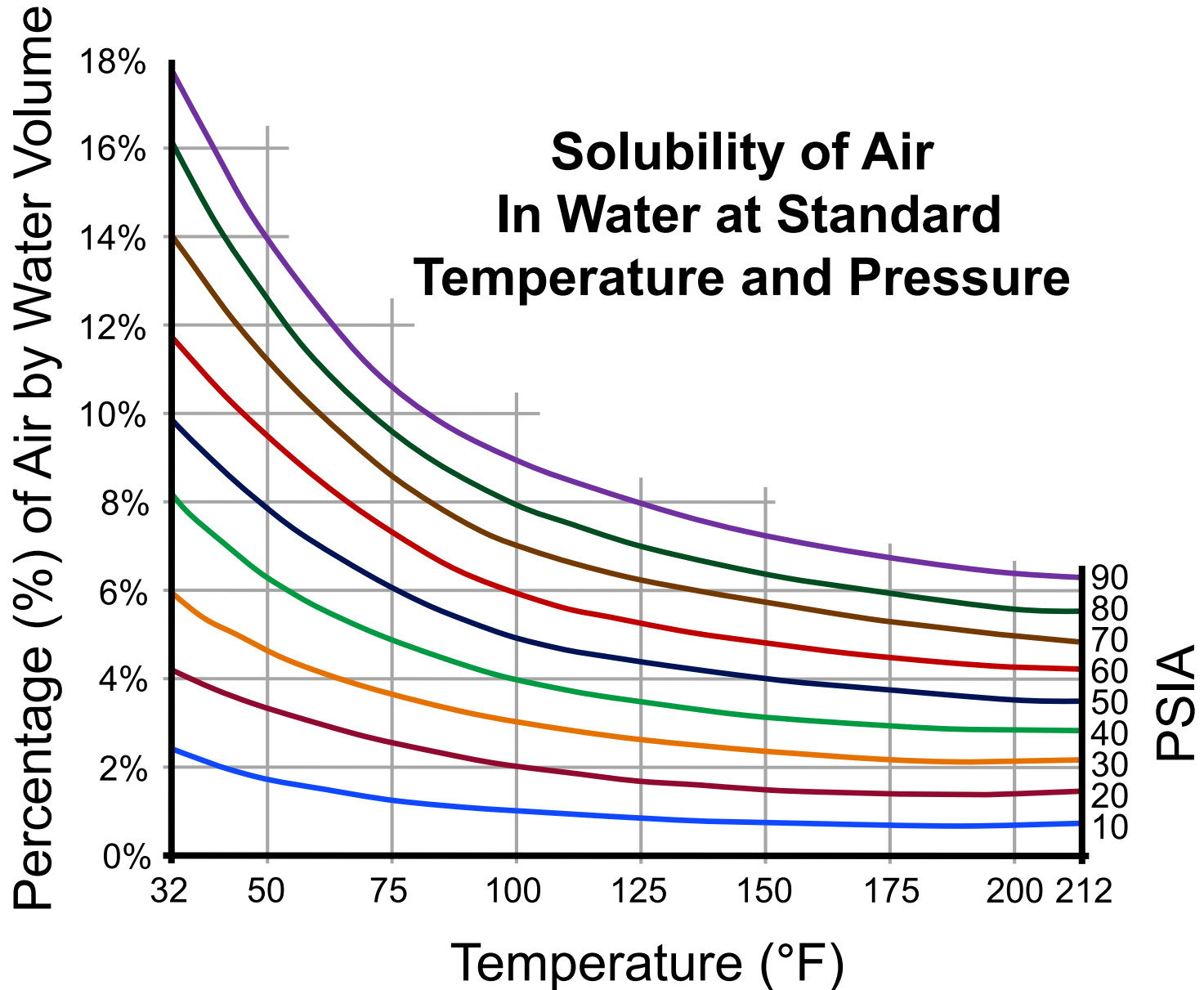
Designed, built, inspected and stamped per  
Section VIII, Div. 1 of ASME Code

# Coalescing Style Air & Sediment Removal Separator

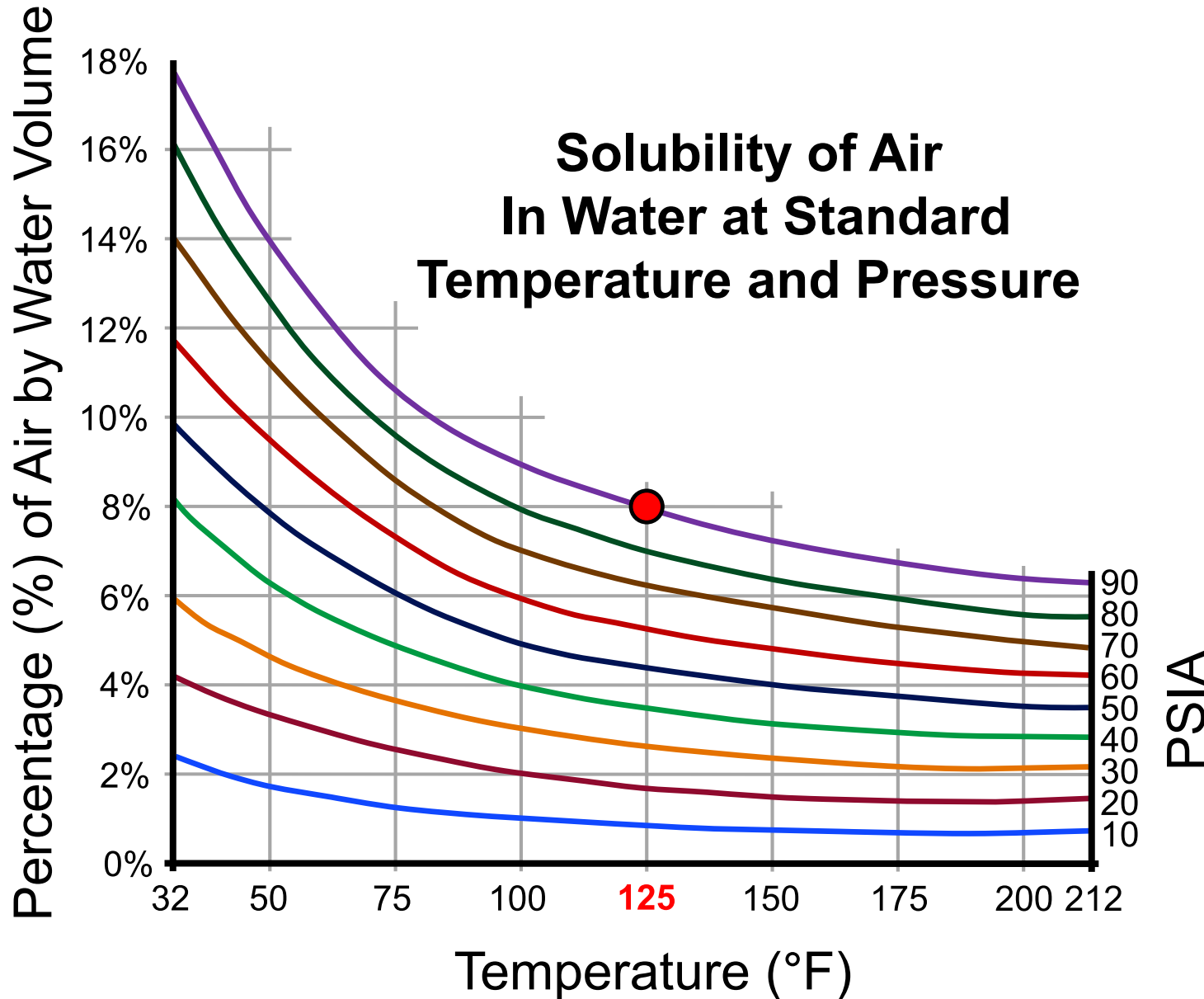


- Lifting Lug
- Threaded Air Release Connection
- Stainless Steel Coalescing Media
- NPT (2"-4"), Flanged and Grooved
- Body 2x larger than Inlet/Outlet Size
- "Optional"** Magnet insert for ferrous sediment
- Removable Head (*Non-Removable available*)
- Dirt collection area
- Threaded Blowdown Connection

# Dissolved Air: The influence of Temperature and Pressure



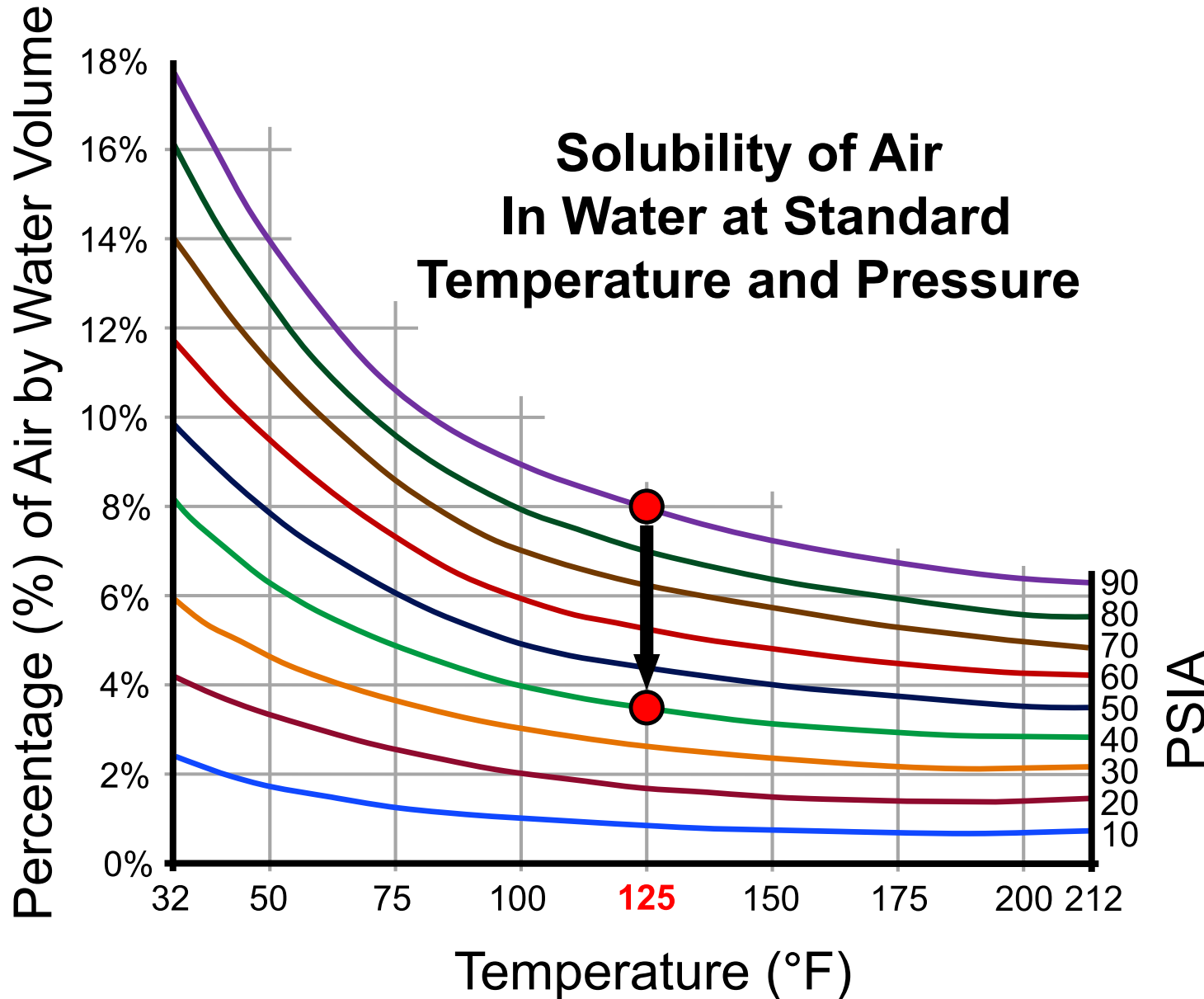
# Dissolved Air: The influence of Temperature and Pressure



## “Hold” Temperature, Lower Pressure

- 125°F water @ 90 PSIA has 8.0% Air

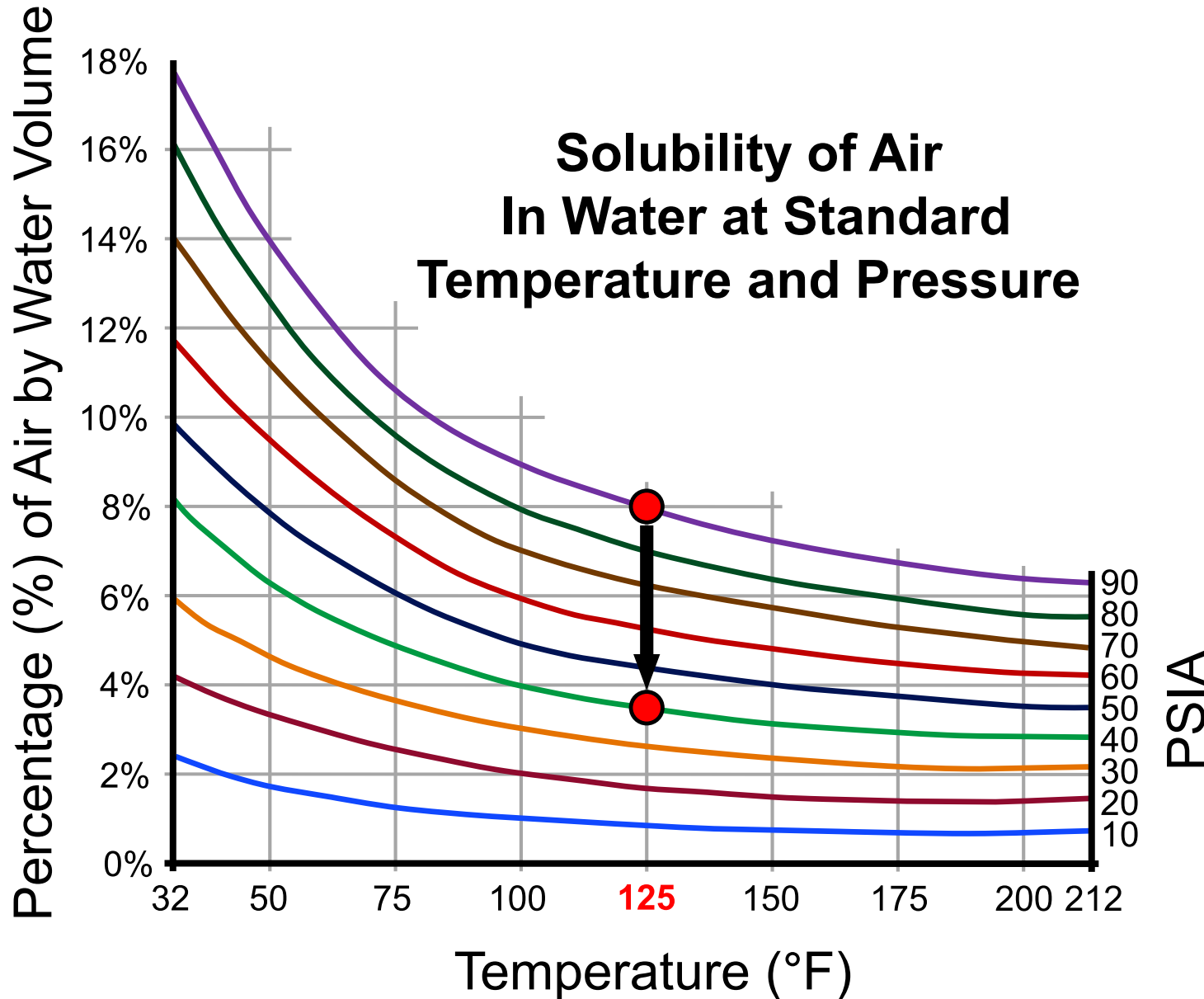
# Dissolved Air: The influence of Temperature and Pressure



## “Hold” Temperature, Lower Pressure

- 125°F water @ 90 PSIA has 8.0% Air
- 125°F water @ 40 PSIA has 3.5% Air

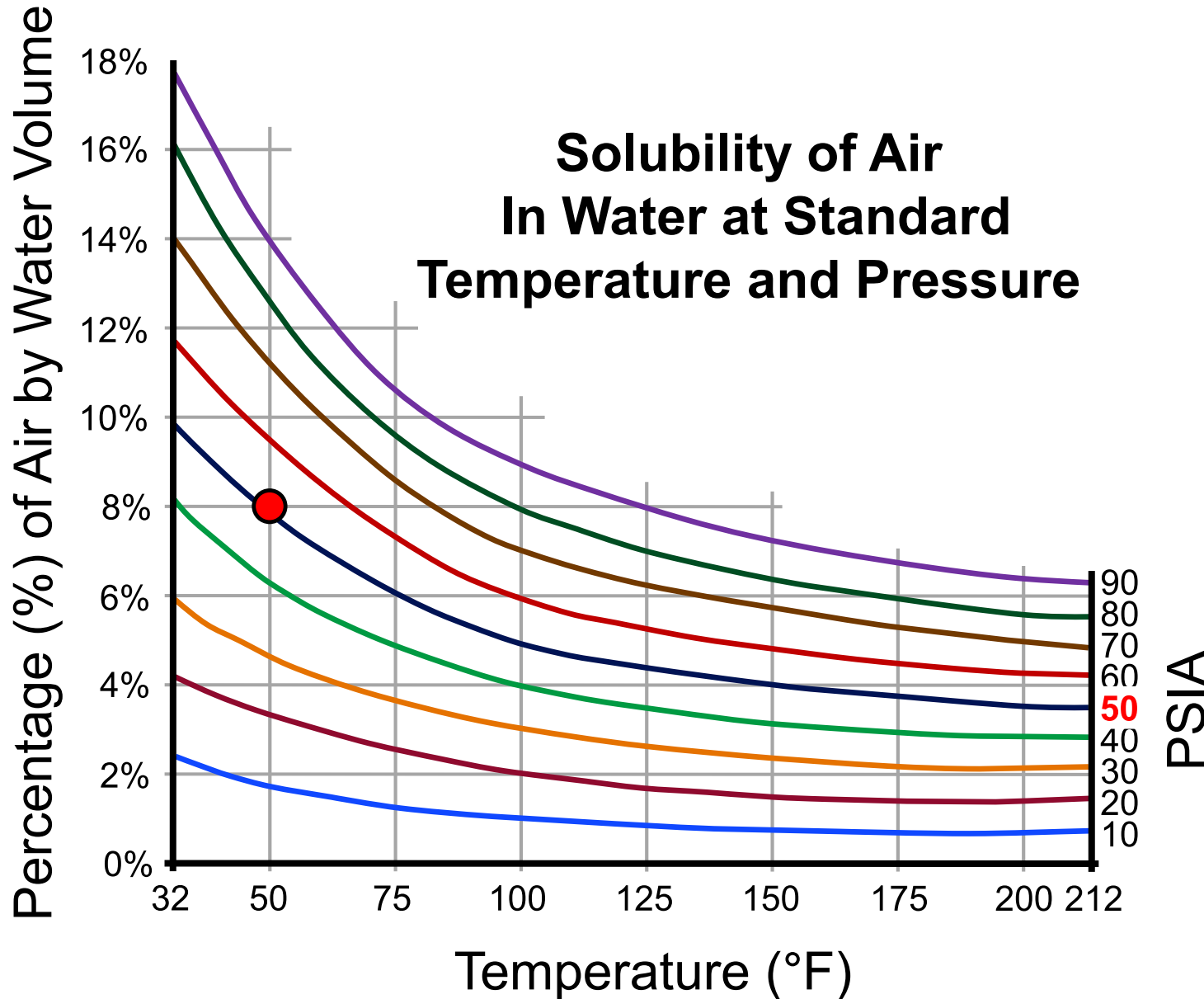
# Dissolved Air: The influence of Temperature and Pressure



**“Hold” Temperature, Lower Pressure**

- 125°F water @ 90 PSIA has 8.0% Air
- 125°F water @ 40 PSIA has 3.5% Air
- **Example:** 1,000 Gallons @ 125°F  
 $1,000 \times (.08 - .035) = 45 \text{ Gal. Released Air}$

# Dissolved Air: The influence of Temperature and Pressure

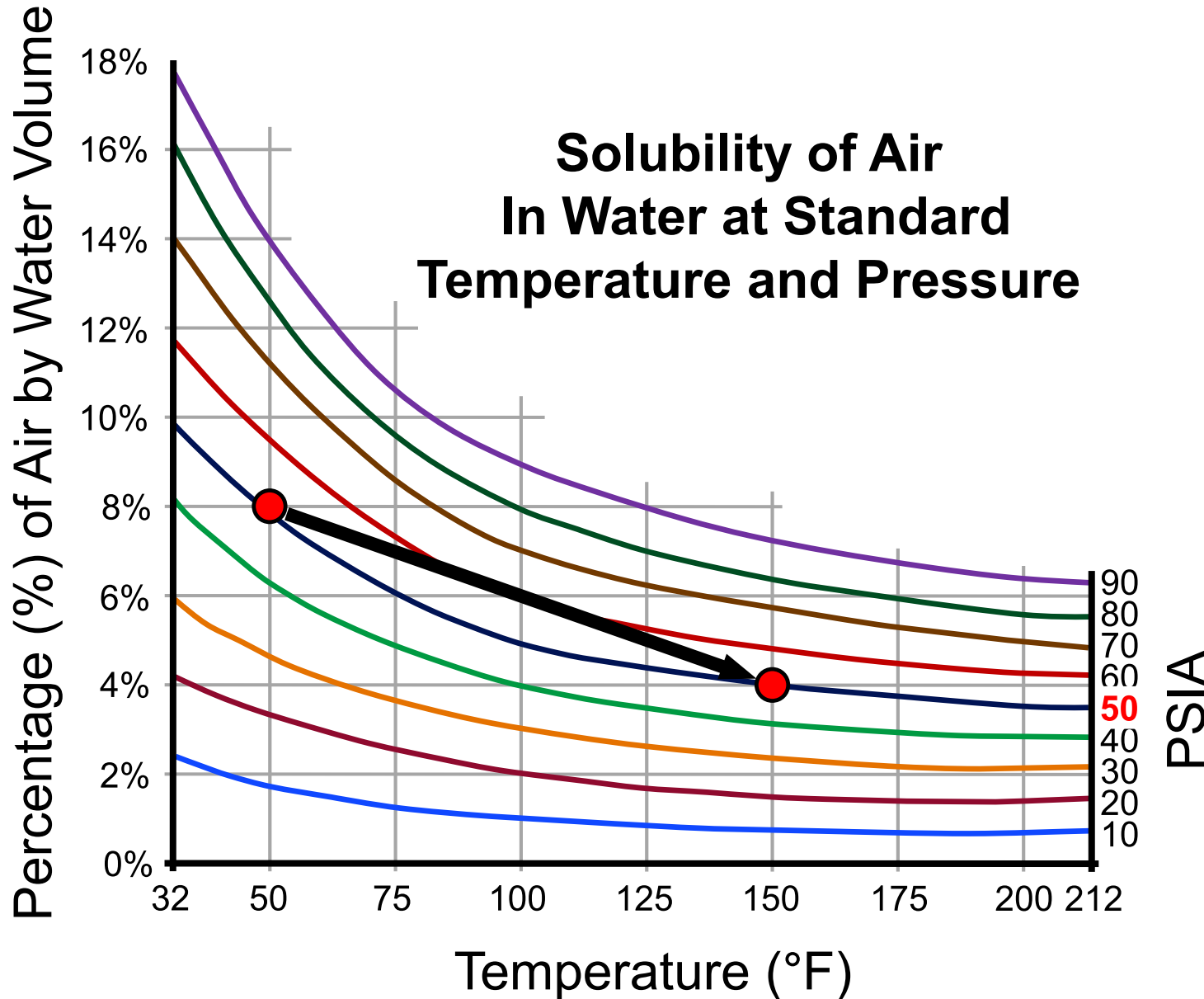


## “Hold” Pressure, Raise Temperature

- 50°F water @ 50 PSIA has 8.0% Air



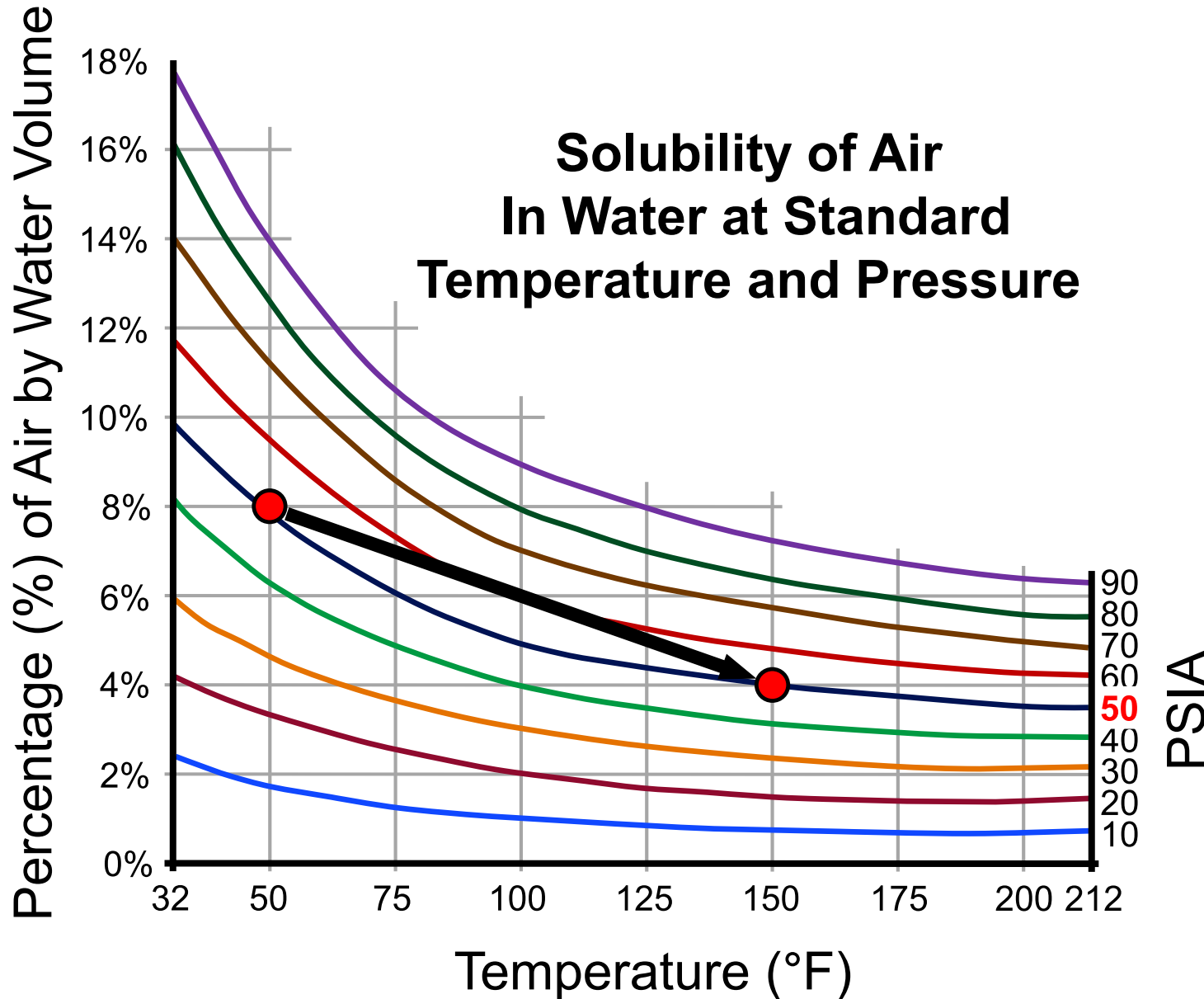
# Dissolved Air: The influence of Temperature and Pressure



### “Hold” Pressure, Raise Temperature

- 50°F water @ 50 PSIA has 8.0% Air
- 150°F water @ 50 PSIA has 4.0% Air

# Dissolved Air: The influence of Temperature and Pressure

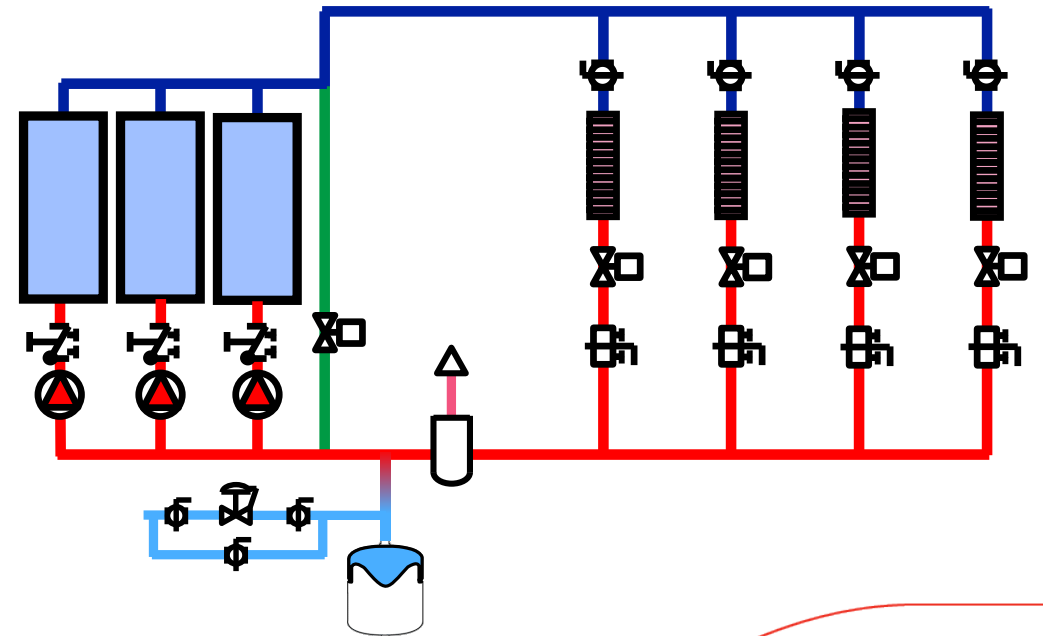
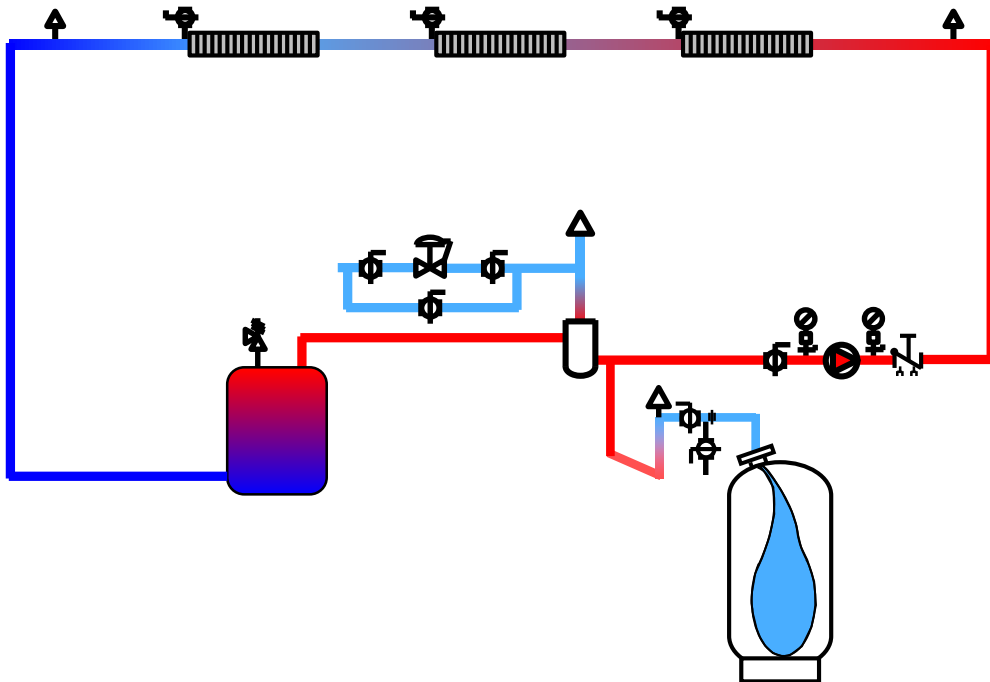


**“Hold” Pressure, Raise Temperature**

- 50°F water @ 50 PSIA has 8.0% Air
  - 150°F water @ 50 PSIA has 4.0% Air
  - **Example:** 1,000 Gallons from 50°F to 150°F
- 1,000 x (.08 - .04) = 40 Gal. **Released Air**

# Air Separation Equipment: Location for Optimal Performance

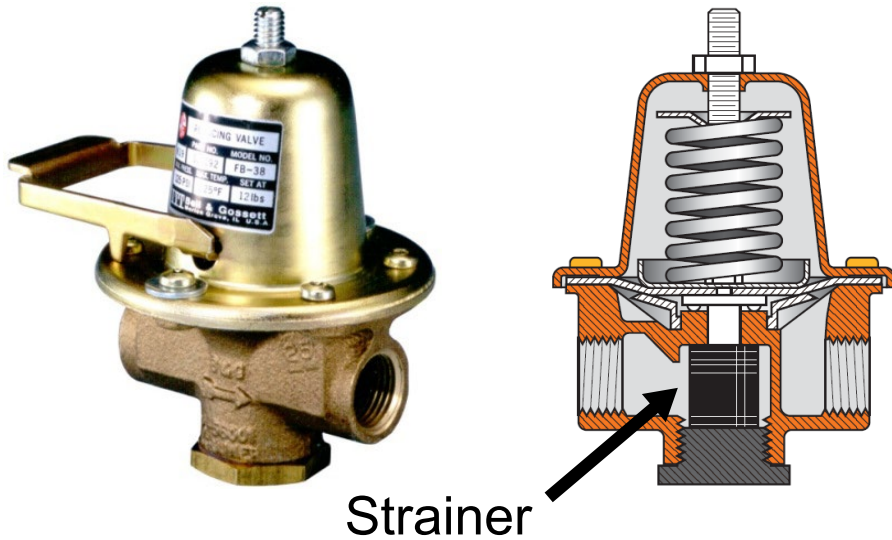
- Recommended Location
  - Where system fluid is warmest
  - Where system pressure is lowest



# Pressurization Equipment

# Pressure Limit Components – Make-up Fluid

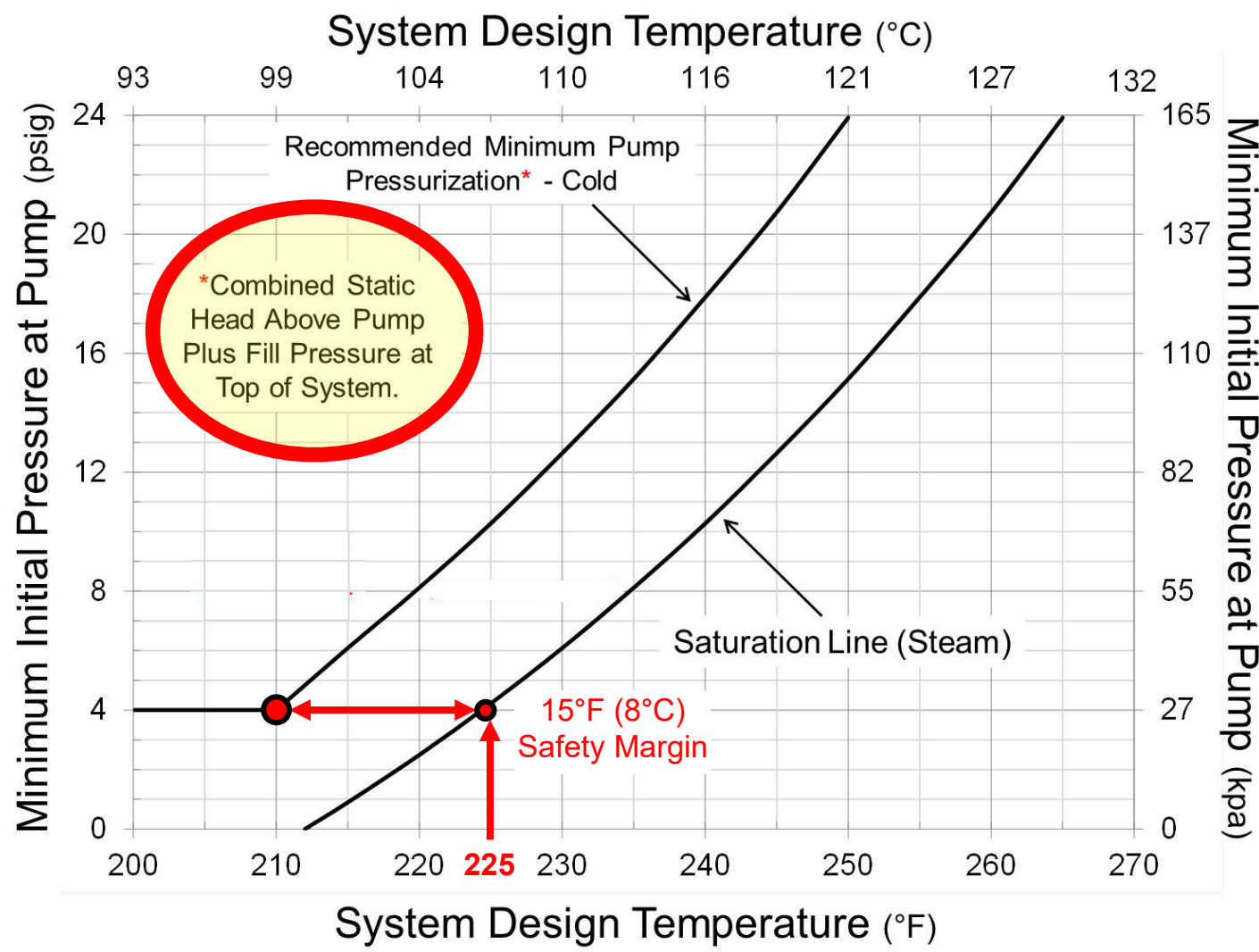
## Water Systems



## Glycol Systems



# Minimum Cold Pressurization at the Pump. Pump Location??



Small/Medium Wet Rotor

Oil Lubricated

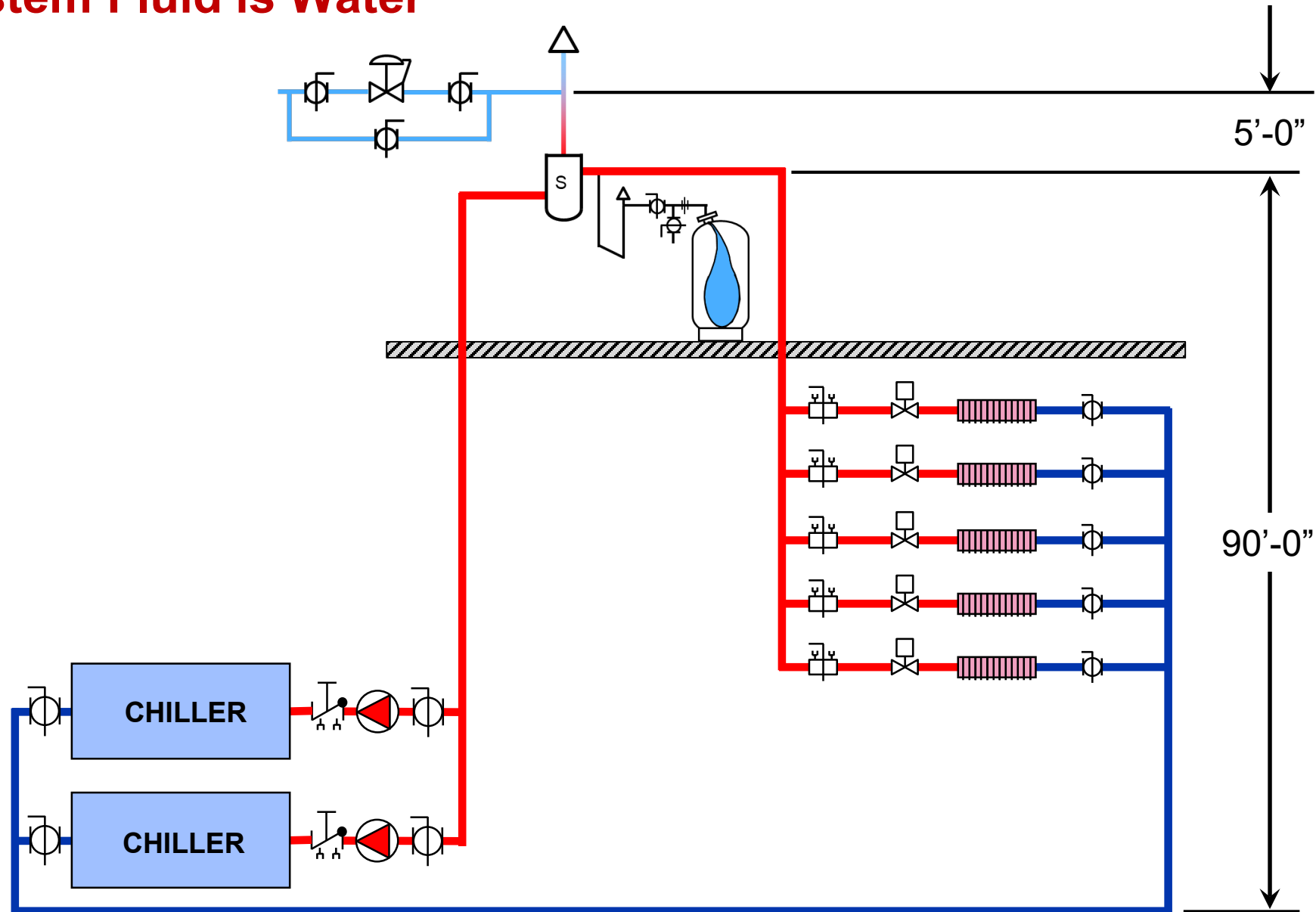


Grease Lubricated

**\* Check Pump's Net Positive Suction Head Requirement (NPSHR)**

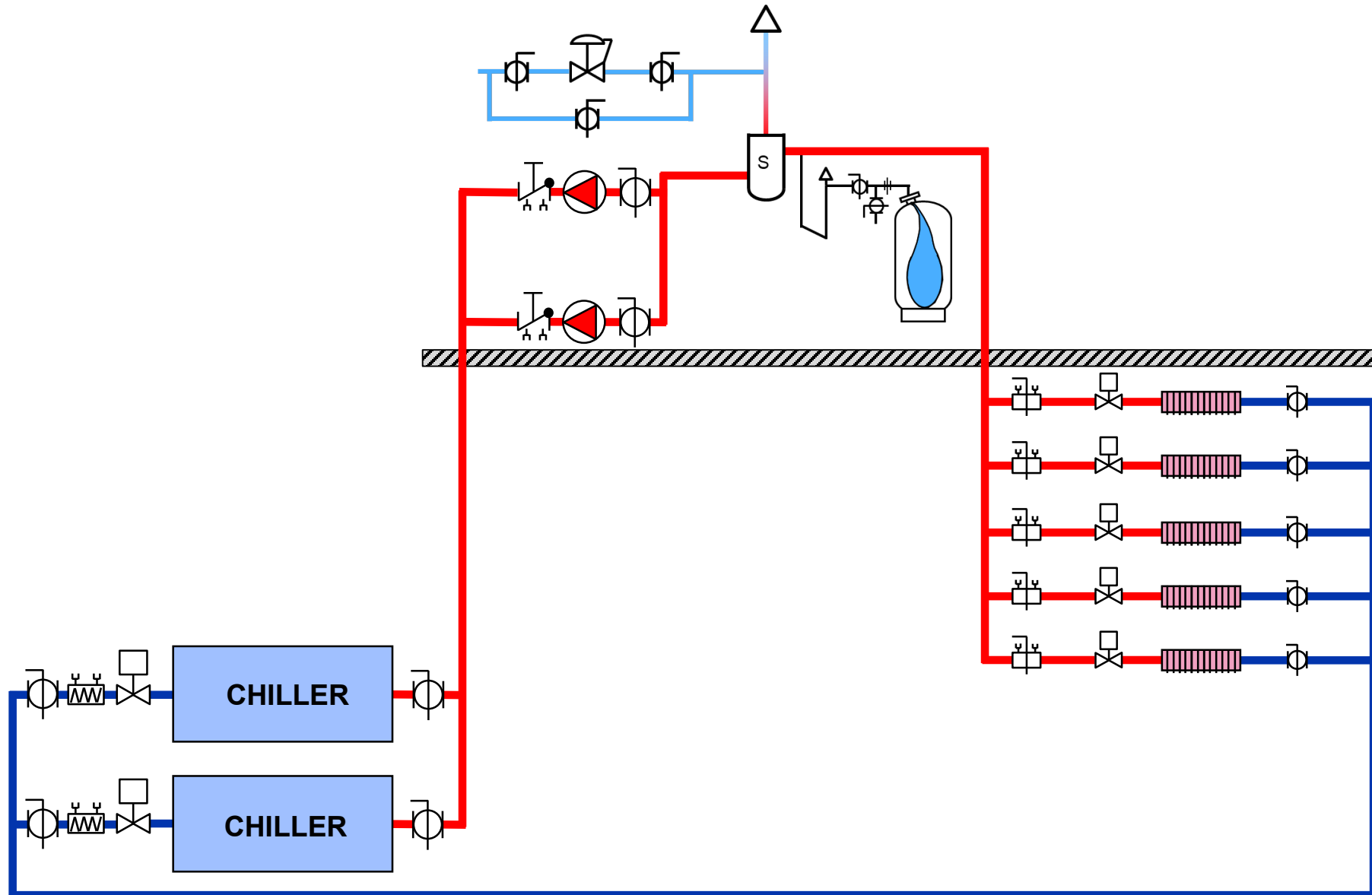
# What's the Cold Static Fill Pressure PRV Setpoint?

**\* System Fluid is Water**



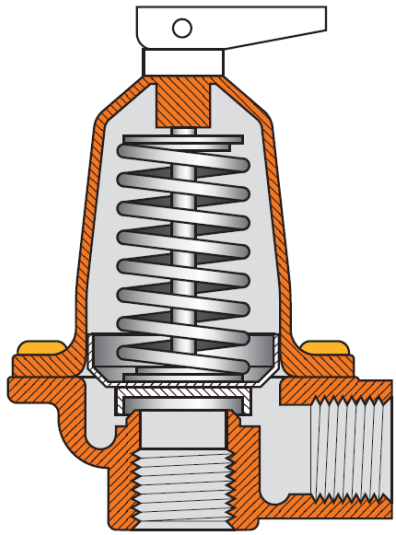
# What's the Cold Static Fill Pressure PRV Setpoint?

**\* What's the required pump NPSH?**





# Pressure Limit Components: ASME Safety Relief Valve



#790 & 1170

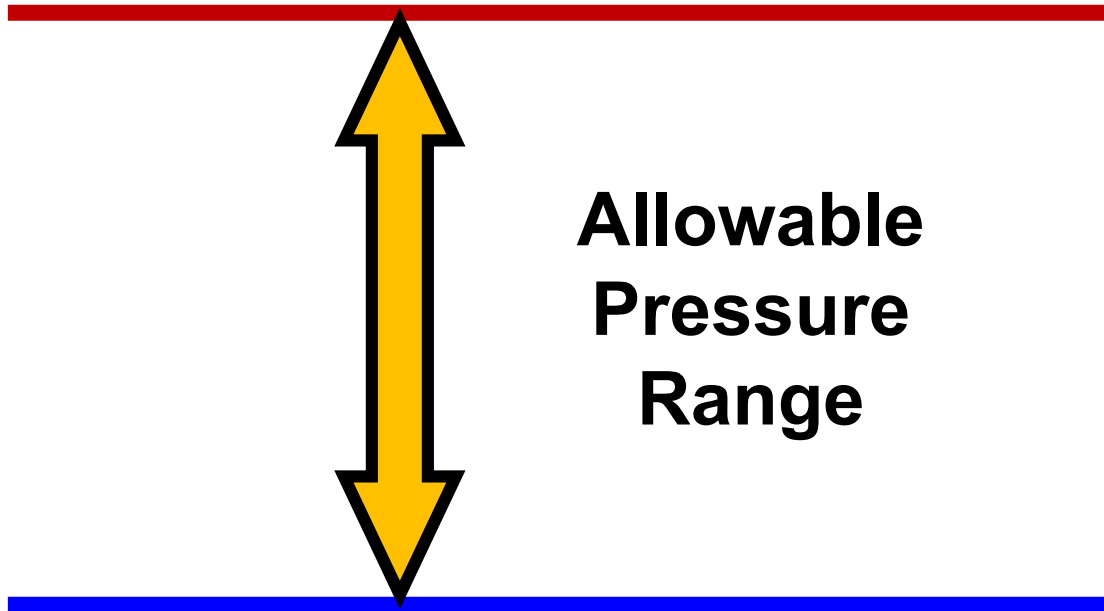


#3301 & 4100

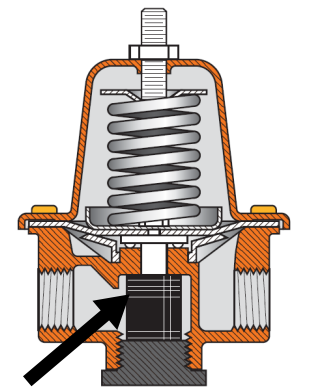
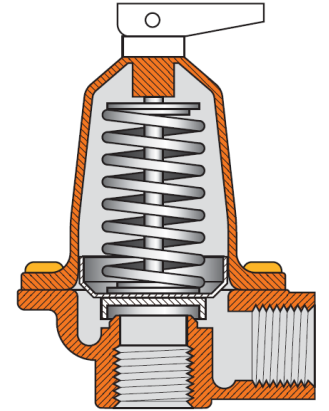
Size, Capacity & Relief Setting for B&G ASME Safety Relief Valves <sup>1</sup>				
Relief Setting PSIG	Model Number Capacity in BTU Per Hour			
	Iron Body		Bronze Body	
30	3301-30	4100-30	790-30	1170-30
	3,300,000	4,100,000	790,000	1,170,000
36	3301-36	4100-36	790-36	1170-36
	3,800,000	4,600,000	900,000	1,330,000
45	3301-45	4100-45	790-45	1170-45
	4,500,000	5,515,000	1,065,000	1,575,000
50	3301-50	4100-50	790-50	1170-50
	4,900,000	5,990,000	1,160,000	1,710,000
75	NOT AVAILABLE		790-75	1170-75
			1,615,000	2,385,000
100	NOT AVAILABLE		790-100	1170-100
			2,075,000	3,060,000
125	NOT AVAILABLE		790-125	1170-125
			2,535,000	3,735,000

# Pressure Limit Components - The “Allowable Pressure Range”

- Upper pressure limit,  $P_2$
- *Safety Relief Valve* setting



- Lower pressure limit,  $P_1$
- *Pressure Reducing Valve* setting

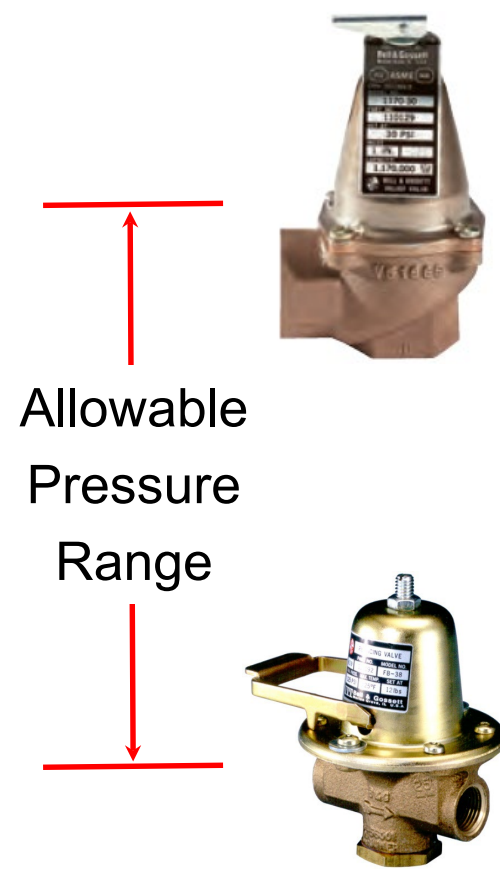
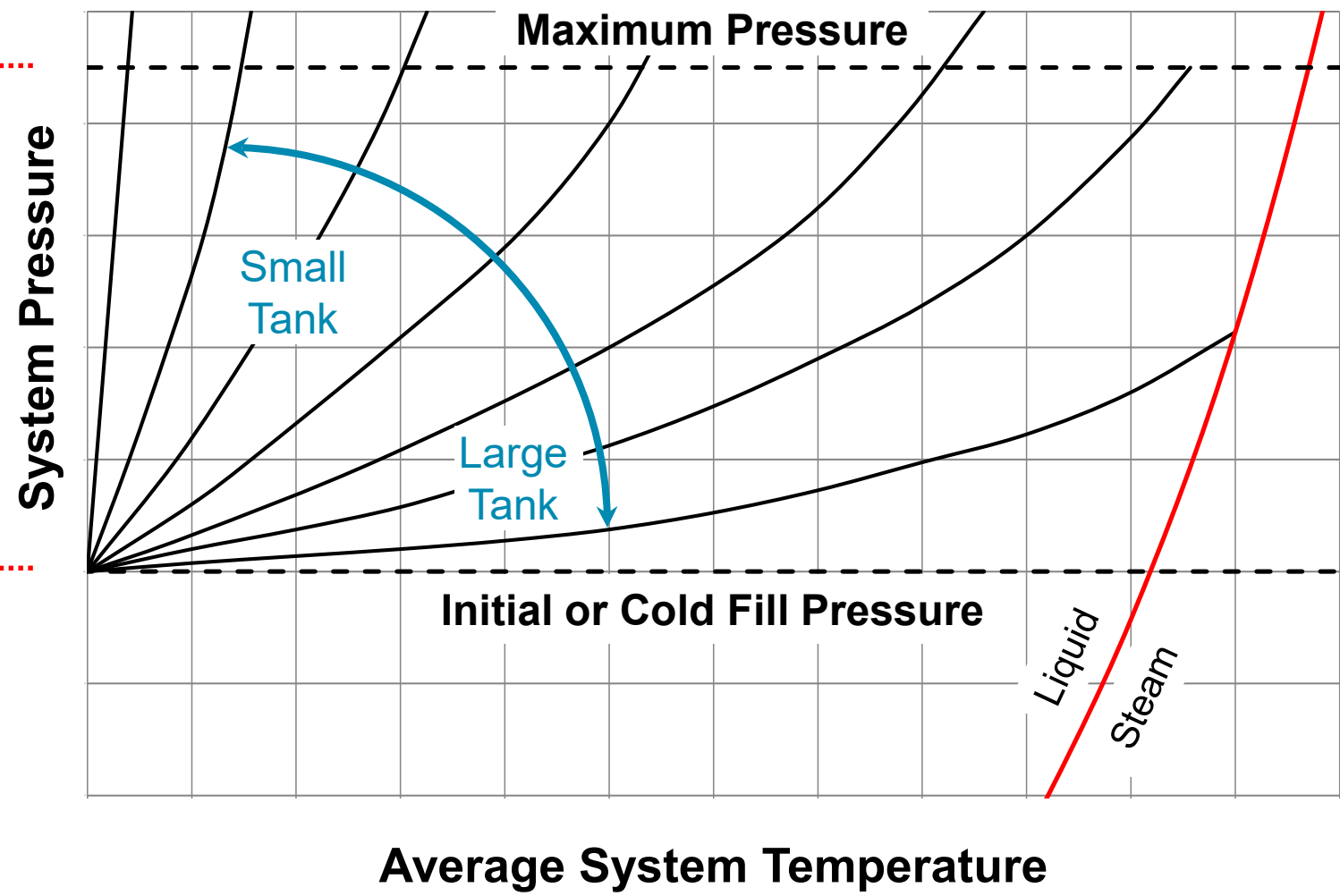


Strainer

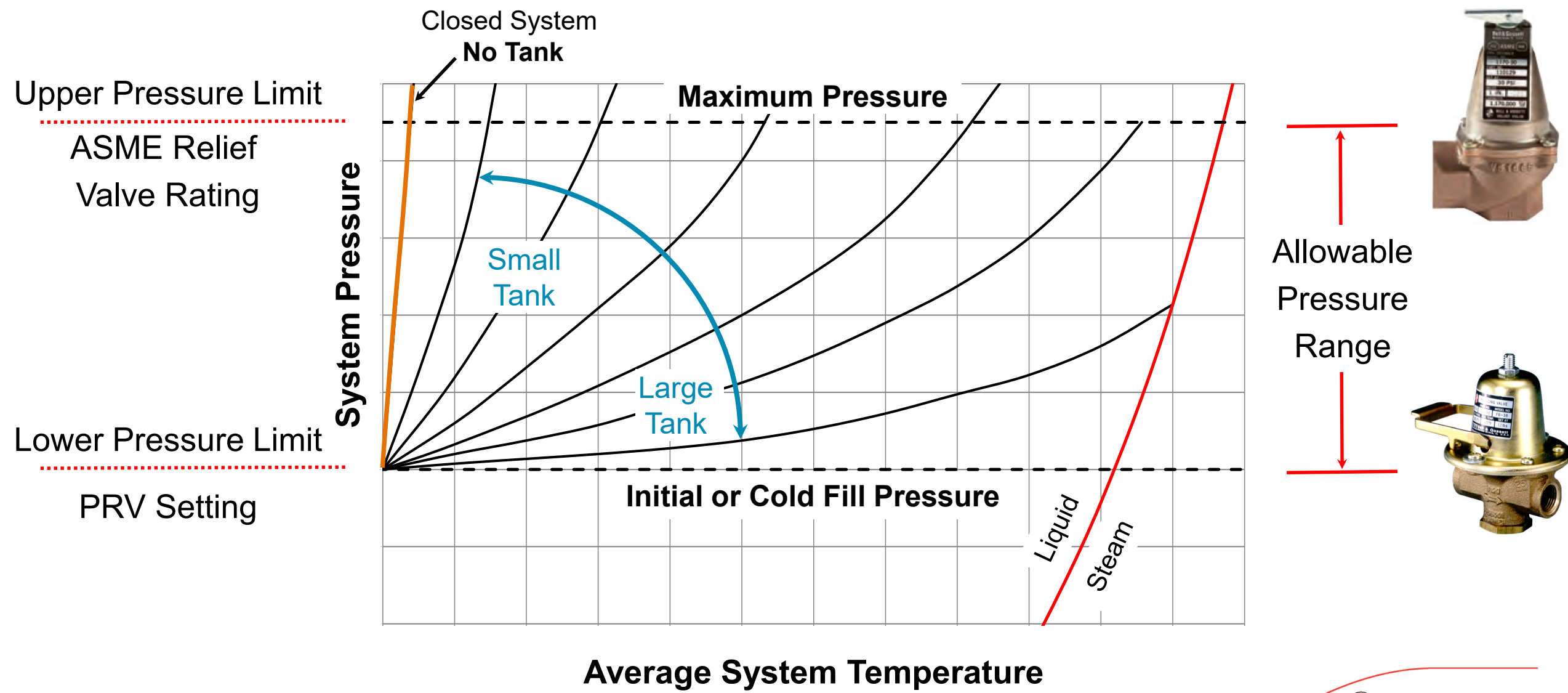
# The "Pressure Range" influence on Air Management Tank sizing

Upper Pressure Limit  
-----  
ASME Relief Valve Rating

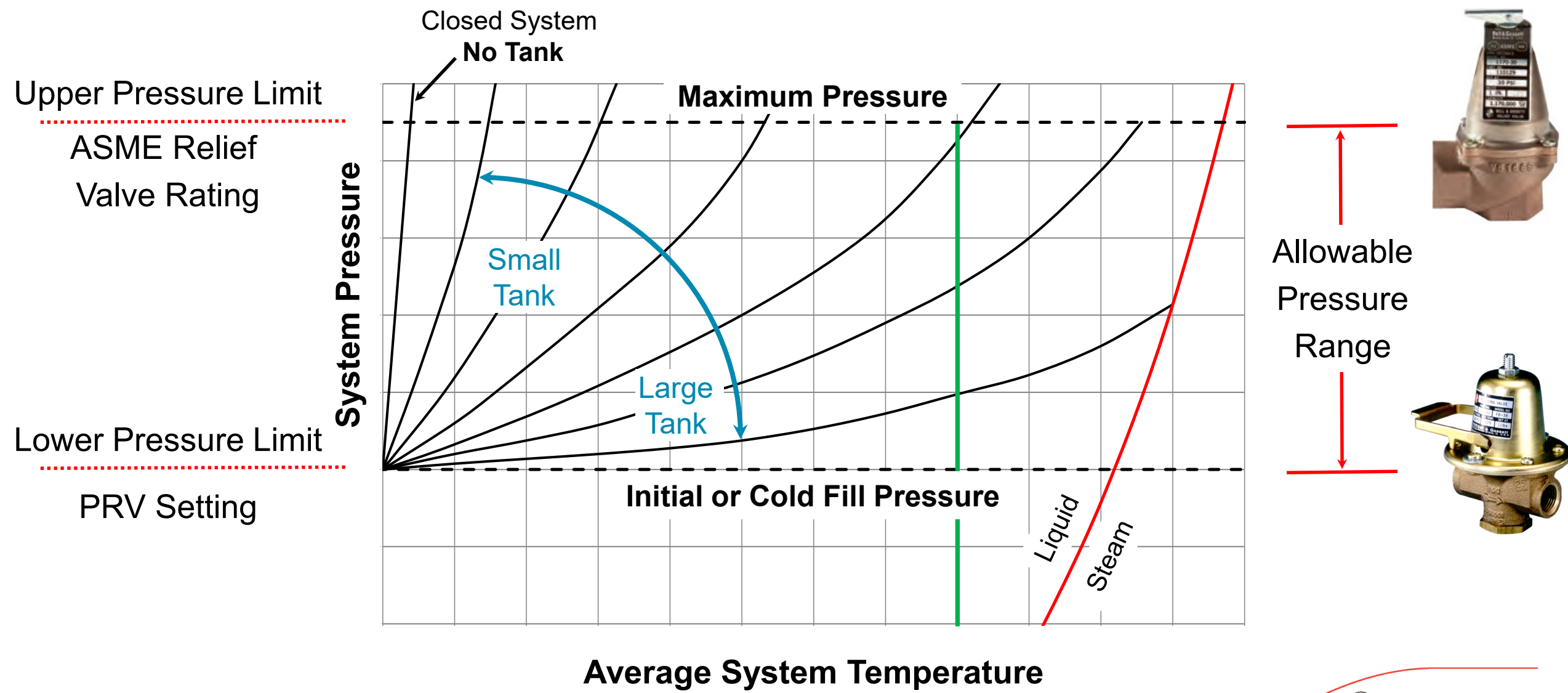
Lower Pressure Limit  
-----  
PRV Setting



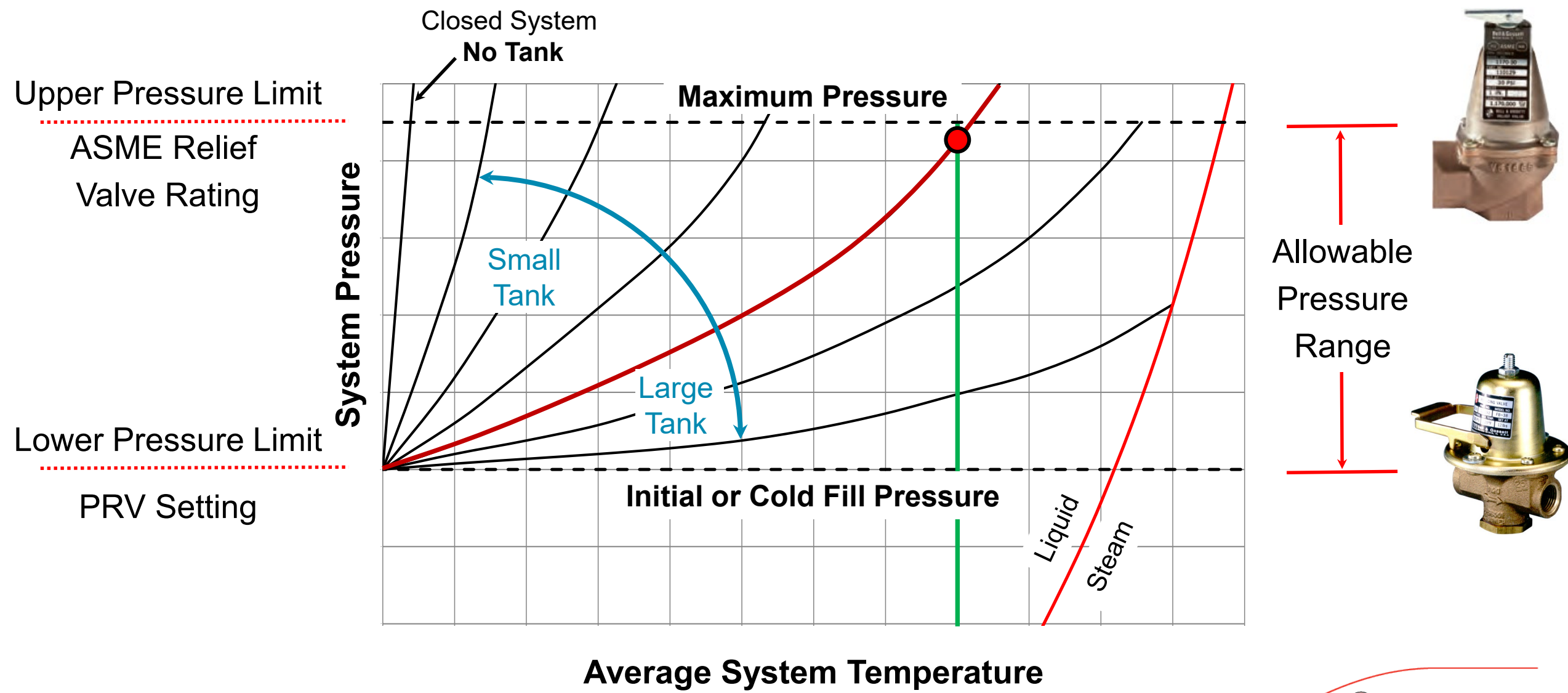
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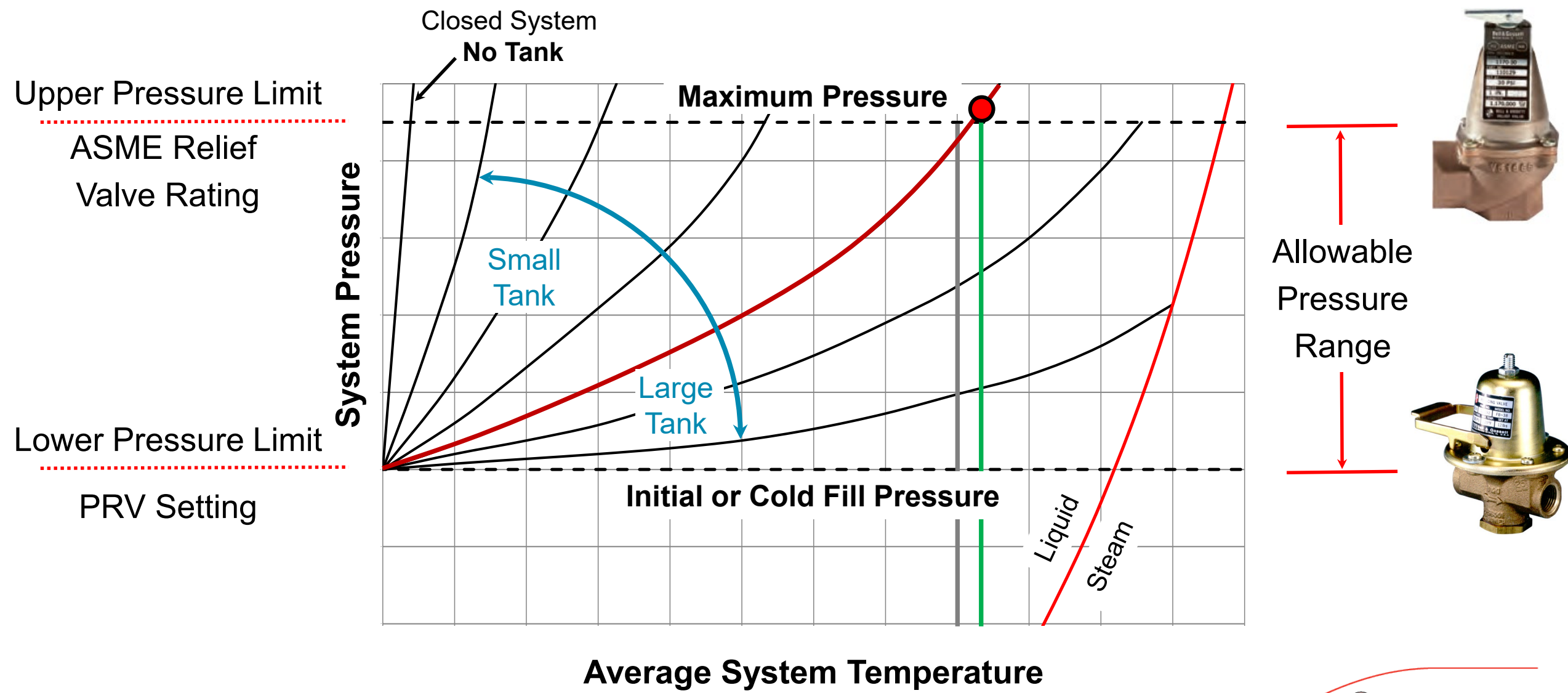
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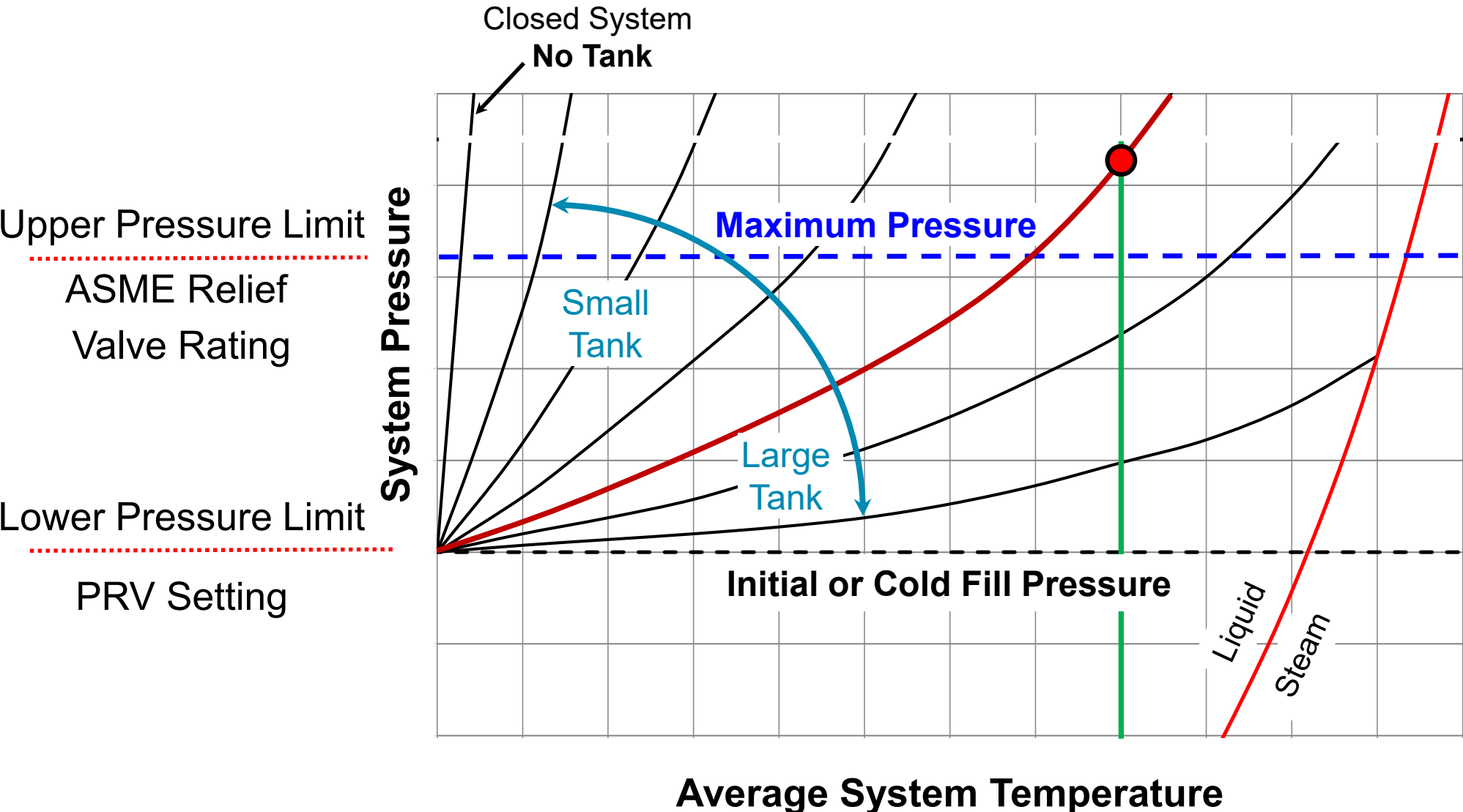
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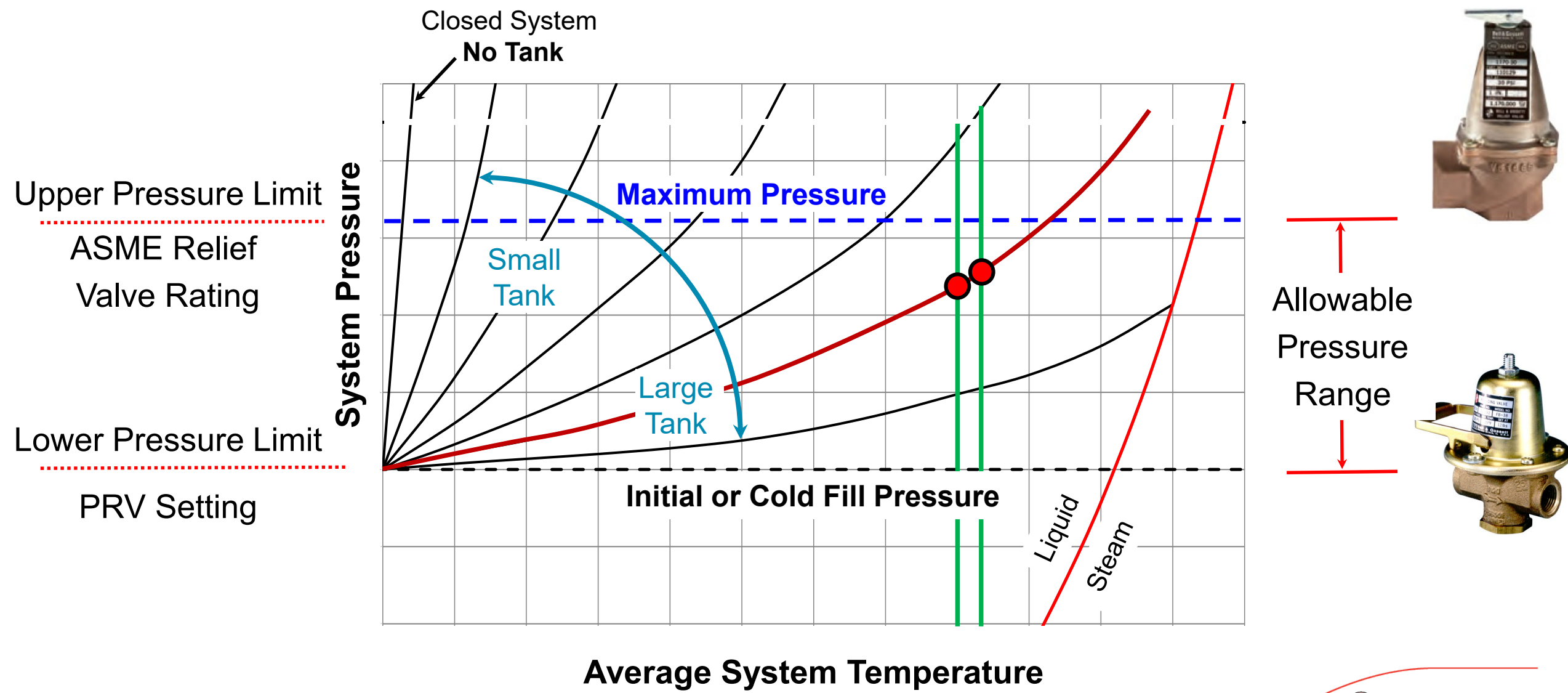
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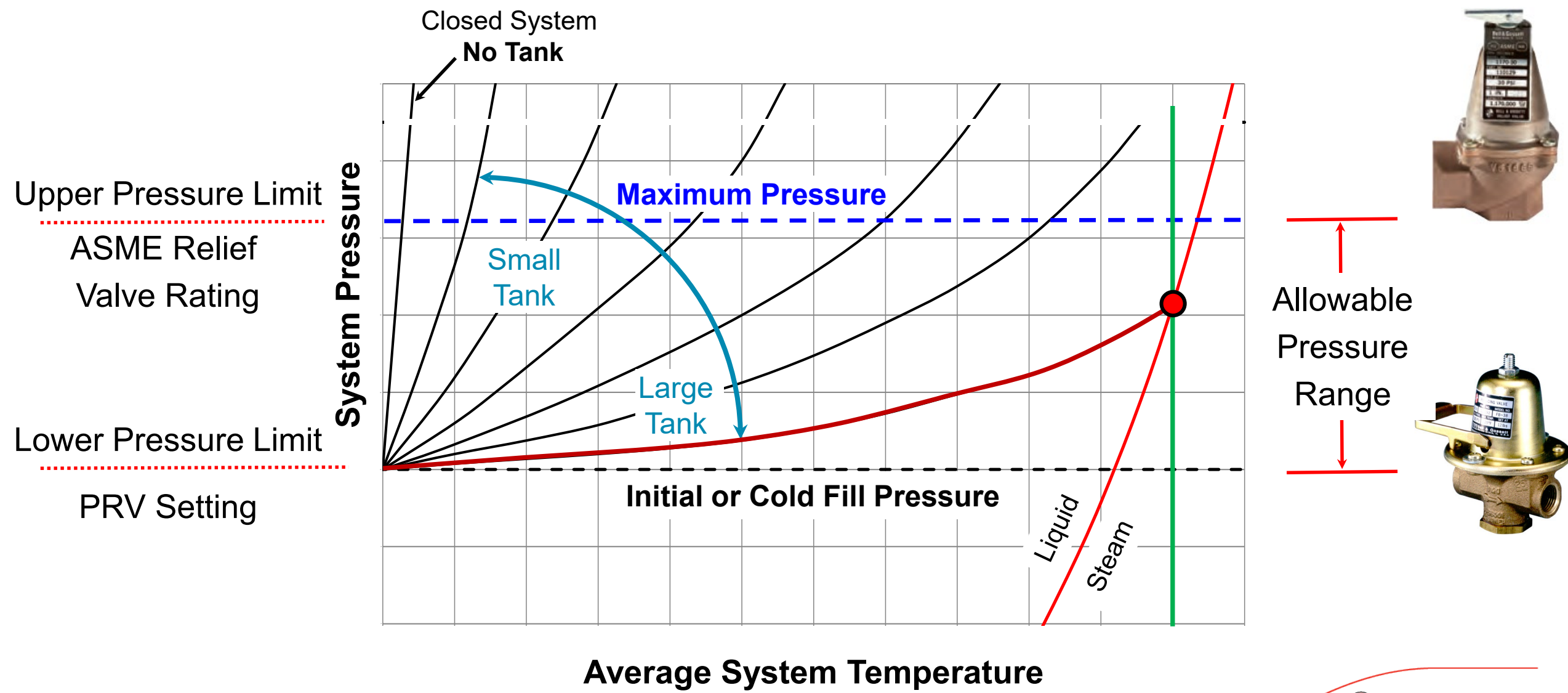
Allowable Pressure Range



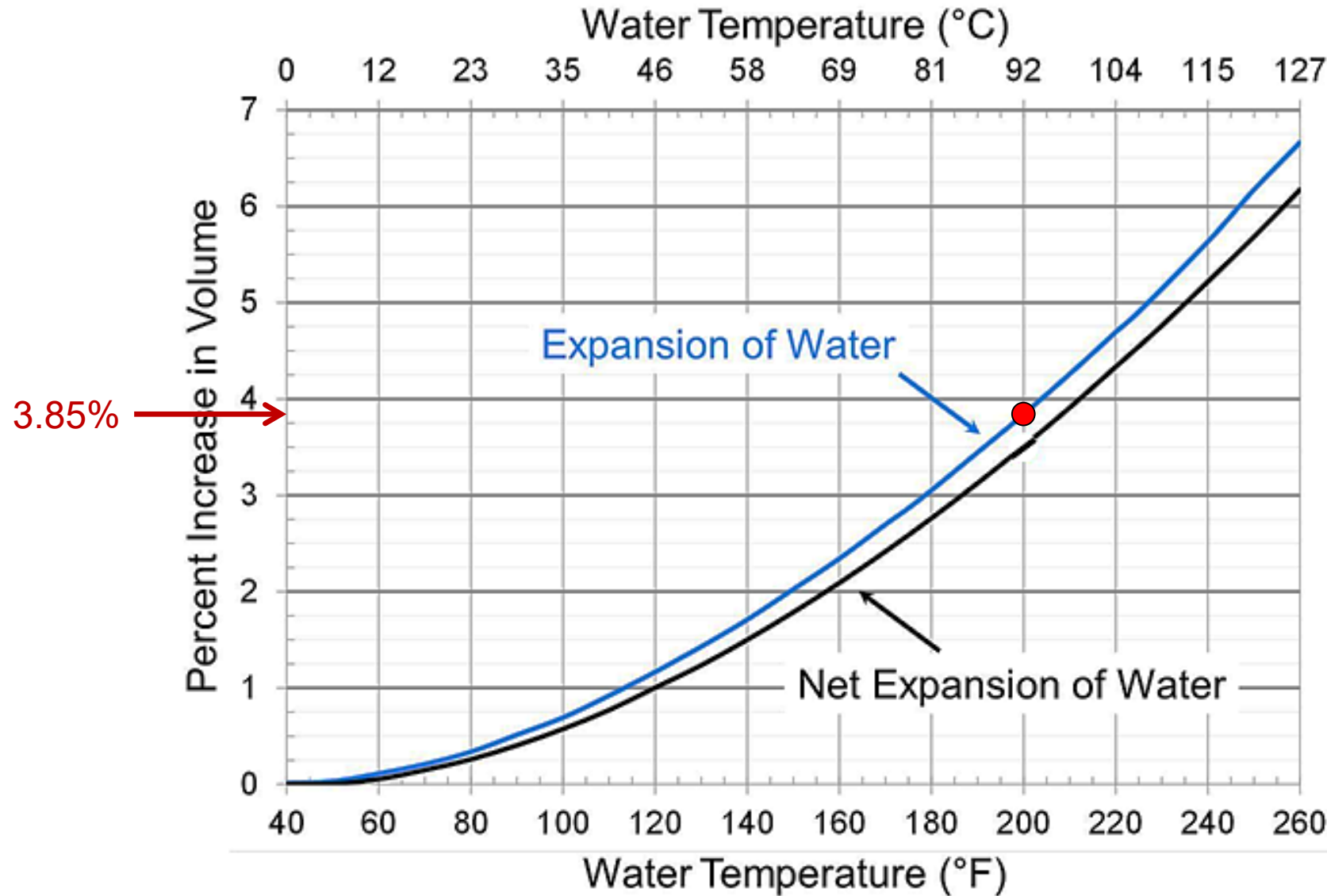
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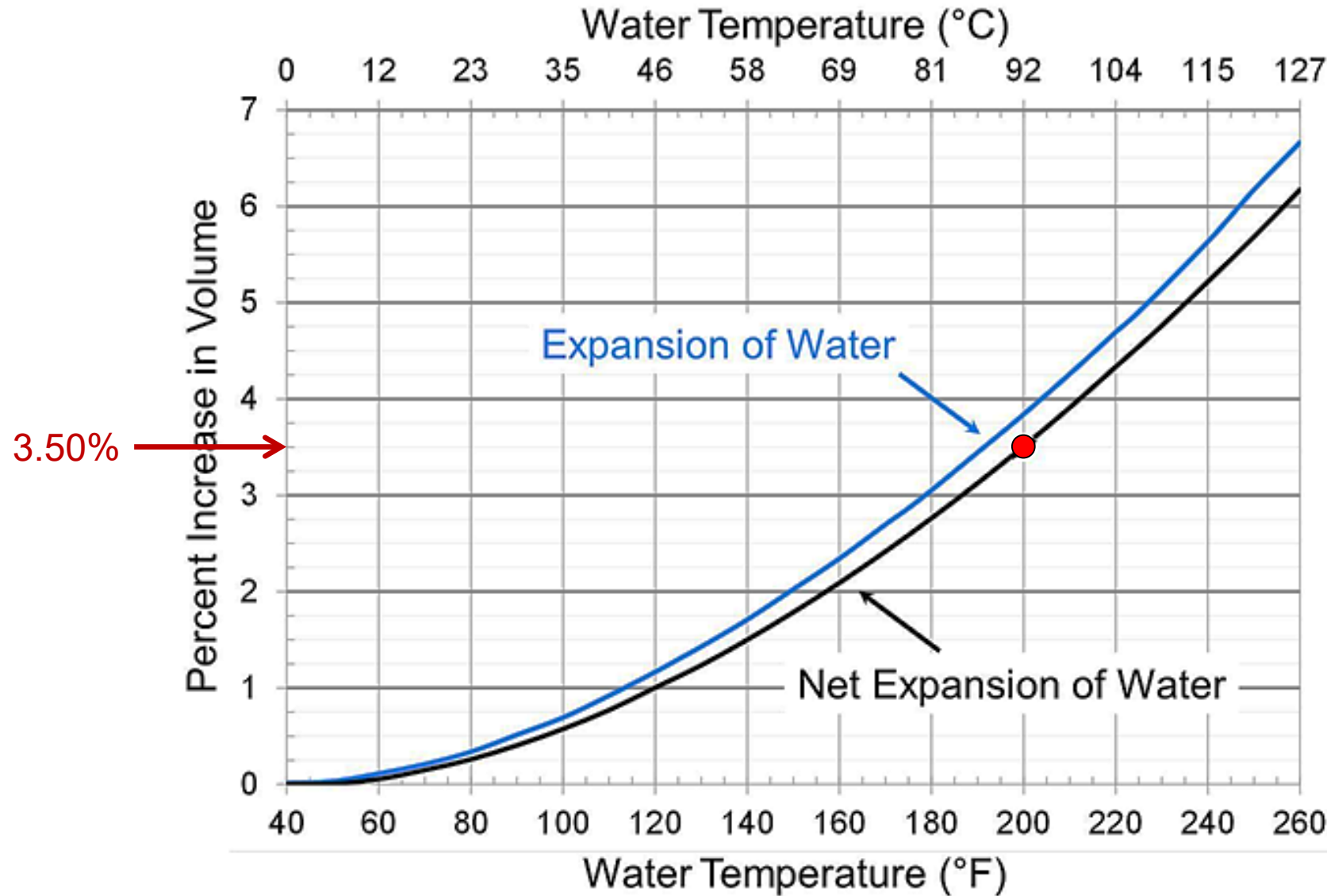
# The "Pressure Range" influence on Air Management Tank sizing



# Water Expansion vs. Temperature

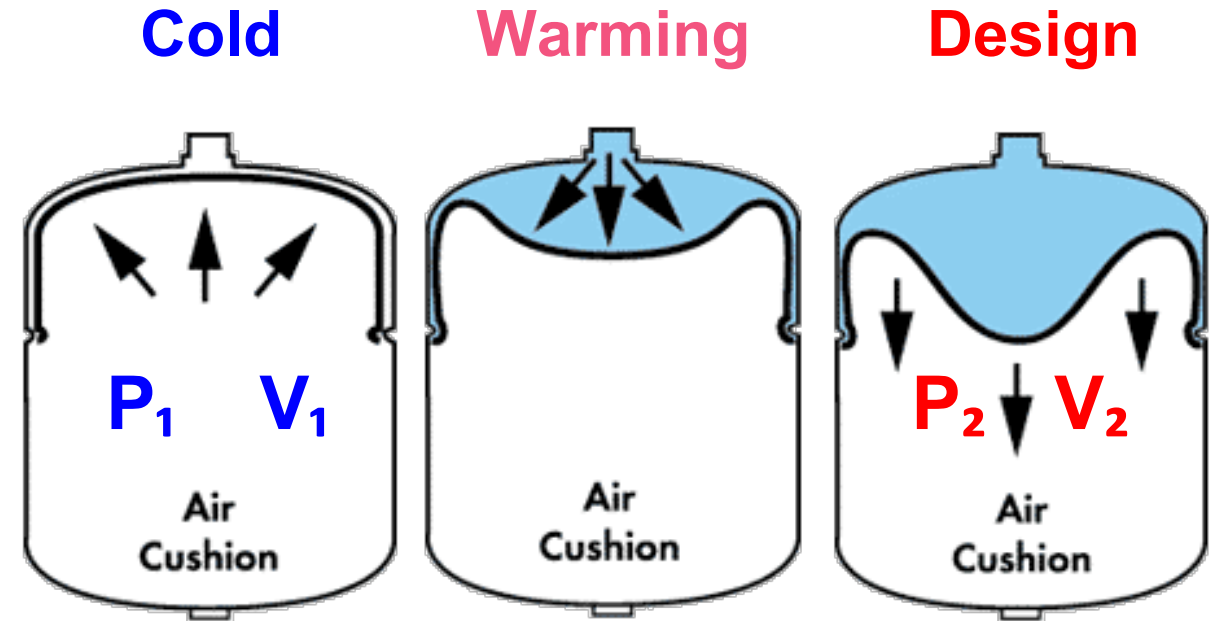
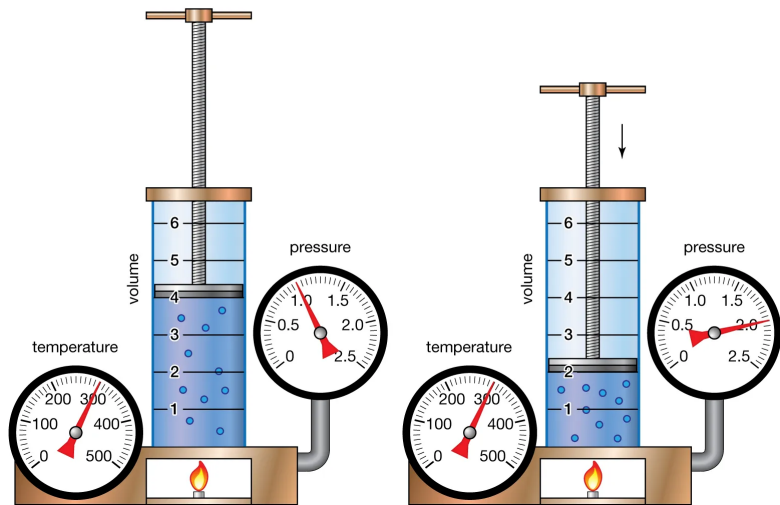


# Water Expansion vs. Temperature



# Boyle's Law – The Behavior of a Gas

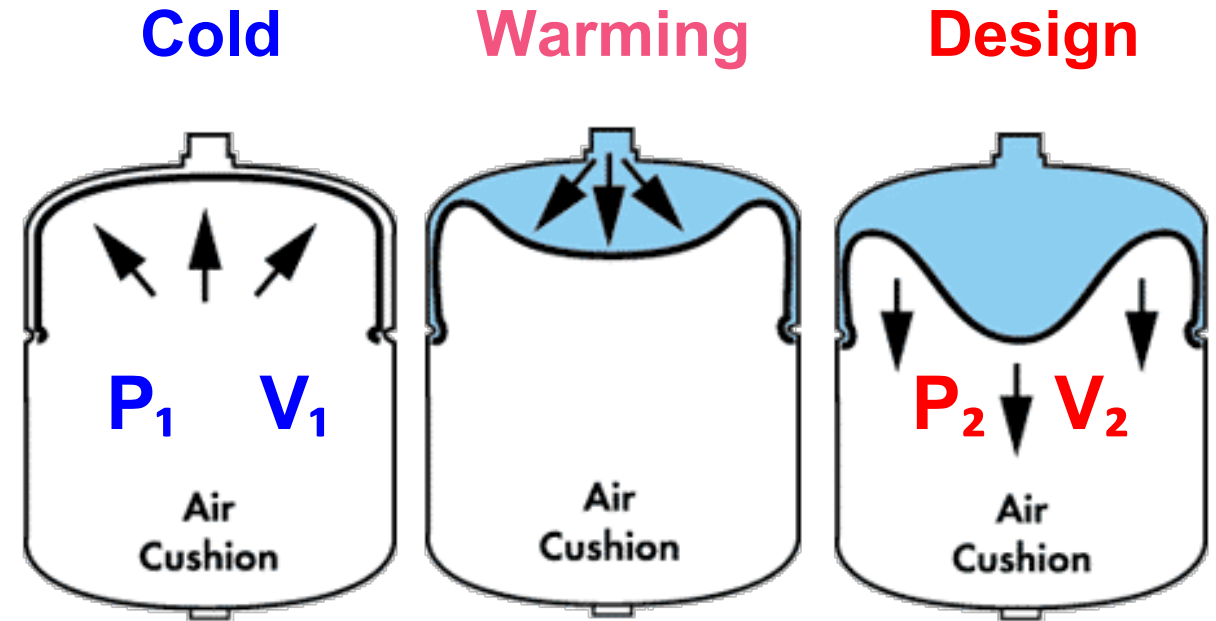
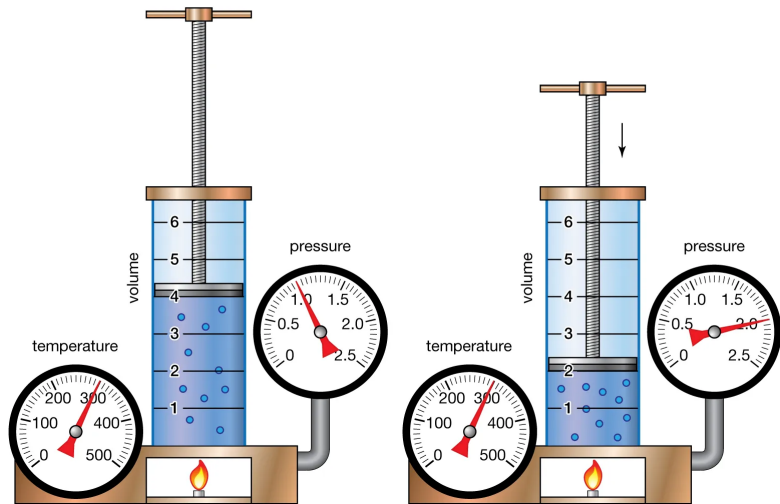
At **Constant Temperature**, the **Volume** of gas is inversely proportional to the **Pressure** exerted by the gas.



$$\frac{P_1 V_1}{T_1} = \frac{P_2 V_2}{T_2}$$

# Boyle's Law – The Behavior of a Gas

At **Constant Temperature**, the **Volume** of gas is inversely proportional to the **Pressure** exerted by the gas.

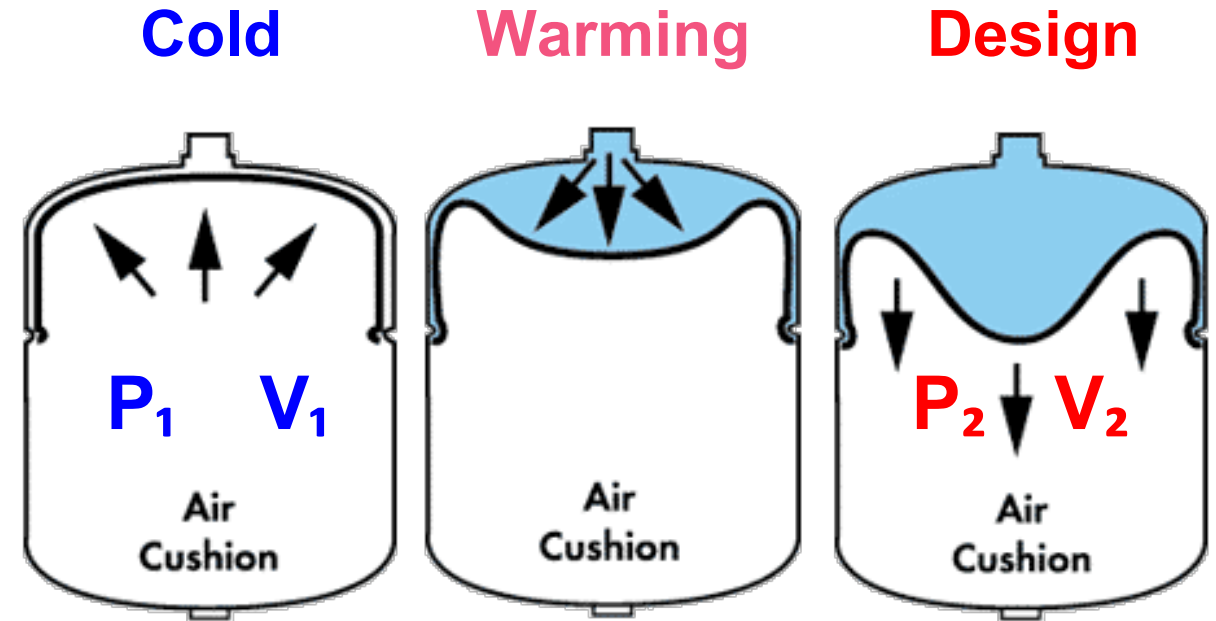
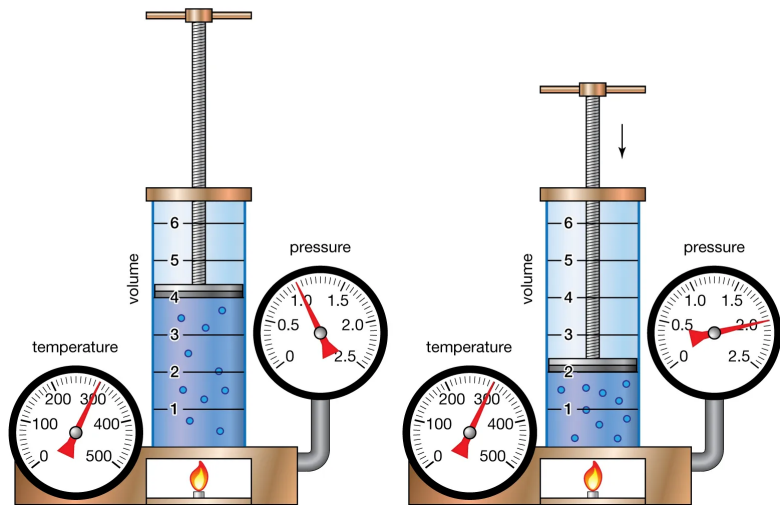


$$\frac{P_1 V_1}{T_1} = \frac{P_2 V_2}{T_2}$$

$$P_1 V_1 = P_2 V_2$$

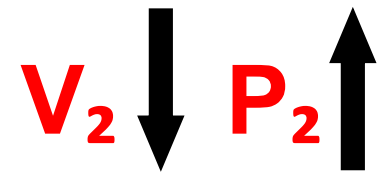
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$$\frac{P_1 V_1}{T_1} = \frac{P_2 V_2}{T_2}$$

$$P_1 V_1 = P_2 V_2$$



# Diaphragm or Bladder Pre-Charged Tank Types (Air Elimination)



Limited Acceptance  
Diaphragm



Limited Acceptance  
Bladder



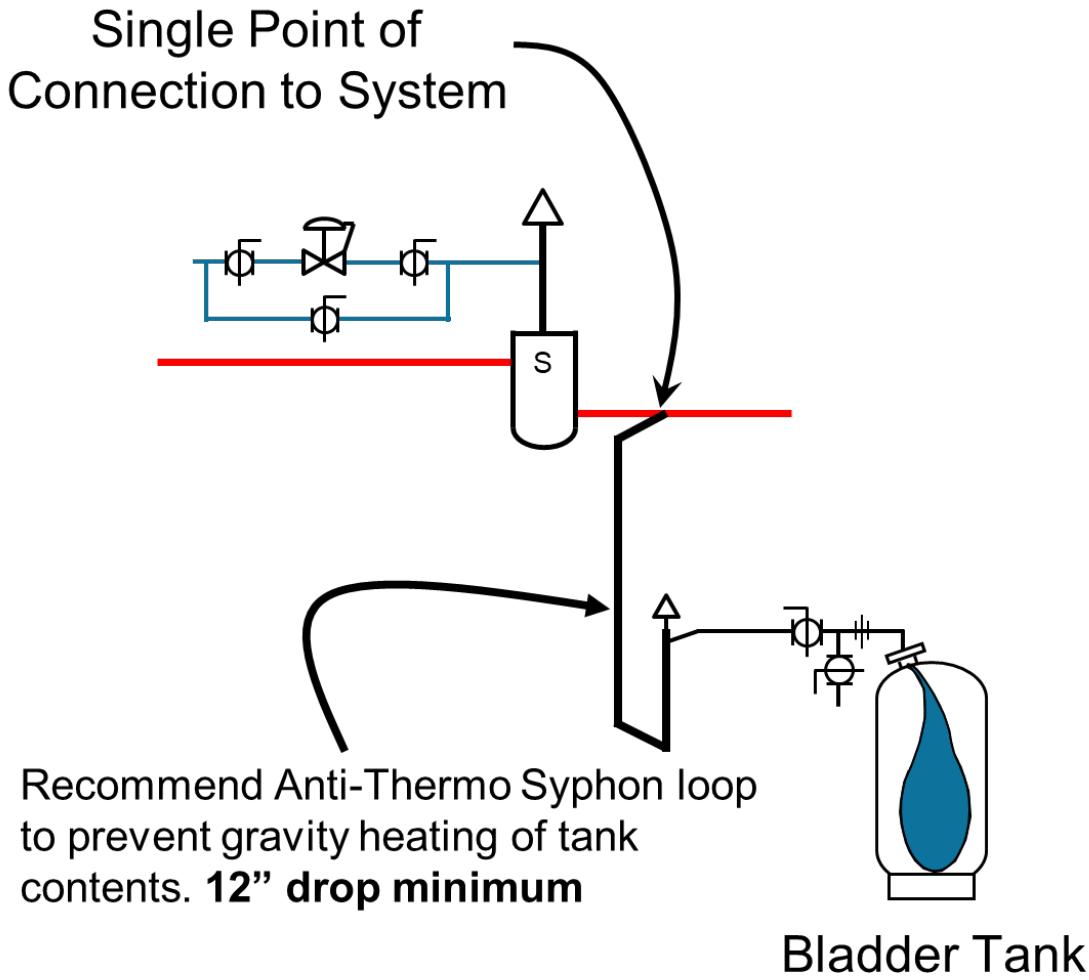
Full Acceptance  
Bladder

**\*NOTE: B&G Tanks for HVAC applications factory "Pre-Charge" is 40 PSI**

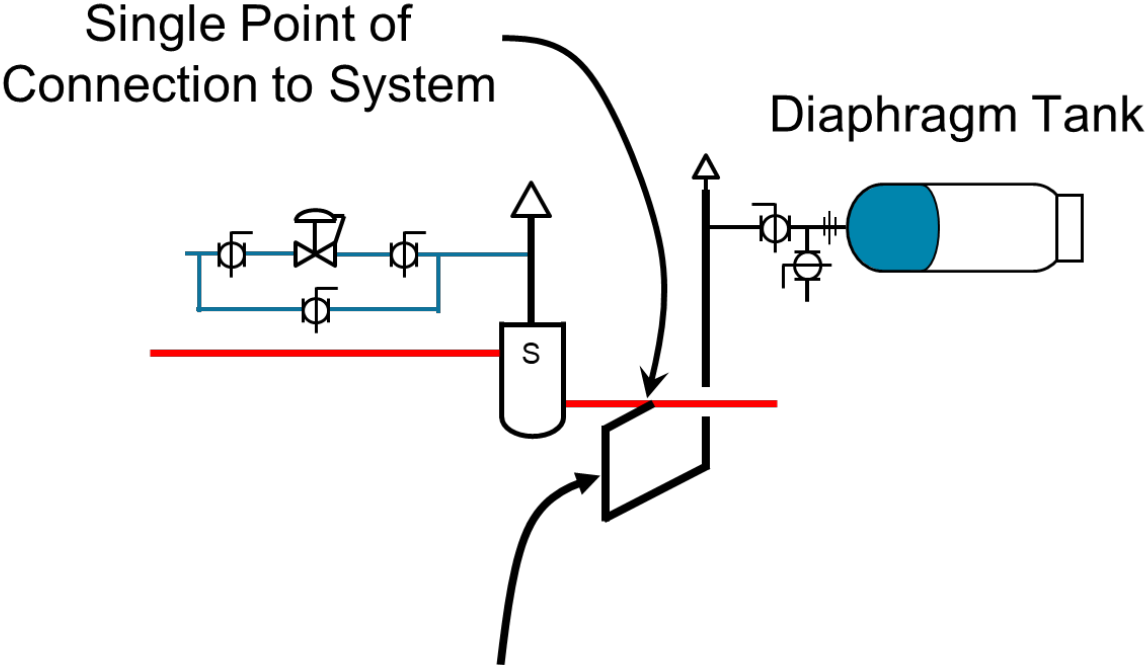
- Field adjust, **with tank empty**, to job specific Cold Static Fill Pressure, prior to introduction to system.



# Pre-Charged Tanks (Air Elimination) - Piping

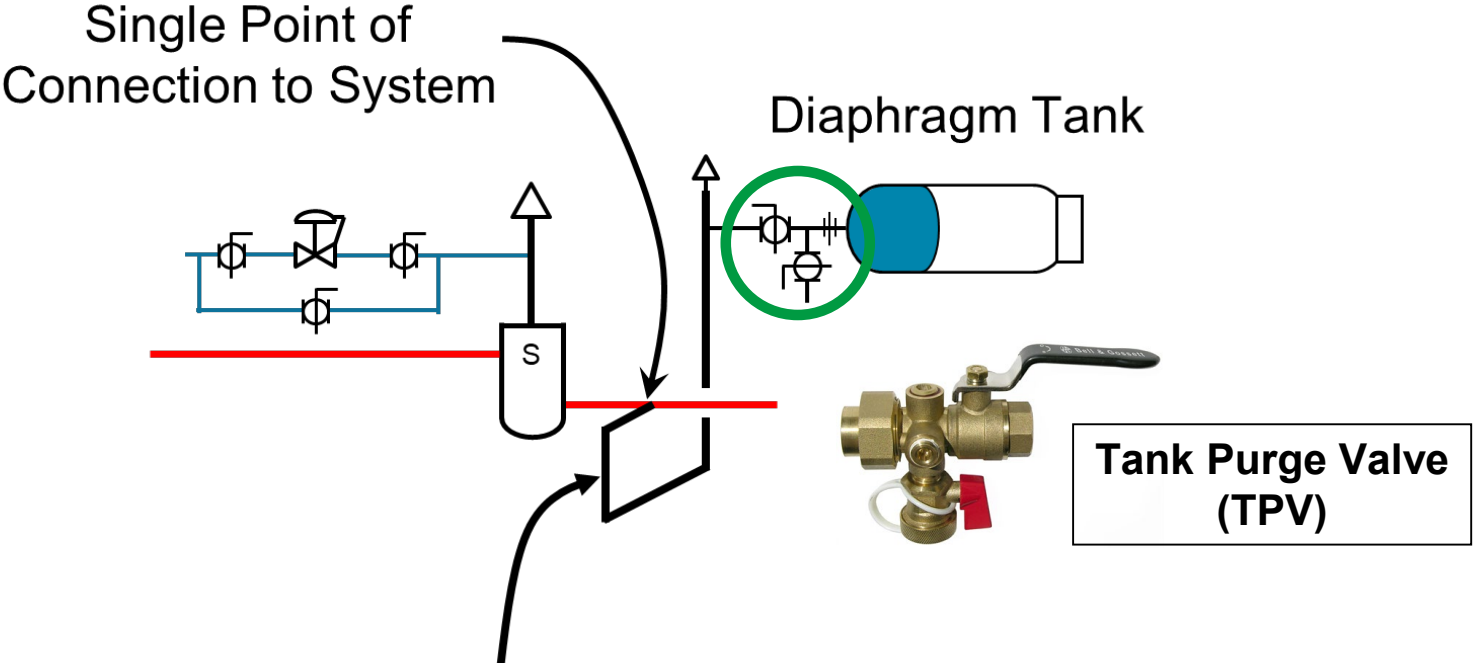


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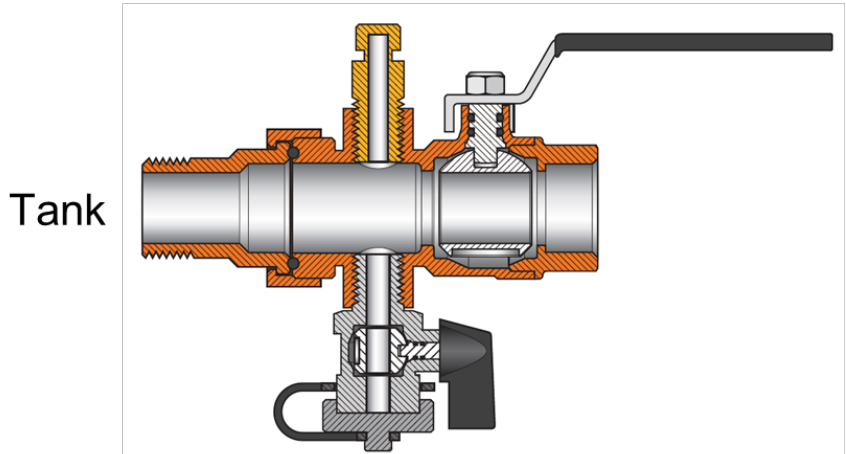
Recommend Anti-Thermo Syphon loop to prevent gravity heating of tank contents. **12" drop minimum**

# Pre-Charged Tanks (Air Elimination) - Piping



Recommend Anti-Thermo Syphon loop to prevent gravity heating of tank contents. **12" drop minimum**

**\* Check State and Local Codes**



**\* Not to be used in Potable Water Systems**

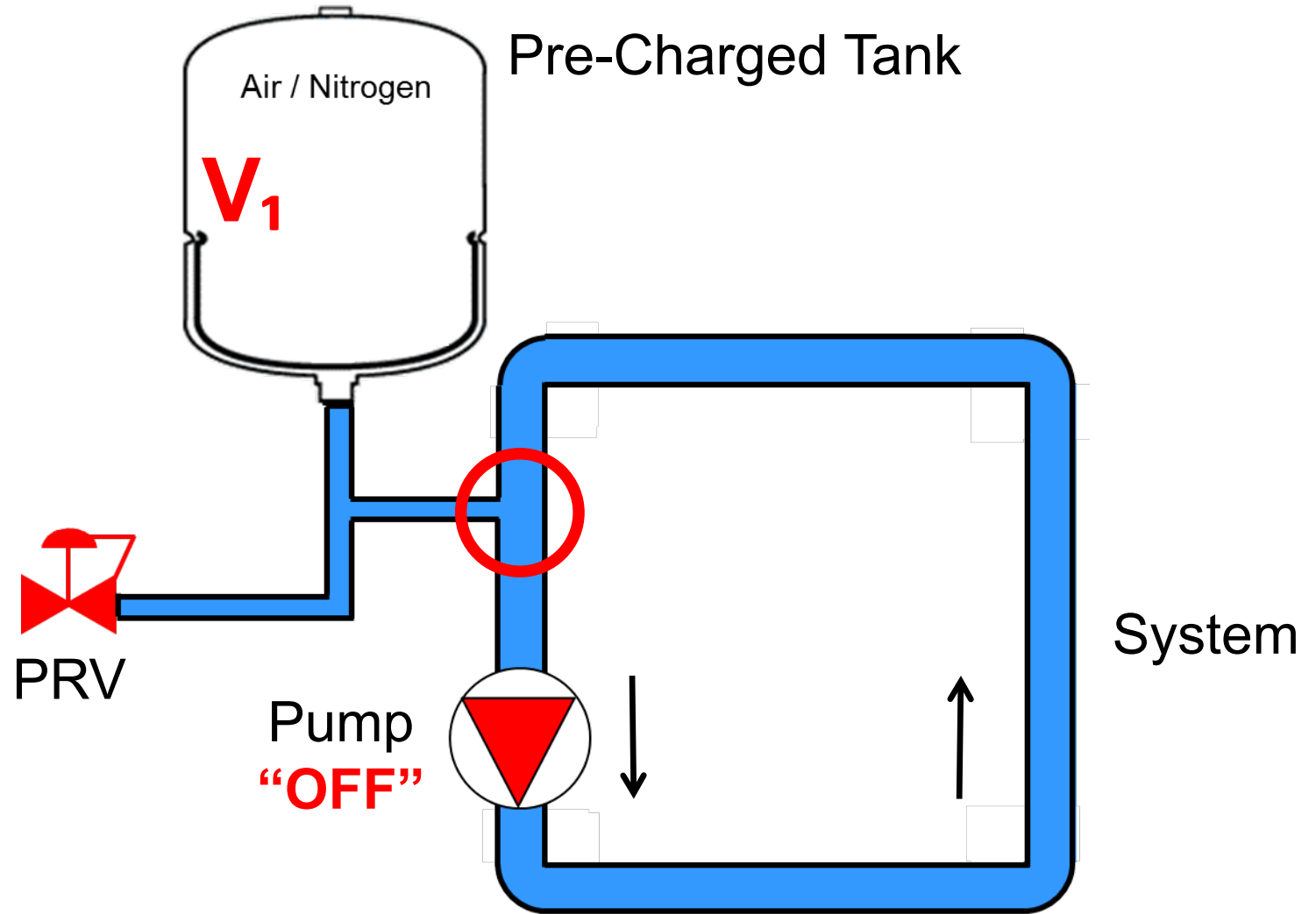
The “Point of No Pressure Change”

# Tank Location – System Pressure Reference

## AIR CHARGE

Pump  
"OFF"

$$\frac{P_1 V_1}{T_1}$$



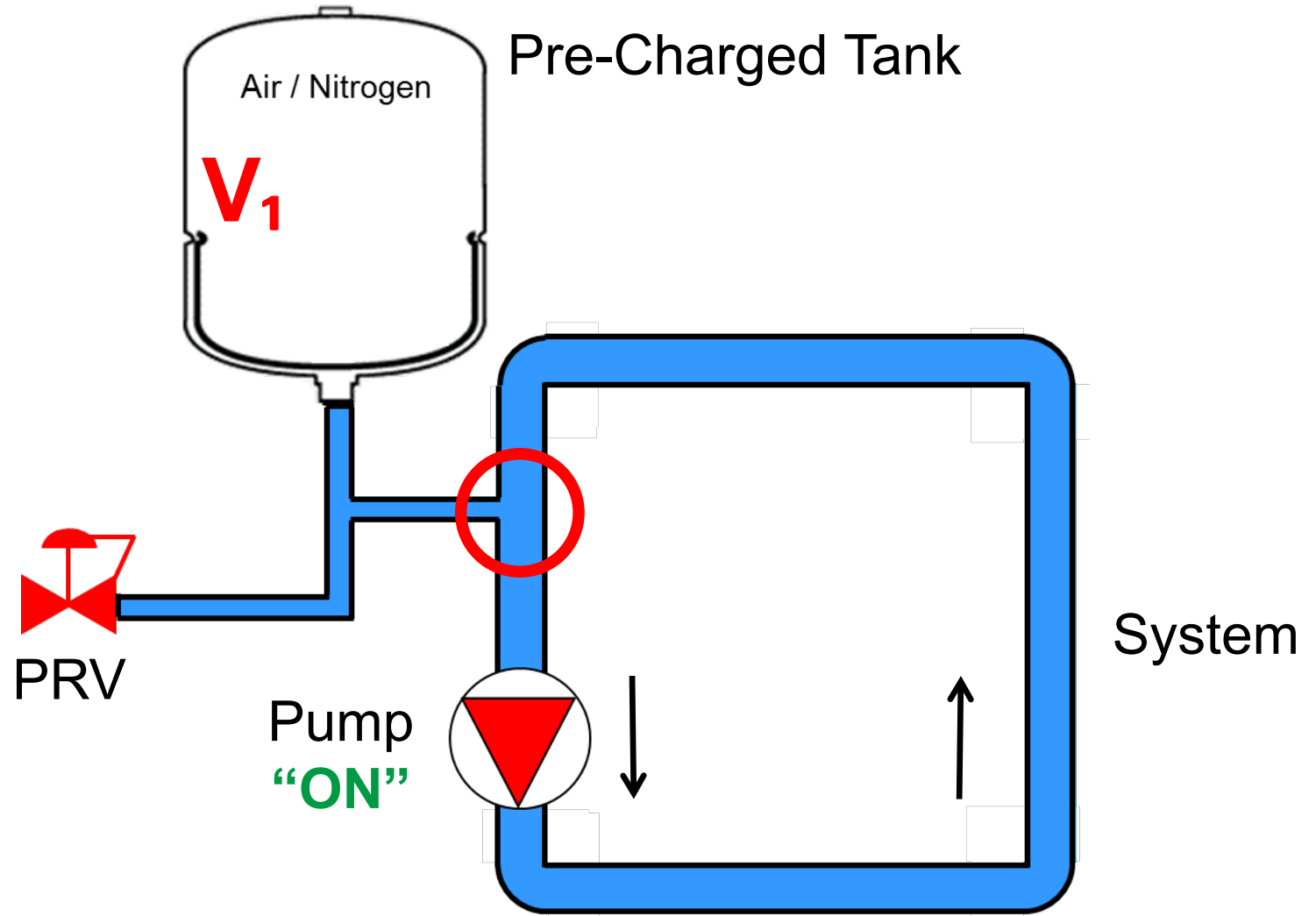
**System at Cold Fill Temperature**

# Tank Location – System Pressure Reference

## AIR CHARGE

Pump      Pump  
"OFF"    "ON"

$$\frac{P_1 V_1}{T_1} = \frac{P_2 V_2}{T_2}$$



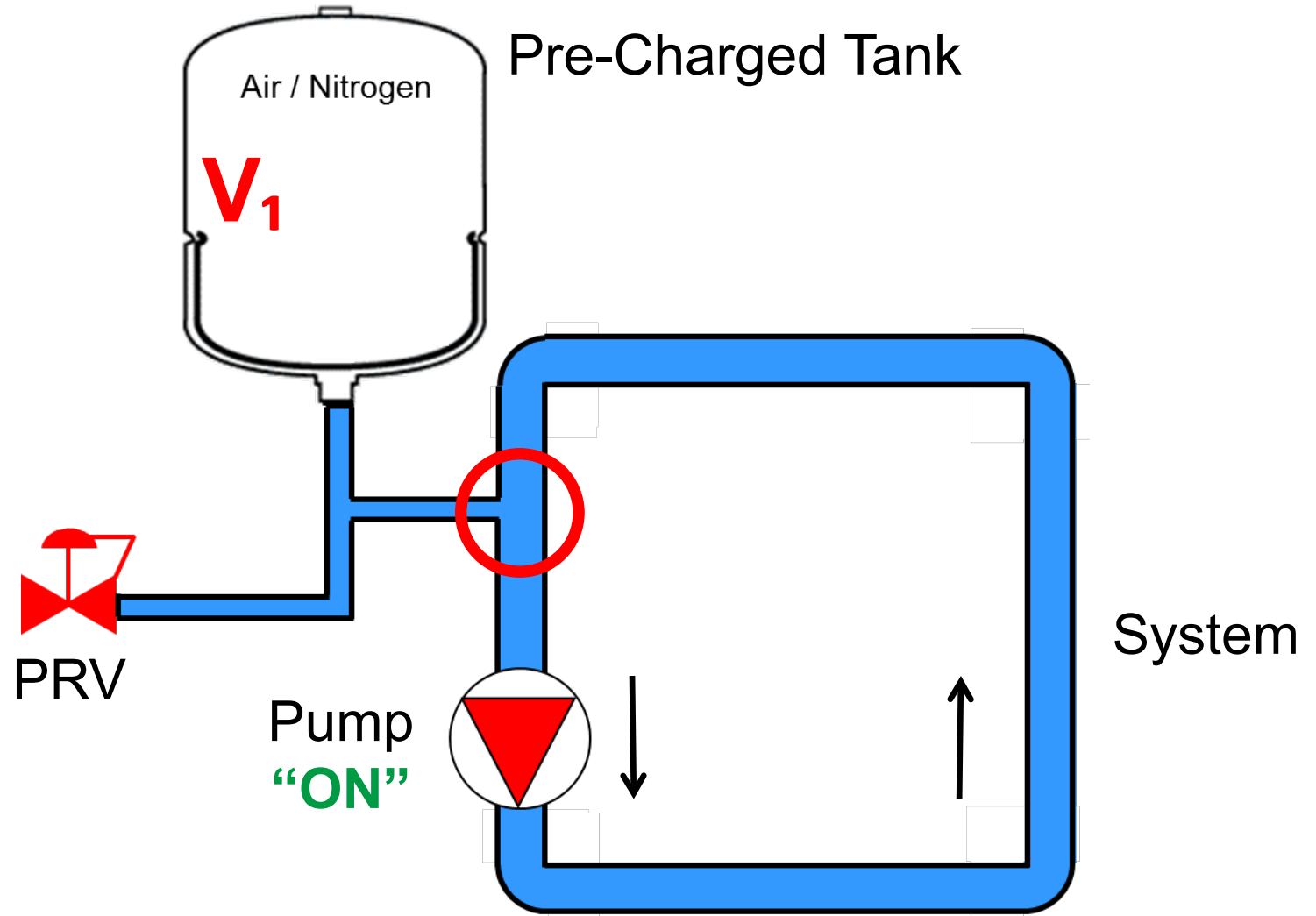
**System at Cold Fill Temperature**

# Tank Location – System Pressure Reference

## AIR CHARGE

Pump      Pump  
"OFF"    "ON"

$$\frac{P_1 V_1}{T_1} = \frac{P_2 V_2}{T_2}$$



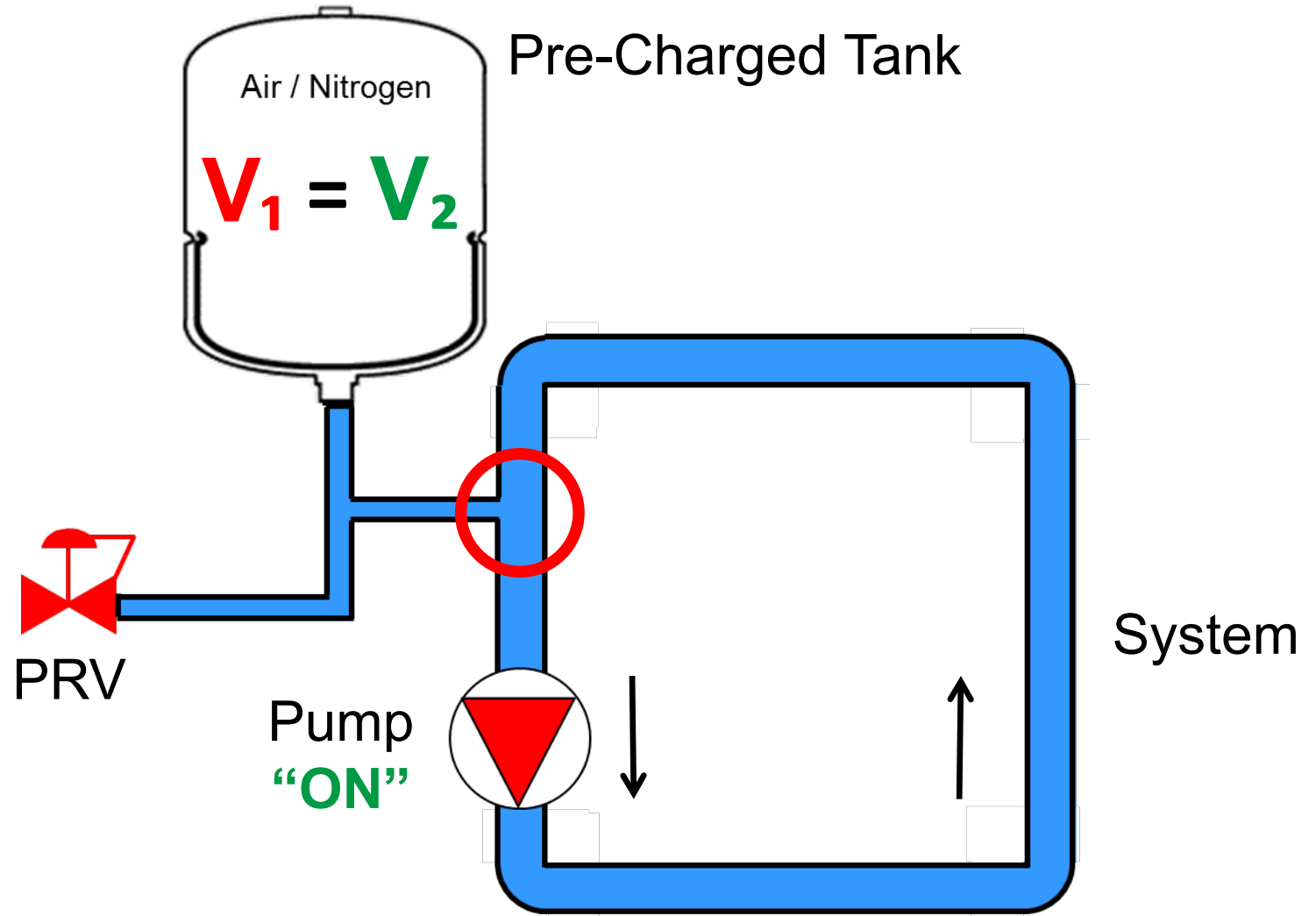
**System at Cold Fill Temperature**

# Tank Location – System Pressure Reference

## AIR CHARGE

Pump  
"OFF"      Pump  
"ON"

$$\frac{P_1 V_1}{T_1} = \frac{P_2 V_2}{T_2}$$



**System at Cold Fill Temperature**



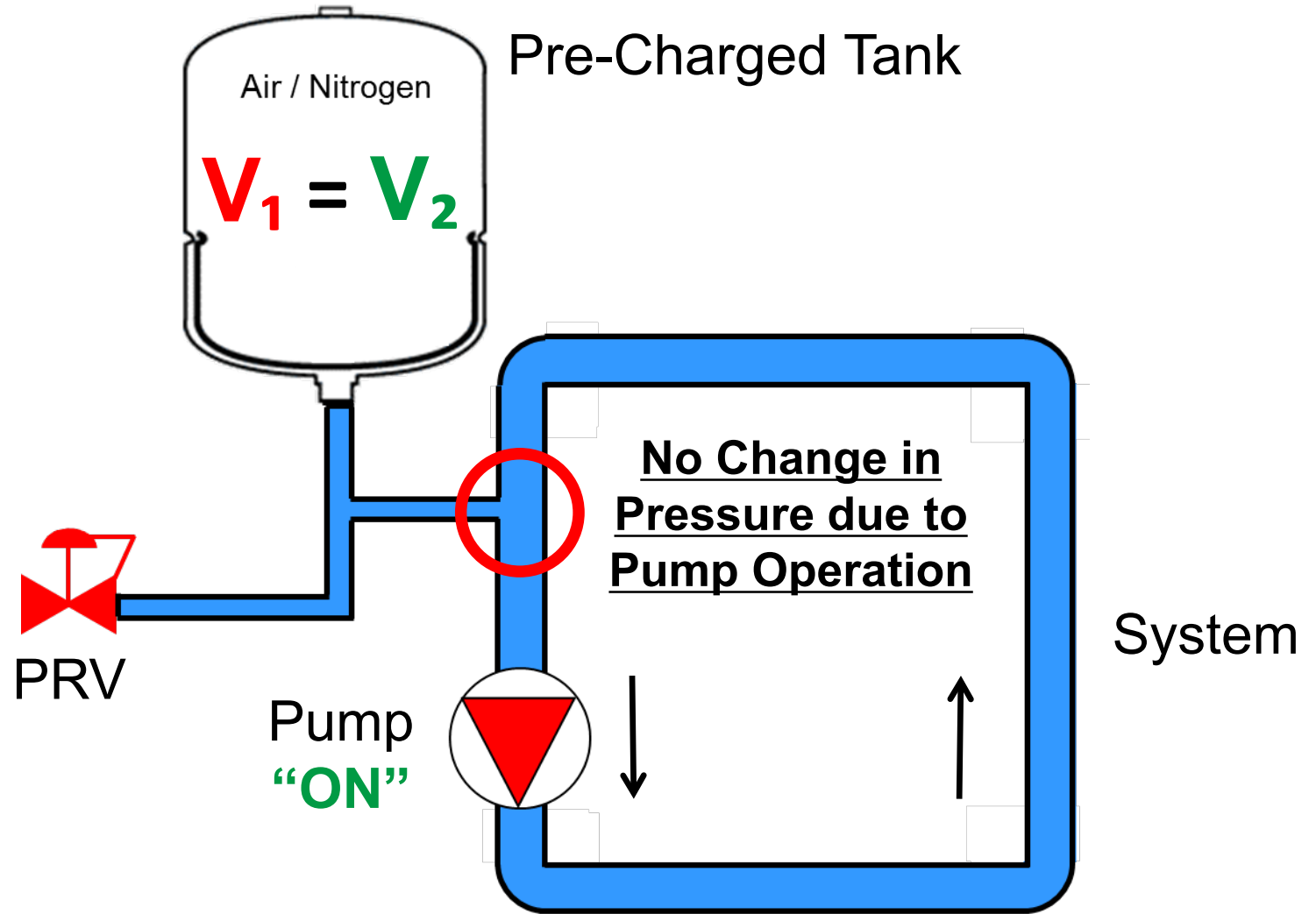
# Tank Location – System Pressure Reference

## AIR CHARGE

Pump “OFF”      Pump “ON”

$$\frac{P_1 V_1}{T_1} = \frac{P_2 V_2}{T_2}$$

$$P_1 = P_2$$



**System at Cold Fill Temperature**

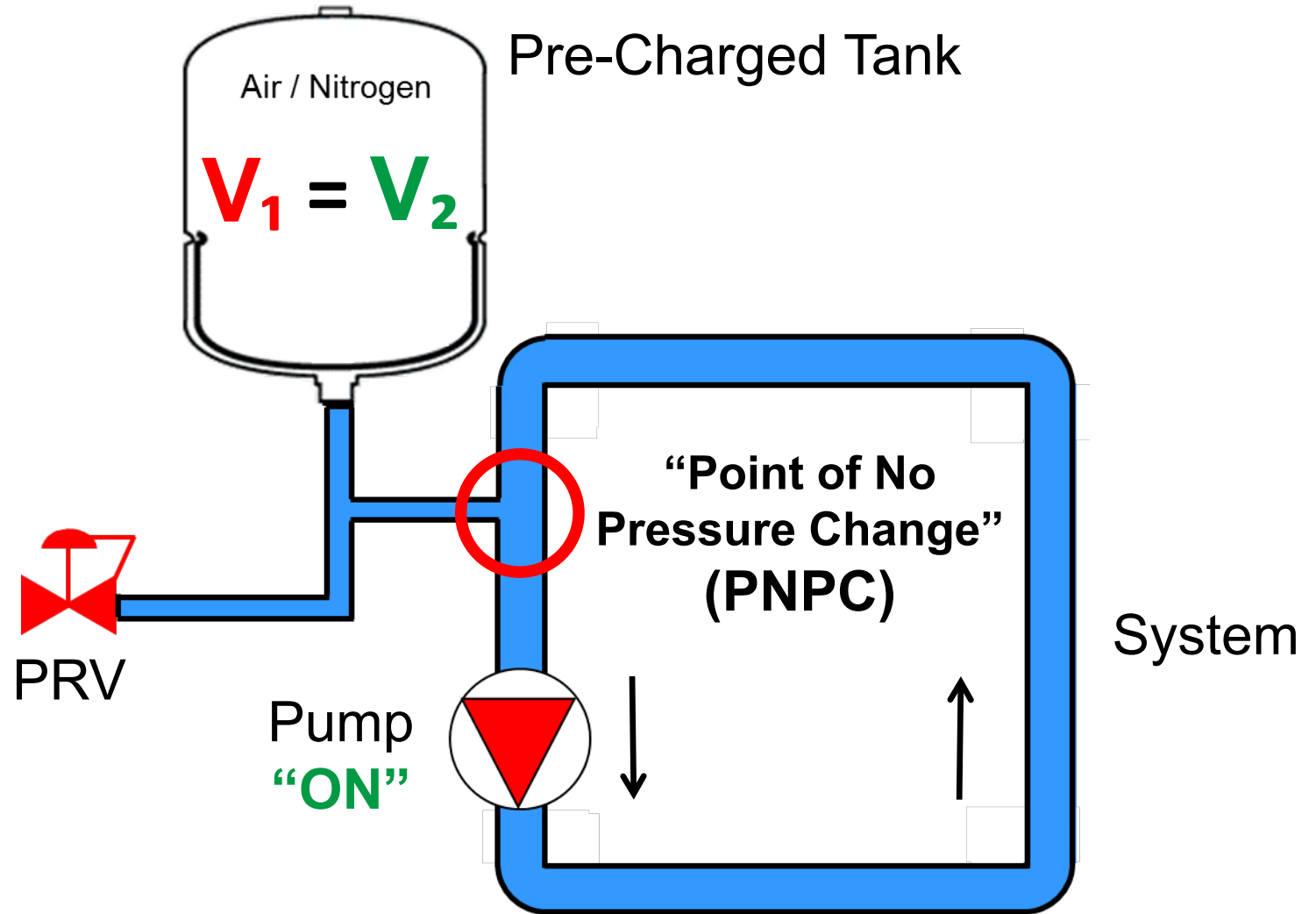
# Tank Location – System Pressure Reference

## AIR CHARGE

Pump      Pump  
"OFF"    "ON"

$$\frac{P_1 \cancel{V_1}}{\cancel{T_1}} = \frac{P_2 \cancel{V_2}}{\cancel{T_2}}$$

$$P_1 = P_2$$



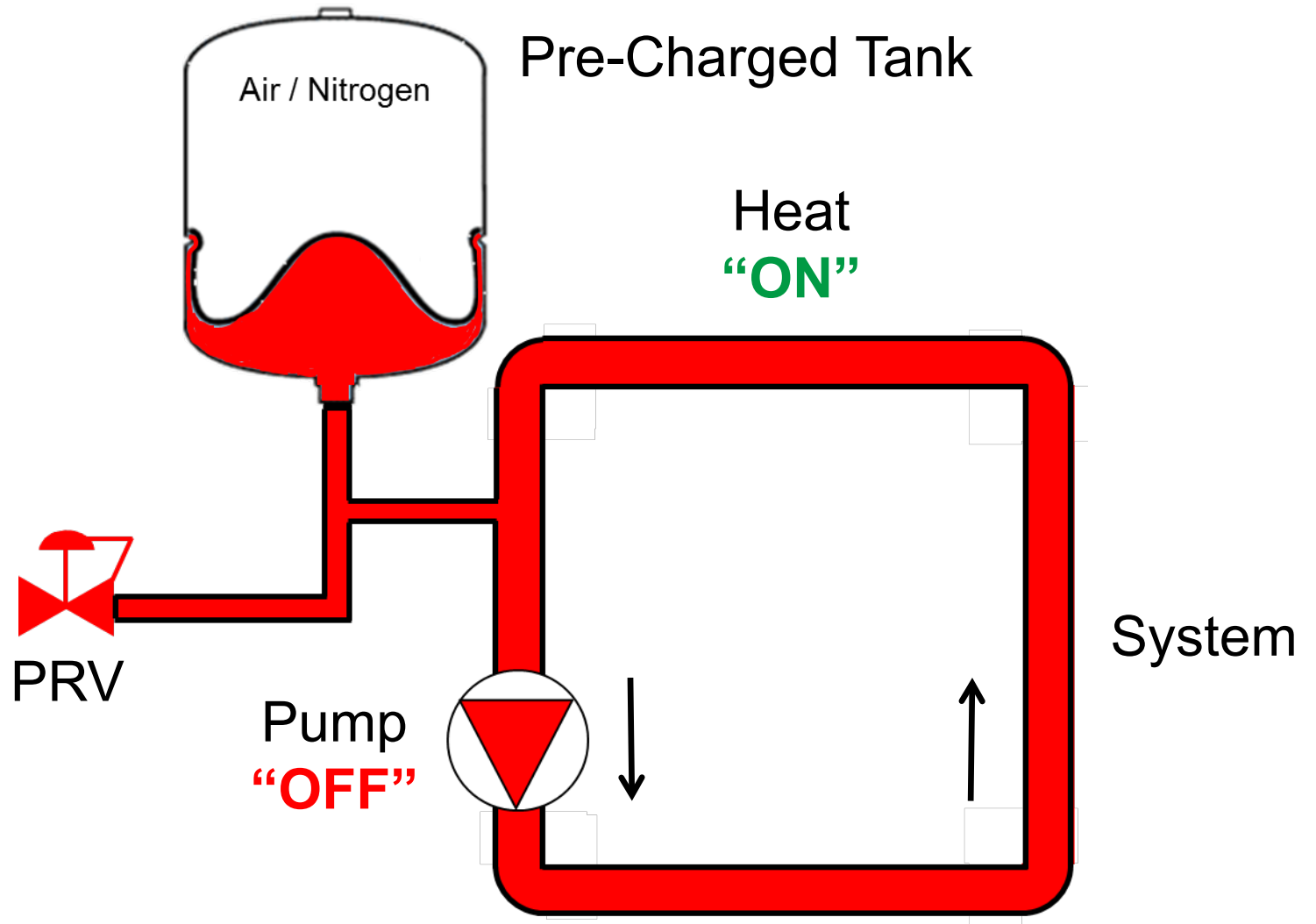
**System at Cold Fill Temperature**

# Tank Location - Point of No Pressure Change (PNPC)

## AIR CHARGE

Heat "OFF"      Heat "ON"

$$\frac{P_1 V_1}{T_1} = \frac{P_2 V_2}{T_2}$$



**System at Average Design Temperature**

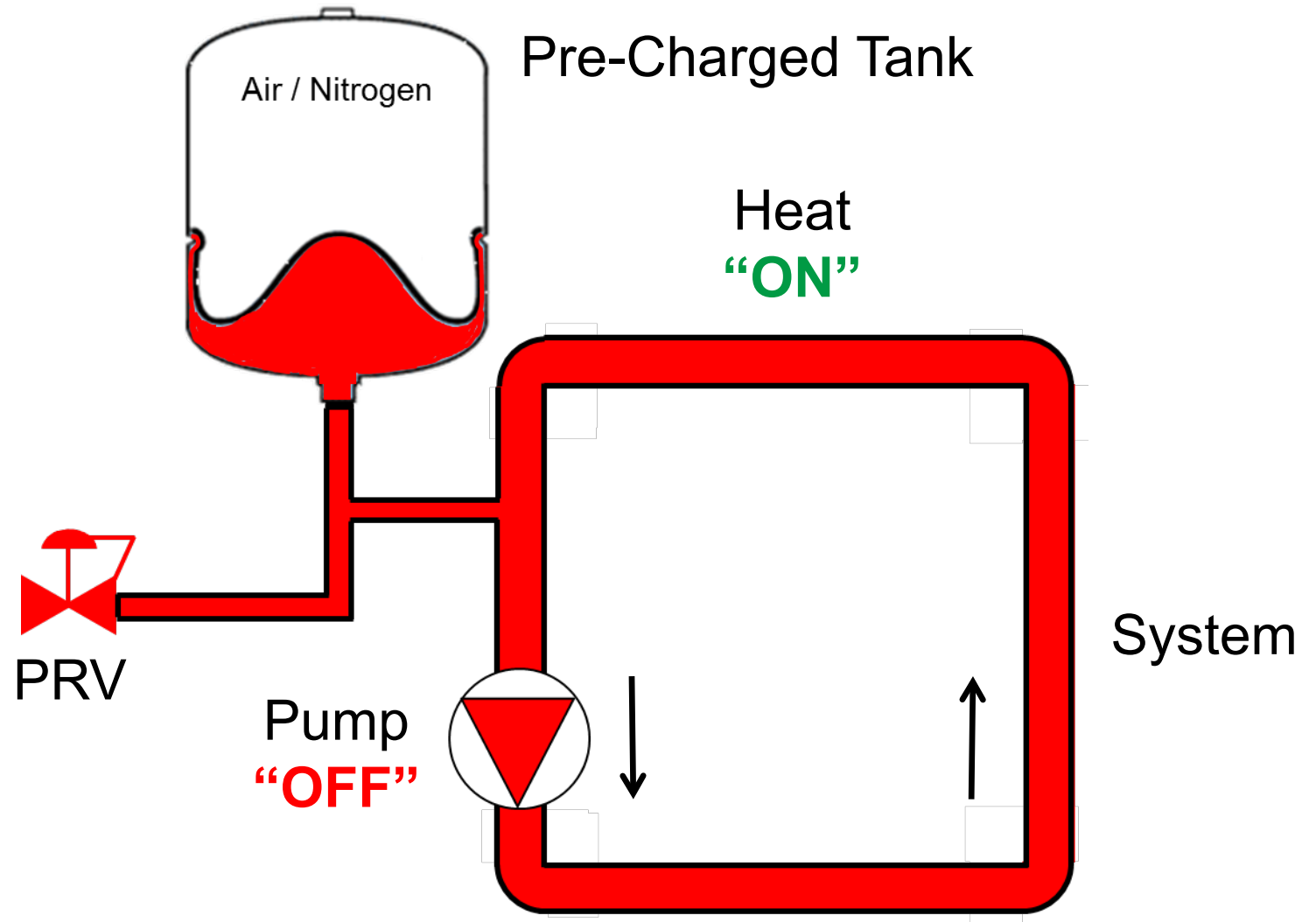
# Tank Location - Point of No Pressure Change (PNPC)

## AIR CHARGE

Heat  
"OFF"

Heat  
"ON"

$$\frac{P_1 V_1}{T_1} = \frac{P_2 V_2}{T_2}$$



**System at Average Design Temperature**

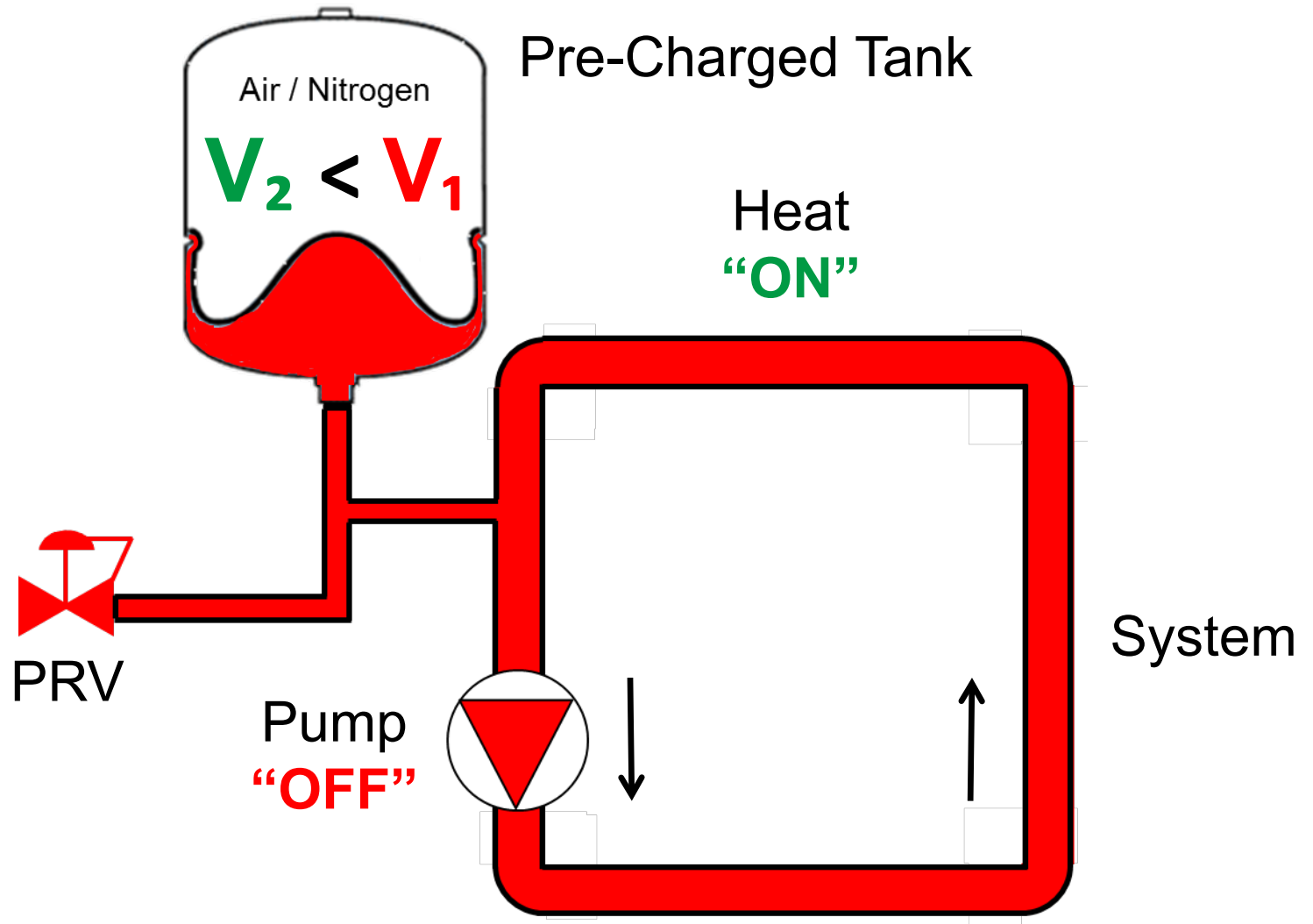
# Tank Location - Point of No Pressure Change (PNPC)

## AIR CHARGE

Heat "OFF"      Heat "ON"

$$\frac{P_1 V_1}{T_1} = \frac{P_2 V_2}{T_2}$$

$$V_2 < V_1$$



**System at Average Design Temperature**

# Tank Location - Point of No Pressure Change (PNPC)

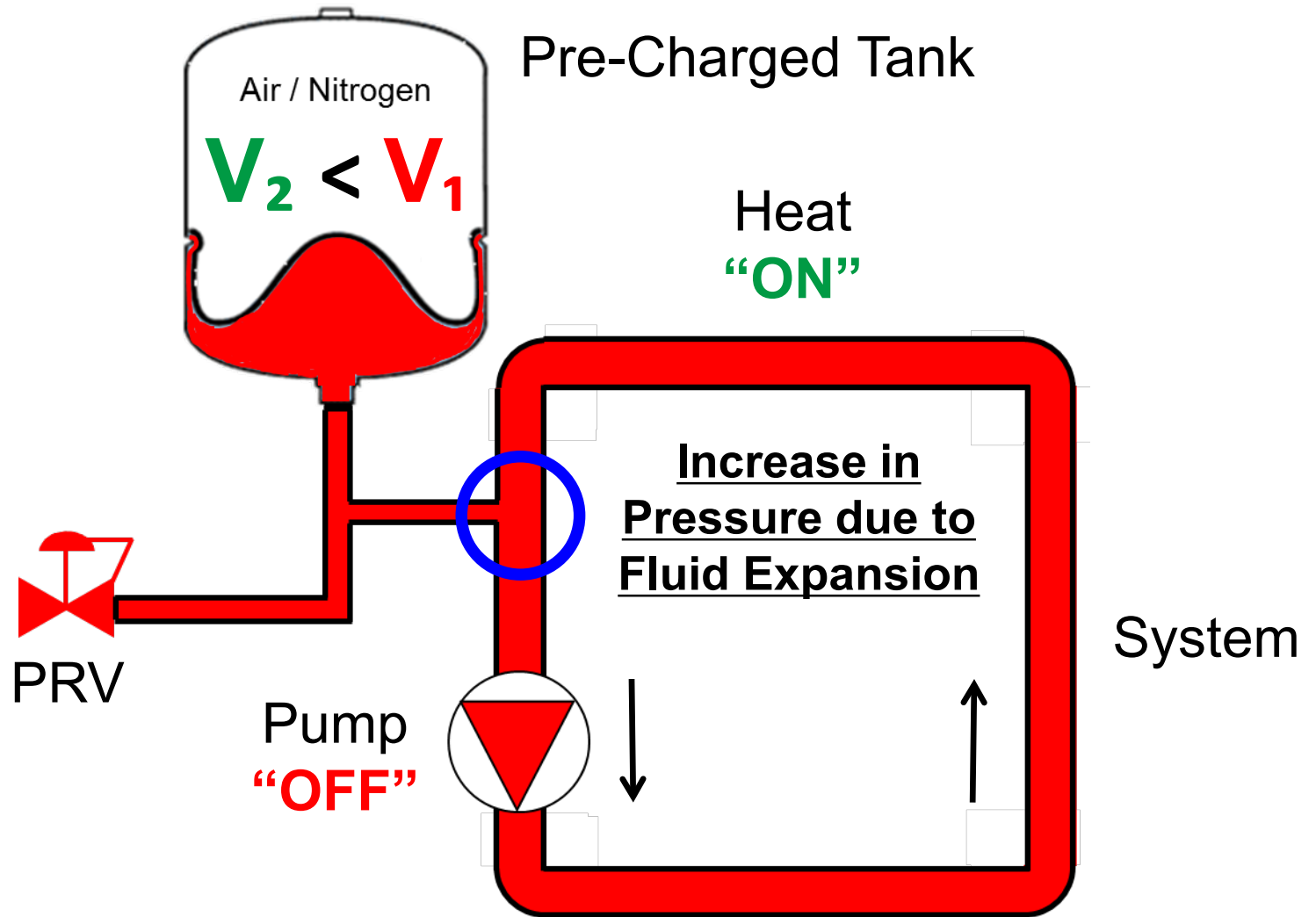
## AIR CHARGE

Heat "OFF"      Heat "ON"

$$\frac{P_1 V_1}{T_1} = \frac{P_2 V_2}{T_2}$$

$$V_2 < V_1$$

$$P_2 > P_1$$



System at Average Design Temperature

# Tank Location - Point of No Pressure Change (PNPC)

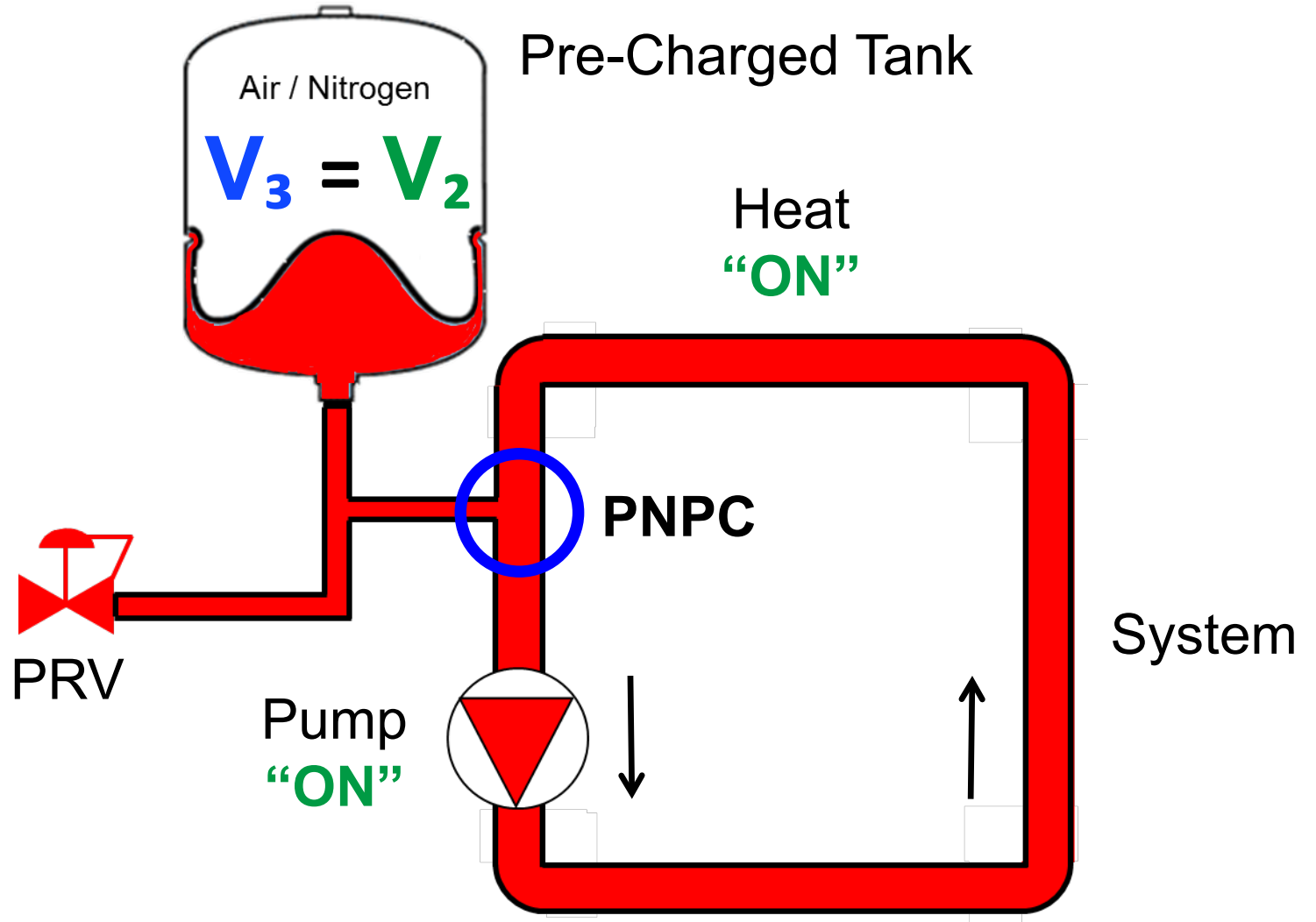
## AIR CHARGE

Heat  
"ON"

Pump  
"ON"

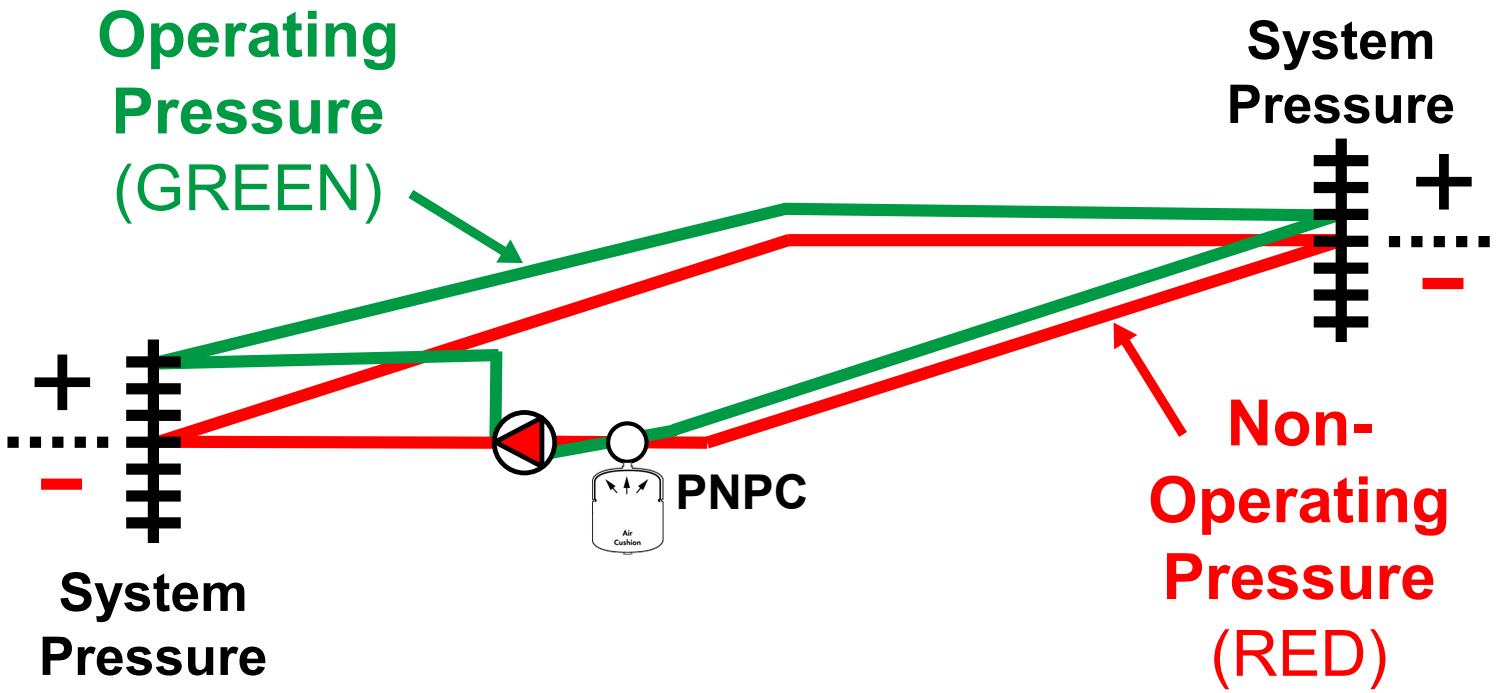
$$\frac{P_2 \cancel{V_2}}{\cancel{T_2}} = \frac{P_3 \cancel{V_3}}{\cancel{T_3}}$$

$$P_2 = P_3$$



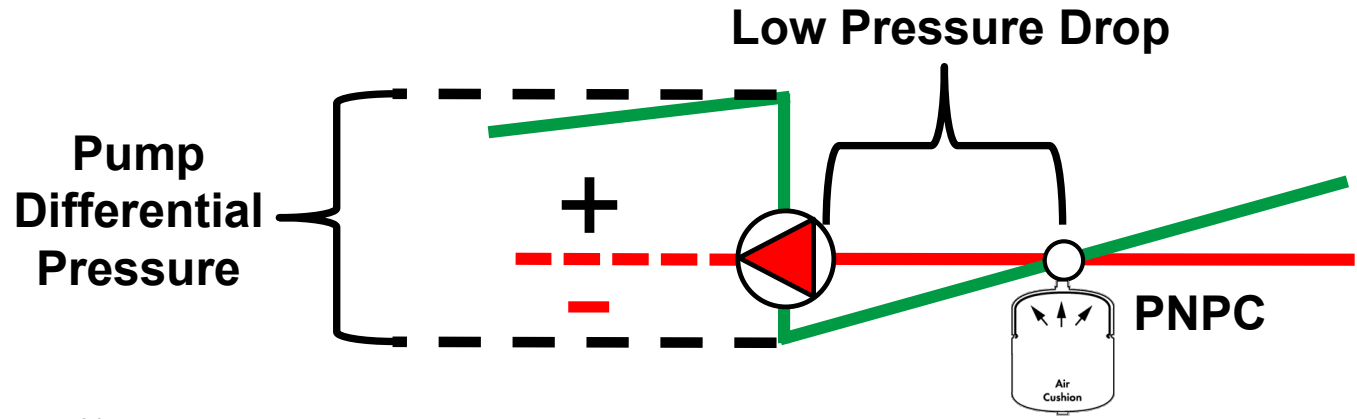
System at Average Design Temperature

# Pumping **Away** from the Point of No Pressure Change



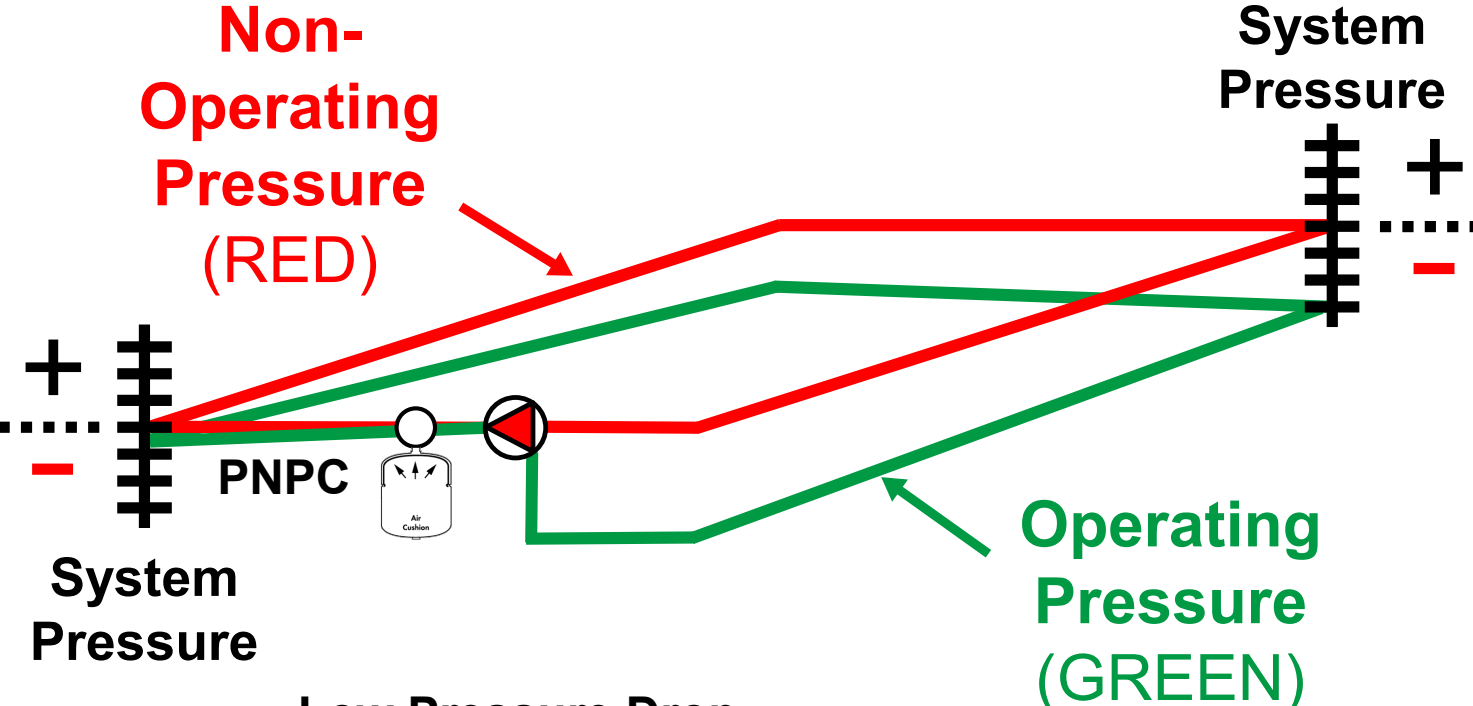
## Benefits

- Proper Venting Pressure
- Prevents Air Release/Boiling
- Stable Pump Suction Pressure



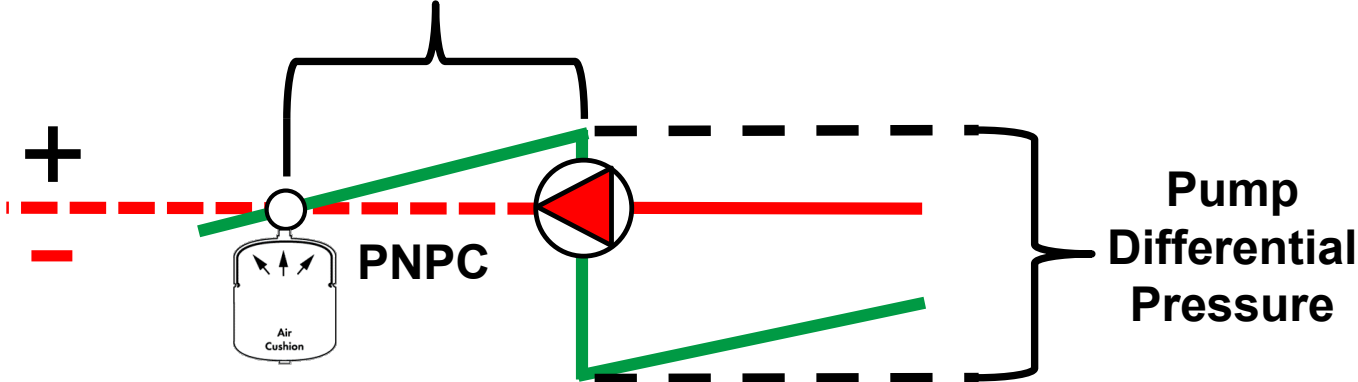


# Pumping **Towards** the Point of No Pressure Change



## Potential Problems

- Vacuum, Vents draw air in
- Air Release/ Possible Boiling
- Addition of Make-up Water?



## Sizing the Expansion Tank

# What information do you need?

- What is the fluid? *(or it's Thermal Properties)*
- How much fluid will the system hold? *(The System Volume)*
- Fluid temperature at time of fill
- Fluid temperature at operating conditions
- Cold static fill pressure *(PRV connection to highest point, plus safety factor)*
- Safety Relief Valve Setting

# Pre-Charged Tank Sizing Equation – Considerations for Simplification

- Isothermal (*Constant Temperature*) conditions in the tank.
- Expansion of the tank and its water can be ignored.
- Air cannot escape from the tank.
- System fills slowly.
- Ignore volume of air liberated during heating.

# Pre-Charged Tank Sizing Equation

$V_t$  = Tank Volume (gallons)

$V_s$  = Volume of System (gallons)

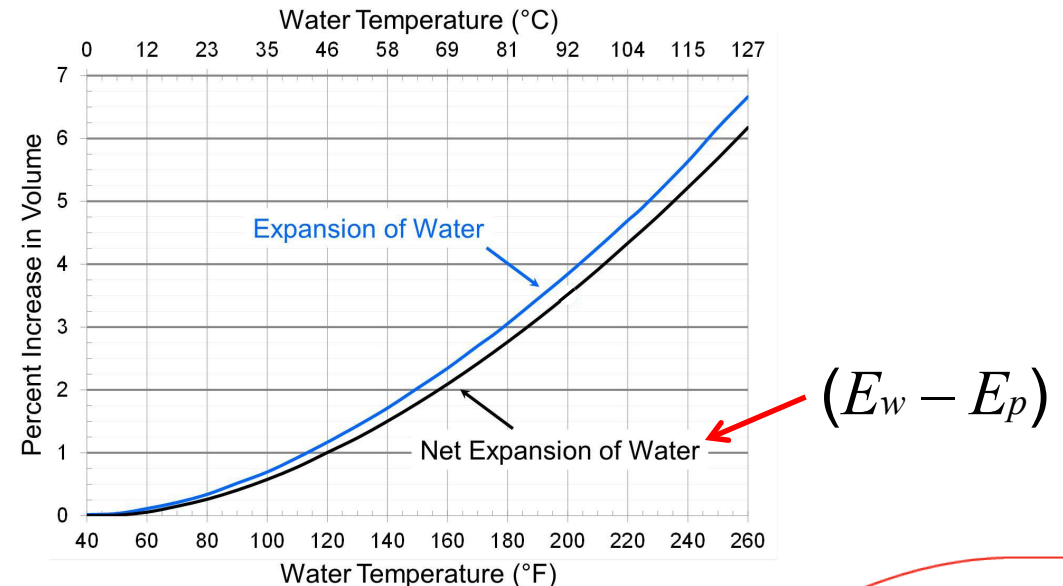
$(E_w - E_p)$  = Net Water Expansion Factor

$P_f$  = Design Tank Fill Pressure (psia)\*

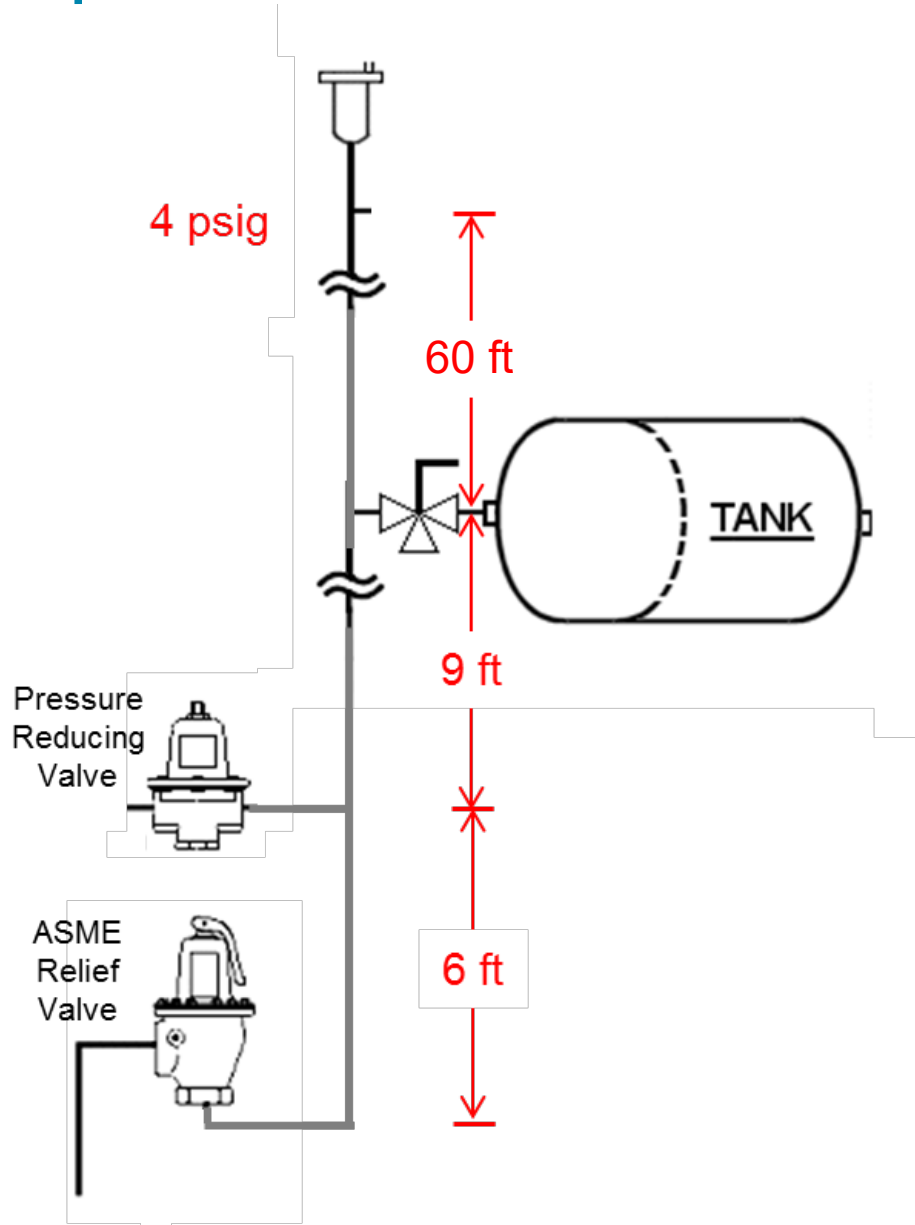
$P_o$  = Final Tank Operating Pressure (psia)\*

\* Absolute pressure

$$V_t = \frac{(E_w - E_p)}{1 - \frac{P_f}{P_o}} V_s$$

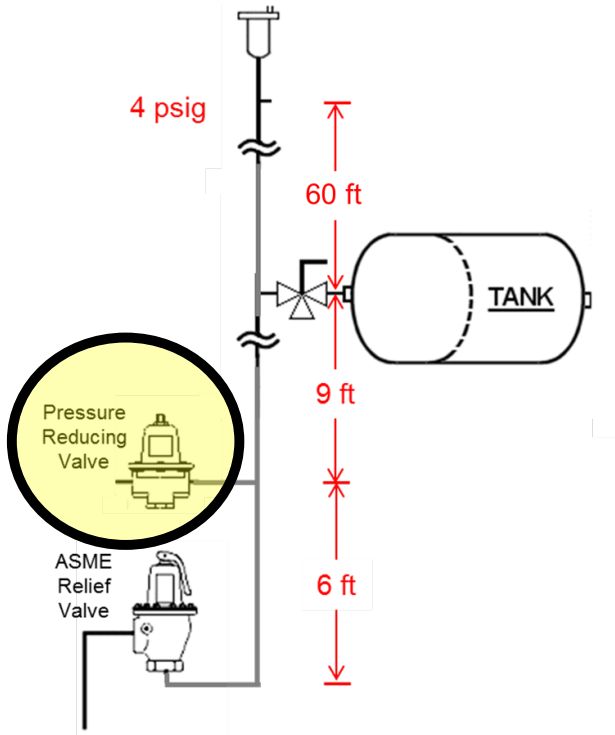


# Example Problem



Water Only System (40°F)
2,600 Gallons System Volume
160°F Design Operating Temperature
30°F ΔT across the Boiler ( <i>System</i> )
4 psig Pressurization at Top of System
50 psig ASME Safety Relief Valve on Boiler

# Step 1: Required PRV Setting



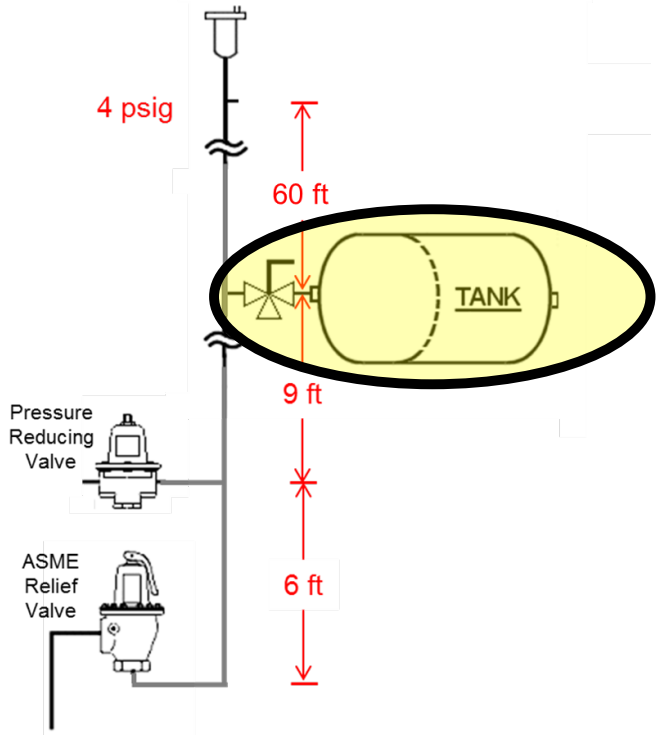
Static Head at PRV:  $69 \text{ ft} \div 2.31 \text{ ft/psi} = 30.0 \text{ psi}$

Pressurization at Top of System: 4.0 psi

**Pressure Reducing Valve Setting: 34.0 psi**

Water Only System
2,600 Gallons System Volume
160°F Design Operating Temperature
30°F ΔT across the Boiler (System)
4 psig Pressurization at Top of System
50 psig ASME Safety Relief Valve on Boiler

# Step 2: Required Design Tank Fill Pressure: *The “Pre-Charge”*



Static Head at Tank:  $60 \text{ ft} \div 2.31 \text{ ft/psi} = 26.0 \text{ psi}$

Pressurization at Top of System: 4.0 psi

**Design Tank Fill Pressure: 30.0 psi**

## Pre-charge Tank to 30.0 PSI

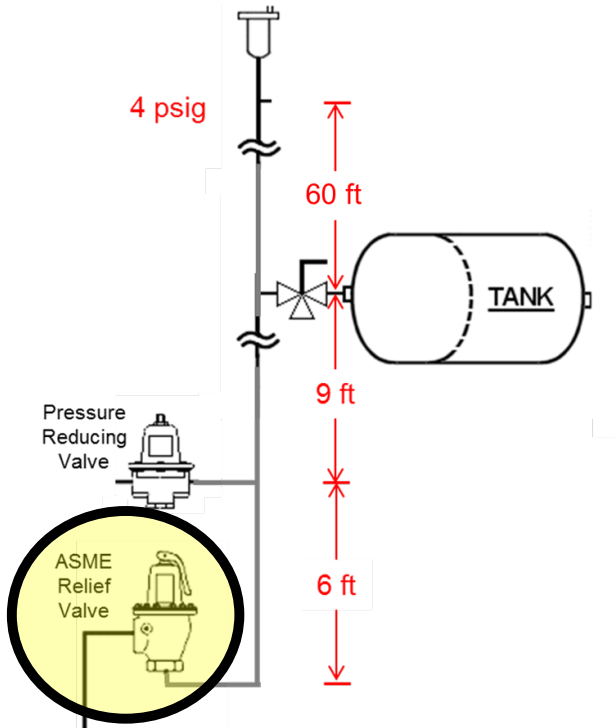
**Prior to Installation**

**No Liquid in the Tank**

Water Only System
2,600 Gallons System Volume
160°F Design Operating Temperature
30°F ΔT across the Boiler (System)
4 psig Pressurization at Top of System
50 psig ASME Safety Relief Valve on Boiler



# Step 3: Final Tank Operating Pressure



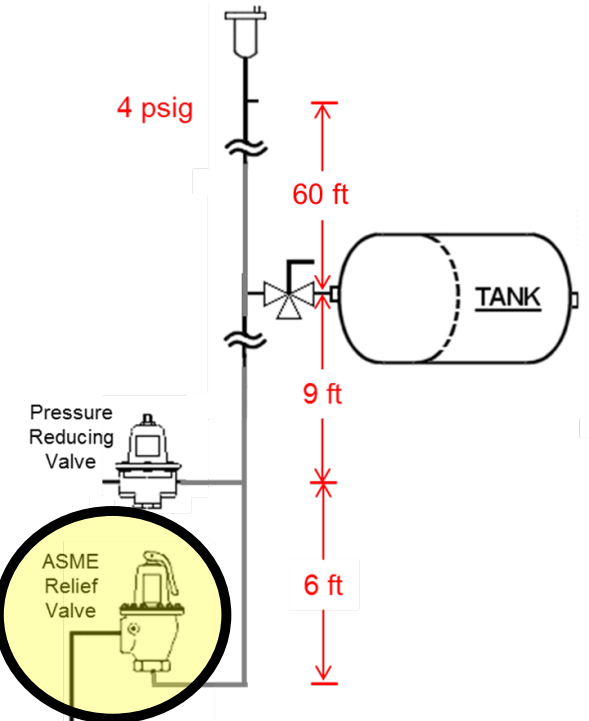
Static Head above ASME Relief Valve:  $75 \text{ ft} \div 2.31 \text{ ft/psi} = 32.5 \text{ psi}$

System Top Pressurization: 4.0 psi

Initial Total Back-Pressure at ASME Relief Valve: 36.5 psi

Water Only System
2,600 Gallons System Volume
160°F Design Operating Temperature
30°F ΔT across the Boiler (System)
4 psig Pressurization at Top of System
50 psig ASME Safety Relief Valve on Boiler

# Step 3: Final Tank Operating Pressure



Static Head above ASME Relief Valve:  $75 \text{ ft} \div 2.31 \text{ ft/psi} = 32.5 \text{ psi}$

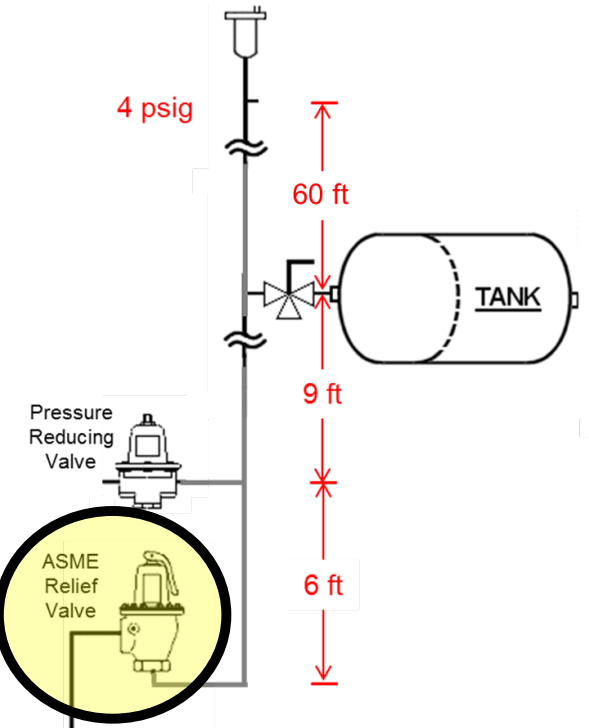
System Top Pressurization: 4.0 psi

Initial Total Back-Pressure at ASME Relief Valve: 36.5 psi

Derate ASME Relief Valve Rating (10% or 5 psig minimum): 45.0 psi

Water Only System
2,600 Gallons System Volume
160°F Design Operating Temperature
30°F ΔT across the Boiler (System)
4 psig Pressurization at Top of System
50 psig ASME Safety Relief Valve on Boiler

# Step 3: Final Tank Operating Pressure



Static Head above ASME Relief Valve:  $75 \text{ ft} \div 2.31 \text{ ft/psi} = 32.5 \text{ psi}$

System Top Pressurization: 4.0 psi

Initial Total Back-Pressure at ASME Relief Valve: 36.5 psi

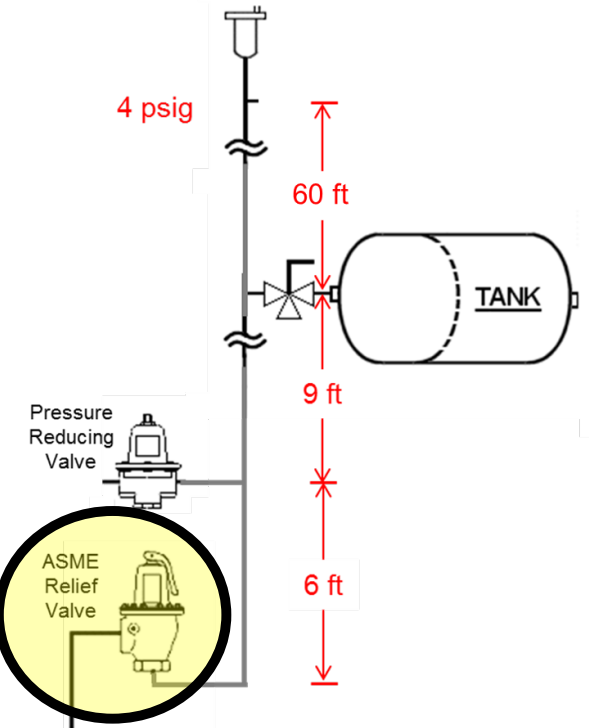
Derate ASME Relief Valve Rating (10% or 5 psig minimum): 45.0 psi

**Maximum Pressure Increase** at ASME Relief Valve:

$45.0 \text{ psi} - 36.5 \text{ psi} = 8.5 \text{ psi}$

Water Only System
2,600 Gallons System Volume
160°F Design Operating Temperature
30°F ΔT across the Boiler (System)
4 psig Pressurization at Top of System
50 psig ASME Safety Relief Valve on Boiler

# Step 3: Final Tank Operating Pressure



Static Head above ASME Relief Valve:  $75 \text{ ft} \div 2.31 \text{ ft/psi} = 32.5 \text{ psi}$

System Top Pressurization: 4.0 psi

Initial Total Back-Pressure at ASME Relief Valve: 36.5 psi

Derate ASME Relief Valve Rating (10% or 5 psig minimum): 45.0 psi

**Maximum Pressure Increase** at ASME Relief Valve:

$$45.0 \text{ psi} - 36.5 \text{ psi} = 8.5 \text{ psi}$$

**Final Tank Operating Pressure (@ System Design Temperature):**

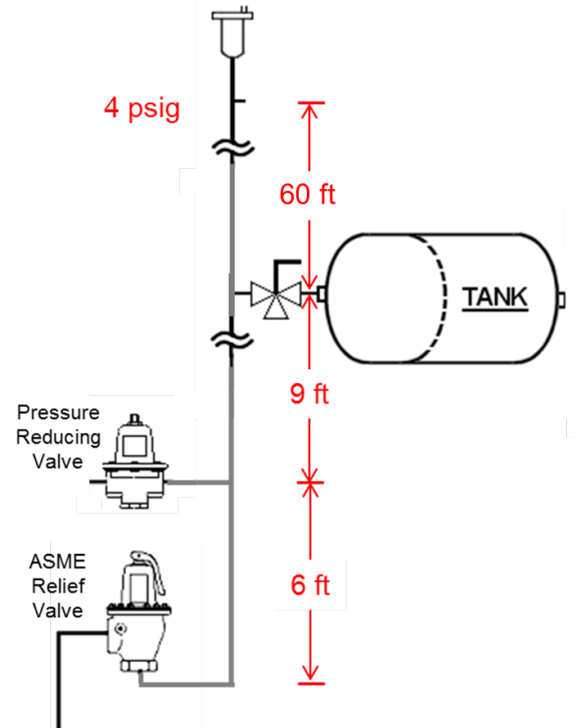
Design Tank Fill Pressure + **Maximum Pressure Increase**

$$30.0 \text{ psi} + 8.5 \text{ psi} = 38.5 \text{ psi}$$

Water Only System
2,600 Gallons System Volume
160°F Design Operating Temperature
30°F ΔT across the Boiler (System)
4 psig Pressurization at Top of System
50 psig ASME Safety Relief Valve on Boiler

# Step 4: Acceptance Factor

$$V_t = \frac{(E_w - E_p)}{1 - \frac{P_f}{P_o}} V_s$$



Pf = Design Tank Fill Pressure = 14.7 + (4 + 26.0) = 44.7 psia

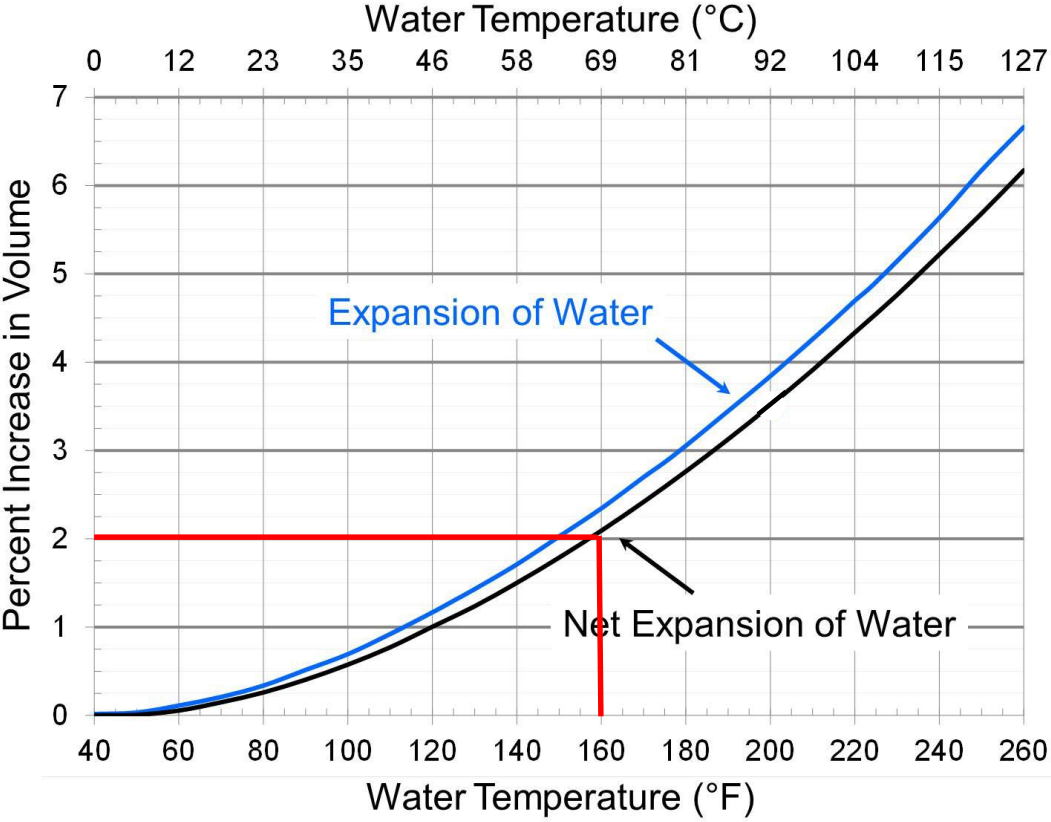
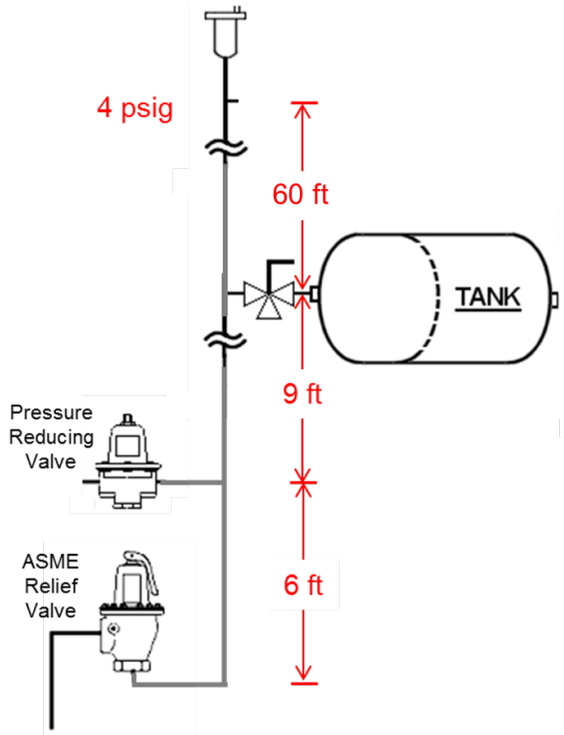
Po = Final Tank Operating Pressure = 14.7 + (4 + 26.0 + 8.5) = 53.2 psia  
*(At System Operating Temperature)*

Acceptance Factor = 1 - (Pf ÷ Po)

Acceptance Factor = 1 - (44.7 ÷ 53.2) = **0.160**

Water Only System
2,600 Gallons System Volume
160°F Design Operating Temperature
30°F ΔT across the Boiler (System)
4 psig Pressurization at Top of System
50 psig ASME Safety Relief Valve on Boiler

# Step 5: Net Water Expansion Volume (Acceptance Volume)

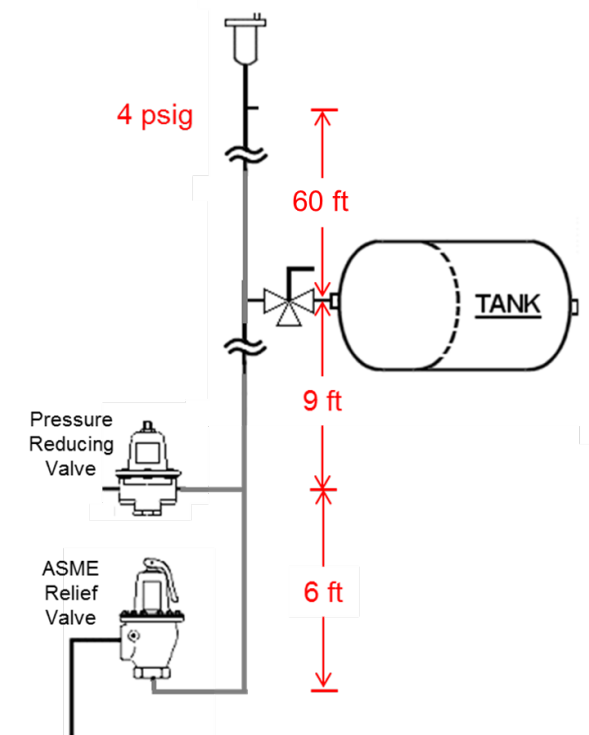


Water Only System (40°F)
2,600 Gallons System Volume
160°F Design Operating Temperature
30°F ΔT across the Boiler (System)
4 psig Pressurization at Top of System
50 psig ASME Safety Relief Valve on Boiler

Net Water Expansion Factor:  $(E_w - E_p)$  is 0.020

Net Water Expansion Volume  $(E_w - E_p)$  Vs:  
 =  $(0.020) * (2,600 \text{ gal}) = \mathbf{52.0 \text{ Gallons}}$

# Step 6: Required Tank Volume Size



$$V_t = \frac{(E_w - E_p)}{1 - \frac{P_f}{P_o}} V_s$$

**V<sub>t</sub>** = (Net Water Expansion Volume) ÷ (Acceptance Factor)

**V<sub>t</sub>** = 52.0 gal ÷ 0.160 = **325.0 gallons**

Water Only System
2,600 Gallons System Volume
160°F Design Operating Temperature
30°F ΔT across the Boiler (System)
4 psig Pressurization at Top of System
50 psig ASME Safety Relief Valve on Boiler

# Step 7a: Select Tank: “B” Series Full Acceptance Bladder

Minimum Tank Acceptance Volume ≥ 52.0 gallons

Minimum Tank Volume ≥ 325.0 gallons



**CONSTRUCTION**

**System Connection:** Forged Steel  
**Shell:** Carbon Steel  
**Bladder:** Heavy Duty Butyl Rubber  
 Designed and Constructed per ASME Section VIII, Division 1

**MAXIMUM OPERATING LIMITS**

**Maximum Design Pressure:** 125 PSI (862 kPa)  
**Design Temperature:** 240°F (115°C)

MODEL NUMBER	PART NUMBER				TANK AND ACCEPTANCE VOLUME GAL (L)	TAGGING INFORMATION	QUANTITY
	PRESSURIZED EXPANSION TANKS	WITH SIGHT GLASS	WITH SEISMIC RESTRAINTS	WITH SIGHT GLASS & SEISMIC RESTRAINTS			
B200	116051	116070	116089	116108	53 (200)		
B300	116052	116071	116090	116109	80 (300)		
B400	116053	116072	116091	116110	106 (400)		
B500	116054	116073	116092	116111	132 (500)		
B600	116055	116074	116093	116112	158 (600)		
B800	116056	116075	116094	116113	211 (800)		
B1000	116057	116076	116095	116114	264 (1,000)		
B1200	116058	116077	116096	116115	317 (1,200)		
B1400	116059	116078	116097	116116	370 (1,400)		<b>1</b>



# Step 7b: Select Tank: “D” Series Limited Acceptance Diaphragm

Minimum Tank Acceptance Volume ≥ 52.0 gallons

Minimum Tank Volume ≥ 325.0 gallons



**CONSTRUCTION**

**System Connection:** Forged Steel  
**Shell:** Carbon Steel  
**Diaphragm:** Heavy Duty Butyl Rubber  
 Designed and Constructed per ASME Section VIII, Division 1

**MAXIMUM OPERATING LIMITS**

**Maximum Design Pressure:** 125 PSI (862 kPa)  
**Design Temperature:** 240°F (115°C)

Model No.	Part Numbers				Volume gal (L)		Tagging Information	Quantity
	PRESSURIZED EXPANSION TANKS	WITH SIGHT GLASS	WITH SEISMIC RESTRAINTS	WITH SIGHT GLASS & SEISMIC RESTRAINTS	Tank	Acceptance		
D-15	116298	116311	116324	116337	7.8 (30)	6.3 (24)		
D-20	116299	116312	116325	116338	11 (42)	8.8 (33)		
D-40	116300	116313	116326	116339	25 (95)	20.2 (76)		
D-60	116301	116314	116327	116340	35 (132)	28 (106)		
D-80	116302	116315	116328	116341	45 (170)	36 (136)		
D-100	116303	116316	116329	116342	60 (227)	48.5 (184)		
D-120	116304	116317	116330	116343	70 (265)	56.5 (214)		
D-144	116305	116318	116331	116344	80 (303)	65 (246)		
D-180	116306	116319	116332	116345	90 (341)	73 (276)		
D-200	116307	116320	116333	116346	115 (435)	93 (352)		
D-240	116308	116321	116334	116347	140 (530)	113.5 (430)		
D-260	116309	116322	116335	116348	158 (598)	128 (485)		
D-280	116310	116323	116336	116349	211 (799)	171 (647)		<b>2</b>

# Step 7b: Select Tank: “D” Series Limited Acceptance Diaphragm

Minimum Tank Acceptance Volume ≥ 52.0 gallons

Minimum Tank Volume ≥ 325.0 gallons



**CONSTRUCTION**

**System Connection:** Forged Steel  
**Shell:** Carbon Steel  
**Diaphragm:** Heavy Duty Butyl Rubber  
 Designed and Constructed per ASME Section VIII, Division 1

**MAXIMUM OPERATING LIMITS**

**Maximum Design Pressure:** 125 PSI (862 kPa)  
**Design Temperature:** 240°F (115°C)

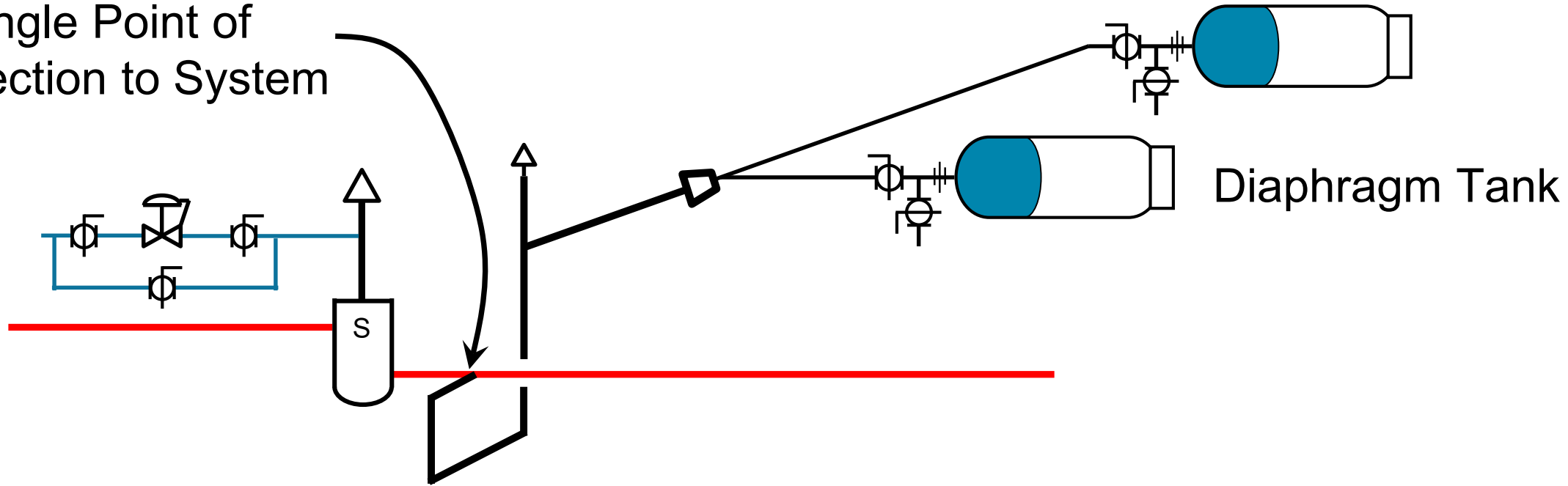
Model No.	Part Numbers				Volume gal (L)		Tagging Information	Quantity
	PRESSURIZED EXPANSION TANKS	WITH SIGHT GLASS	WITH SEISMIC RESTRAINTS	WITH SIGHT GLASS & SEISMIC RESTRAINTS	Tank	Acceptance		
D-15	116298	116311	116324	116337	7.8 (30)	6.3 (24)		
D-20	116299	116312	116325	116338	11 (42)	8.8 (33)		
D-40	116300	116313	116326	116339	25 (95)	20.2 (76)		
D-60	116301	116314	116327	116340	35 (132)	28 (106)		
D-80	116302	116315	116328	116341	45 (170)	36 (136)		
D-100	116303	116316	116329	116342	60 (227)	48.5 (184)		
D-120	116304	116317	116330	116343	70 (265)	56.5 (214)		
D-144	116305	116318	116331	116344	80 (303)	65 (246)		
D-180	116306	116319	116332	116345	90 (341)	73 (276)		
D-200	116307	116320	116333	116346	115 (435)	93 (352)		1
D-240	116308	116321	116334	116347	140 (530)	113.5 (430)		
D-260	116309	116322	116335	116348	158 (598)	128 (485)		
D-280	116310	116323	116336	116349	211 (799)	171 (647)		1

Different Size Tanks?

115 + 211 = 326 gal

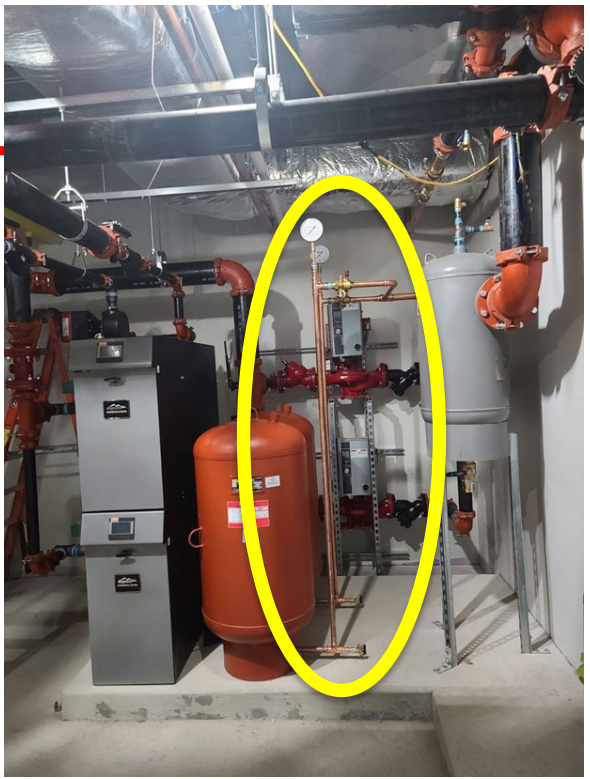
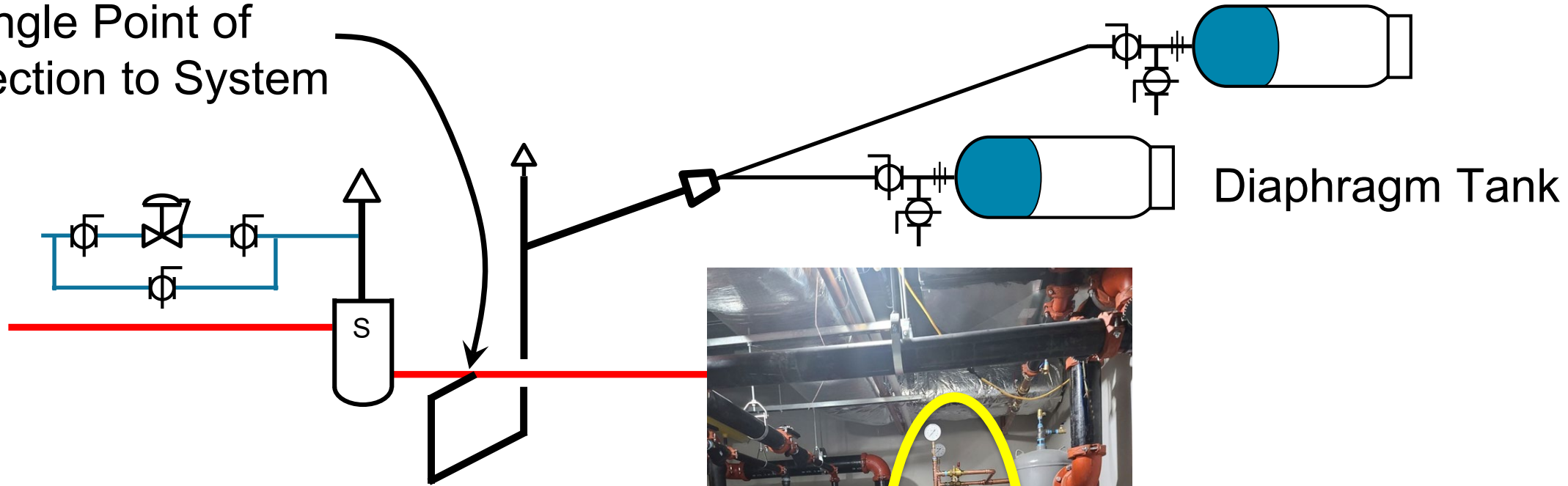
# Multiple Diaphragm or Bladder Pre-Charged Tanks - Piping

Single Point of Connection to System



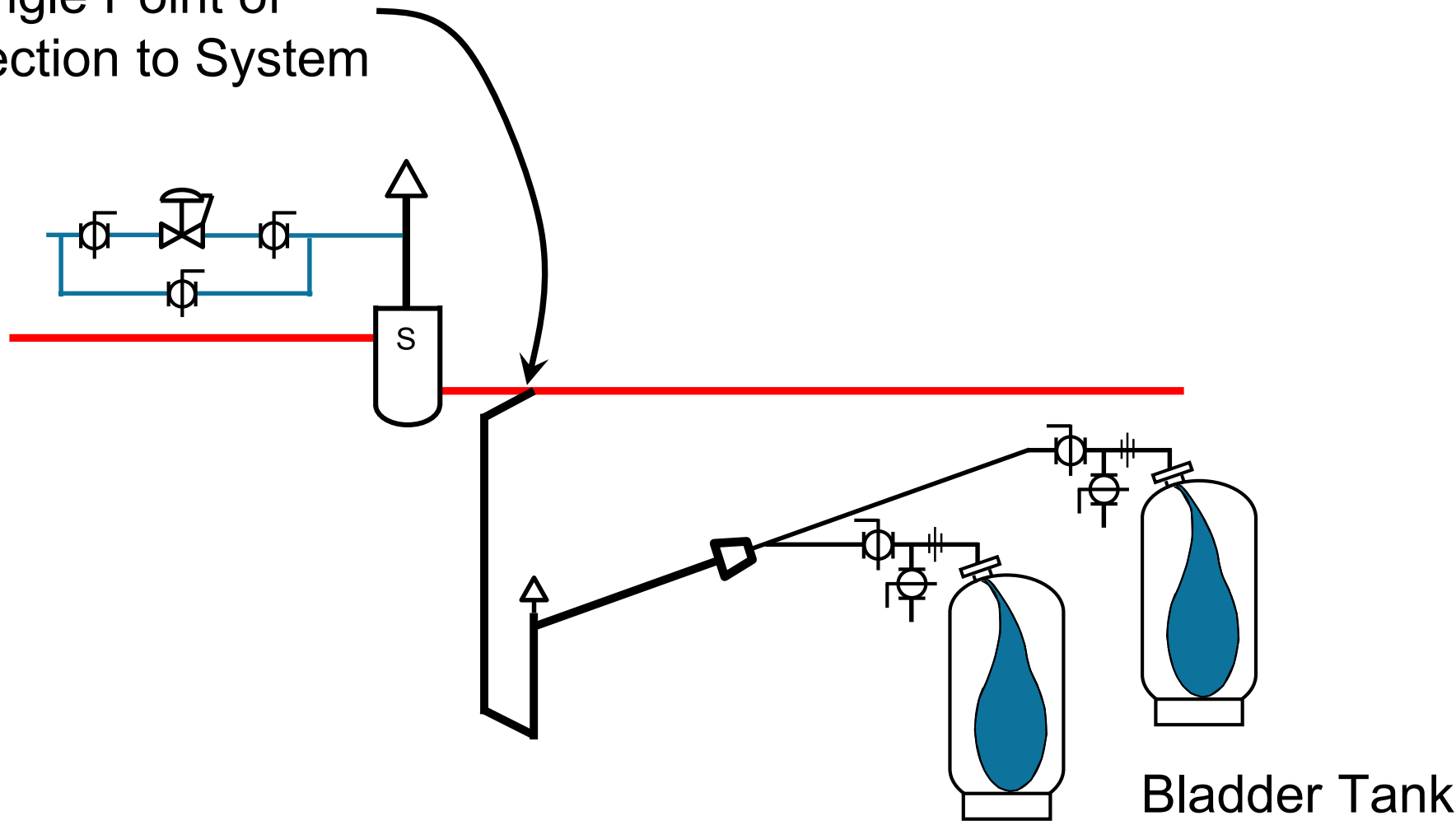
# Multiple Diaphragm or Bladder Pre-Charged Tanks - Piping

Single Point of Connection to System



# Multiple Diaphragm or Bladder Pre-Charged Tanks - Piping

Single Point of Connection to System



# The “Easy Way” – ESP Systemwise

Clear Inputs >>

Expansion Tanks

Choose Products

**HVAC**  HVAC Tanks

**Plumbing**  Potable Water Expansion  Well Water System

**Selections**

Fill Temperature: 40 °F

Max Temperature: 90 °F

Tank Fill Pressure: 60 psi

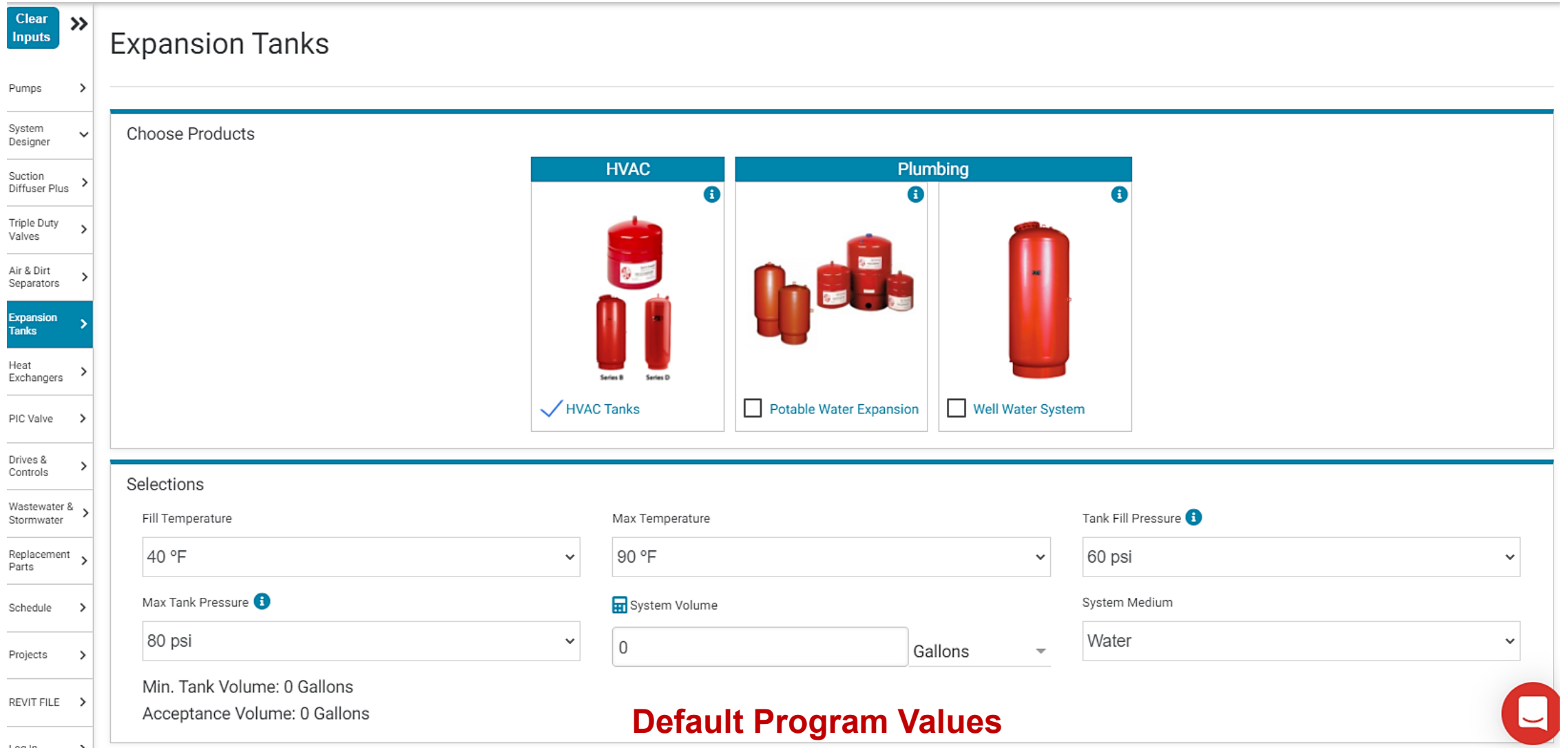
Max Tank Pressure: 80 psi

System Volume: 0 Gallons

System Medium: Water

Min. Tank Volume: 0 Gallons  
Acceptance Volume: 0 Gallons

**Default Program Values**



# The “Easy Way” – ESP Systemwise

System Designer ▾

Suction Diffuser Plus >

Triple Duty Valves >

Air & Dirt Separators >

**Expansion Tanks >**

Heat Exchangers >

PIC Valve >

Drives & Controls >

Wastewater & Stormwater >

Replacement Parts >

Schedule >


Projects >

REVIT FILE >

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### Choose Products


**HVAC** ⓘ



Series B Series D

HVAC Tanks

**Plumbing** ⓘ



Potable Water Expansion

Well Water System

---

### Selections

Fill Temperature	Max Temperature	Tank Fill Pressure ⓘ
40 °F ▾	160 °F ▾	30 psi ▾
Max Tank Pressure ⓘ	System Volume	System Medium
39 psi ▾	2600 Gallons ▾	Water ▾

**Min. Tank Volume: 324.54 Gallons**

**Acceptance Volume: 54.39 Gallons**

# The “Easy Way” – ESP Systemwise

Required Tank Volume (gal)	Required Acceptance Volume (gal)	Recommended Models	Qty	Actual Tank Volume (gal)	Actual Acceptance Volume (gal)	Price Index	Orientation ↕	Type ↕	ASME Rated	Max Design Temperature F (C)	Max Working Pressure PSIG (kPa)	Shipping Weight (lbs)	Actions
324.54	54.39	B1400	1	370.0	370.0	---	Horizontal/Vertical	Bladder	Yes	240.0 (116)	125.0 (862)	950.0	<a href="#">+</a> Select <a href="#">↓</a> Documents <a href="#">↓</a> Note
324.54	54.39	D280	2	211.0	84.0	---	Horizontal/Vertical	Diaphragm	Yes	240.0 (116)	125.0 (862)	827.0	<a href="#">+</a> Select <a href="#">↓</a> Documents <a href="#">↓</a> Note
324.54	54.39	B800	2	211.0	211.0	---	Horizontal/Vertical	Bladder	Yes	240.0 (116)	125.0 (862)	475.0	<a href="#">+</a> Select <a href="#">↓</a> Documents <a href="#">↓</a> Note
324.54	54.39	D200	3	110.0	34.0	---	Horizontal/Vertical	Diaphragm	Yes	240.0 (116)	125.0 (862)	400.0	<a href="#">+</a> Select <a href="#">↓</a> Documents <a href="#">↓</a> Note
324.54	54.39	B500	3	132.0	132.0	---	Horizontal/Vertical	Bladder	Yes	240.0 (116)	125.0 (862)	410.0	<a href="#">+</a> Select <a href="#">↓</a> Documents <a href="#">↓</a> Note



# What if System Fluid is changed to 30% Propylene Glycol?

System Designer

Suction Diffuser Plus

Triple Duty Valves

Air & Dirt Separators

**Expansion Tanks**

Heat Exchangers

PIC Valve

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HVAC Tanks

Potable Water Expansion

Well Water System

**Selections**

Fill Temperature: 40 °F

Max Temperature: 160 °F

Tank Fill Pressure: 30 psi

Max Tank Pressure: 39 psi

System Volume: 2600 Gallons

System Medium: Propylene Glycol

Medium Mixture: 30%

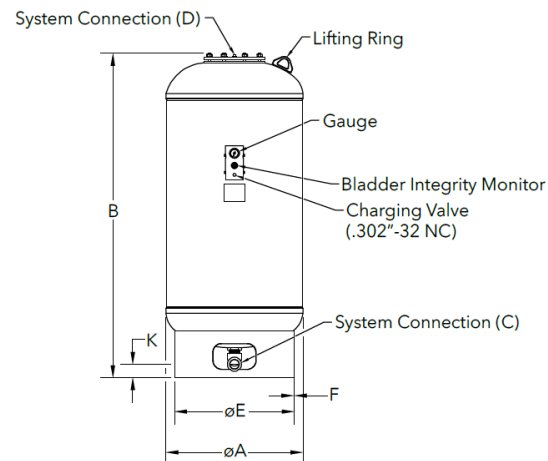
Min. Tank Volume: 558.48 Gallons

Acceptance Volume: 93.6 Gallons

# What if System Fluid is changed to 30% Propylene Glycol?

Required Tank Volume (gal)	Required Acceptance Volume (gal)	Recommended Models	Qty	Actual Tank Volume (gal)	Actual Acceptance Volume (gal)	Price Index	Orientation	Type	ASME Rated	Max Design Temperature F (C)	Max Working Pressure PSIG (kPa)	Shipping Weight (lbs)	Actions
558.48	93.6	B2500	1	660.0	660.0	---	Horizontal/Vertical	Bladder	Yes	240.0 (116)	125.0 (862)	1510.0	<a href="#">+</a> Select <a href="#">↓</a> Documents <a href="#">↓</a> Note
558.48	93.6	B1200	2	317.0	317.0	---	Horizontal/Vertical	Bladder	Yes	240.0 (116)	125.0 (862)	795.0	<a href="#">+</a> Select <a href="#">↓</a> Documents <a href="#">↓</a> Note
558.48	93.6	D280	3	211.0	84.0	---	Horizontal/Vertical	Diaphragm	Yes	240.0 (116)	125.0 (862)	827.0	<a href="#">+</a> Select <a href="#">↓</a> Documents <a href="#">↓</a> Note
558.48	93.6	B800	3	211.0	211.0	---	Horizontal/Vertical	Bladder	Yes	240.0 (116)	125.0 (862)	475.0	<a href="#">+</a> Select <a href="#">↓</a> Documents <a href="#">↓</a> Note

SERIES "B" (ASME) PRESSURIZED EXPANSION TANKS



**Will the single tank fit through the doorway??**  
**How much heavier is it??**

# Is a Single Tank still an option?

## DIMENSIONS AND WEIGHTS

Model	A in (mm)	B in (mm)	C FNPT(in)	D (in)	E in (mm)	F in (mm)	G in (mm)	H in (mm)	I in (mm)	J in (mm)	K in (mm)	Shipping Wt. lbs (kg)	Flooded Wt.* lbs (kg)
B-200	24(610)	43(1,092)	1-1/2	3/4	20(508)	0.14(4)	9/16(14)	22(559)	2(51)	2(51)	5.25(133)	210(95)	651(295)
B-300	24(610)	55(1,397)	1-1/2	3/4	20(508)	0.14(4)	9/16(14)	22(559)	2(51)	2(51)	5.25(133)	225(102)	891(404)
B-400	30(762)	49(1,245)	1-1/2	3/4	24(610)	0.14(4)	9/16(14)	27(686)	3(76)	3(76)	5.25(133)	300(136)	1,183(537)
B-500	30(762)	57(1,448)	2	3/4	24(610)	0.14(4)	9/16(14)	27(686)	3(76)	3(76)	5.25(133)	335(152)	1,435(651)
B-600	30(762)	65(1,651)	2	3/4	24(610)	0.14(4)	9/16(14)	27(686)	3(76)	3(76)	5.25(133)	360(163)	1,676(760)
B-800	32(813)	76(1,930)	2	3/4	28(711)	0.14(4)	9/16(14)	31(787)	3(76)	3(76)	5.25(133)	475(215)	2,233(1,013)
B-1000	36(914)	76(1,930)	1-1/2	3/4	30(762)	0.14(4)	9/16(14)	33(838)	3(76)	3(76)	N/A	552(250)	2,751(1,248)
B-1200	36(914)	88(2,235)	1-1/2	3/4	30(762)	0.14(4)	9/16(14)	33(838)	3(76)	3(76)	N/A	679(308)	3,320(1,506)
B-1400	36(914)	100(2,540)	1-1/2	3/4	30(762)	0.14(4)	9/16(14)	33(838)	3(76)	3(76)	N/A	688(312)	3,770(1,710)
B-1600	48(1,219)	74(1,880)	1-1/2	3/4	42(1,067)	0.14(4)	9/16(14)	45(1,143)	3(76)	3(76)	N/A	1,046(474)	4,561(2,068)
B-2000	48(1,219)	86(2,184)	1-1/2	3/4	42(1,067)	0.20(5)	9/16(14)	45(1,143)	3(76)	3(76)	N/A	1,150(522)	5,548(2,516)
B-2500	48(1,219)	104(2,642)	2	3/4	42(1,067)	0.20(5)	9/16(14)	46(1,168)	4(102)	4(102)	N/A	1,444(655)	6,942(3,148)

# Is a Single Tank still an option?

## DIMENSIONS AND WEIGHTS

Model	A in (mm)	B in (mm)	C FNPT(in)	D (in)	E in (mm)	F in (mm)	G in (mm)	H in (mm)	I in (mm)	J in (mm)	K in (mm)	Shipping Wt. lbs (kg)	Flooded Wt.* lbs (kg)
B-200	24(610)	43(1,092)	1-1/2	3/4	20(508)	0.14(4)	9/16(14)	22(559)	2(51)	2(51)	5.25(133)	210(95)	651(295)
B-300	24(610)	55(1,397)	1-1/2	3/4	20(508)	0.14(4)	9/16(14)	22(559)	2(51)	2(51)	5.25(133)	225(102)	891(404)
B-400	30(762)	49(1,245)	1-1/2	3/4	24(610)	0.14(4)	9/16(14)	27(686)	3(76)	3(76)	5.25(133)	300(136)	1,183(537)
B-500	30(762)	57(1,448)	2	3/4	24(610)	0.14(4)	9/16(14)	27(686)	3(76)	3(76)	5.25(133)	335(152)	1,435(651)
B-600	30(762)	65(1,651)	2	3/4	24(610)	0.14(4)	9/16(14)	27(686)	3(76)	3(76)	5.25(133)	360(163)	1,676(760)
B-800	32(813)	76(1,930)	2	3/4	28(711)	0.14(4)	9/16(14)	31(787)	3(76)	3(76)	5.25(133)	475(215)	2,233(1,013)
B-1000	36(914)	76(1,930)	1-1/2	3/4	30(762)	0.14(4)	9/16(14)	33(838)	3(76)	3(76)	N/A	552(250)	2,751(1,248)
B-1200	36(914)	88(2,235)	1-1/2	3/4	30(762)	0.14(4)	9/16(14)	33(838)	3(76)	3(76)	N/A	679(308)	3,320(1,506)
B-1400	36(914)	100(2,540)	1-1/2	3/4	30(762)	0.14(4)	9/16(14)	33(838)	3(76)	3(76)	N/A	688(312)	3,770(1,710)
B-1600	48(1,219)	74(1,880)	1-1/2	3/4	42(1,067)	0.14(4)	9/16(14)	45(1,143)	3(76)	3(76)	N/A	1,046(474)	4,561(2,068)
B-2000	48(1,219)	86(2,184)	1-1/2	3/4	42(1,067)	0.20(5)	9/16(14)	45(1,143)	3(76)	3(76)	N/A	1,150(522)	5,548(2,516)
B-2500	48(1,219)	104(2,642)	2	3/4	42(1,067)	0.20(5)	9/16(14)	46(1,168)	4(102)	4(102)	N/A	1,444(655)	6,942(3,148)

# Is a Single Tank still an option?

## DIMENSIONS AND WEIGHTS

Model	A in (mm)	B in (mm)	C FNPT(in)	D (in)	E in (mm)	F in (mm)	G in (mm)	H in (mm)	I in (mm)	J in (mm)	K in (mm)	Shipping Wt. lbs (kg)	Flooded Wt.* lbs (kg)
B-200	24(610)	43(1,092)	1-1/2	3/4	20(508)	0.14(4)	9/16(14)	22(559)	2(51)	2(51)	5.25(133)	210(95)	651(295)
B-300	24(610)	55(1,397)	1-1/2	3/4	20(508)	0.14(4)	9/16(14)	22(559)	2(51)	2(51)	5.25(133)	225(102)	891(404)
B-400	30(762)	49(1,245)	1-1/2	3/4	24(610)	0.14(4)	9/16(14)	27(686)	3(76)	3(76)	5.25(133)	300(136)	1,183(537)
B-500	30(762)	57(1,448)	2	3/4	24(610)	0.14(4)	9/16(14)	27(686)	3(76)	3(76)	5.25(133)	335(152)	1,435(651)
B-600	30(762)	65(1,651)	2	3/4	24(610)	0.14(4)	9/16(14)	27(686)	3(76)	3(76)	5.25(133)	360(163)	1,676(760)
B-800	32(813)	76(1,930)	2	3/4	28(711)	0.14(4)	9/16(14)	31(787)	3(76)	3(76)	5.25(133)	475(215)	2,233(1,013)
B-1000	36(914)	76(1,930)	1-1/2	3/4	30(762)	0.14(4)	9/16(14)	33(838)	3(76)	3(76)	N/A	552(250)	2,751(1,248)
B-1200	36(914)	88(2,235)	1-1/2	3/4	30(762)	0.14(4)	9/16(14)	33(838)	3(76)	3(76)	N/A	679(308)	3,320(1,506)
B-1400	36(914)	100(2,540)	1-1/2	3/4	30(762)	0.14(4)	9/16(14)	33(838)	3(76)	3(76)	N/A	688(312)	3,770(1,710)
B-1600	48(1,219)	74(1,880)	1-1/2	3/4	42(1,067)	0.14(4)	9/16(14)	45(1,143)	3(76)	3(76)	N/A	1,046(474)	4,561(2,068)
B-2000	48(1,219)	86(2,184)	1-1/2	3/4	42(1,067)	0.20(5)	9/16(14)	45(1,143)	3(76)	3(76)	N/A	1,150(522)	5,548(2,516)
B-2500	48(1,219)	104(2,642)	2	3/4	42(1,067)	0.20(5)	9/16(14)	46(1,168)	4(102)	4(102)	N/A	1,444(655)	6,942(3,148)

# Is a Single Tank still an option?

## DIMENSIONS AND WEIGHTS

Model	A in (mm)	B in (mm)	C FNPT(in)	D (in)	E in (mm)	F in (mm)	G in (mm)	H in (mm)	I in (mm)	J in (mm)	K in (mm)	Shipping Wt. lbs (kg)	Flooded Wt.* lbs (kg)
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B-300	24(610)	55(1,397)	1-1/2	3/4	20(508)	0.14(4)	9/16(14)	22(559)	2(51)	2(51)	5.25(133)	225(102)	891(404)
B-400	30(762)	49(1,245)	1-1/2	3/4	24(610)	0.14(4)	9/16(14)	27(686)	3(76)	3(76)	5.25(133)	300(136)	1,183(537)
B-500	30(762)	57(1,448)	2	3/4	24(610)	0.14(4)	9/16(14)	27(686)	3(76)	3(76)	5.25(133)	335(152)	1,435(651)
B-600	30(762)	65(1,651)	2	3/4	24(610)	0.14(4)	9/16(14)	27(686)	3(76)	3(76)	5.25(133)	360(163)	1,676(760)
B-800	32(813)	76(1,930)	2	3/4	28(711)	0.14(4)	9/16(14)	31(787)	3(76)	3(76)	5.25(133)	475(215)	2,233(1,013)
B-1000	36(914)	76(1,930)	1-1/2	3/4	30(762)	0.14(4)	9/16(14)	33(838)	3(76)	3(76)	N/A	552(250)	2,751(1,248)
B-1200	36(914)	88(2,235)	1-1/2	3/4	30(762)	0.14(4)	9/16(14)	33(838)	3(76)	3(76)	N/A	679(308)	3,320(1,506)
B-1400	36(914)	100(2,540)	1-1/2	3/4	30(762)	0.14(4)	9/16(14)	33(838)	3(76)	3(76)	N/A	688(312)	3,770(1,710)
B-1600	48(1,219)	74(1,880)	1-1/2	3/4	42(1,067)	0.14(4)	9/16(14)	45(1,143)	3(76)	3(76)	N/A	1,046(474)	4,561(2,068)
B-2000	48(1,219)	86(2,184)	1-1/2	3/4	42(1,067)	0.20(5)	9/16(14)	45(1,143)	3(76)	3(76)	N/A	1,150(522)	5,548(2,516)
B-2500	48(1,219)	104(2,642)	2	3/4	42(1,067)	0.20(5)	9/16(14)	46(1,168)	4(102)	4(102)	N/A	1,444(655)	6,942(3,148)

# What Have We Learned?

- Good piping practice enhances Air Management efficiency
- Cold Static Fill Pressure: From the **PRV location** to highest point
- Locate the Air Separator in warmest water with lowest pressure
- The Point of No Pressure Change: *Always Pump Away!!*
- Tank Pre-Charge pressure not always equal to Cold Static Fill Pressure
- Glycol Solutions will expand more than water
- Multiple tanks can be used and should be piped in parallel

Questions?

Comments?

Observations?